



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

Heemskirk Tin Project

Severn Further Flowsheet Development and Optimisation

201010-00575-PM-REP-002

12 June 2015

Minerals, Metals & Chemicals

Level 12, 333 Collins Street

Melbourne VIC 3000

Australia

Telephone: +61 3 8676 3500

Facsimile: +61 3 8676 3505

www.worleyparsons.com

ABN 61 001 279 812

© Copyright 2015 WorleyParsons Services Pty Ltd



STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Disclaimer

This report has been prepared on behalf of and for the exclusive use of Stellar Resources Limited, and is subject to and issued in accordance with the agreement between Stellar Resources Limited and WorleyParsons. WorleyParsons accepts no liability or responsibility whatsoever for it in respect of any use of or reliance upon this report by any third party.

Copying this report without the permission of Stellar Resources Limited and WorleyParsons is not permitted.

PROJECT 201010-00575 - HEEMSKIRK TIN PROJECT

REV	DESCRIPTION	ORIG	REVIEW	WORLEY-PARSONS APPROVAL	DATE	CLIENT APPROVAL	DATE
A	Issued for internal review	J Resta	S McKenna	N/A	6-Jun-2015	N/A	
B	Issued for use	JR J Resta	MPJR S McKenna		12-Jun-2015		



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

CONTENTS

1	SUMMARY	1
2	INTRODUCTION	3
3	OUTLINE OF PROGRAM	4
4	SAMPLES USED IN TESTWORK PROGRAM	5
5	SAMPLE CHARACTERISATION	6
5.1	Mineralogy	9
6	COMMINUTION	14
7	HEAVY MEDIA SEPARATION	16
7.1	Application of HMS in the Heemskirk Flowsheet	17
8	SULFIDE FLOTATION	19
8.1	Primary Grind Size	19
8.2	Regrind Size	23
8.3	Production of Sulfide Flotation Tailings for Downstream Testwork	26
8.4	Impact of Sulfur Head Grade	27
8.5	Key Outcomes	28
8.6	Mineralogy of Sulfide Flotation Tails/Gravity Circuit Feed	29
9	GRAVITY SEPARATION	34
9.1	Gravity Separation Batch Testing	34
9.2	Gravity Separation Lock Cycle Testing	35
9.2.1	Tin Recovery from “-106 µm Tails” Stream	40
9.3	Key Outcomes	44
10	GRAVITY CONCENTRATE DRESSING	45
10.1	Sulfide Dressing Flotation	45
10.2	Dressing Magnetic Separation	46
10.2.1	Alternative approaches to magnetite rejection	47
10.3	Concentrate Leach	47
10.4	Final Gravity Concentrate Quality	48



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

11	DE-SLIME AND TIN FLOTATION	50
11.1	De-Slime	50
11.2	Tin Flotation	52
11.2.1	Sample Aging Issue	61
11.2.2	Estimated Closed Circuit Tin Flotation Performance	63
11.2.3	Tin Flotation Concentrate Composition	64
11.3	Key Outcomes	66
12	CONCENTRATE LEACHING	67
13	TAILINGS CHARACTERISTICS	70
14	CONCLUSIONS	75
14.1	Overall Metallurgical Performance	76
15	PROPOSED PROCESS FLOWSHEET	79
15.1	Major design criteria	81
15.2	Key changes from PFS Process Flowsheet	83
16	RECOMMENDED FURTHER WORK	86
16.1	Specific issues requiring further definition	86
APPENDIX 1	– SAMPLE DETAILS	
APPENDIX 2	– MINERALOGY	
APPENDIX 3	– COMMINUTION TESTWORK	
APPENDIX 4	– HEAVY MEDIA SEPARATION RESULTS	
APPENDIX 5	– HMS EVALUATION	
APPENDIX 6	– SULFIDE FLOTATION RESULTS	
APPENDIX 7	– GRAVITY SEPARATION RESULTS	
APPENDIX 8	– GRAVITY CONCENTRATE DRESSING	
APPENDIX 9	– FINAL GRAVITY CONCENTRATE ANALYSIS	
APPENDIX 10	– DE-SLIMING RESULTS	
APPENDIX 11	– TIN FLOTATION RESULTS	
APPENDIX 12	– FINAL TIN FLOTATION CONCENTRATE ANALYSIS	



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

- APPENDIX 13 – CONCENTRATE LEACH RESULTS
- APPENDIX 14 – OVERALL TIN BALANCES
- APPENDIX 15 – PROPOSED PROCESS FLOWSHEET
- APPENDIX 16 – TESTWORK SCOPE OF WORK
- APPENDIX 17 – ALS METALLURGY REPORT



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

1 SUMMARY

The Severn metallurgical testing program has focused on the optimisation of the process flowsheet utilising a large “global” composite sample representing the typical Severn mineralogy, composition and tin grades. This has provided a number of important improvements to metallurgical performance, and flowsheet simplifications, in addition to generating more robust information with respect to optimum process design criteria and processing conditions.

Key outcomes of the program include:

- Elimination of the heavy media separation circuit.

This has provided a simplification to the overall process flowsheet and a reduction in associated tin losses, and is expected to provide an improved project outcome.
- Coarser primary grind; grind size optimisation test work has demonstrated a significantly coarser primary grind size (P80 = 250 µm) is more optimum than that considered in the PFS (P80 = 130 µm). This provides the following benefits;
 - reduced tin losses due to reduced fines production,
 - reduction in primary grind operating and capital costs, and overall comminution energy requirements.

Significantly, the percentage of tin passing 30 µm (below which size gravity recovery is relatively poor) is estimated to decrease from ~43% passing 30 µm at a primary grind size of 130 µm (as assumed in the PFS), to only ~30% passing 30 µm at a primary grind size of 240 µm. This is equivalent to ~30% reduction in fine tin generation, and is a key contributor to the improved gravity recovery achieved.

- Optimisation of the sulfide flotation circuit has led to a significant reduction in tin losses to the final sulphide concentrate tailings stream. This, together with the elimination of the heavy media circuit has increased the amount of tin available for recovery within the gravity and tin flotation circuits.
- Optimisation of the gravity circuit configuration, combine with upstream flowsheet improvements, has led to ~10% improvement in tin recovery via gravity.
- Improvements with the concentrate dressing circuit have led to improved gravity concentrate quality and clearly demonstrated a high quality concentrate, low in penalty elements, can be readily produced.
- Elimination of the silica flotation circuit has provided a simplification to the overall process flowsheet.
- Optimisation of the De-slime cut point has allowed minimisation of combine slimes and tin flotation tailings losses.
- Tin flotation test work has robustly demonstrated commercially meaningful tin flotation concentrate grades can be achieved at acceptable recoveries.



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

- Based on the outcomes of the optimisation program overall tin recovery is estimated at 79.5% at a final concentrate grade of 45% Sn.

Importantly, the overall performance has been demonstrated across a consistent, robust test work program, covering all major sections (including sulfide flotation, gravity separation, de-sliming, tin flotation, concentrate dressing and concentrate leaching) of the proposed process flowsheet.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

2 INTRODUCTION

The Severn metallurgical testing program has focused on the optimisation of the Heemskirk Tin Project process flowsheet utilising a large “global” composite sample representing the typical Severn mineralogy, composition and tin grades. The current program has focused on the Severn deposit which forms approximately 60% of the overall tin resource for the Heemskirk Tin Project

A significant amount of testwork has previously been completed on the Heemskirk project over a number of separate programs, carried out on various samples from the Upper Queen Hill, Lower Queen Hill, Severn and Saint Dizier deposits. Review of the previous work highlighted that separately these programs were very much ‘development’ type programs, and were often limited by availability of sample to allow more detailed optimisation work to be completed. The review highlighted the need for significant additional flowsheet development and optimisation testwork which the current program has aimed to address.

Keys aims of the Severn metallurgical testing program were:

- Achieve improved overall performance with respect to tin recovery to saleable concentrate grades.
- Better define the optimum process flowsheet, process design criteria and expected performance.
- Demonstrate achievable overall tin recovery to saleable concentrate grades.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

3 OUTLINE OF PROGRAM

The Severn metallurgical testing program focused on optimisation of the PFS process flow-sheet using a large, ~120 kg, “global composite” sample representing typical Severn mineralogy, composition and tin grade. The program was completed under the supervision of WorleyParsons via ALS Metallurgy Burnie laboratory (ALS job no. T0879).

The testwork scope of work contained in Appendix 1 details the original program planned to be completed.

Keys aims of the program were to:

- Achieve improved overall performance with respect to tin recovery to saleable concentrate grades.
- Better define the optimum flowsheet, process design criteria and expected performance.
- Demonstrate achievable overall tin recovery to saleable concentrate grades.

In addition to detailed sample characterisation the testwork undertaken covered all major unit processes including:

- Comminution
- HMS
- Sulfide flotation
- Gravity Separation
- Gravity Concentrate Dressing
- De-sliming
- Tin flotation
- Concentrate leach

The general approach to the overall program was to progressively optimise each of the upstream flowsheet areas, then generate sample under the ‘optimised’ conditions to form the feed for downstream testwork. This approach was taken to ensure testwork on the downstream areas of the flowsheet was conducted on a reasonably representative feed.

For example, the sulfide flotation testwork initially focused on optimisation of primary grind size, followed by regrind size, then optimisation of the overall float. Following optimisation of the sulfide float a series of larger (12 kg) batch flotation tests were completed to produce sulfide flotation tailings as feed to the downstream (gravity separation, de-sliming and tin flotation) testwork. Likewise, initial gravity separation work focused on optimising the circuit configuration prior to generating sample for subsequent de-sliming and tin flotation work and gravity concentrate dressing.



STELLAR RESOURCES LIMITED HEEMSKIRK TIN PROJECT SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

4 SAMPLES USED IN TESTWORK PROGRAM

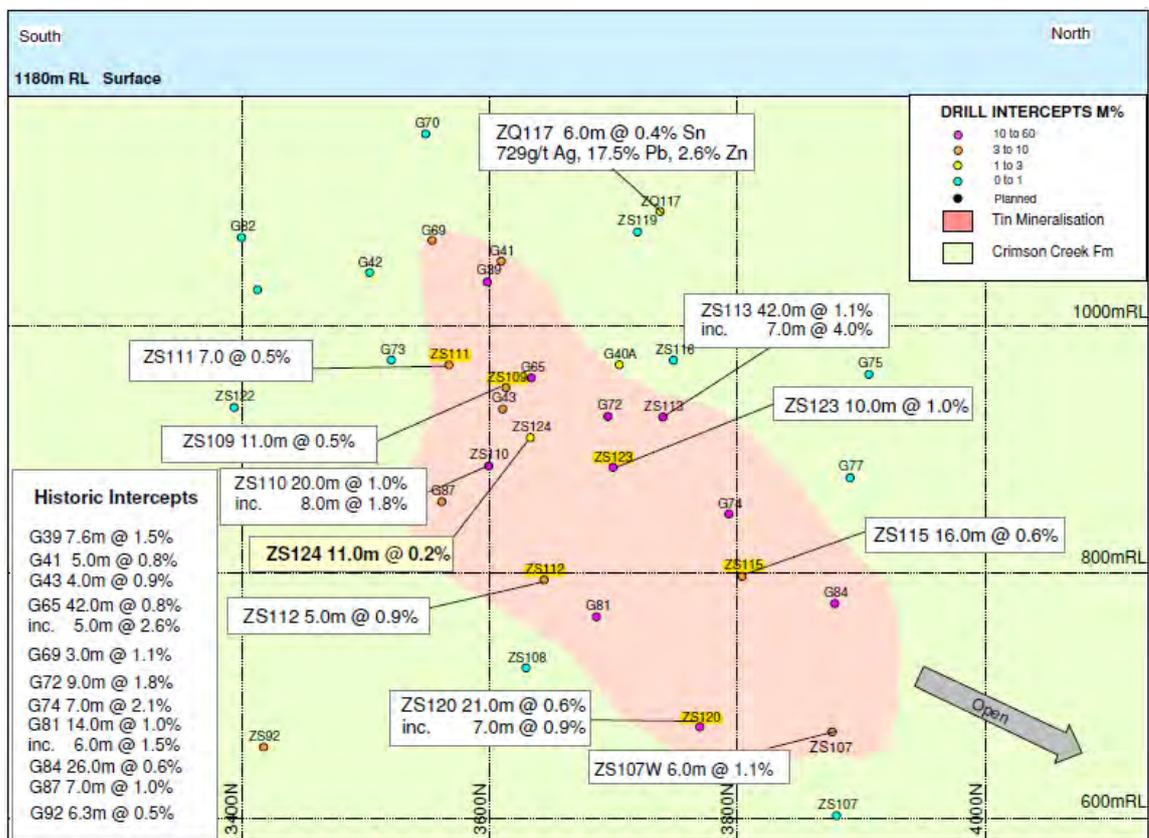
The Severn metallurgical testing program has focused on optimisation of the PFS process flow-sheet using a large, ~120 kg, “global composite” sample representing typical Severn mineralogy, composition and tin grade.

Throughout this report this composite is referred to as; Severn Bulk Composite (SBC).

The Severn Bulk Composite (SBC) sample was produced from ½ core from intersections of the following drill holes; ZS-109, ZS-111, ZS-111W, ZS-112a, ZS-112b, ZS-112c, ZS-112d, ZS-112W, ZS-115, ZS-120 and ZS-123, with remaining material from Severn composites from previous test programs also added to argument the total quantity of sample. Full details of the intervals and previous composites forming the Severn Bulk Composite are contained in Appendix 1.

Figure 4-1 shows a long projection of the Severn deposit with the intervals forming the Severn Bulk Composite highlighted in yellow. The intervals forming Severn Bulk Composite represent a reasonable spread across the tin mineralisation both spatially and in terms of composition.

Figure 4-1 Severn Long Projection



Overall the Severn Bulk Composite is thought to be “typical” of the majority of the Severn deposit.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

5 SAMPLE CHARACTERISATION

Samples characterisation consisted of the following:

- Full Head assay
- Size by size assay
- Optical mineralogy – Fully and Sn scan
- Heavy liquid testing (refer Section 7)

Table 1 shows the head analysis for the Severn Bulk Composite, along with the estimated overall Severn Mineral Resource analysis for comparison.

Table 1 – Severn Bulk Composite Head Analysis

	Sn	Sn Acid Sol	Fe	As	S	SiO ₂	CaO	MgO	Al ₂ O ₃	Mn	Cu	Pb	Zn
	%	ppm	%	%	%	%	%	%	%	%	%	%	%
Severn Bulk Composite	1.00	170	26.1	0.28	14.6	30.1	0.71	2.74	6.29	0.40	0.09	0.63	0.77
Severn Mineral Resource	0.98	177	-	-	9.06	-	-	-	-	-	-	0.03	-

Table 2 shows basic statistics from 1 m composites of Severn drill core assays for comparison with the Severn Bulk Composite sample head analysis.

Table 2 – Basic Statistics from 1 m composites of Severn Drill Core Assays

Variable	Sn %	AS_Sn ppm	S %	Cu ppm	Pb ppm	Zn ppm	Ag ppm	As ppm	Fe %	Bi ppm	W ppm	Ni ppm
Number of samples	370	135	292	331	251	323	227	199	234	182	141	191
Minimum value	0.01	10	0.14	8	7	10	1	0.05	6.39	0.01	0.01	5
Maximum value	11.1	1000	32.5	4400	19000	18500	88	20400	44.0	560	120	476
Mean	0.89	171	8.99	585	235	227	4	1077	21.7	60	2	62
Median	0.50	100	7.50	407	20	59	2	80	21.0	30	0	50
Geometric Mean	0.48	121	6.61	390	32	55	2	95	20.7	22	0	43
Variance	1.46	27100	42.1	313628	1838117	2011248	68	8976723	39.3	6152	196	4014
Standard Deviation	1.21	165	6.49	560	1356	1418	8	2996	6.27	78	14	63
Coefficient of variation	1.36	0.96	0.72	0.96	5.77	6.24	2.11	2.78	0.29	1.30	5.61	1.02

Sn grade of the Severn Bulk Composite compares very closely with that of the overall Severn Mineral Resource Sn grade, and is marginally lower than the overall Heemskirk mineral resource, which averages 1.14% Sn.

Although S content of the SBC sample is higher than average, it is not untypical of Severn, being well within the range of sulfur contents typically seen.

Fe content of the Severn Bulk Composite is also reasonably typical of Severn.

Soluble Sn content of the Severn Bulk Composite (and overall Severn resource) is negligible.



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

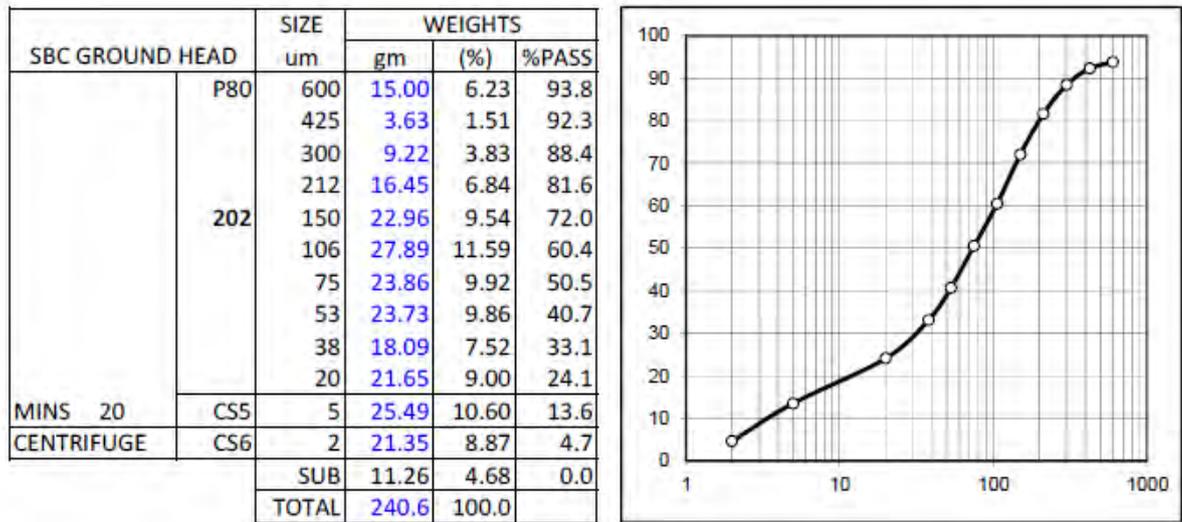
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Table 3 shows size distribution and size by size metal distribution for the Severn Bulk Composite sample ground to a P80 of 203 μm . Generally Sn distribution follows the mass distribution, with minor upgrading of Sn in sizes ranges $-106\mu\text{m} +8\mu\text{m}$, while $-8\mu\text{m}$ fractions are relatively low Sn grade, representing only 4.5% of the total Sn distribution compared with 13.6% of the total mass.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 3 - Size Distribution and Size by Size Analysis of Severn Bulk Composite



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mount Number
		%	dist	%	dist	%	dist	%	dist	%	dist	
600	6.23	0.97	6.2	21.30	5.1	0.17	3.7	9.85	4.1	40.40	8.7	
212	12.18	0.64	8.0	20.40	9.6	0.15	6.3	9.41	7.7	40.80	17.1	879064
150	9.54	0.84	8.2	25.60	9.4	0.25	8.2	15.35	9.8	32.30	10.6	879065
106	11.59	0.98	11.6	27.50	12.3	0.31	12.4	17.80	13.8	28.90	11.5	879066
75	9.92	1.10	11.1	28.30	10.8	0.34	11.6	18.60	12.3	26.80	9.1	879067
53	9.86	1.26	12.7	28.90	11.0	0.35	11.9	19.65	13.0	25.30	8.6	879068
38	7.52	1.31	10.1	29.50	8.5	0.38	9.9	19.50	9.8	24.20	6.3	879069
20	9.00	1.37	12.6	29.50	10.2	0.35	10.9	18.40	11.1	23.40	7.2	879070
8	10.60	1.40	15.1	29.80	12.1	0.35	12.8	18.15	12.9	21.30	7.8	879071
2	8.87	0.43	3.9	23.10	7.9	0.16	4.9	7.67	4.6	31.30	9.5	
CAL <2	4.68	0.13	0.6	17.49	3.1	0.46	7.5	3.26	1.0	22.77	3.7	
ASSAY	100.0	0.98	100.0	26.00	100.0	0.29	100.0	14.95	100.0	29.10	100.0	

SIZE um	WT %	MnO		CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist	%	dist
600	6.23	0.21	4.0	0.56	5.2	2.63	6.3	7.93	8.2
212	12.18	0.27	10.0	0.59	10.7	3.03	14.1	7.36	14.8
150	9.54	0.32	9.3	0.64	9.1	2.56	9.3	5.62	8.9
106	11.59	0.33	11.6	0.63	10.9	2.35	10.4	5.03	9.7
75	9.92	0.33	9.9	0.67	9.9	2.21	8.4	4.73	7.8
53	9.86	0.34	10.2	0.65	9.6	2.12	8.0	4.36	7.1
38	7.52	0.34	7.7	0.69	7.7	2.13	6.1	4.30	5.4
20	9.00	0.35	9.5	0.74	9.9	2.32	8.0	4.76	7.1
8	10.60	0.37	11.9	0.80	12.7	2.35	9.5	4.62	8.1
2	8.87	0.32	8.6	0.78	10.3	3.87	13.1	9.68	14.2
CAL <2	4.68	0.52	7.4	0.56	3.9	3.86	6.9	11.33	8.8
ASSAY	100.0	0.33	100.0	0.67	100.0	2.62	100.0	6.04	100.0



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

5.1 Mineralogy

The full report for optical mineralogy carried out on the Severn Bulk Composite is contained in Appendix 2.

Optical mineralogy was completed on the Severn Bulk Composite by MODA. Four scans using standard MODA techniques were carried out as detailed below;

In a first scan, for each fraction, 100 grains were selected at random and the area % of each mineral present was visually estimated. The minerals logged were: *pyrite+marcasite* (Py), *pyrrhotite* (Po), *cassiterite* (Cs), *stannite* (St), *arsenopyrite* (As), *chalcopyrite* (Cp), *sphalerite+galena* (SpGn) and *gangue* (*quartz, silicates, carbonates, etc*, Ga). This allowed calculation of an overall mineralogical composition.

In a second scan, for each fraction, 100 grains containing pyrite or pyrrhotite were selected at random and logged as per the first scan. This improved the count statistics for the Fe sulphides.

In a third scan, for each fraction, 100 grains containing cassiterite or stannite were selected at random and logged as per the first scan. This improved the count statistics for the Sn mineralisation.

In a fourth scan, for each fraction, 100 grains containing sphalerite, galena, chalcopyrite, stannite or tetrahedrite were selected at random and logged as per the first scan. This improved the count statistics for miscellaneous base metal mineralisation.

The mineralogy is summarised in the extracts and tables below (reproduced from MODA's report);

The following minerals were identified, in approximate descending order:

- Gangue (*quartz, silicates, carbonate, rutile, carbonaceous matter, fluorite, talc* etc.)
- Pyrite (95.4% crystalline and 4.6% *melnikovite*)
- Pyrrhotite
- Magnetite
- Sphalerite
- Cassiterite
- Marcasite
- Galena
- Arsenopyrite
- Chalcopyrite
- Goethite
- Hematite
- Stannite (rare)
- Tetrahedrite (very rare)
- Bismuthinite (very rare)
- Native bismuth (very rare)



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Severn Bulk Comp Composition Vol% (from total scan)

Fraction	Wt%	Py	Po	Cs [#]	St [#]	As [#]	Cp [#]	SpGn	Ga
+212µm	12.2	11.7	0.2	0.4	0.0	0.0	0.1	0.8	86.9
+150µm	9.5	22.9	1.7	0.2	0.0	0.1	0.0	1.4	73.8
+106µm	11.6	23.0	4.6	0.2	0.0	1.0	0.0	1.1	70.1
+75µm	9.9	31.4	1.2	1.0	0.0	0.1	Tr	0.0	66.3
+53µm	9.9	26.3	3.5	1.2	1.0	0.0	0.1	2.1	66.0
+38µm	7.5	26.6	9.5	0.5	0.0	0.0	0.2	2.1	61.1
+20µm	9.0	29.9	6.2	1.3	0.0	0.0	0.2	4.0	58.4
+8µm	10.6	28.3	6.7	2.0	0.0	0.0	0.0	3.0	60.1
TOTAL	80.2	24.5	3.9	0.8	0.1	0.2	0.1	1.7	68.6

Py=pyrite, Po=pyrrhotite, Cs=cassiterite, St=stannite, As=arsenopyrite, Cp=chalcopyrite, SpGn=sphalerite+galena, Ga=gangue
count statistics are very poor for the scarce minerals

Severn Bulk Comp Composition Vol% (from Sn scan)

Fraction	Sn Wt%	Py	Po	Cs	St	As	Cp	SpGn	Ga
+212µm	6.2	15.6	4.2	12.9	0.4	0	0.1	0.1	66.8
+150µm	8.0	19.6	2.2	23.8	0.1	0.9	0.1	0	53.4
+106µm	8.2	11.0	4.9	32.2	2.6	0	0.7	2.0	46.7
+75µm	11.6	6.1	1.6	43.2	1.8	0	1.1	0.7	45.6
+53µm	11.1	10.0	1.6	44.1	4.2	0	0.8	2.2	37.2
+38µm	12.7	3.8	3.1	64.8	4.2	Tr	0.8	1.6	21.8
+20µm	10.1	4.1	0.1	82.0	1.3	0	0.1	0.1	12.5
+8µm	12.6	1.8	0.4	87.8	2.1	0	0.4	0	7.6
TOTAL	80.5	7.9	2.1	53.2	2.3	0.1	0.6	0.9	33.1

Notably the residence of Sn in cassiterite sums to 99% with 1% in stannite.

Also of note the estimated Zn and Pb head grades of the Severn Bulk Composite are 0.9%Zn and 0.6% Pb, present as sphalerite and galena and are in reasonable agreement with the head assays shown in Table 1.



STELLAR RESOURCES LIMITED
 HEEMSKIRK TIN PROJECT
 SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Severn Bulk Comp Cassiterite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary+
			Py	Po	St	Cp	As	Ga	
+212µm	6.2	0	1	1	0	0	0	71	26
+150µm	8.0	17	9	0	0	0	0	41	32
+106µm	8.2	28	8	0	0	0	0	45	17
+75µm	11.6	46	2	0	0	0	0	41	11
+53µm	11.1	59	3	0	0	0	0	36	2
+38µm	12.7	66	2	1	0	1	0	25	4
+20µm	10.1	72	0	1	0	1	0	21	3
+8µm	12.6	83	1	1	0	1	0	14	0
TOTAL	80.5	52	3	1	0	0	0	34	10

Severn Bulk Comp Cassiterite association%

Fraction	Sn Wt%	%associated with					
		Py	Po	St	Cp	As	Ga
+212µm	6.2	21	9	2	5	0	94
+150µm	8.0	36	6	0	2	0	73
+106µm	8.2	21	4	0	0	0	62
+75µm	11.6	7	3	5	5	0	50
+53µm	11.1	5	0	0	1	0	38
+38µm	12.7	4	2	0	1	0	28
+20µm	10.1	2	1	0	2	0	24
+8µm	12.6	1	1	0	1	0	14
TOTAL	80.5	10	3	1	2	0	43



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Severn Bulk Comp Stannite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary
			Py	Po	Cs	Cp	As	Ga	
+212µm	6.2	0	0	0	0	0	0	0	100
+150µm	8.0	0	0	0	0	0	0	0	100
+106µm	8.2	39	0	0	0	29	0	14	18
+75µm	11.6	57	0	0	0	6	0	0	37
+53µm	11.1	24	0	0	0	22	0	1	42
+38µm	12.7	24	0	0	0	68	0	0	3
+20µm	10.1	0	4	0	0	0	0	86	10
+8µm	12.6	98	2	0	0	0	0	0	0
TOTAL	80.5	35	1	0	0	18	0	12	32

Severn Bulk Comp Stannite association%

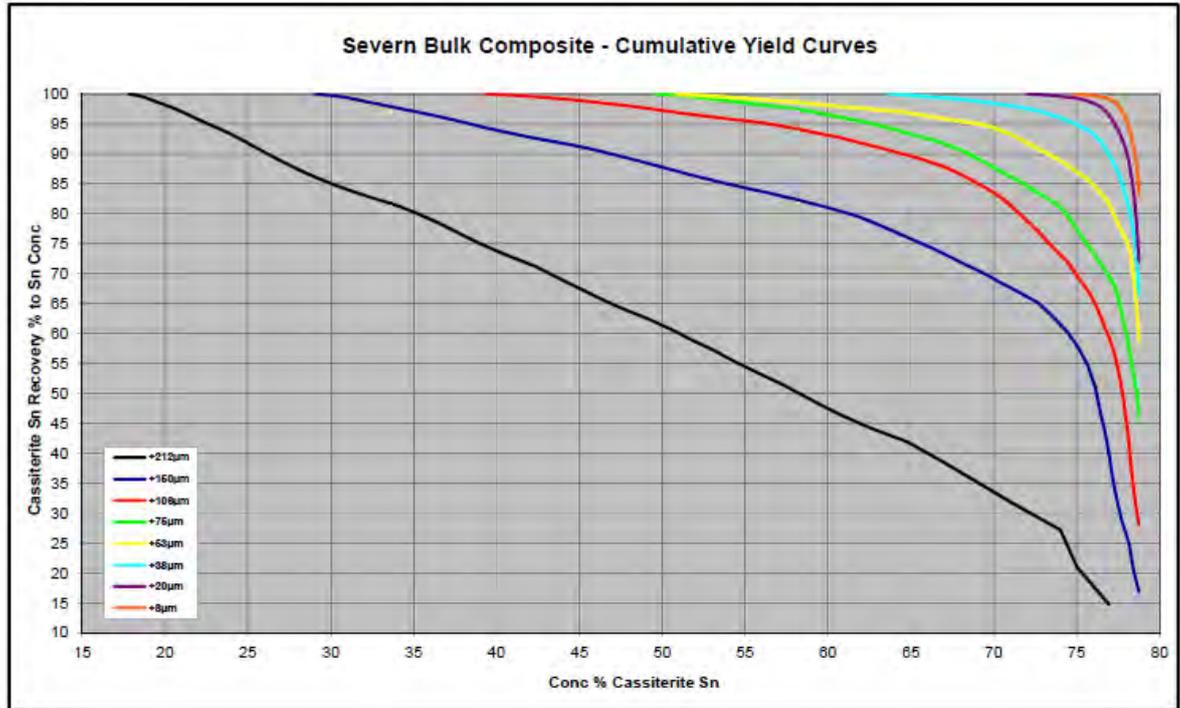
Fraction	Sn Wt%	%associated with					
		Py	Po	Cs	Cp	As	Ga
+212µm	6.2	0	100	97	97	0	3
+150µm	8.0	0	0	100	62	0	100
+106µm	8.2	0	0	0	46	0	32
+75µm	11.6	11	0	12	41	0	26
+53µm	11.1	2	2	12	61	0	28
+38µm	12.7	0	0	0	70	0	3
+20µm	10.1	4	0	10	0	0	96
+8µm	12.6	2	0	0	0	0	0
TOTAL	80.5	3	8	22	44	0	34

Stannite is a rare fine-grained component, mainly hosted by chalcopyrite, but also sphalerite, galena, pyrite, cassiterite and gangue.

The observations of stannite are in-line with the soluble Sn content of the Severn Bulk Composite (and overall Severn resource). Stannite is likely responsible for the major portion of Sn loss from the sulfide flotation circuit under the optimised conditions (refer Section 8).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**



Notably pyrite and pyrrhotite are reasonably well liberated at much coarser sizes compared to cassiterite (refer Table 4), indicating a relatively coarse primary grind should provide adequate sulfide roughing performance, while a significantly heavier regrind is required in the gravity circuit. However, given the associations of cassiterite with both pyrite and pyrrhotite a heavy regrind in the sulfide circuit is expected to be required to minimise Sn losses to the final sulfide concentrate.

Table 4 – Comparison of Liberation of Pyrite, Pyrrhotite and Cassiterite

Fraction (µm)	+212	+150	+106	+75	+53	+38	+20	+8
Pyrite	46	49	67	74	70	85	87	97
Pyrrhotite	53	62	73	70	67	91	76	88
Cassiterite	0	17	28	46	59	59	72	83



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

6 COMMINUTION

Comminution testing of the Severn Bulk Composite sample consisted of determination of Bond Ball Mill Work Index, Bond Rod Mill Work Index and bulk SG.

Full results are contained in Appendix 3 and summarised in Table 5, along with those for the Saint Dizier Bulk Composite for comparison.

Table 5 – Severn Bulk Composite Comminution Parameters

Parameter	Severn Bulk Composite	Saint Dizier Bulk Composite	Units
Bond Ball Mill Work Index	20.1	17.7	kWh/t
Bond Rod Mill Work Index	20.5	19.0	kWh/t
Bulk SG	1.8	1.8	

Results indicate the Severn ore is moderately hard.

Comminution testing in previous Heemskirk testwork was limited to a single Bond Ball Mill Work Index determination for Severn Comp 3. The Bond Ball Mill Work Index for Severn Comp 3 was; BWI = 17.5 kWh/t, indicating this sample was softer than the Severn Bulk Composite.

Laboratory grind sizes and times of the Severn Bulk Composite, previous Lower Queen Hill metallurgical composites, along with the Saint Dizier metallurgical composites were compared in order to determine relative grindability to give an indication of the variability in comminution properties of these deposits.

Relative grindability was calculated as;

$$\text{Relative grindability} = W_{i_t}/W_{i_r} = (10/\sqrt{P_r} - 10/\sqrt{F_r}) / (10/\sqrt{P_t} - 10/\sqrt{F_t})$$

for samples ground for the same length of time under the same conditions, where

W_{i_t} = estimated Bond index of test sample

W_{i_r} = measured Bond index of reference sample

P_r = P80 of reference sample

F_r = F80 of reference sample

P_t = P80 of test sample

F_t = F80 of test sample

Results are summarised in Table 6.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 6 – Relative Grindability of Various Heemskirk Composites

PROJECT Ore Sample	T0879 Severn Severn Bulk Composite	T0887 Saint Dizier St Dizier Bulk Composite	T0887 Saint Dizier Comp 2	T0887 Saint Dizier Comp 3	T0887 Saint Dizier Comp 4	T0887 Saint Dizier Comp 2+3	T0819 Lower Queen Hill Comp 6 Sinks/Fines	T0819 Lower Queen Hill Comp 6 Sinks/Fines/Floats (whole ore)	T0714 Severn Comp 3
DATE	20/05/2014	15/05/2014	24/07/2014	25/07/2014	25/07/2014	5/09/2014	6/05/2013	11/06/2013	26/10/2012
Measured:									
BBWi (kWh/t)	20.1	17.7	-	-	-	-	-	-	17.5
BRWi (kWh/t)	20.5	19.0	-	-	-	-	-	-	-
Relative Grindability	1.00	0.90	1.69	1.30	1.23	1.43	0.76	0.78	-
Estimated:									
BBWi (kWh/t)	20.1	17.7	34.0	26.2	24.8	28.7	14.9	15.4	-
BRWi (kWh/t)	20.5	19.0	34.6	26.7	25.3	29.3	16.0	16.5	-

Across the composites from the 3 deposits compared in Table 7 there is considerable variability in ore competency.

The Saint Dizier composites shown are significantly more competent (harder) than the Severn Bulk Composite, with those produced from drill hole ST06 (Comp 2, 3, 4 and 2+3) being exceptionally hard ores.

The Lower Queen Hill composites shown are somewhat softer than the Severn Bulk Composite, being more in line with 'typical' base metals ores. Comparing the two Lower Queen Hill samples it can be seen heavy media separation had minimal impact on grindability.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

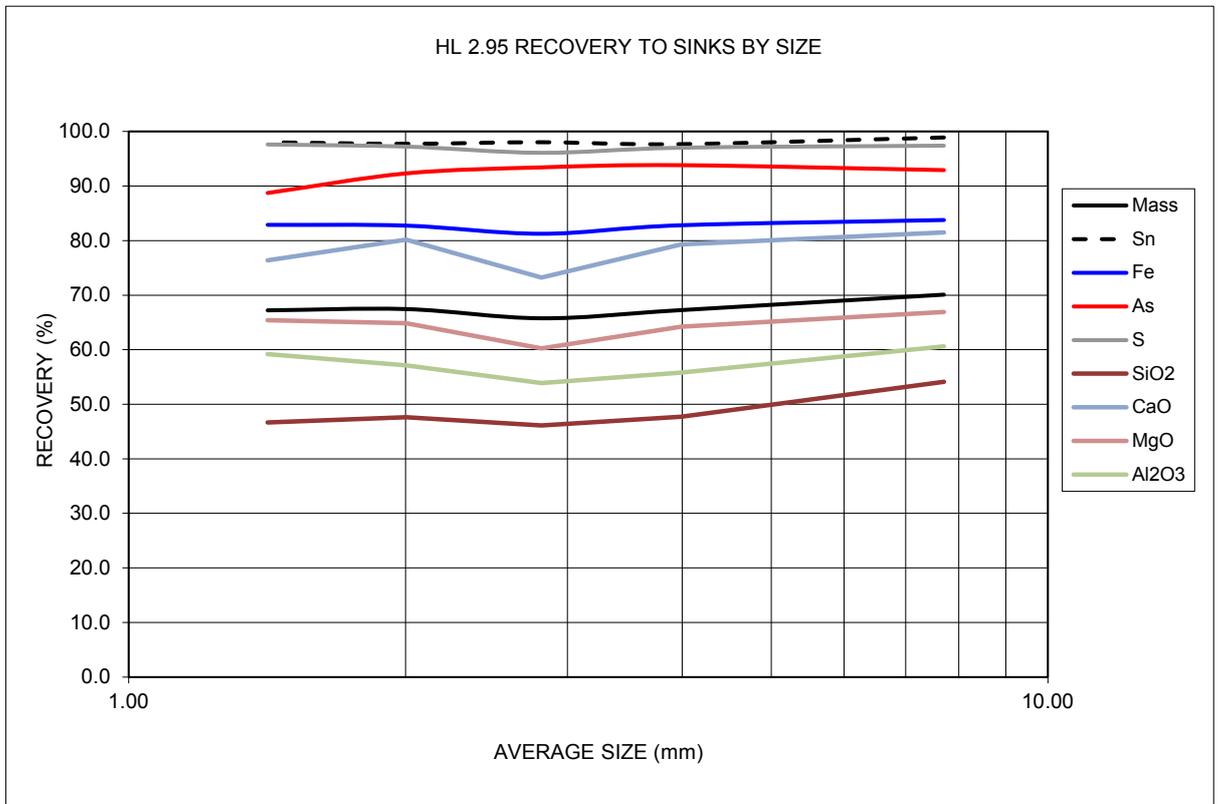
7 HEAVY MEDIA SEPARATION

Heavy Media Separation (HMS) testwork on the Severn Bulk Composite sample included both heavy liquid testing and small pilot scale heavy media testing. Results for these are summarised in Table 7, Figure 7-1 and Table 8 with full results contained in Appendix 4.

Table 7 – Summary of Heavy Liquid Separation Results; SBC, HL SG = 2.95

FRACTIONS mm	Picno SG	WT %	Overall															
			%Sn	dist	%Fe	dist	%As	dist	%S	dist	%SiO2	dist	%CaO	dist	%MgO	dist	%Al2O3	dist
Sinks+4.75	18.70	2.32	30.86	29.30	23.18	0.28	23.01	14.60	27.66	28.40	15.02	0.79	22.27	2.88	18.13	7.45	16.15	
Sinks+3.35	16.45	1.85	21.64	28.50	19.83	0.37	26.74	14.00	23.33	24.70	11.49	0.82	20.33	2.79	15.45	7.16	13.65	
Sinks+2.36	13.89	2.34	23.13	28.10	16.52	0.37	22.59	14.75	20.76	24.90	9.78	0.67	14.03	2.58	12.07	6.72	10.83	
Sinks+1.70	7.32	1.68	8.75	28.70	8.89	0.29	9.33	13.75	10.20	24.80	5.13	0.84	9.27	2.95	7.27	7.49	6.36	
Sinks+1.18	3.84	1.86	5.09	28.40	4.62	0.19	3.21	13.30	5.18	24.20	2.63	0.75	4.35	3.01	3.90	8.05	3.59	
Floats+4.75		7.98	0.06	0.34	13.30	4.49	0.05	1.75	0.91	0.74	56.40	12.72	0.42	5.05	3.34	8.97	11.35	10.50
Floats+3.35		8.01	0.09	0.51	12.15	4.12	0.05	1.76	0.88	0.71	55.60	12.59	0.44	5.31	3.19	8.60	11.65	10.82
Floats+2.36		7.23	0.09	0.46	12.45	3.81	0.05	1.59	1.15	0.84	55.90	11.44	0.47	5.13	3.27	7.97	11.05	9.27
Floats+1.70		3.53	0.08	0.20	12.40	1.85	0.05	0.78	0.81	0.29	56.50	5.64	0.43	2.29	3.31	3.94	11.65	4.77
Floats+1.18		1.87	0.09	0.12	12.15	0.96	0.05	0.41	0.67	0.13	57.30	3.04	0.48	1.36	3.30	2.08	11.50	2.50
Total Sinks		60.20	2.09	89.46	28.67	73.04	0.32	84.87	14.28	87.12	25.88	44.05	0.77	70.25	2.80	56.82	7.25	50.58
Total Floats		28.63	0.08	1.64	12.58	15.23	0.05	6.29	0.93	2.71	56.12	45.43	0.44	19.14	3.27	31.56	11.40	37.86
Fines -1.18		11.17	1.12	8.90	24.80	11.72	0.18	8.84	8.99	10.17	33.30	10.52	0.63	10.61	3.09	11.62	8.93	11.57
CALC FEED		100.00	1.41	100.00	23.63	100.00	0.23	100.00	9.87	100.00	35.36	100.00	0.66	100.00	2.97	100.00	8.62	100.00

Figure 7-1 Heavy Liquid Separation: Recovery by Size Fraction





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 8 - Heavy Media Separation Results: SBC, Fractions 9.50 to 2.35mm, Media SG = 2.95

PRODUCT	Wt (kg)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	Al2O3 (%)	Dist (%)
DMS Sinks (> 2.95)	8365	42.98	2.31	77.0	30.00	55.5	22.40	27.6	16.95	72.0	6.20	30.2
DMS Floats (< 2.95)	6917	35.54	0.14	3.9	14.70	22.5	51.50	52.5	1.61	5.7	12.05	48.6
Fines (<2.35mm)	4180	21.48	1.15	19.2	23.80	22.0	32.40	19.9	10.55	22.4	8.69	21.2
CALC Head	19462	100.00	1.29	100.0	23.23	100.0	34.89	100.0	10.12	100.0	8.81	100.0

Both the heavy liquid and heavy media testing were completed at an equivalent media SG of 2.95.

Both heavy liquid and heavy media testing gave moderate mass rejection to the floats fraction with fairly low Sn losses.

As expected both mass rejection and Sn loss for the heavy media testing were somewhat higher (1.24 times and 2.4 times respectively) than for the heavy liquid testing.

The heavy media testing results are considered more indicative of likely industrial scale performance.

These results are better than the majority of the previous heavy liquid / heavy media testing completed on the Heemskirk ores.

Previous work showed:

- Heavy liquid separation on Severn Comp 2 (from T0714) gave 23.3% mass rejection, with 1.5% Sn loss at 0.1% Sn grade to the floats product.
- Dense media separation on Severn Comp 2 (from T0714) gave 38.3% mass rejection, with 7.0% Sn loss @ 0.2% Sn to the floats product.
- Heavy Liquid work on Queen Hill comp 1 and 2 (T0587) shows low Sn loss and moderate mass rejection; 17.9% mass rejection, 1.2% Sn loss for comp 1 and 8.8% mass rejection, 0.55% Sn loss for comp 2. For composite 2 mass rejection is quite poor.
- Heavy media work on Lower Queen Hill (T0819) showed unacceptably high Sn losses; 13.7% Sn for comp 4, 14.8% for comp 6, and 2.8% Sn for comp 5 but with minimal mass loss at only 6.6%.
- Heavy media work on Severn comp 4 (T0797) gave 6.3% Sn loss with 42.2% mass rejection.

7.1 Application of HMS in the Heemskirk Flowsheet

The Heemskirk Tin Project Prefeasibility Study process flowsheet included heavy media separation (HMS) prior to the primary milling circuit. However, due to the variability seen in results of earlier heavy media and heavy liquid testwork (completed prior to the current program) and results of the current work (refer Section 7), a review of the merits of inclusion of HMS in the flowsheet was completed.

The review completed is contained in Appendix 5, with the key conclusions and recommendations reproduced below;

Conclusions:



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

- *Over the range of mass rejection considered removal of HMS from the flowsheet is expected to have negligible impact on total CAPEX (within the accuracy of the estimate). However, operating costs are expected to rise with removal of HMS.*
- *The expected improvement in overall Sn recovery by the removal of HMS is expected to more than offset the increase in OPEX, leading to an improvement in net revenue of the order of \$2.6 M/y.*
- *Exclusion of HMS from the flowsheet simplifies the overall process flowsheet, and eliminates a loss opportunity (via HMS floats product) for Sn from the flowsheet.*
- *Previous testwork has shown HMS is not applicable to all ore types to be treated by the Heemskirk project.*
- *When considered from a processing only perspective HMS has no merits.*

Recommendations:

Based on the analysis completed heavy media separation detracts value from the Heemskirk project when the treatment of the same ROM (grade and tonnages of ore) is considered. That is, HMS detracts value when considered from a processing only perspective. On this basis inclusion of HMS in the Heemskirk flowsheet is not recommended.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

8 SULFIDE FLOTATION

Previous testwork on Severn had considered flotation of both whole of ore and HMS sinks plus fines material. This earlier work had generally given reasonable results (of the order of 7% Sn loss) with a reagent regime consisting of sulfuric acid, copper sulfate, PAX, MIBC and guar, in a circuit consisting of roughing plus regrind and 2 stage cleaning. This work had highlighted both;

- use of gangue depressant has significant benefit; This is critical to achieving low tin losses
 - Guar was identified as is very effective and outperformed other reagents tested
- regrind is also critical to achieving low tin losses

Review of this early work identified the need for further testwork to optimise both primary and regrind sizes and confirm appropriate target sulfur grades for both sulfide tails and final sulfide concentrate.

All sulfide flotation testwork completed in the current program, was carried out on the Severn Bulk Composite sample (whole of ore). This initially focused on optimisation of primary grind size, followed by regrind size, then optimisation of the overall float. Following optimisation of the sulfide float a series of larger (12 kg) batch flotation tests were completed to produce sulfide flotation tailings as feed to the downstream (gravity separation, de-sliming and tin flotation) testwork.

Complete results for the sulfide flotation testwork are contained in Appendix 6.

8.1 Primary Grind Size

A series of roughing tests (T02 to T06) were completed at primary grind sizes in the range P80 = 100 to 240 µm to aid in identifying the optimum grind size. Results are summarised in Figure 8-1 to Figure 8-4.

Over the range tested tin and sulfur flotation rates were quite comparable, with no significant shift in tin/sulfur selectivity observed.

Notably, tin and sulfur deportment to rougher concentrate did not vary significantly over this range of grind sizes; refer Table 9.

Table 9 – Tin and Sulfur Recovery to Rougher Concentrate with Varying Primary Grind Size

Test no.	Primary Grind Size (µm)	% Sn Recovery to Rougher Concentrate	% S Recovery to Rougher Concentrate
T02	100	11.9	93.8
T03	130	12.5	87.5
T04	160	12.6	91.7
T05	240	11.1	90.2
T06	240	11.6	92.5



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 8-1

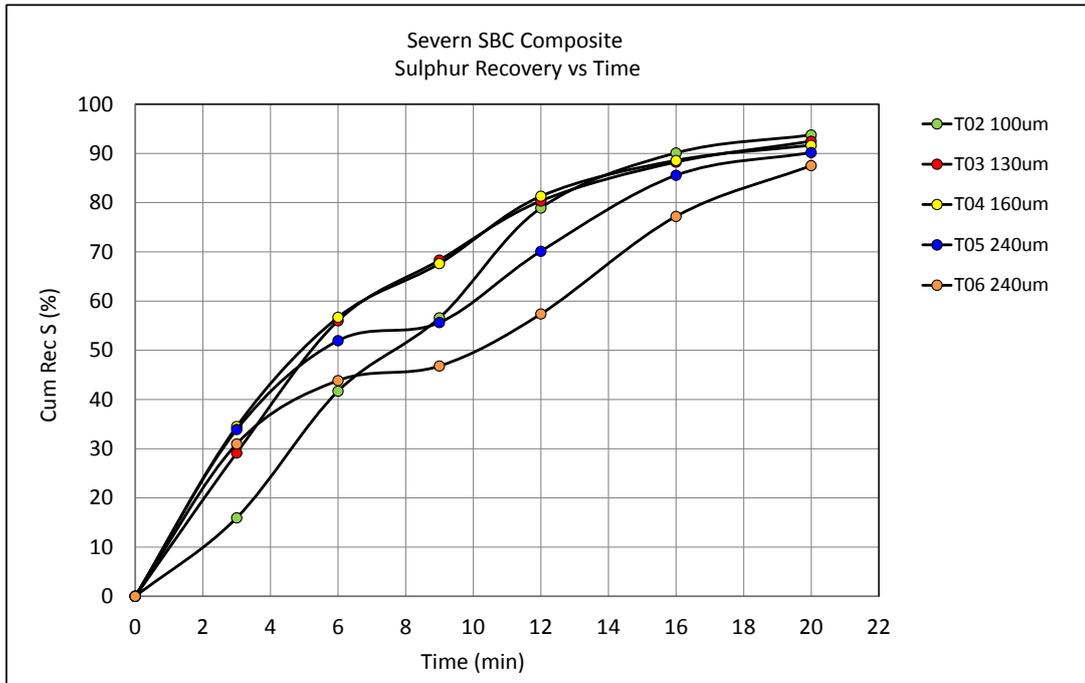
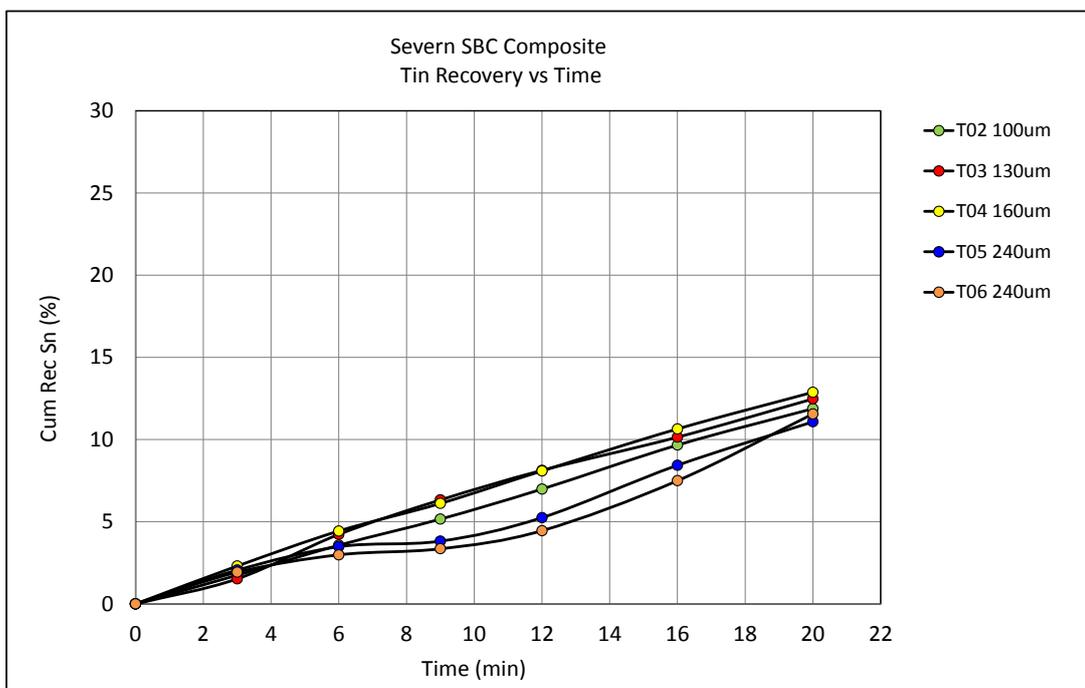


Figure 8-2





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 8-3

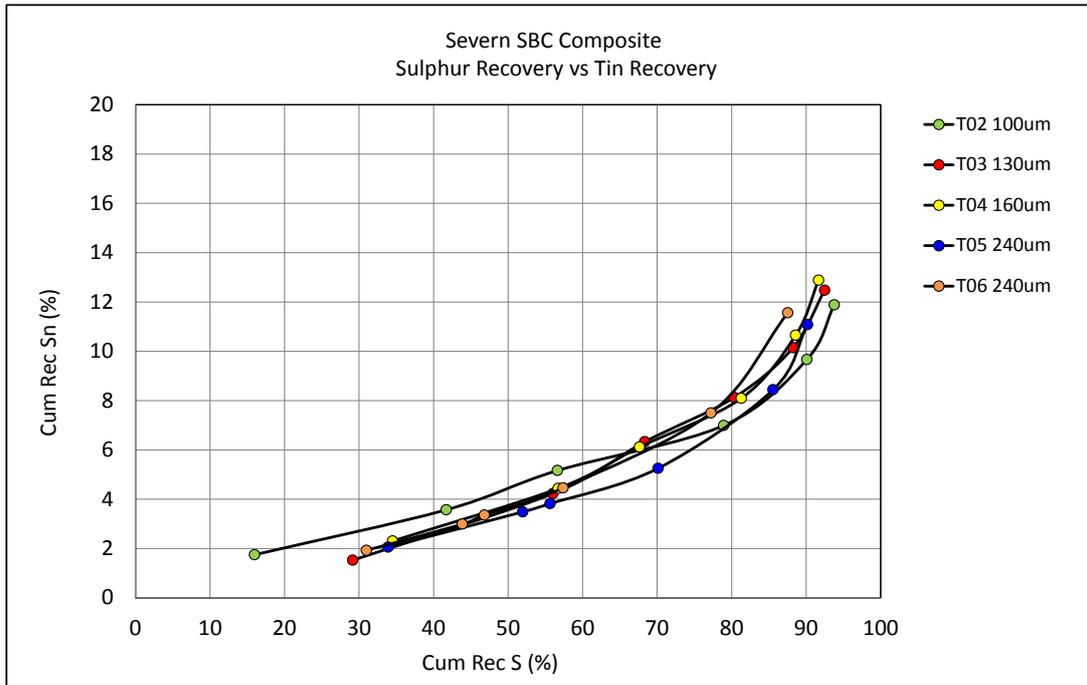
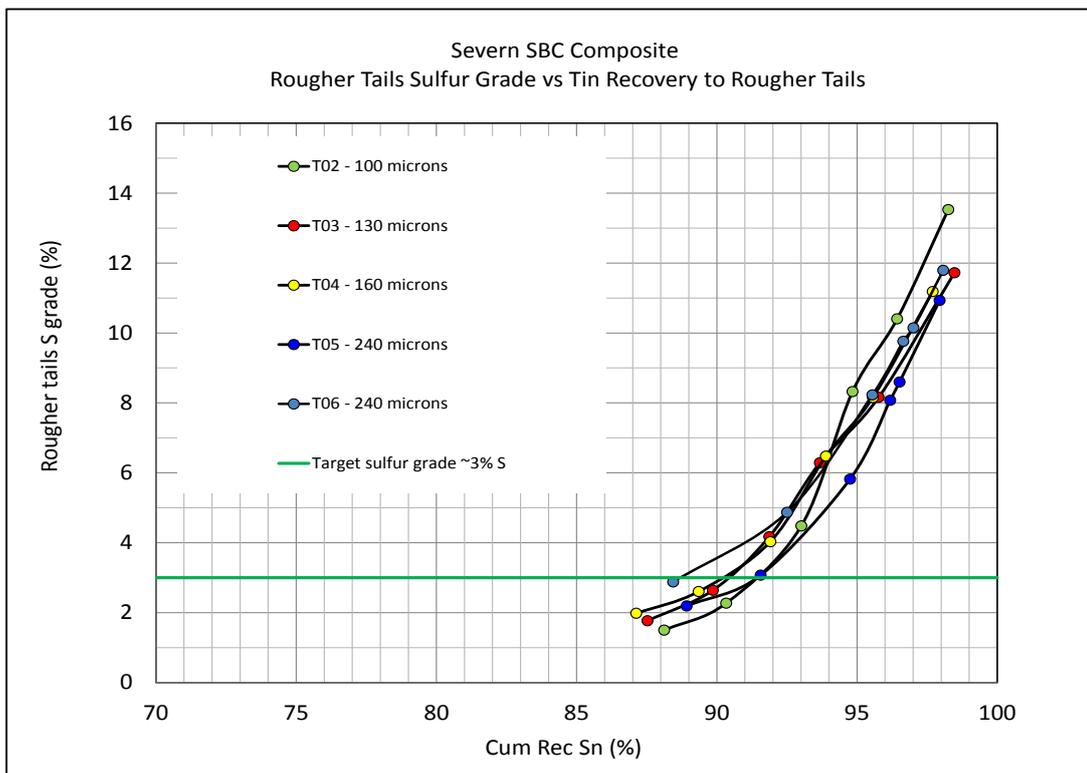


Figure 8-4





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 10 and Figure 8-5 show the variation in size by size tin distribution in sulfide rougher tails for varying primary grind sizes over the range P80 = 100 to 240 µm.

Table 10 – Variation in Size by Size Tin Distribution in Sulfide Rougher Tails with Primary Grind Size

Test	T02		T03		T04		T05		T06	
Primary Grind size (P80 µm)	100		130		160		240⁽¹⁾		240	
Rougher Tails Mass P80 (µm)	104		131		185		278		258	
Rougher Tails Sn P80 (µm)	75		93		118		160		179	
	Sn		Sn		Sn		Sn		Sn	
SIZE um	%	dist	%	dist	%	dist	%	dist	%	dist
600	1.25	2.4	0.91	2.4	1.02	5.4	0.98	7.9	0.93	3.6
212	0.44	0.9	0.43	1.7	0.57	4.0	0.71	7.6	0.87	12.8
150	0.44	1.5	0.62	3.0	0.84	4.7	1.00	5.4	1.07	6.6
106	0.70	4.7	0.97	7.6	1.15	8.1	1.31	7.6	1.31	8.7
75	1.22	10.6	1.47	12.3	1.59	11.0	1.75	9.4	1.57	9.6
<75	1.61	80.0	1.57	73.1	1.60	66.8	1.58	62.1	1.49	58.7
CALC	1.38	100.0	1.35	100.0	1.36	100.0	1.34	100.0	1.30	100.0
ASSAY	1.38		1.35		1.31		1.32		1.30	

Note 1: Significant coarse material present. Primary grind method modified for subsequent tests to eliminate excessive coarse material.

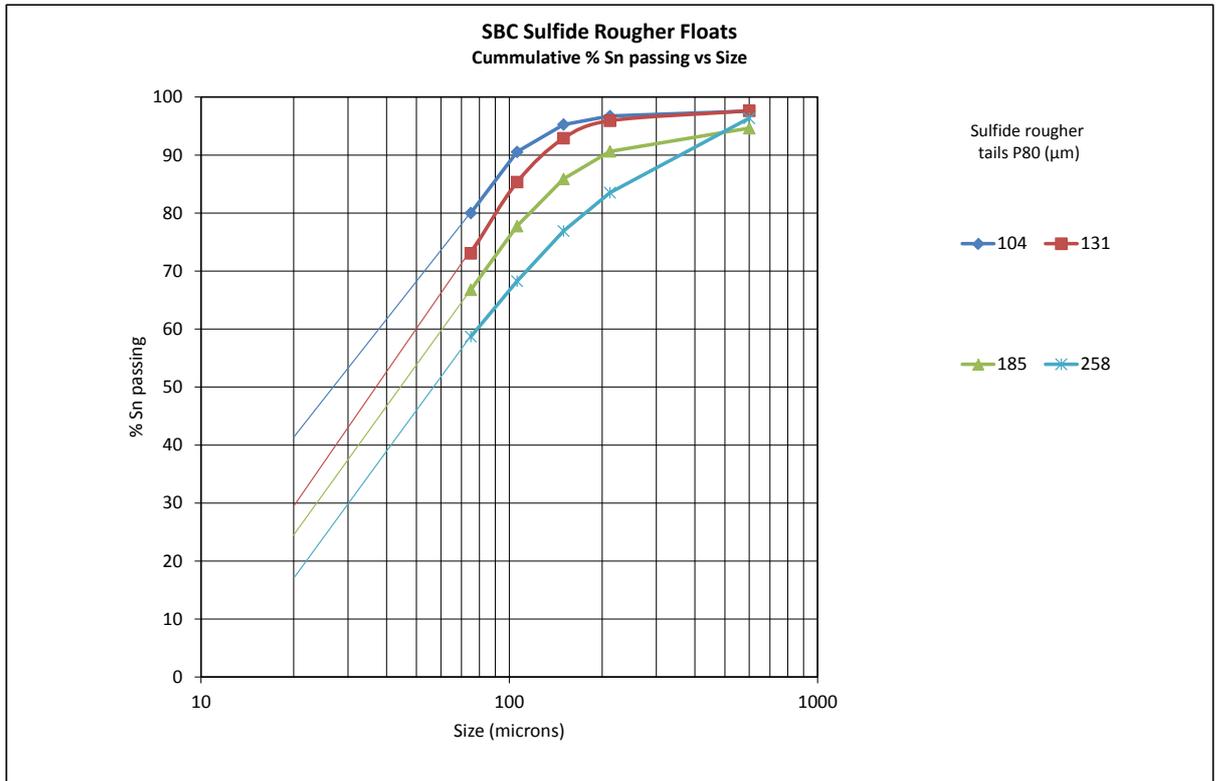
Over this size range tin P80 in the sulfide rougher tails increases from 75 µm following a primary grind of 106 µm, to 179 µm following a primary grind of 240 µm.

Significantly, the percentage of tin passing 30 µm (below which size gravity recovery is poor) is estimated to decrease from ~43% passing 30 µm at a primary grind size of 130 µm (grind size assumed in the PFS), to only ~30% passing 30 µm at a primary grind size of 240 µm. This is equivalent to ~30% reduction in fine tin generation, and is a key contributor to the improved gravity recovery achieved (refer Section 9).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 8-5



There is likely some scope to further coarsen primary grind size beyond 240 μm. However, this must be balanced against issues such as the handling of coarse solids and their 'floatability' through the sulfide flotation circuit, increasing sulfide regrind circuit power requirements and to a lesser extent gravity regrind power requirements. Given these considerations a primary grind P80 of 250 μm is recommended.

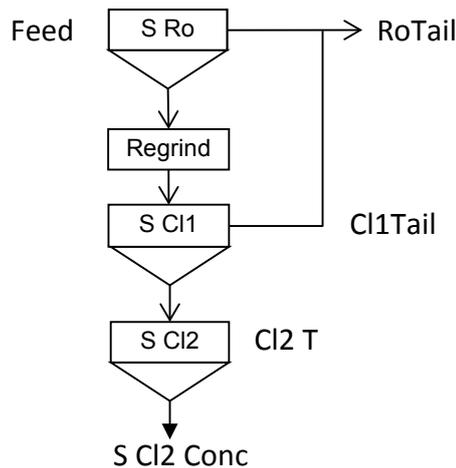
8.2 Regrind Size

Regrind optimisation tests, T07 to T13, were carried out following a primary grind of P80 = 250 μm and roughing at pH ~5.4, with ~900 g/t H₂SO₄, 225 g/t guar, 100 g/t CuSO₄, 140 g/t PAX and 70 g/t MIBC. Figure 8-6 shows the flowsheet tested, which consisted of roughing followed by regrind of the rougher concentrate and two stage open circuit cleaning of the regrind rougher concentrate. Cleaner 1 tails and rougher tails were combined to form the total sulfide flotation tails.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

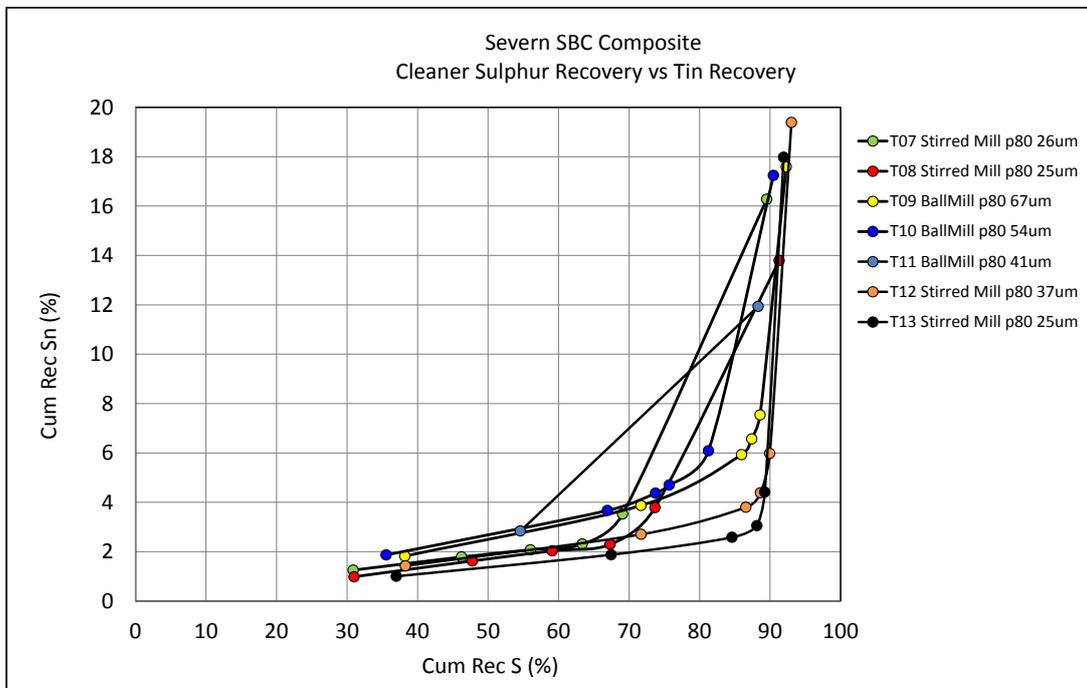
Figure 8-6 Roughing plus regrind and 2 stage cleaning flowsheet



For the regrind duty both ball milling and stirred milling with ceramic media were investigated.

Results are summarised in Figure 8-7, Figure 8-8 and Figure 8-9.

Figure 8-7





STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Figure 8-8

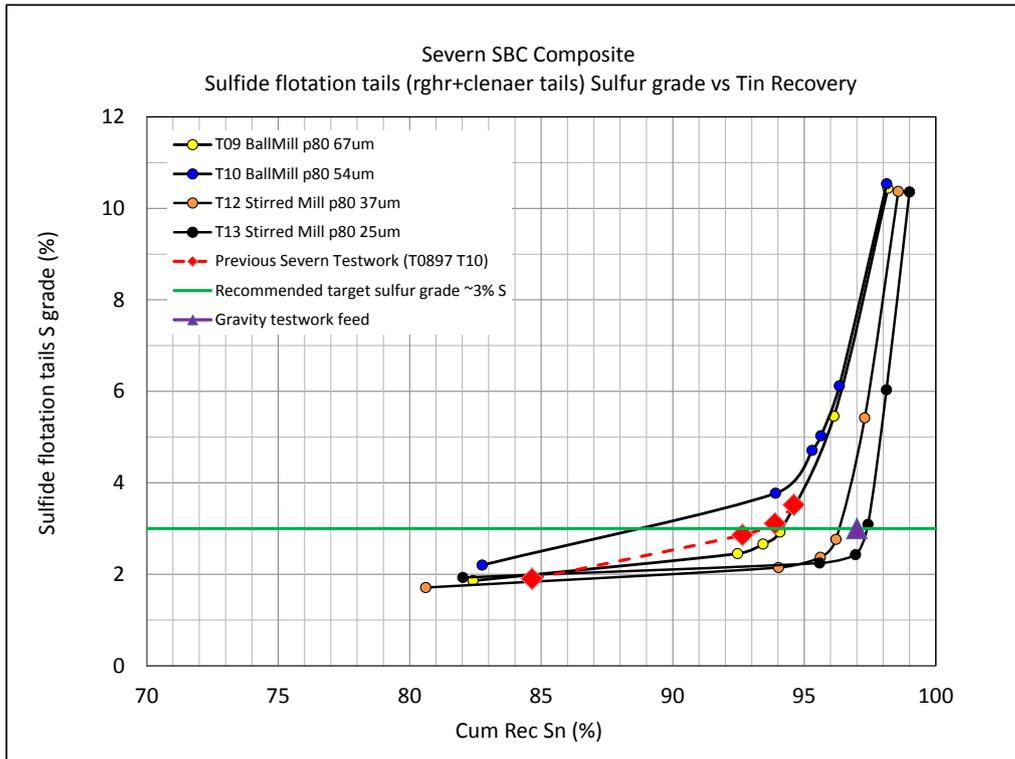
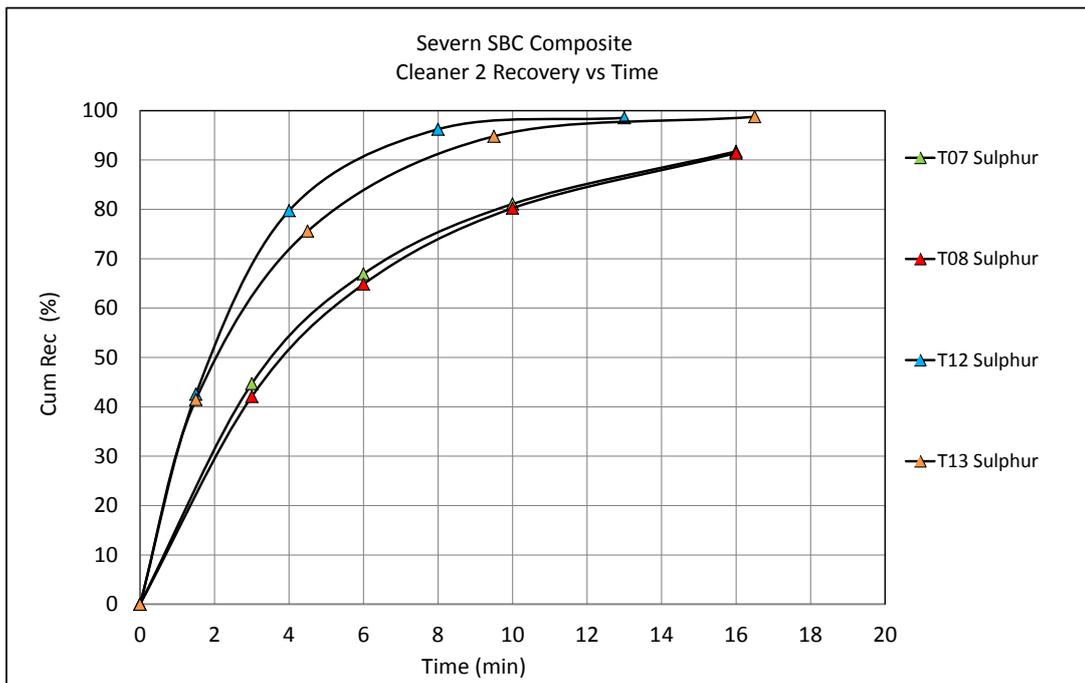


Figure 8-9





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Initial stirred milling tests, T07 and T08, which gave a P80 to 26 and 25 μm , performed relatively poorly due to sluggish sulfide kinetics. However, following optimisation of reagent scheme post regrind extremely good results were achieved with a regrind P80 of 25 μm , with 97.4 % Sn recovery achieved to sulfide flotation tails a grade of 3% sulfur.

Referring to Figure 8-8 it can be seen a target sulfide flotation tails grade of 3% sulfur is appropriate. A 3% sulfur grade is considered readily manageable through the gravity circuit (Renison Bell successfully has operated for many years at this target sulfur grade), while very low tin losses are achievable at this grade following appropriate regrind and cleaning. Targeting a lower sulfur grade would significantly increase tin losses, while higher grades would place additional load on the gravity circuit, sulfide dressing circuit and sulfide scavenger circuit.

Comparing results of T12 and T13 which reground to P80 of 37 and 25 μm respectively a Sn recovery improvement of over 1% can be achieved at sulfide flotation tails a grade of 3% sulfur at the finer regrind size.

Comparing results for tests with ball milling and stirred milling shows significantly improved performance is achievable utilising stirred milling for regrind.

- A target regrind size of P80 = 25 μm is recommended. Required regrind energy input to achieve this regrind size = 20 kWh/t
- Recommended target sulfide flotation tails grade = 3% sulfur
- Recommended target final sulfide flotation concentrate grade = 45% sulfur (~85% sulfide mineral).

Examination of the overall sulfide flotation results shows tin losses to final sulfide concentrate are strongly affected by final sulfide concentrate sulfur grade, with low losses favoured by high sulfur grades (hence reduced entrainment).

- Stirred milling for the sulfide regrind gives a clearly better outcome compared to ball milling. At the target regrind size stirred milling is expected to provide improved energy efficiency (of the order of 20%-30%), reduced media consumption costs and is also expected to provide advantages in installation costs compared to conventional ball milling.

8.3 Production of Sulfide Flotation Tailings for Downstream Testwork

Tests T14 to T21 were completed under the optimised conditions to produce sulfide flotation tailings for downstream testwork.

These larger scale sulfide flotation tests (12 kg batch floats) completed to generate sample for gravity and other downstream testwork produced ~80 kg sulfide flotation tailings at 3% sulfur with >97% Sn recovery as gravity circuit feed.

This demonstrated the optimised conditions at larger scale across a significant quantity of sample.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Notably both guar and frother consumption was reduced for these larger scale tests to 93 g/t and 64 g/t respectively compared with 325 g/t and 125 g/t for the smaller scale tests without adverse impact on performance.

8.4 Impact of Sulfur Head Grade

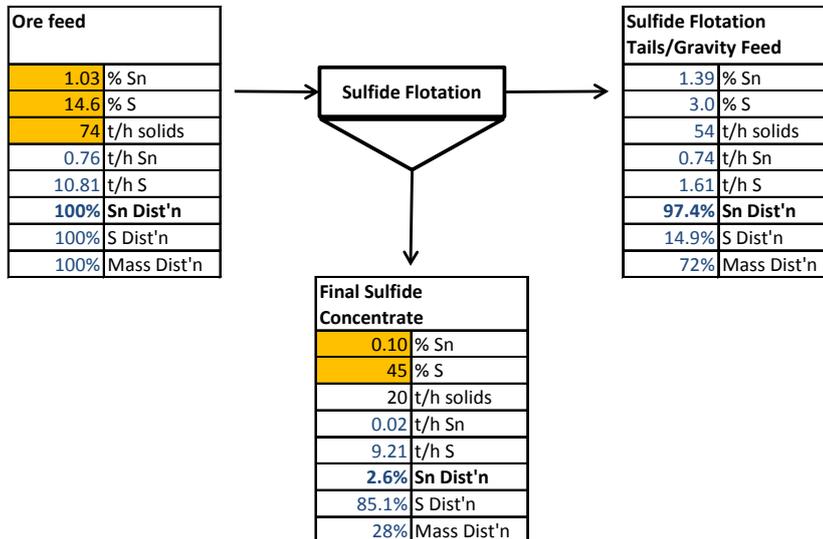
Although not considered untypical, S content of the Severn Bulk Composite sample is higher than the average for the overall Severn Mineral Resource at 14.6% S compared with 9.06% S. This results in a higher than average mass department to final sulfide concentrate for the SBC, and likely higher Sn losses than average. Figure 8-10 summarises mass, Sn and S department across the sulfide flotation circuit as per the optimised testwork results achieved on the Severn Bulk Composite .

Estimated mass, Sn and S department across the sulfide flotation circuit at 9.06% S head grade (average for the overall Severn Mineral Resource) is shown in Figure 8-11. This assume similar tin grades in final sulfide concentrate can be achieved at the resources average S grade.

At a sulfur head grade equal to the overall Severn Mineral Resource of 9.06% S, tin loss to the final sulfide concentrate is estimated at 1.4%, with 98.6% Sn recovery to the gravity circuit feed.

Figure 8-10 Tin Department Across Sulfide Flotation Circuit at 14.6% S head grade

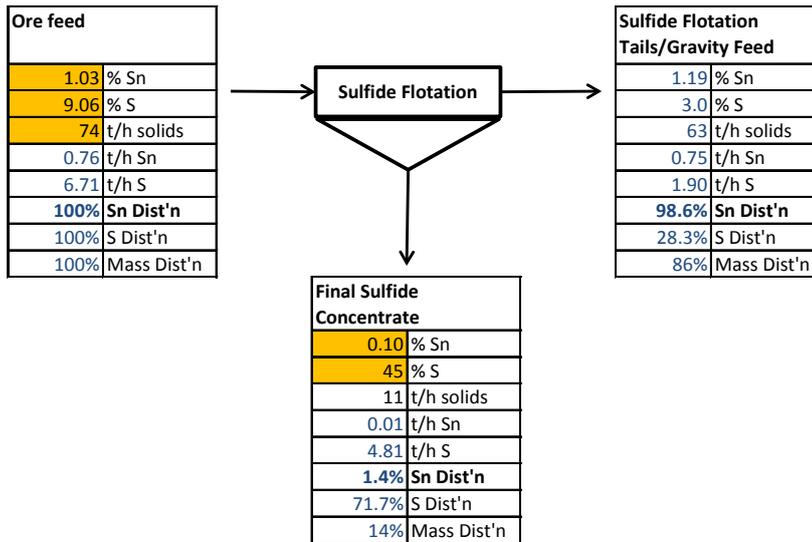
(as per optimised testwork on Severn Bulk Composite)





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 8-11 Estimated Tin Department Across Sulfide Flotation Circuit at 9.06% S head grade
(equivalent to overall Severn Mineral Resource S grad; assumes same performance as SBC)



Assuming similar tin grades in final sulfide concentrate can be achieved at the resources average sulfur grade, tin loss to the final sulfide concentrate is estimated at 1.4%, with 98.6% Sn recovery to the gravity circuit feed. This compares with a loss of 2.6% the final sulfide concentrate for the Severn Bulk Composite.

This represents some additional upside in overall tin recovery compared to that presented in Section 14.1.

8.5 Key Outcomes

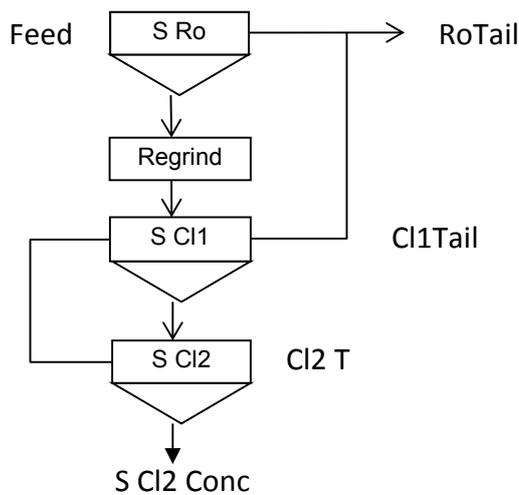
- Primary grind size can be significantly coarser than what was considered in the PFS; a P80 of 250 µm is recommended. This compares with a P80 of 130 µm which was assumed for the PFS.
- A target regrind size of P80 = 25 µm is recommended. Required regrind energy input to achieve this regrind size = 20 kWh/t.
- Recommended target sulfide flotation tails grade = 3% sulfur
- Recommended target final sulfide flotation concentrate grade = 45% sulfur (~85% sulfide mineral).
- At the above target sulfur grades and grind sizes tin loss to final sulfide concentrate was 2.6% for the Severn Bulk Composite. Tin grade of the final sulfide concentrate was 0.10%.
- At a sulfur head grade equal to the overall Severn Mineral Resource of 9.06% S, tin loss to the final sulfide concentrate is estimated at 1.4%.
- Stirred milling for the sulfide regrind gives a clearly better outcome compared to ball milling. At the target regrind size stirred milling is expect to provide improved energy efficiency (of the



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

order of 20-30%), reduced media consumption costs and is also expected to provide advantages in installation costs compared to conventional ball milling.

Figure 8-12 – Recommended Circuit Configuration



The expected reagent consumptions for the sulfide flotation circuit based on dose rates observed in the testwork are summarised in Table 11.

Table 11 – Expected Sulfide Float Reagent Consumptions

pH	5.4
Sulfuric Acid	732 g/t
Copper Sulphate	200 g/t
PAX	225 g/t
Frother (MIBC)	64 g/t
Guar	93 g/t

8.6 Mineralogy of Sulfide Flotation Tails/Gravity Circuit Feed

Full reports for optical mineralogy carried out on the sulfide flotation tailings produced as feed to downstream gravity testwork are contained in Appendix 2. Initially standard MODA scans were completed (refer report dated July 2014). The slides were subsequently re-logged to assess siderite/cassiterite associations (refer report dated July 2014).

Figure 8-13 shows size distribution and size by size assays and metal department of the sulfide flotation tailings.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

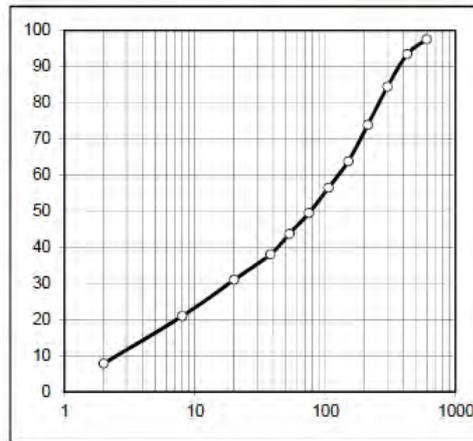
Figure 8-13 SBC Sulphide Flotation Tailings Size Distribution and Size by Size assays



BURNIE LABORATORY
SIZE ANALYSIS REPORT SHEET WITH CS6

PROJECT	T0879
SAMPLE	SBC Sulphide Tails
DATE	70614
TECHNICIAN	MS

SBC Sulphide Tails	SIZE um	WEIGHTS			
		gm	(%)	%PASS	
P80	600	4.32	2.44	97.6	
	425	7.34	4.15	93.4	
	300	15.89	8.99	84.4	
	263	212	18.62	10.54	73.9
		150	17.83	10.09	63.8
		106	12.92	7.31	56.5
		75	12.33	6.98	49.5
		53	10.21	5.78	43.7
		38	10.02	5.67	38.1
		20	12.48	7.06	31.0
MINS 20	CS5	8	17.75	10.04	21.0
CENTRIFUGE	CS6	2	23.24	13.15	7.8
	SUB	13.79	7.80	0.0	
	TOTAL	176.7	100.0		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mount Number
		%	dist	%	dist	%	dist	%	dist	%	dist	
212	26.12	0.68	13.3	16.85	22.5	0.09	13.8	3.05	25.9	48.70	31.1	879194
106	17.40	1.37	17.8	18.40	16.4	0.08	8.2	2.45	13.8	45.60	19.4	879195
53	12.75	1.75	16.7	18.00	11.7	0.05	3.8	2.75	11.4	39.50	12.3	879196
20	12.73	2.23	21.2	21.20	13.8	0.16	12.0	2.71	11.2	39.90	12.4	879197
8	10.04	2.39	17.9	24.60	12.6	0.38	22.4	3.00	9.8	31.60	7.8	897198
2	13.15	0.51	5.0	21.70	14.6	0.25	19.3	4.16	17.8	34.70	11.2	
CAL <2	7.80	1.41	8.2	20.87	8.3	0.45	20.5	4.01	10.2	30.64	5.8	
ASSAY	100.0	1.34	100.0	19.55	100.0	0.17	100.0	3.08	100.0	40.90	100.0	

SIZE um	WT %	MnO		CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist	%	dist
212	26.12	0.44	20.2	0.84	23.1	3.76	26.5	9.05	27.7
106	17.40	0.63	19.2	1.00	18.3	3.62	17.0	7.87	16.0
53	12.75	0.61	13.6	1.01	13.6	3.01	10.4	6.34	9.5
20	12.73	0.71	15.9	1.29	17.3	3.28	11.3	6.64	9.9
8	10.04	0.78	13.7	1.20	12.7	3.27	8.9	6.28	7.4
2	13.15	0.44	10.2	0.85	11.8	4.13	14.7	10.65	16.4
CAL <2	7.80	0.53	7.2	0.40	3.3	5.32	11.2	14.50	13.2
ASSAY	100.0	0.57	100.0	0.95	100.0	3.70	100.0	8.55	100.0



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

The mineralogy is summarised in the extract and tables below (reproduced from MODA's report);

The following minerals were identified, in approximate descending order:

- Gangue (*quartz, silicates, carbonate, rutile, carbonaceous matter, fluorite, talc* etc.)
- *Magnetite* (preferentially represented in the +106µm fraction)
- *Pyrite* (78% crystalline and 22% *melnikovite*)
- *Cassiterite*
- *Pyrrhotite*
- *Sphalerite*
- *Marcasite*
- *Galena*
- *Arsenopyrite*
- *Chalcopyrite*
- *Goethite*
- *Hematite*
- *Stannite* (rare)
- *Native bismuth* (very rare)

Severn Bulk Comp Sulphide Tail Composition Vol% (from total scan)

Fraction	Wt%	Py	Po	Cs [#]	St [#]	As [#]	Cp [#]	SpGn [#]	Ga
+212µm	26.1	2.3	0.5	0.3	Tr	0	Tr	0.5	96.5
+106µm	17.4	5.1	0.4	1.9	Tr	0	0	0.1	92.5
+53µm	12.8	2.5	1.1	2.0	Tr	1.0	0	0	93.4
+20µm	12.7	2.8	1.0	0.1	Tr	0	0	0	96.2
+8µm	10.0	4.4	0	2.3	0	0	0	1.0	92.3
TOTAL	79.0	3.3	0.6	1.1	Tr	0.2	Tr	0.3	94.5

*Py=pyrite, Po=pyrrhotite, Cs=cassiterite, St=stannite, As=arsenopyrite, Cp=chalcopyrite, SpGn=sphalerite+galena, Ga=gangue
count statistics are very poor for the scarce minerals*

Severn Bulk Comp Sulphide Tail Composition Vol% (from Sn scan)

Fraction	Sn Wt%	Sd	Qz	Cs	PyMa	Po	Fl	OS	OG	Siderite fraction% of non-sulphide Ga
+212µm	13.3	16.1	36.6	12.9	1.2	1.0	1.4	0.2	30.8	19
+106µm	17.8	18.7	17.1	41.6	4.4	0.3	0.5	0.2	17.3	35
+53µm	16.7	16.4	9.9	54.6	2.5	0	1.0	0	15.5	38
+20µm	21.2	14.1	10.2	67.7	0.8	0	1.4	Tr	5.7	45
+8µm	17.9	7.7	1.0	88.1	0	0	1.0	0	2.3	64
TOTAL	86.9	14.5	13.7	55.7	1.8	0.2	1.1	0.1	13.1	34

Sd=siderite, Qz=quartz, Cs=cassiterite, PyMa=pyrite/marcasite, Po=pyrrhotite, Fl=fluorite, OS=other sulphides, OG=other gangue



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Severn Bulk Comp Sulphide Tail Cassiterite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary+
			Py	Po	St	Cp	As	Ga	
+212µm	13.3	0	0	0	0	0	0	73	27
+106µm	17.8	14	3	3	0	0	0	70	10
+53µm	16.7	50	0	0	0	0	0	47	2
+20µm	21.2	71	0	0	0	1	0	27	1
+8µm	17.9	87	0	1	0	0	0	10	1
TOTAL	86.9	48	1	1	0	0	0	43	7

Severn Bulk Comp Sulphide Tail Cassiterite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary+
			Sd	Qz	PyMa	Po	Fl	OG	
+212µm	13.3	0	0	11	0	0	0	18	71
+106µm	17.8	26	16	9	2	0	0	22	22
+53µm	16.7	55	6	4	2	0	0	23	10
+20µm	21.2	64	11	4	0	0	0	14	7
+8µm	17.9	92	3	2	0	0	0	3	0
TOTAL	86.9	50	8	6	1	0	0	16	19

Severn Bulk Comp Sulphide Tail Cassiterite association%

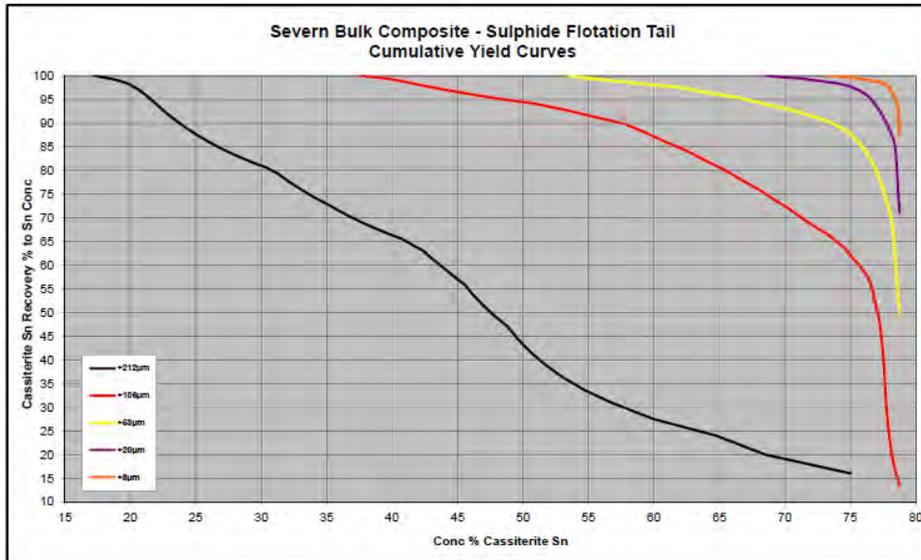
Fraction	Sn Wt%	%associated with					
		Py	Po	St	Cp	As	Ga
+212µm	13.3	18	16	0	1	0	100
+106µm	17.8	12	5	0	1	0	80
+53µm	16.7	0	1	0	2	2	50
+20µm	21.2	0	0	0	1	0	28
+8µm	17.9	0	2	0	0	0	11
TOTAL	86.9	5	4	0	1	0	50

Severn Bulk Comp Sulphide Tail Cassiterite association%

Fraction	Sn Wt%	%associated with					
		Sd	Qz	PyMa	Po	Fl	OG
+212µm	13.3	40	72	4	9	8	59
+106µm	17.8	31	17	6	2	1	37
+53µm	16.7	11	12	4	2	0	28
+20µm	21.2	14	9	0	0	0	19
+8µm	17.9	3	2	0	0	0	3
TOTAL	86.9	19	19	3	2	1	27



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**



Notably the residence of Sn in cassiterite sums to >99.9% with <0.1% in stannite.

Sn liberation is limited in the coarser fractions. However, this increases to >50% in the +53 µm, clearly indicating the need for significant regrind within the gravity circuit.

Overall 19% of the cassiterite observed is associated with siderite. Generally association with siderite increases in the coarser fractions with 40% of cassiterite +212 µm being associated with siderite. Given the relatively high SG of siderite and association with cassiterite it is expected this will tend to concentrate within the gravity circuit.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

9 GRAVITY SEPARATION

Following optimisation of the sulfide flotation a series of larger (12 kg) batch flotation tests (tests T14 to T21) were completed on the Severn Bulk Composite under the optimised conditions to produce sulfide flotation tailings for downstream testwork. This produced ~80 kg of sulfide flotation tailings at 3% sulfur with >97% Sn recovery which was composited to form the gravity circuit feed.

Gravity separation testing consisted of initial batch testing, followed by lock cycle testing. In both cases testing was completed using a laboratory Mozley table, with size based separations completed via cycloning and screening. Two tests were also completed to assess the ability of the UF Falcon centrifugal separator to scavenge additional tin from the “-106 µm tails” stream produced from the lock testing.

The basic concept of the gravity circuit flowsheet was to produce a crude heavy mineral concentrate suitable for upgrading to saleable tin concentrate grades via dressing and (if required) concentrate leaching.

Full gravity testing results are contained in Appendix 7.

9.1 Gravity Separation Batch Testing

Initial batch testing results are summarized in Table 12 with Figure 9-1 summarising the overall mass balance based on sulfide flotation feed for the batch testing.

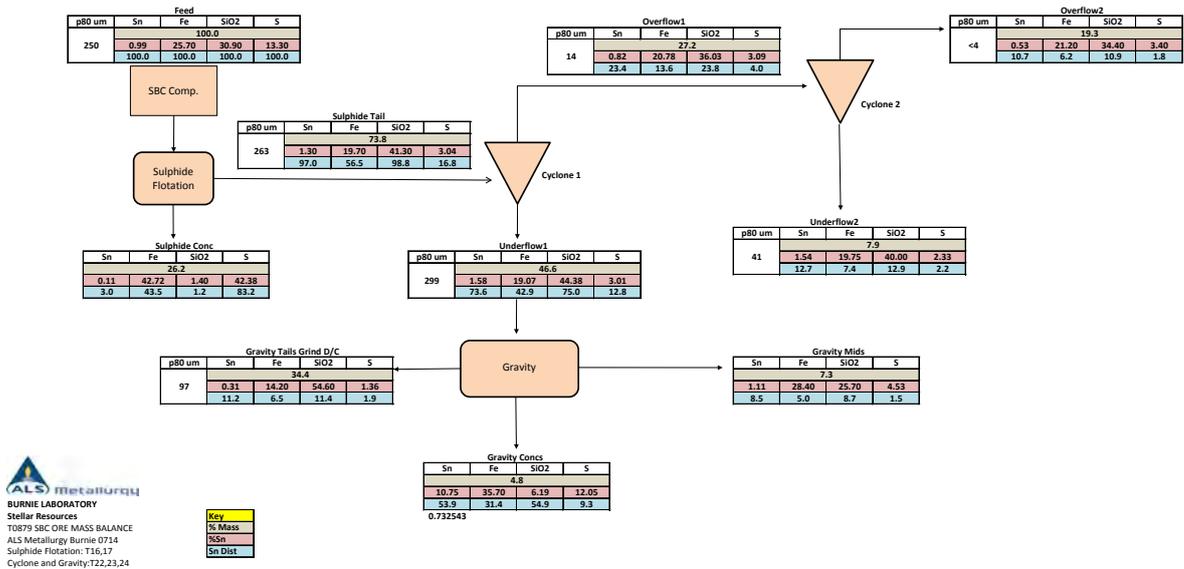
Table 12 – Gravity Batch Testing Results

<p>BURNIE LABORATORY: SEPARATION REPORT SHEET</p>				<table border="1"> <tr><td>PROJECT</td><td>T0879</td></tr> <tr><td>TEST NO</td><td>T22, T23, T24</td></tr> <tr><td>DATE</td><td>21/07/14</td></tr> <tr><td>TECH</td><td>MS</td></tr> </table>	PROJECT	T0879	TEST NO	T22, T23, T24	DATE	21/07/14	TECH	MS					
PROJECT	T0879																
TEST NO	T22, T23, T24																
DATE	21/07/14																
TECH	MS																
<table border="1"> <tr><td>TEST TYPE</td><td>Cyclone & Gravity Separation</td></tr> <tr><td>Stage 1</td><td>Cyclone T22</td></tr> <tr><td>Stage 2</td><td>Cyclone T23</td></tr> <tr><td>Stage 3</td><td>Mozley Separation T24</td></tr> </table>	TEST TYPE	Cyclone & Gravity Separation	Stage 1	Cyclone T22	Stage 2	Cyclone T23	Stage 3	Mozley Separation T24	<table border="1"> <tr><td>START MATERIAL</td><td>SBC - SRT (T22 cyclone) Feed</td></tr> <tr><td>FROM TEST NO</td><td></td></tr> <tr><td>START WEIGHT (gm)</td><td>1852.45</td></tr> </table>		START MATERIAL	SBC - SRT (T22 cyclone) Feed	FROM TEST NO		START WEIGHT (gm)	1852.45	
TEST TYPE	Cyclone & Gravity Separation																
Stage 1	Cyclone T22																
Stage 2	Cyclone T23																
Stage 3	Mozley Separation T24																
START MATERIAL	SBC - SRT (T22 cyclone) Feed																
FROM TEST NO																	
START WEIGHT (gm)	1852.45																
SEPARATION RESULTS																	
Product	Weight (gm)	P80 (Sizing) (%)	Weight (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	As (%)	Dist (%)	S (%)	Dist (%)	SiO2 (%)	Dist (%)	MnO (%)	Dist (%)		
T23 Overflow	484.30	<8	26.14	0.53	11.0	21.20	28.5	0.21	38.8	3.40	29.6	34.40	21.6	0.44	20.8		
Underflow	198.80	41	10.73	1.54	13.1	19.75	10.9	0.20	15.2	2.33	8.3	40.00	10.3	0.65	12.6		
T24 Gravity Conc	120.39		6.50	10.75	55.6	35.70	11.9	0.52	23.9	12.05	26.0	6.19	1.0	1.07	12.6		
Gravity Mids	184.36		9.95	1.11	8.8	28.40	14.5	0.08	5.6	4.53	15.0	25.70	6.1	1.12	20.2		
Gravity Tail Grind D/C	864.60	97	46.67	0.31	11.5	14.20	34.1	0.05	16.5	1.36	21.1	54.60	61.1	0.40	33.8		
Total	1852.45		100.00	1.26	100.0	19.44	100.0	0.14	100.0	3.01	100.0	41.73	100.0	0.55	100.0		
Product	Weight (gm)	P80 (Sizing) (%)	Weight (%)	CaO (%)	Dist (%)	MgO (%)	Dist (%)	Al2O3 (%)	Dist (%)	Sample No							
T23 Overflow	484.30	>8	26.14	0.52	15.8	4.35	31.4	11.90	36.4	879201							
Underflow	198.80	41	10.73	1.13	14.0	3.33	9.9	6.64	8.3	879202							
T24 Gravity Conc	120.39		6.50	0.69	5.2	2.02	3.6	2.17	1.6	879203							
Gravity Mids	184.36		9.95	1.37	15.8	3.60	9.9	6.33	7.4	879204							
Gravity Tail Grind D/C	864.60	97	46.67	0.91	49.2	3.52	45.3	8.49	46.3	879205							
Total	1852.45		100.00	0.86	100.0	3.63	100.0	8.56	100.0								



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 9-1 – Gravity Batch Testing Results



These initial results showed good promise achieving 53.9% Sn recovery to the gravity concentrate with an additional 19.7% of tin contained within middling streams.

Significantly ~74% of feed Sn units were recovered to the primary gravity cyclone underflow.

9.2 Gravity Separation Lock Cycle Testing

Lock cycle testing was completed with three basic aims:

1. Optimise the gravity circuit configuration
2. Quantify achievable gravity circuit performance
3. Produce representative feed sample for downstream testwork; de-slime, sulfide scavenging and tin flotation

To meet number 3 of these aims the lock cycling testing was carried on over a much larger number of cycles (a total of 31 cycles) than would typically be completed. Aside from producing the required quantity of sample for downstream testwork this also provided considerable confidence in the achievable results.

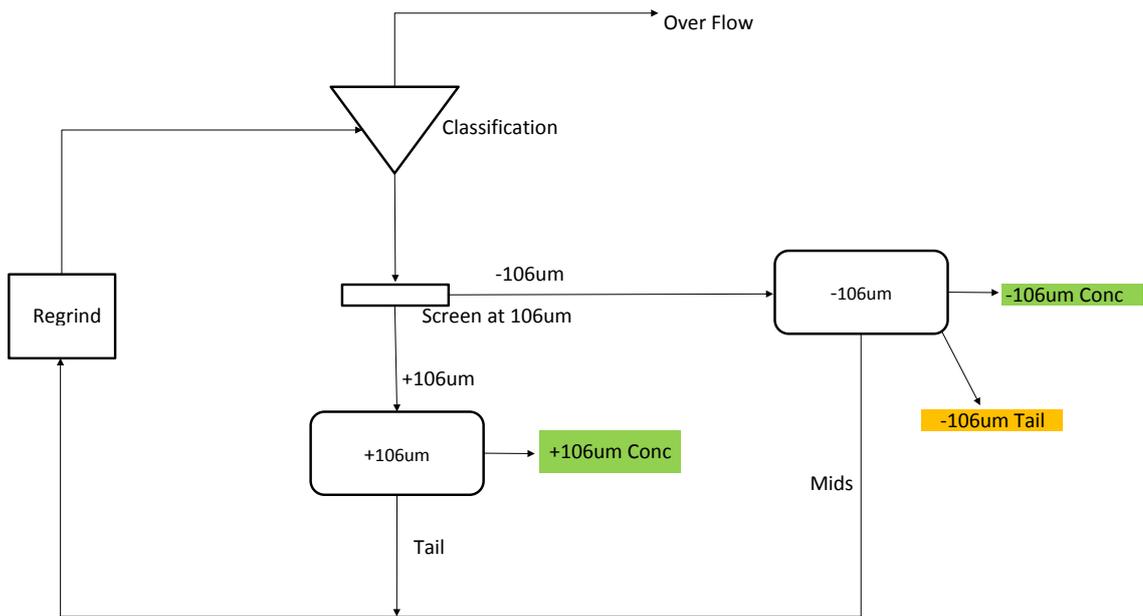
Over the initial 6 cycles the configuration of the lock cycle flowsheet was modified to optimise overall performance. For cycles 1 to 4 the circuit consisted of primary gravity classification via cyclone, with cyclone underflow screened at 106 µm to produce “coarse gravity” (labelled as +106 µm) and “fine gravity” (labelled as -106µm) feed streams, with a single roughing stage in the “coarse” and “fine” streams. Coarse tailings and fine mids were recycled following regrinding, while fine tails formed a final tailings stream (refer Figure 9-2).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

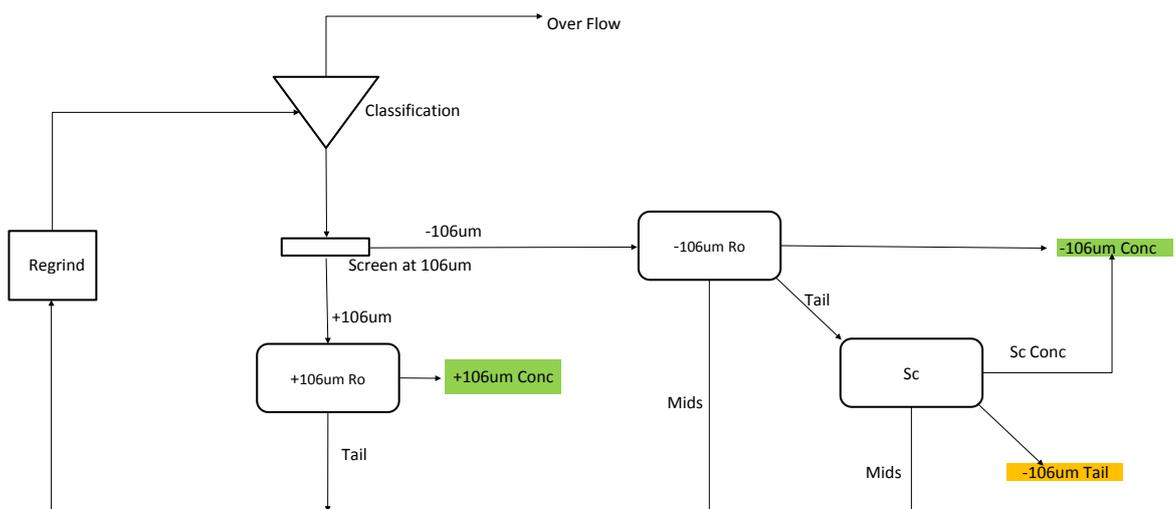
An additional fine scavenger stage was added in cycle 5 (refer Figure 9-3), with cleaner stages for both the fine rougher and fine scavenger added for cycles 6 to 31 (refer Figure 9-4).

Figure 9-2 - Gravity Lock Cycle Test Flowsheet: Cycles 1 to 4



T0879 LC01 C1-4

Figure 9-3 - Gravity Lock Cycle Test Flowsheet: Cycle 5

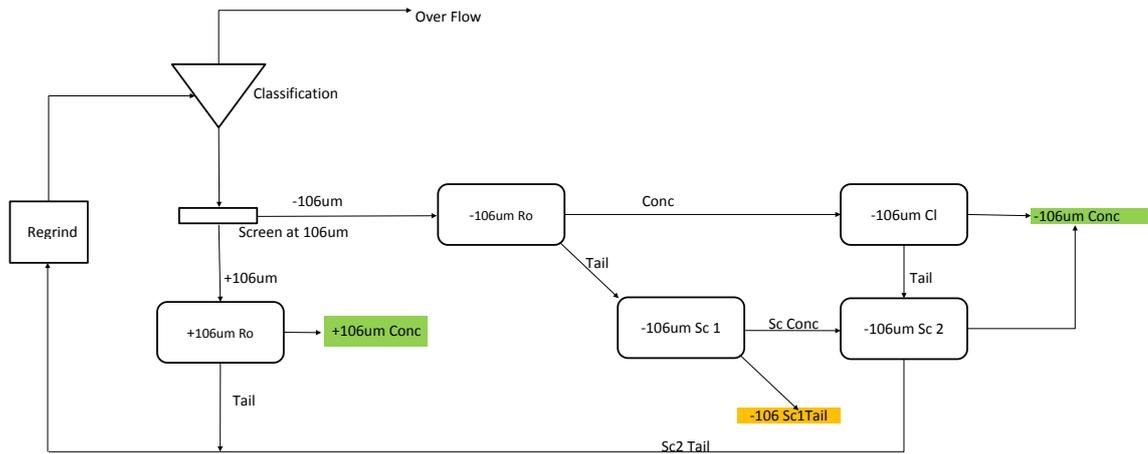


T0879 LC01 C05



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 9-4 - Gravity Lock Cycle Test Flowsheet: Cycles 6 to 31



T0879 LC01 C06

Table 13 shows the overall results for the lock cycle test across all cycles completed (cycles 1 to 31), with Table 14 shows a summary of grades, mass and metal distributions for cycles 16 to 31. Over the course of the lock cycle testing a number of sizing surveys were completed with size distributions and size by size assays results contained in Appendix 7.



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Table 13 – Overall Gravity Lock Cycle Test results



Table with 2 columns: Field (PROJECT, TEST NO, FEED, FROM TEST, DATE, TECH) and Value (T0879, LC01, SULPHIDE TAILS, 50814, ID)

Main data table for Table 13 showing Gravity Lock Cycle Test results. Columns include CYCLE NO (1-31) and AVERAGE. Rows include Gravity final conc 1 (+106 Conc), Gravity final conc 2 (-106 Conc), Gravity Final Tail (-106 Tails), Over Flow, and Combined Concentrate. Each row lists components like gm, %Sn, %Fe, %S, %SiO2.

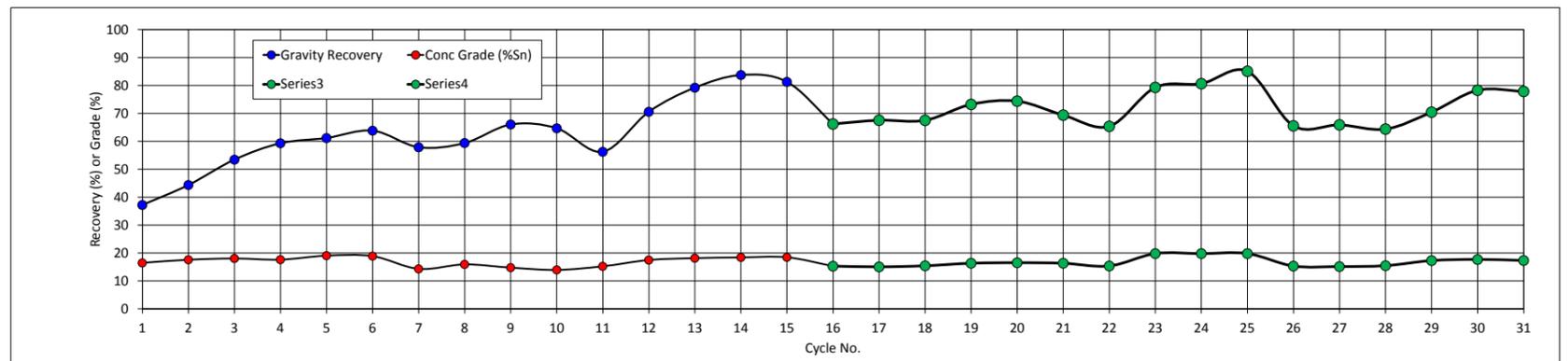
Table with 2 columns: Field (New Feed (gm) (dry), Regrind feed Damp Wt (gm), Regrind Time (min per 100gm), Regrind Time (min.sec), Regrind D/C underflow (%Wt)) and values for cycles 2003-2007.

DISTRIBUTIONS table showing AV 16-31 and FROM NEW FEED (%) for various components (MASS, TIN, IRON, SULPHUR, SILICA) across cycles 1-31. Rows include +106 Conc, -106 Conc, -106 Tail, Over Flow, and Calc Recycle.

INTERNAL STREAMS table with 2 columns: Field (Final Regrind Feed, gm, %Sn, %Fe, %S, %SiO2, p80) and Value (1116.6, 0.63, 21.00, 3.09, 40.80, 342)

Final Reg Discharge table with 2 columns: Field (gm, %Sn, %Fe, %S, %SiO2, p80) and Value (1080.0, 1.34, 21.00, 3.09, 40.80, 84)

NEW FEED and CALC table with 2 columns: Field (gm, %Sn, %Fe, %S, %SiO2) and Value (62476, 2015.4, 1.33, 19.54, 19.55, 2.97, 3.08, 41.27, 40.90)





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 14 – Gravity Lock Cycle Test results: Average of Cycles 16 to 31

		Grade	Distribution
Gravity final conc 1 (+106 Conc)	gm	870	2.7
"Coarse concentrate"	%Sn	11.3	23.1
	%Fe	37.9	5.2
	%S	12.7	11.5
	%SiO ₂	6.1	0.4
Gravity final conc 2 (-106 Conc)	gm	968	3.0
"Fine Concentrate"	%Sn	21.6	48.9
	%Fe	36.0	5.5
	%S	17.8	18.0
	%SiO ₂	2.5	0.2
Gravity Final Tail (-106 Tails)	gm	16510	51.2
	%Sn	0.39	15.1
	%Fe	17.1	44.9
	%S	1.61	27.7
	%SiO ₂	48.1	59.7
Over Flow	gm	13755	42.7
	%Sn	0.47	15.2
	%Fe	20.7	45.1
	%S	3.14	45.0
	%SiO ₂	37.4	38.7
Combined Concentrate	gm	1838	5.7
	%Sn	16.7	71.9
	%Fe	36.9	10.8
	%S	15.4	29.4
	%SiO ₂	4.20	0.6

Referring to Table 14 it can be seen that the circuit configuration shown in Figure 9-4 provided excellent performance, achieving an overall tin recovery of 71.9% (based on gravity circuit feed) to the combine fine and coarse concentrates at a grade of 16.7% Sn. Of this total, the coarse concentrate contributed 23.1% Sn recovery at a grade of 11.3% Sn, while the fine concentrate contributed 48.9% recovery at a grade of 21.6% Sn.

A total 42.7% of the mass deported to the primary cyclone overflow along with 15.2% of the tin units giving a grade of 0.47% Sn.

51.2% of the mass deported to the “-106 µm tails” stream, along with 15.2% of the tin units at a grade of 0.39% Sn. Recovery of additional tin units from this stream is discussed in Section 9.2.1.

Analysis of the combine (fine plus coarse) concentrate produced from cycles 1 to 31 is shown in Table 15. Clearly pyrite/pyrrhotite, magnetite and siderite are the major diluents in the concentrate.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 15 – Analysis of combine concentrate produced from cycles 1 to 31

Sn %	Fe %	As %	S %	SiO ₂ %	Mn %	CaO %	MgO %	Al ₂ O ₃ %	C %	C organic %	C inorg %
19.2	34.4	0.91	12.3	3.84	0.53	0.43	1.4	1.33	2.34	0.48	1.86

9.2.1 Tin Recovery from “-106 µm Tails” Stream

With >50% of the gravity circuit feed mass deporting to the “-106 µm Tails” stream, this stream offers a significant opportunity to reject mass ahead of tin flotation if directed to final tails. However, at a grade of ~0.4% Sn this would represent a significant loss (of ~15.1%).

Table 16 shows size distribution and size by size assays and metal distribution of this stream. Sn is clearly concentrated in the minus 38 µm fractions, while relatively barren silicates are concentrated in the plus 38 µm fractions, reflecting the sharp drop off in gravity performance below 38 µm. The plus 38 µm fractions contained 56% of the mass with only 27.8% of the Sn at a grade of 0.22%.

Screening of this stream at ~38-40 µm would allow the rejection of ~29% of the gravity circuit feed mass to the screen oversize at a Sn grade of 0.22% (less than the tin flotation tailings grade), representing a loss of only 4.2% of gravity circuit feed units. Additionally Sn in this size range (-106+40 µm) is expected largely locked within Sn lean composites.

At a cut point of ~38-40 µm screen undersize is expected to contain ~72.2% of the screen feed Sn units at an Sn grade of ~0.72%, and ~44% of the screen feed mass.

Application of the UF Falcon centrifugal concentrator for scavenging tin from this stream was also tested, both on the whole stream and the <38 µm. Results are shown in Table 17 and Table 18 respectively.

In both cases only relatively poor performance was achieved; Sn recovery and upgrade, and mass rejection were poor when compared with that expected for a size based separation.



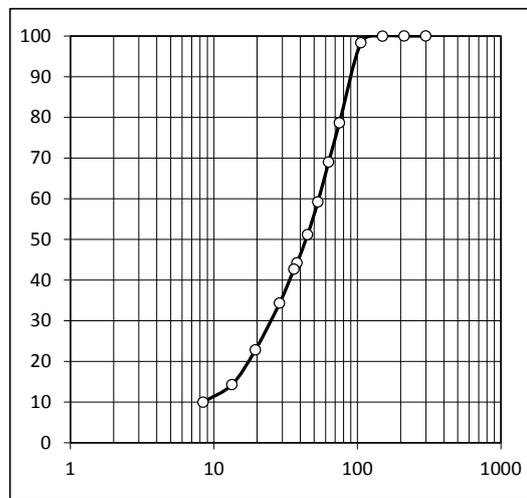
**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 16 – Size Distribution and Size by Size Metal Distribution of “-106 µm Tails” Stream



PROJECT	T0879
SAMPLE NAME	LC01 Cyc6 -106
	Mozley Tail
DATE	110814
TECHNICIAN	MS

LC01 Cyc6 -106 Mozley Tail		SIZE µm	WEIGHTS		
			gm	(%)	%PASS
p80	77	850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	0.02	0.02	100.0
		106	1.91	1.62	98.4
		75	23.19	19.68	78.7
		63	11.41	9.68	69.0
		53	11.55	9.80	59.2
		45	9.45	8.02	51.2
		38	8.16	6.92	44.3
CYCLOSIZER	CS1	36	1.88	1.60	42.7
FLOW 185	CS2	29	9.79	8.31	34.4
TEMP 21	CS3	19	13.56	11.51	22.9
SG 2.60	CS4	13	10.06	8.54	14.3
MINS 20	CS5	8	5.09	4.32	10.0
		SUB	11.78	10.00	0.0
		TOTAL	117.85	100.00	



ANALYSES

SIZE µm	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	21.32	0.23	11.1	12.05	15.7	0.06	13.5	0.77	9.8	57.40	24.8	0.26	13.6
63	9.68	0.22	4.8	12.55	7.4	0.05	5.1	0.90	5.2	57.20	11.2	0.29	6.9
53	9.80	0.22	4.9	12.70	7.6	0.06	6.2	0.91	5.3	57.50	11.4	0.31	7.5
45	8.02	0.22	4.0	13.75	6.7	0.06	5.1	1.06	5.1	55.90	9.1	0.35	6.9
38	6.92	0.20	3.1	14.45	6.1	0.05	3.6	1.04	4.3	53.80	7.5	0.40	6.8
26	9.90	0.49	10.9	23.90	14.5	0.08	8.3	2.48	14.7	35.90	7.2	0.71	17.3
12	20.04	0.77	34.8	19.50	23.9	0.14	29.5	2.42	29.1	42.60	17.3	0.50	24.6
8	14.31	0.82	26.5	20.70	18.1	0.19	28.6	3.08	26.4	39.70	11.5	0.47	16.5
CALC	100.00	0.44	100.0	16.37	100.0	0.09	100.0	1.67	100.0	49.39	100.0	0.41	100.0
ASSAY		0.41		16.45		0.10		1.68		49.70		0.40	

ANALYSES

SIZE µm	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
75	21.32	0.92	19.3	3.62	22.0	8.82	23.8				
63	9.68	0.93	8.9	3.47	9.6	8.46	10.4				
53	9.80	0.92	8.9	3.38	9.5	8.29	10.3				
45	8.02	1.01	8.0	3.47	7.9	8.13	8.3				
38	6.92	1.07	7.3	3.48	6.9	7.98	7.0				
26	9.90	1.25	12.2	3.28	9.3	6.85	8.6				
12	20.04	1.06	20.9	3.42	19.6	7.05	17.9				
8	14.31	1.04	14.6	3.75	15.3	7.59	13.8				
CALC	100.00	1.02	100.0	3.51	100.0	7.89	100.0				
ASSAY		0.99		3.65		8.21					



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 17 – UF Falcon Separation of “-106 µm Tails” Stream



BURNIE LABORATORY: BATCH UF FALCON SEPARATION

PROJECT	T0879
TEST NO	T25
DATE	120814
TECHNICIAN	ID

CONDITIONS

Separation of	Sn
Feed Pulp Density (%)	12
Feed In Time (min)	16
UF-100 Speed (g's)	218
Total Feed Weight (gm)	3987.7
Calc Feed Rate (gm/min)	249.2

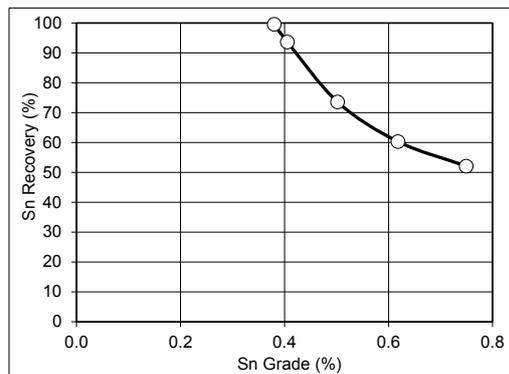
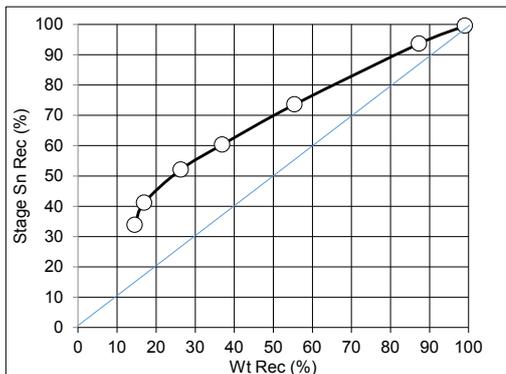
34.3 Ltr H2O

FEED MATERIAL
LC01 cyc 1-6
Mozley tail -106

Product	Feed on Time (min)	Product Mass (gm)	Product Mass (%)	Calc Feed Mass (gm)	Calc Mass to Conc (gm)	Calc Mass to Conc (%)	Sn Tail (%)	Sn Dist (%)	Sn Stage Rec (%)	Sn Calc Conc (%)
Tail	1.00	2.3	0.1	249.2	246.9	99.1	0.19	0.0	99.5	0.38
Tail	2.00	60.8	1.5	498.5	435.4	87.3	0.19	0.8	93.6	0.41
Tail	4.00	381.1	9.6	996.9	552.7	55.4	0.23	5.8	73.6	0.50
Tail	6.00	499.3	12.5	1495.4	551.9	36.9	0.25	8.3	60.3	0.62
Tail	8.00	525.8	13.2	1993.9	524.6	26.3	0.26	9.1	52.1	0.75
Tail	12.00	1015.1	25.5	2990.8	508.7	16.9	0.30	20.2	41.2	0.92
Tail	16.00	923.6	23.2	3987.7	579.7	14.5	0.36	22.0	33.8	0.88
Conc		579.7	14.5				0.88	33.8		
Total		3987.7	100.0				0.38	100.0		
Head							0.52			

	Fe %	Dist %	S %	Dist %	SiO2 %	Dist %	Al2O3 %	Dist %	As %	Dist %
Tail	12.25	0.0	1.11	0.0	57.20	0.1	10.30	0.1	0.08	0.1
Tail	11.00	1.0	0.64	0.7	60.50	1.9	8.66	1.7	0.05	1.0
Tail	13.95	7.9	0.97	6.4	53.40	10.4	8.36	10.0	0.05	6.1
Tail	16.00	11.9	1.20	10.4	51.20	13.1	8.23	13.0	0.07	11.1
Tail	16.45	12.9	1.40	12.8	48.90	13.2	8.08	13.4	0.06	10.0
Tail	17.25	26.1	1.10	19.3	49.00	25.5	7.98	25.5	0.07	22.6
Tail	17.15	23.6	1.72	27.5	48.00	22.7	7.75	22.6	0.08	23.5
SRT Con	19.20	16.6	2.28	22.9	43.80	13.0	7.52	13.7	0.14	25.8
Calc Head	16.83	100.0	1.45	100.0	48.88	100.0	7.95	100.0	0.08	100.0
Assay Head	17.45		1.79		46.60		7.66		0.1	

*Number in red means less





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 18– UF Falcon Separation of “-106 µm Tails” Stream; -38 µm fraction



BURNIE LABORATORY: BATCH UF FALCON SEPARATION

PROJECT	T0879
TEST NO	T26
DATE	180814
TECHNICIAN	ID

CONDITIONS

Separation of	Sn
Feed Pulp Density (%)	12
Feed In Time (min)	8
UF-100 Speed (g's)	218
Total Feed Weight (gm)	1206.6
Calc Feed Rate (gm/min)	150.8

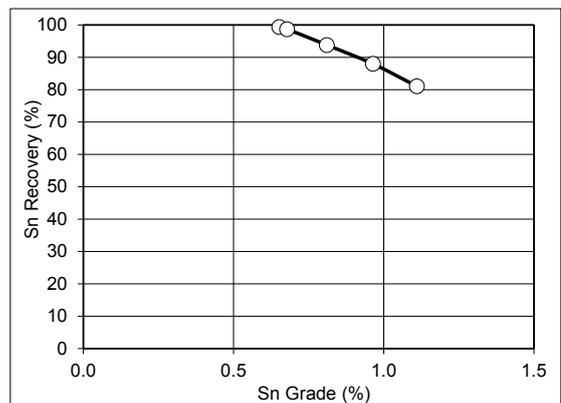
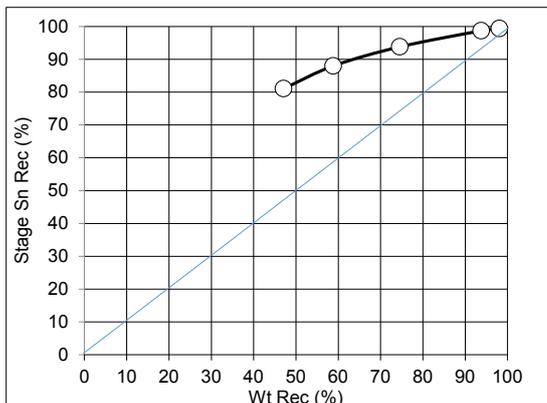
FEED MATERIAL
LC01 cyc 1-6
-106 Mozley tail
-38um

32.2 Ltr H2O

Product	Feed on Time (min)	Product Mass (gm)	Product Mass (%)	Calc Feed Mass (gm)	Calc Mass to Conc (gm)	Calc Mass to Conc (%)	Sn Tail (%)	Sn Dist (%)	Sn Stage Rec (%)	Sn Calc Conc (%)
Tail	1.00	2.8	0.2	150.8	148.0	98.1	0.23	0.1	99.3	0.65
Tail	2.00	15.8	1.3	301.7	283.1	93.8	0.12	0.2	98.7	0.68
Tail	4.00	134.7	11.2	603.3	450.0	74.6	0.16	2.8	93.8	0.81
Tail	6.00	219.2	18.2	905.0	532.5	58.8	0.21	5.9	88.0	0.96
Tail	8.00	266.1	22.1	1206.6	568.0	47.1	0.29	9.9	81.1	1.11
Conc		568.0	47.1				1.11	81.1		
Total		1206.6	100.0				0.64	100.0		
Head							0.58			

	Fe %	Dist %	S %	Dist %	SiO2 %	Dist %	Al2O3 %	Dist %	As %	Dist %
Tail	17.45	0.2	1.93	0.2	40.20	0.2	14.00	0.4	0.11	0.2
Tail	10.35	0.6	0.61	0.3	61.90	2.1	9.49	1.7	0.05	0.5
Tail	14.95	7.6	0.85	3.7	52.80	15.5	8.75	13.3	0.07	5.7
Tail	18.80	15.5	1.34	9.5	44.20	21.1	8.10	20.0	0.06	8.0
Tail	21.00	21.0	1.89	16.3	40.80	23.7	7.73	23.2	0.08	13.0
SRT Con	25.90	55.2	3.79	69.9	30.10	37.3	6.44	41.3	0.21	72.6
Calc Head	22.08	100.0	2.55	100.0	38.00	100.0	7.34	100.0	0.14	100.0
Assay Head	21.70		2.45		38.30		7.36		0.12	

*Number in red means less





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

9.3 Key Outcomes

- The gravity lock cycle testing demonstrated excellent gravity separation performance is achievable, with an overall tin recovery of 71.9% (based on gravity circuit feed) to the combine fine and coarse concentrates at a grade of 16.7% Sn achieved across 16 cycles.
- Pyrite/pyrrhotite, magnetite and siderite are the major diluents in the combine gravity concentrate. These can be readily rejected from the concentrate by a combination of flotation, magnetic separation and leaching.
- Based on the outcomes of the gravity testing the recommended overall gravity configuration is shown in Figure 9-5. However, further larger scale testing utilising spirals for the coarse roughing and fine roughing and scavenging duties is recommended.
- Screening of the fine scavenger tails stream at ~38-40 µm is recommended as this would allow the rejection of ~29% of the gravity circuit feed mass to the screen oversize at a Sn grade of ~0.22% (less than the expected tin flotation tailings grade), representing a loss of only ~4.2% of gravity circuit feed units. This allows a significant reduction in the total de-slime/tin flotation feed tonnage.

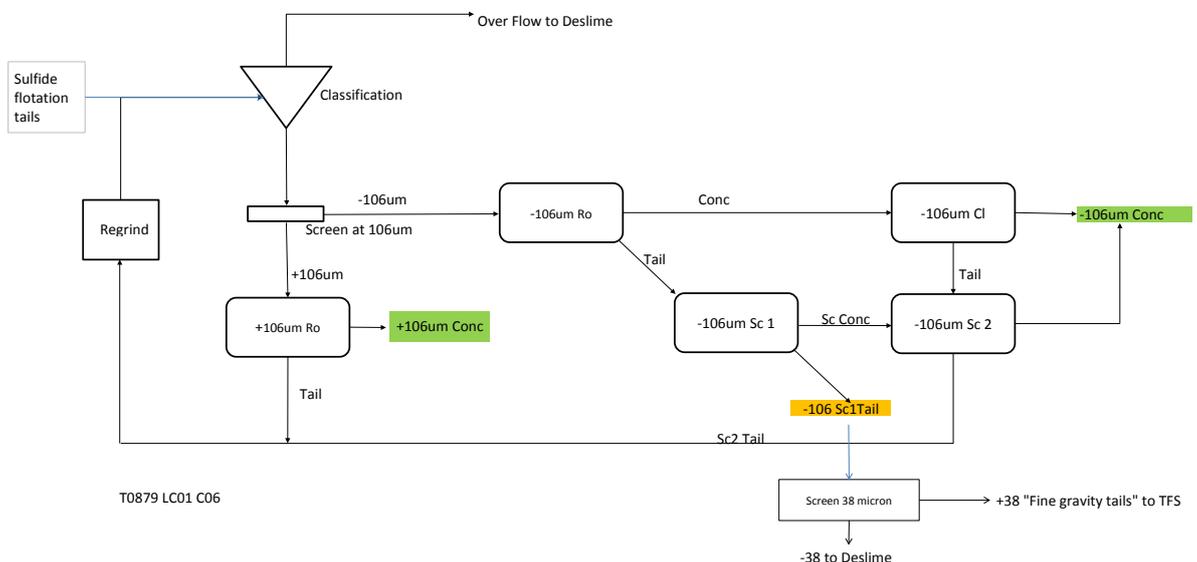
This “fine gravity tailings” stream (screen undersize) would form a final tailing stream from the circuit, and could potentially be useful for paste fill underground.

The screen undersize would be directed to the de-slime circuit feed along with the primary gravity cyclone overflow.

Fine screening rather than cycloning is strongly recommended for this duty to avoid the miss reporting of Sn fines to the “fine gravity tailings”.

- To achieve adequate liberation significant regrind is required within the gravity circuit. Recommended target regrind size is nominally P80 = 52 µm (based on the weighted average size distributions of the various exit streams).

Figure 9-5 – Recommended Overall Gravity Configuration





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

10 GRAVITY CONCENTRATE DRESSING

Gravity concentrate dressing testwork consisted of sulfide dressing flotation, dressing magnetic separation (low intensity) and concentrate leaching to remove the major diluents pyrite/pyrrhotite, magnetite and siderite present in the combine gravity concentrate.

Feed to gravity concentrate dressing testwork was gravity concentrate produced from cycles 1-31 of the gravity lock cycle test (LC01).

10.1 Sulfide Dressing Flotation

Sulfide dressing flotation results are contained in Appendix 8.

Sulfide dressing flotation consisted of a simple single roughing stage with a single cleaner stage. A number of tests were performed largely to treat the various batches of gravity concentrate produced and optimise sulfur grade in the tailings. Expected reagent consumptions based on the various tests performed are shown in Table 19, with Figure 10-1 showing sulfide dressing flotation tailings grade versus Sn recovery to tails.

Roughing and cleaning flotation times (laboratory) of 15 and 12 minutes respectively are expected to be sufficient based on the various tests completed.

Table 19 – Expected Sulfide Dressing Flotation Reagent Consumptions

pH	~4.2
Sulfuric Acid	16 g/t
Copper Sulphate	65 g/t
PAX	200 g/t
Frother (MIBC)	200 g/t
Acidified sodium silicate (ASS)	350 g/t



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 10-1 – Test T030

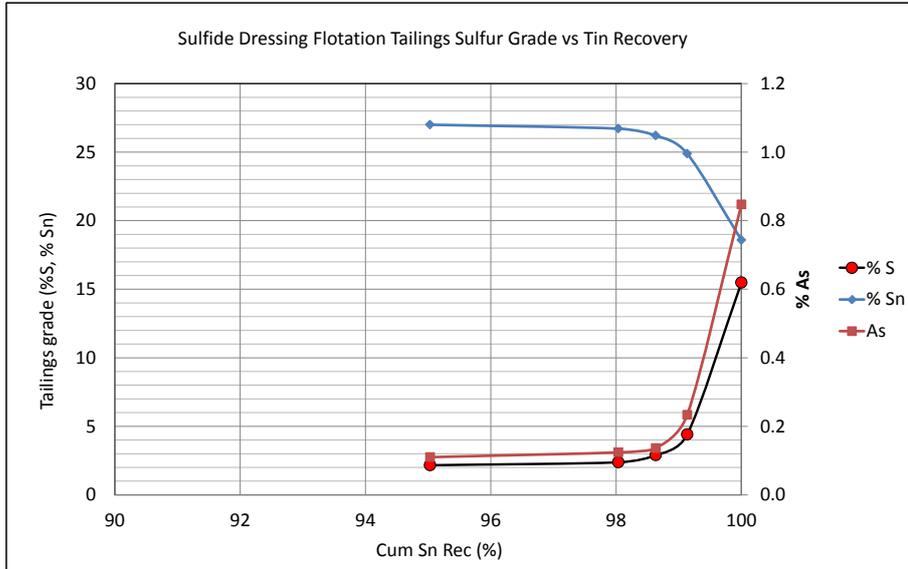


Figure 10-1 shows a plot of sulfide dressing flotation tailings grade versus Sn recovery. The gravity concentrate upgrades significantly across dressing flotation from ~18.6% Sn to ~27% Sn with S levels readily reduced to <2%, and As levels to ~0.1%. Further scavenging in T57 showed before S and As levels can readily be reduced to <1% and <0.1% respectively (refer Table 20).

Table 20 – Test T57

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
Ro Tail+Cl1 Tail+Cl1 C3	455.3	96.4	26.8	99.6	21.9	93.8	0.10	83.4	1.54	58.6	7.02	96.6	1.35	99.0
Ro Tail+Cl1 Tail	437.2	92.5	27.7	98.9	21.3	87.5	0.09	74.0	0.81	29.8	7.00	92.5	1.39	97.6
Ro Tail	417.1	88.3	28.4	96.8	20.9	82.0	0.09	69.9	0.68	23.8	6.87	86.6	1.39	93.2

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorg %	CUM
Ro Tail+Cl1 Tail+Cl1 C3	455.3	96.4	1.11	98.7	2.52	97.1	2.80	97.6	4.54	98.1	0.08	90.7	4.45	98.2
Ro Tail+Cl1 Tail	437.2	92.5	1.13	96.6	2.55	94.3	2.81	94.0	4.59	95.2	0.08	81.7	4.51	95.5
Ro Tail	417.1	88.3	1.15	93.6	2.48	87.6	2.79	89.1	4.57	90.5	0.07	72.3	4.50	90.9

As the sulfide dressing flotation cleaner concentrate is expected to contain Sn in contained in sulfide cassiterite composites (as well as entrained Sn) this stream should be recycled to the sulfide regrind circuit, where it can be adequately liberated.

10.2 Dressing Magnetic Separation

Following sulfide dressing flotation dressing magnetic separation is aimed at further upgrading the concentrate by rejecting magnetite.

Dressing magnetic separation testing consisted of roughing, followed by regrind to a P80 of 34 µm and cleaning of the magnetic product (refer tests T34, T50 and T55 in Appendix 8).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Overall this provided a mass rejection of 20% (based on dressing magnetic separation feed) with an Sn loss of only 0.4% to the magnetic product.

As the magnetic product would only build-up if recycled within the circuit the dressing magnetic separation cleaner magnetic product will form a final tailings stream from the circuit.

10.2.1 Alternative approaches to magnetite rejection

As an alternative to dealing with magnetite rejection within the gravity concentrate dressing circuit, magnetic separation of the whole of the sulfide flotation tails, prior to gravity separation was considered in test T35 (refer Appendix 8 for results).

T35 consisted of a single roughing magnetic separation (LIWMS). This resulted in an overall loss to the magnetic product of 2.8% Sn based on sulfide flotation tails. Potentially with regrind and cleaning this loss could be reduced.

As dealing with magnetite rejection within the gravity concentrate dressing circuit will require smaller equipment sizings, and is expected to give lower Sn losses this approach is recommended. However, if magnetite levels in ROM are expected to increase significantly beyond those seen in the Severn Bulk Composite (for example with co-treatment of Severn with Saint Dizier) further consideration should be given to rejection of magnetite ahead of the gravity circuit, as increasing magnetite loads will impact equipment sizings, and potentially performance within the gravity circuit.

High intensity magnetic separation of the whole of the sulfide flotation tails, prior to gravity separation was considered in tests T39, T40 and T41 (refer Appendix 8 for results) at 3,000, 6,000 and 10,000 gauss respectively. In addition to rejecting magnetite, high intensity magnetic separation rejects siderite, which potentially reduces issues in tin flotation, along with giving significantly increased mass rejection (compared to LIMS). Results are summarised in Table 21.

Table 21 - High intensity magnetic separation of sulfide flotation tails

Gauss	% mass rejection	% Sn loss	Non-mags Fe grade ⁽¹⁾
3,000	18.5	9.9	14.1 %
6,000	52.8	32.6	6.8 %
10,000	67.1	49.6	5.4 %

Notes; 1. Fe feed grade = 19.6%

Generally this approach resulted in very high losses of tin to the magnetic fraction (even in the finer size fractions). As such it was not pursued further.

10.3 Concentrate Leach

Refer Section 12.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

10.4 Final Gravity Concentrate Quality

The dressing testwork completed showed the major diluents present can be readily rejected from the concentrate by a combination of flotation, low intensity magnetic separation and leaching to upgrade the concentrate to saleable Sn grades with minimal Sn losses.

Final gravity concentrate analysis is detailed in Table 22 and Table 23.

Table 22 – Severn Bulk Composite: Final Gravity Concentrate Analysis

Element	Sn	Fe	As	S	SiO ₂	Mn	CaO	MgO	Al ₂ O ₃	C _{total}	C _{organic}	C _{inorganic}	Ag	Au	B	Ba	Be	Bi	Cd	Ce	Co	Cr	Cs	Cu	Ga	Ge	Hf	Hg	In	
Units	%	%	%	%	%	%	%	%	%	%	%	%	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm
Value	55.3	3.82	0.13	1.145	13.1	0.11	0.705	0.56	2.79	0.59	0.15	0.435	3.2	0.2	20	185	2.8	18.38	<0.01	59.4	4.85	257	1.57	150	1.82	0.11	0.15	0.33	1.11	
Element	K	La	Li	Mg	Mo	Na	Nb	Ni	P	Pb	Rb	Re	Sb	Sc	Se	Sn	Sr	Ta	Te	Th	Ti	Tl	U	V	W	Y	Zn	Zr		
Units	%	ppm	ppm	%	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm		
Value	0.1	27.7	6.8	0.16	133	0.01	<0.05	28.9	90	658	15.2	0.002	5.66	1.15	0.25	495	34.8	<0.01	0.01	2.05	0.01	0.27	0.55	6	145	5.68	55.5	5.05		



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 23 - Severn Bulk Composite: Final Gravity Concentrate QXRD Analysis

Phase	Weight%
Arsenopyrite	0.2
Cassiterite	70.1
Chlorite	0
Diopside	0
Dolomite	0
Dravite	4.2
Gypsum	0.9
Marcasite	0
Microcline	0
Phlogopite	0
Pyrite	0.7
Pyrrhotite-4C	1
Quartz	7.4
Rhodocrosite?	0.4
Rutile	1.6
Scheelite	0.7
Siderite	12
Topaz	0.6
Zircon	0.1

The outcomes of the Severn optimisation program have led to improved gravity concentrate quality and clearly demonstrated a high quality final gravity concentrate, low in penalty elements, can be readily produced.

Comments:

- No significant impurities impacting the saleability of the concentrate are present.
- Generally, the levels of impurities elements which are present, are not expected to incur significant penalties charges.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

11 DE-SLIME AND TIN FLOTATION

Feed to de-slimes and tin flotation was the combine primary gravity overflow stream and <40µm fraction of the fine scavenger tailings stream produced from cycles 1-31 of the gravity lock cycle test (LC01).

Initially a series of “scouting” tests were carried out on a composite of the primary gravity overflow stream; this includes tin flotation tests T29 to T44, and separate composite of <40µm fraction of the fine scavenger tailings stream; this includes T45 to T48 produced from cycles 1 to 10.

Primary gravity overflow stream and <40µm fraction of the fine scavenger tailings stream produced from cycles 11-31 of the gravity lock cycle test (LC01) were composited together and formed the feed to de-slimes tests T56 onwards and tin flotation tests T58 onwards.

11.1 De-Slime

De-slimes results are contained in Appendix 10.

De-slimes testing was completed using a cyclone test rig fitted with a 44 mm Mozley cyclone, with vortex finder and spigot sizes adjusted to manipulate cut point.

The variation in mass and metal department with de-slimes cut point across the range 4 to 12 µm is shown in Table 24 along with the Sn upgrade ratio, and ratios of Fe, SiO₂, S and CaO to Sn in the underflow. Notably at coarser cut-points moderate upgrade of tin is achieved across de-slimes, with a significant decrease in the Fe:Sn ratio compared to the de-slimes feed material. That is, siderite is rejected reasonably strongly at coarser cut-points. However, Sn recovery is only modest.

As the cut-point is reduced, Sn recovery improves considerably at the expense of Sn upgrade ratio and in particular Fe rejection.

Table 24 – Variation in Mass and Metal Department with De-slimes Cut Point

Test no.	D50 (µm)	% Mass Recovery to U/F	U/F % <CS5 (<8 µm)	% Sn Recovery to U/F	% Fe Recovery to U/F	% SiO ₂ Recovery to U/F	% S Recovery to U/F	% CaO Recovery to U/F	Sn upgrade ratio	Fe/Sn ratio	SiO ₂ /Sn ratio	S/Sn ratio	CaO/Sn ratio					
T56	12.1	39.3	9.7	0.93	60.1	18.7	37.1	44.1	43.9	2.45	35.8	0.98	45.8	1.54	20.1	47.4	2.6	1.05
T63	6.1	61.8	27.1	0.76	77.8	21.5	62.4	39.3	62.5	2.55	63.3	1.05	70.2	1.26	28.3	51.7	3.4	1.38
T70	4	79.9	40.6	0.64	84.7	21.2	79.5	39.0	80.1	2.86	91.8	0.95	82.1	1.06	33.1	60.9	4.5	1.48
Feed	0	100.0	53.0	0.60	100.0	21.3	100.0	38.9	100.0	2.49	100.0	0.92	100.0	1.00	35.3	64.4	4.1	1.53

Figure 11-1 shows the variation in mass recovery to de-slimes underflow/tin flotation feed with de-slimes cut point, while Figure 11-2 shows the variation in Sn losses to slime tails and Figure 11-3 shows impact on tin flotation feed slimes content.



STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Figure 11-1

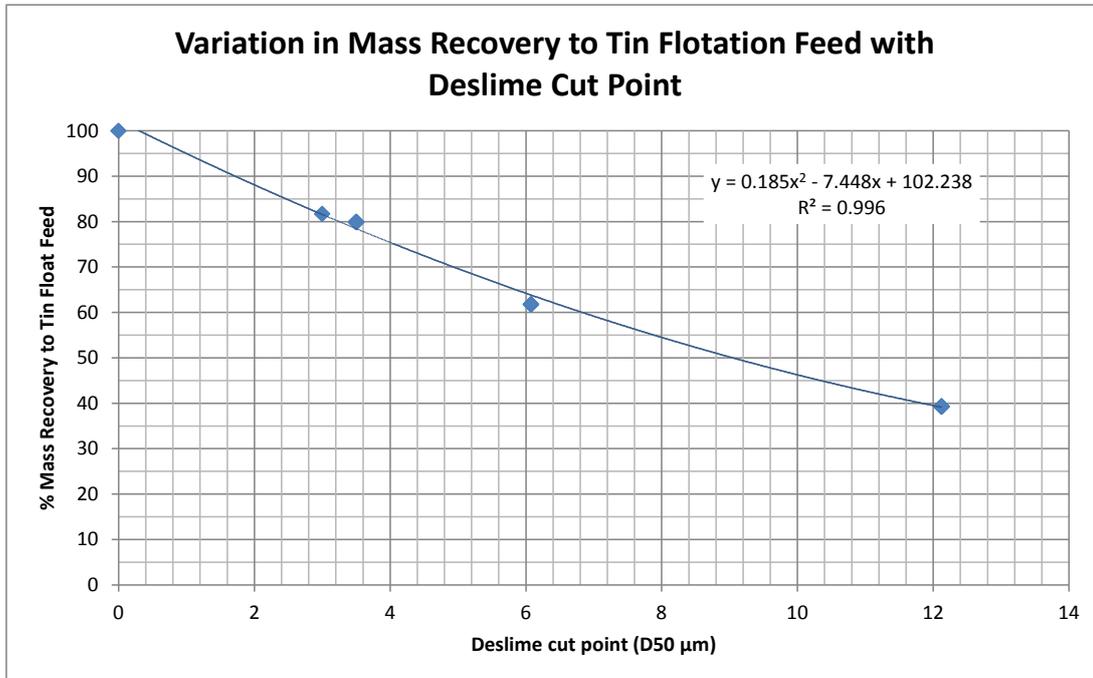
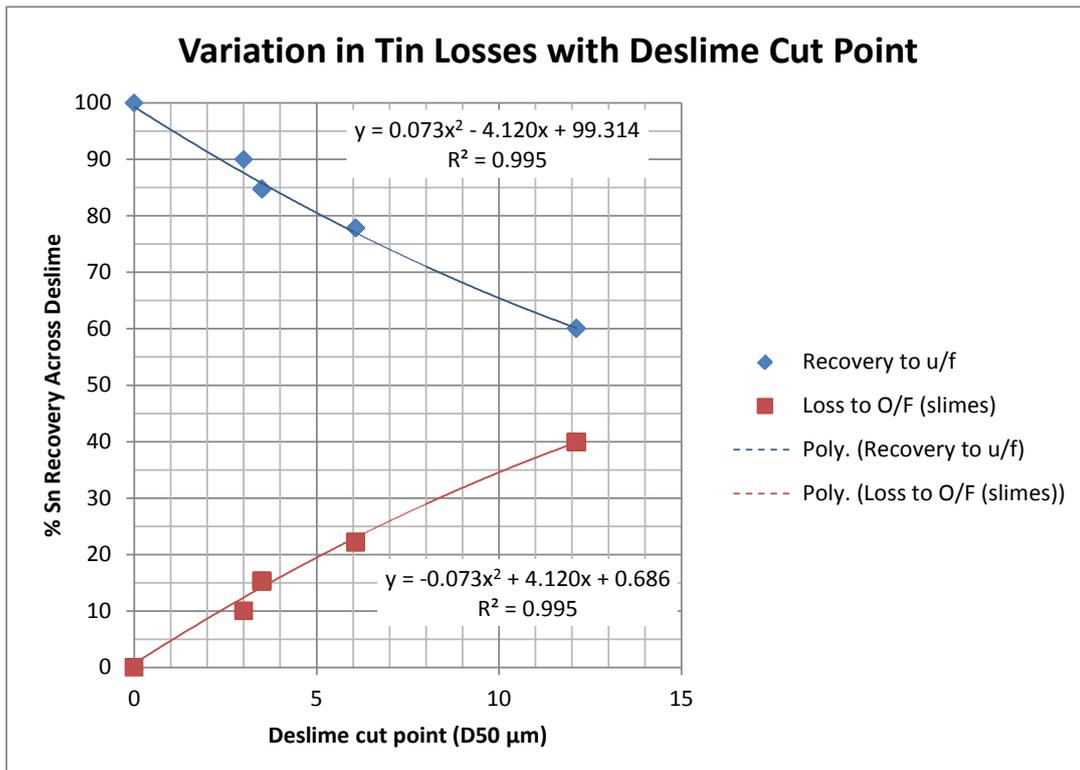


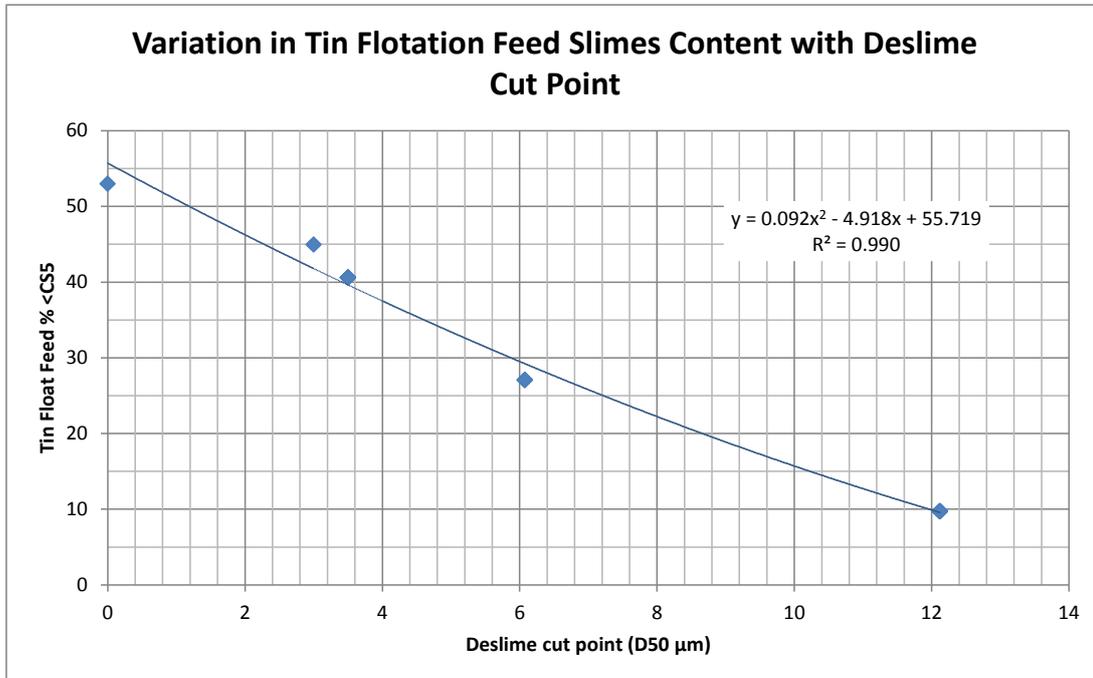
Figure 11-2





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-3



Once tin flotation conditions were optimised tin flotation testing was carried out on the underflow produced at various de-slime cut points to assess the trade-off between Sn losses to slimes tails and tailing flotation performance. This is discussed further in Section 11.2.

11.2 Tin Flotation

Complete tin flotation results are contained in Appendix 11.

Initial sighter tests were focused on investigating response of sulfide scavenging and tin roughing. These initial sighter tests highlighted challenges with achieving adequate sulfide rejection in sulfide scavenging and selectivity against Fe/siderite.

Use of a low pH high intensity conditioning (HIC) stage with addition of SSF, followed by a “water change” (following the HIC the pulp was filtered and repulped in fresh water for flotation) ahead of sulfide scavenging provided a step change in sulfide rejection, allowing sulfur levels to be consistently reduced to well <1%S, and improved subsequent Sn grade recovery response.

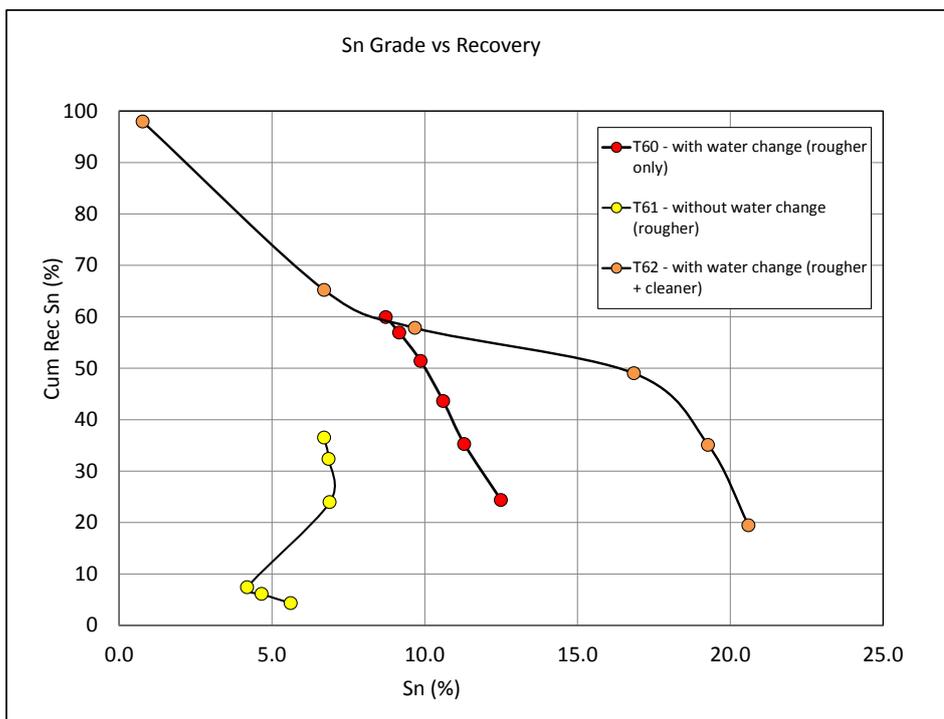
These initial sighter tests also showed Sn losses to the sulfide scavenger concentrate could be significantly reduced by cleaning of the sulfide scavenger concentrate. With a single stage of cleaning Sn losses to the sulfide scavenger concentrate of the order of 1% of tin flotation feed units are expected to be readily achievable. Although the sulfide scavenger concentrate will ultimately be recycled to the sulfide regrind circuit, minimising Sn department here will reduce Sn recirculating loads across the circuit and reduce loss opportunities.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-4 shows a comparison of tests with and without “water change” post the high intensity conditioning stage, immediately prior sulfide scavenger flotation. Clearly removal of the “water change” step in T61 was extremely detrimental to grade/recovery response. The “water change” post the high intensity conditioning stage, immediately prior sulfide scavenger flotation was used in all subsequent tests.

Figure 11-4 – Effect of “Water Change” post HIC



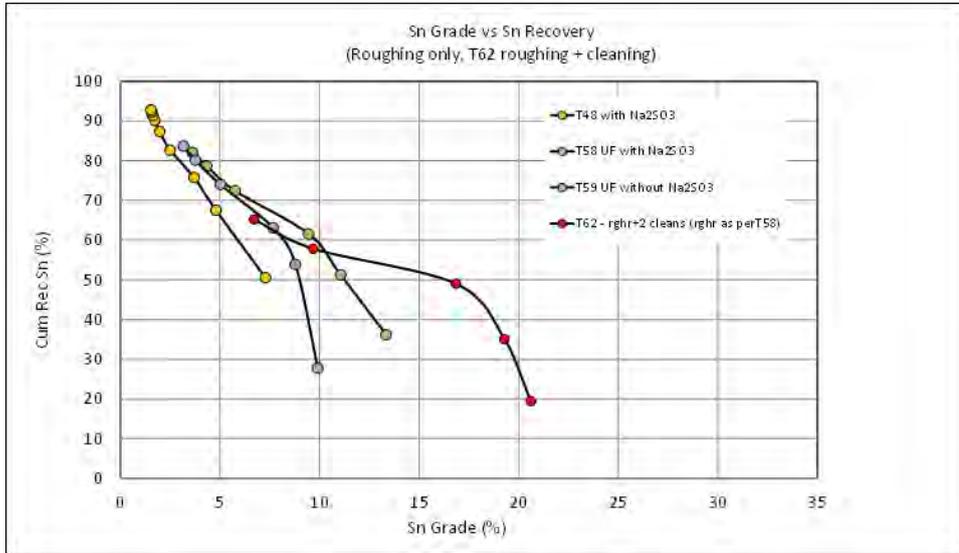
It is strongly suspected the detrimental effect seen in T61 is a result of excessive levels of soluble ions, particularly Fe present, and it is speculated that this could potentially be mitigated by chemical means such as increased dose of SSF or addition of a Fe complexing agent. From a practical plant design perspective a chemical means of addressing the impacts of soluble ions would be far preferable to installation of the necessary additional equipment to facilitate an effective “water change”. As such it is strongly recommended to carry out further work to determine if this can be successfully eliminated/solution chemistry issues can mitigated by other means.

Tin flotation tests investigating roughing response with low SPA dosages with and without sodium sulfite (Na_2SO_3), at a relatively coarse de-slime size (12 μm) size were completed (refer Figure 11-5).



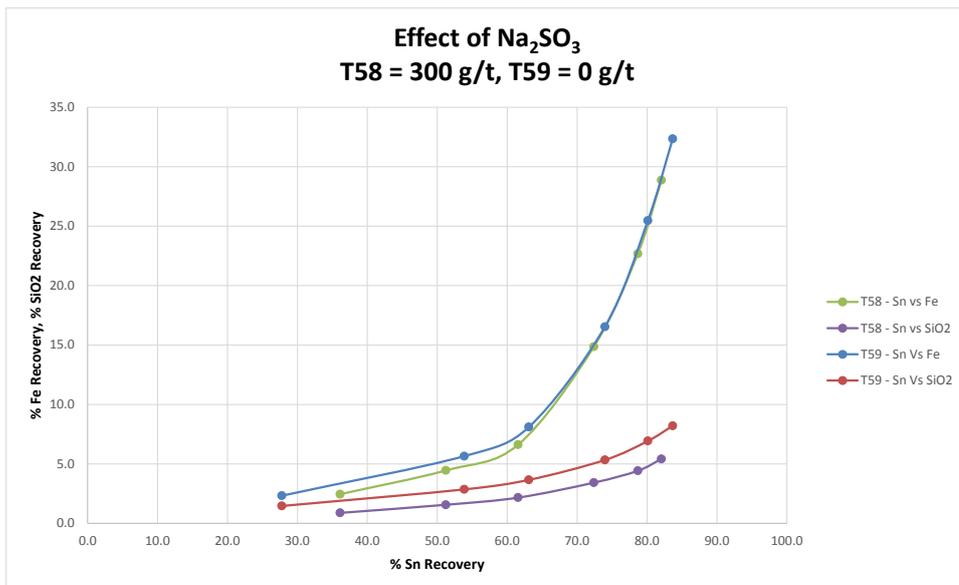
**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-5



Good response was achieved with approximately 60% Sn recovery achieved to a concentrate grade of 10% Sn from roughing flotation only with addition of sodium sulfite (refer T58 in Figure 11-5. T48 represents the previous best result). T62 included roughing plus 2 stage cleaning under conditions as per T58 and achieved a very good result; achieving a recovery of 52% to a concentrate grade of 15% tin, and 49% recovery at 16.8% tin grade.

Figure 11-6

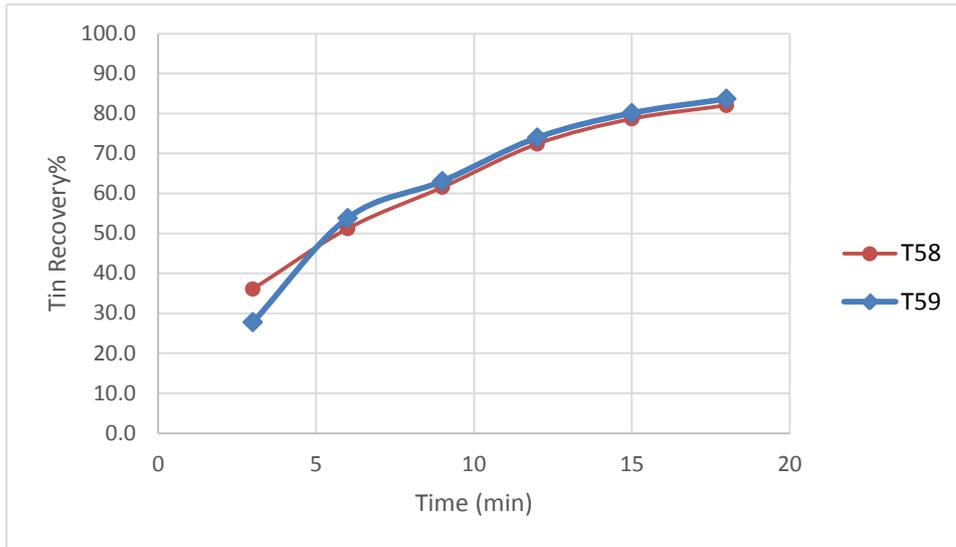




**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Sodium sulfite was expected to act as a siderite depressant. However, its action appears to be more via improved initial cassiterite kinetics (refer Figure 11-6 and Figure 11-7).

Figure 11-7 – Rougher Flotation Rate with (T58) and without Na₂SO₃ (T59)



Earlier tests highlighted issues with poor selectivity against siderite. This selectivity issue is exacerbated at high SPA dosages. This can be seen in Figure 11-8 and Figure 11-9 which show rough flotation rate and selectivity for T48. In T48 290 g/t SPA was stage doses at 0, 9 and 18 minutes to give a total dose of 870 g/t. Referring to Figure 11-8 it can be seen that Fe and mass recovery rates steepen considerably with each additional SPA dose beyond the initial 290 g/t, resulting in significantly poorer selectivity.

Results for T58 with a total SPA dose of 400 g/t are shown in Figure 11-9 for comparison; clearly limiting SPA dosage results in significantly improved selectivity.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-8 - T48 Rougher Flotation Rate

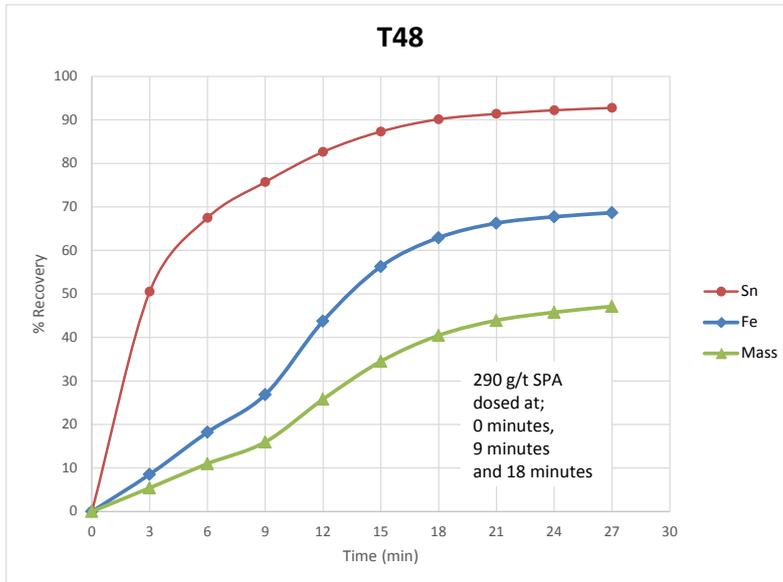


Figure 11-9 - Rougher Selectivity

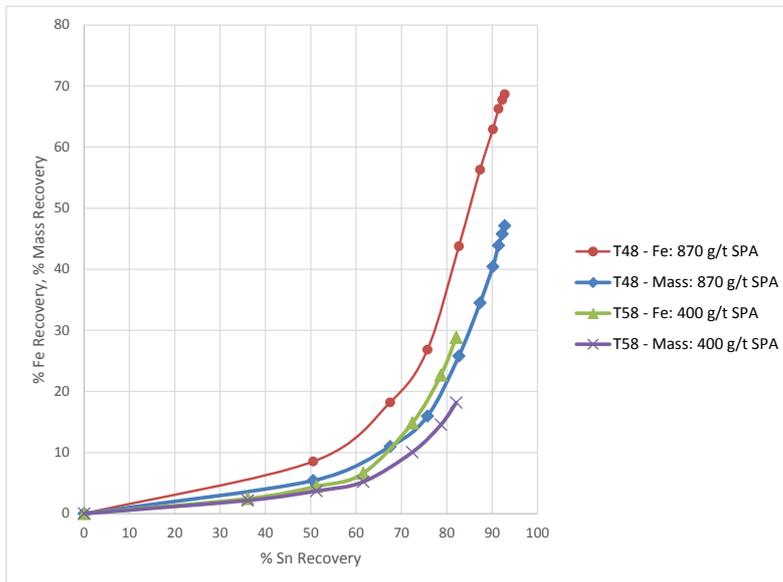


Table 25 shows a summary of conditions and results for test T58 to T79. This series of tests were fed with a composite of the primary gravity overflow stream and <40µm fraction of the fine scavenger tailings stream produced from cycles 11-31 of the gravity lock cycle test, LC01 de-slimes at sizes ranging from 12.1 µm to 0 µm (i.e. no de-slime).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 25 - Summary of Tin Flotation Tests T58 to T79

(De-slime feed sample; Primary gravity overflow stream and <40µm fraction of the fine scavenger tailings stream produced from cycles 11-31 of the gravity lock cycle test, LC01)

Tin Flotation Test No.	Feed material			Deslime mass recovery to u/f % wt	Sulfide scav.				Tin float					Tin Flotation Response				Deslime Performance		Overall Tin department to Deslime feed % of ore feed Sn units	Overall Tin to Tin Float Feed % of ore feed Sn units	Overall Tin recovery to flotation con				
	Deslime cut point (D50) µm	Produced from test no.	% <CS5 (<8 µm)		H ₂ SO ₄ g/t	SSF g/t	Water change g/t	SIPX g/t	H ₂ SO ₄ g/t	SSF g/t	Na ₂ SO ₃ g/t	SPA7080 g/t	MIBC g/t	Roughing		Cleaning		Tin recovery to U/F	Tin loss to O/F			% of ore feed Sn units	% of ore feed Sn units	Roughing (at ~4% Sn) % of ore feed Sn units	Cleaning (at 12% Sn) % of ore feed Sn units	Cleaning (at 15% Sn) % of ore feed Sn units
														Grade (% Sn)	Roughing recovery	Grade (% Sn)	Cleaning recovery									
T58	12.1	UF from T56	9.7	39.3	401	200	yes	50	180	200	301	401	99	4.0	80.2		9.0	62.9	60.1	39.9	24.4	14.7	11.8			
T59	12.1	UF from T56	9.7	39.3	440	200	yes	50	200	200	0	400	119	4.0	79.0		9.0	48.9	60.1	39.9	24.4	14.7	11.6			
T60	12.1	UF from T56	9.7	39.3	399	200	yes	50	100	200	299	299	99	4.0	82.7			60.1	39.9	24.4	14.7	12.1				
T61	12.1	UF from T56	9.7	39.3	298	199	no	50	0	199	298	398	98	4.0	64.7			60.1	39.9	24.4	14.7	9.5				
T62	12.1	UF from T56	9.7	39.3	400	200	yes	50	180	200	300	400	79	4.0	80.1	12.0	55.0	15.0	51.3	60.1	39.9	24.4	14.7	11.7	8.1	7.5
T65	12.1	UF from T56	9.7	39.3	199	199	yes	50	100	199	299	398	79	4.0	78.2			15.0	42.8	60.1	39.9	24.4	14.7	11.5	6.3	
T64	6.1	UF from T63	27.1	61.8	397	199	yes	50	179	199	298	397	88	4.0	76.4			77.8	22.2	24.4	19.0	14.5				
T67	6.1	UF from T63	27.1	61.8	499	200	yes	50	120	200	300	399	99	4.0	62.3			15.0	32.1	77.8	22.2	24.4	19.0	11.8	6.1	
T79	6.1	UF from T63	27.1	61.8	1010	202	yes	50	242	303	404	656	130	4.0	66.4	12.0	41.6	14.7	20.4	77.8	22.2	24.4	19.0	12.6	7.9	3.9
T71	4	UF from T70	40.6	79.9	592	197	yes	49	197	197	296	395	88	4.0	57.5	12.0	37.0	15.0	32.1	84.7	15.3	24.4	20.7	11.9	7.7	6.6
T72	4	UF from T70	40.6	79.9	394	197	yes	49	177	197	296	394	88	4.0	59.8			84.7	15.3	24.4	20.7	12.4				
T74	4	UF from T70	40.6	79.9	596	199	yes	50	199	199	298	397	79	4.0	37.1			15.0	21.9	84.7	15.3	24.4	20.7	7.7	4.5	
T75	4	UF from T70	40.6	79.9	595	198	yes	50	198	298	397	496	79	4.0	37.5			15.0	23.1	84.7	15.3	24.4	20.7	7.8	4.8	
T76	4	UF from T70	40.6	79.9	1203	200	yes	50	241	301	401	601	129	4.0	67.3	12.0	49.7	15.0	28.2	84.7	15.3	24.4	20.7	13.9	10.3	5.8
T69	3	LC Cyc 11-31: - 40 Fine Tails + O/F, +CS6	45.0	81.7	783	196	yes	49	176	196	294	392	97	3.9	12.3					90	10.0	24.4	22.0	2.7		
T68	0	LC Cyc 11-31: - 40 Fine Tails + O/F	53.0	100.0	298	198	yes	50	298	198	298	397	88	3.4	8.7					100	0.0	24.4	24.4	2.1		



STELLAR RESOURCES LIMITED HEEMSKIRK TIN PROJECT SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Figure 11-10 and Figure 11-11 show the impact of varying de-slime size (D50 cut point) on tin flotation roughing and cleaning grade/recovery response, while Figure 11-12 and Figure 11-13 show Sn recovery and mass recovery vs flotation time.

Figure 11-10

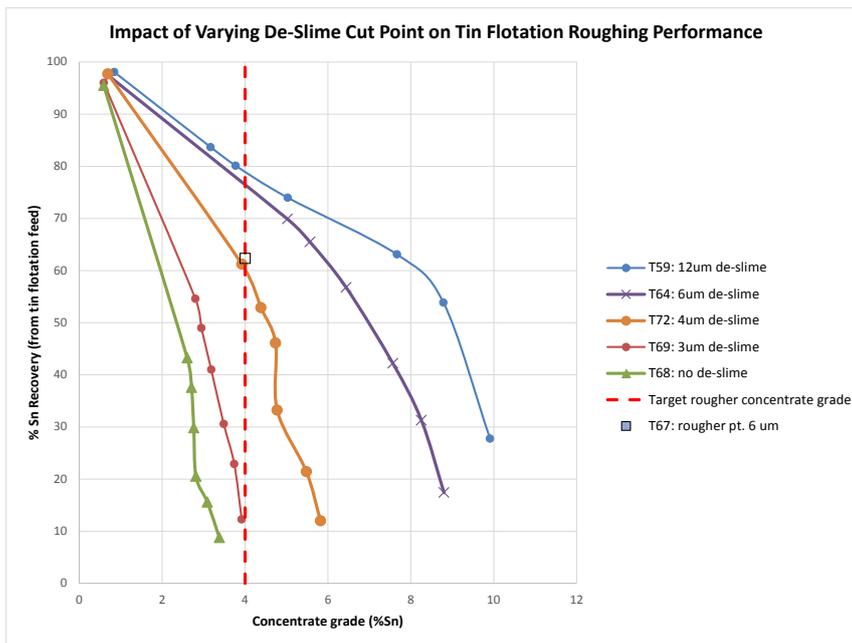
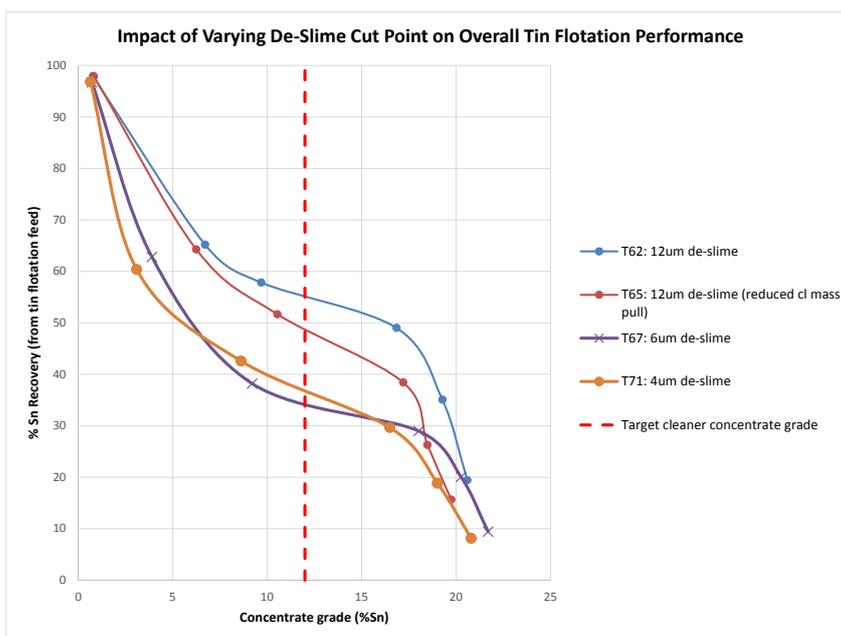


Figure 11-11





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-12 Sn Recovery vs Flotation Time

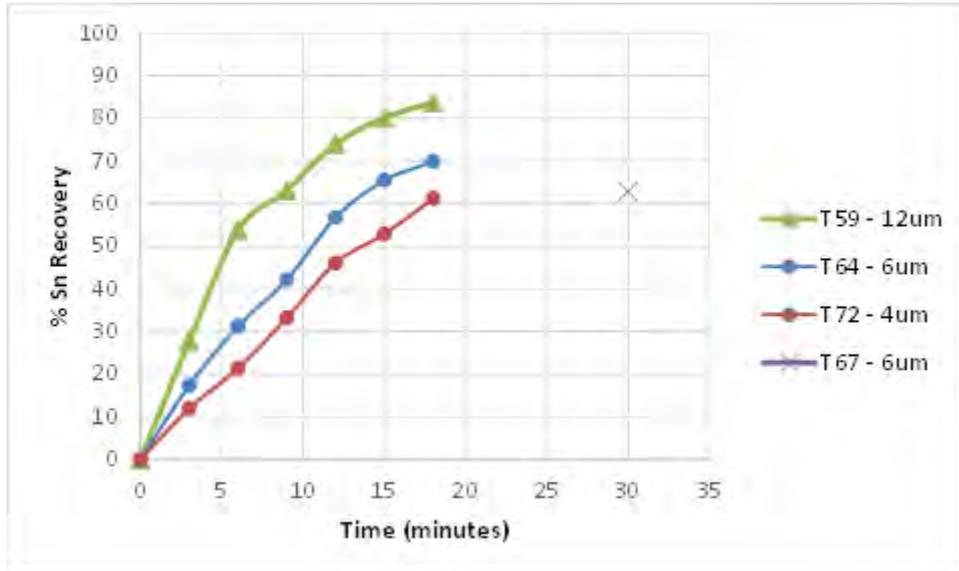
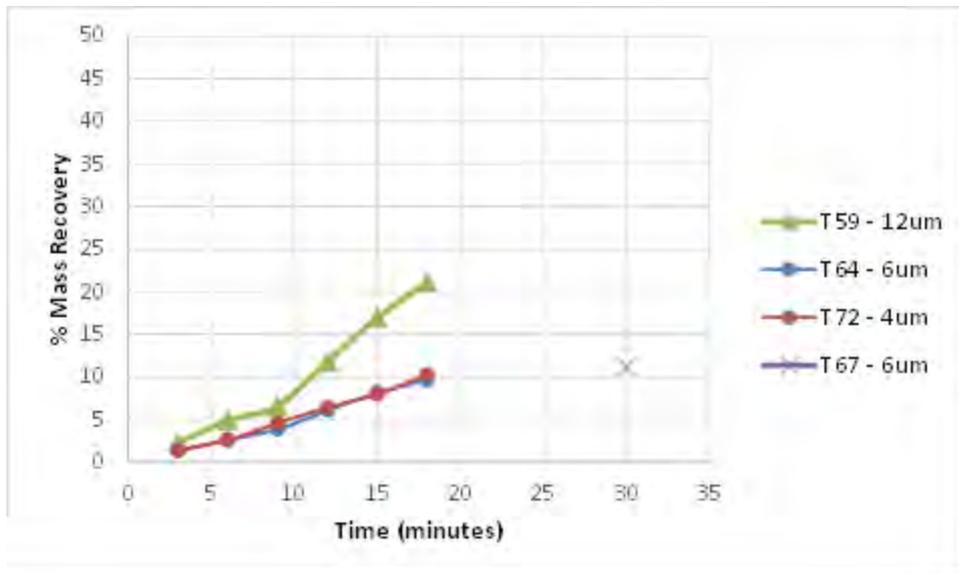


Figure 11-13 Mass Recovery vs Flotation Time



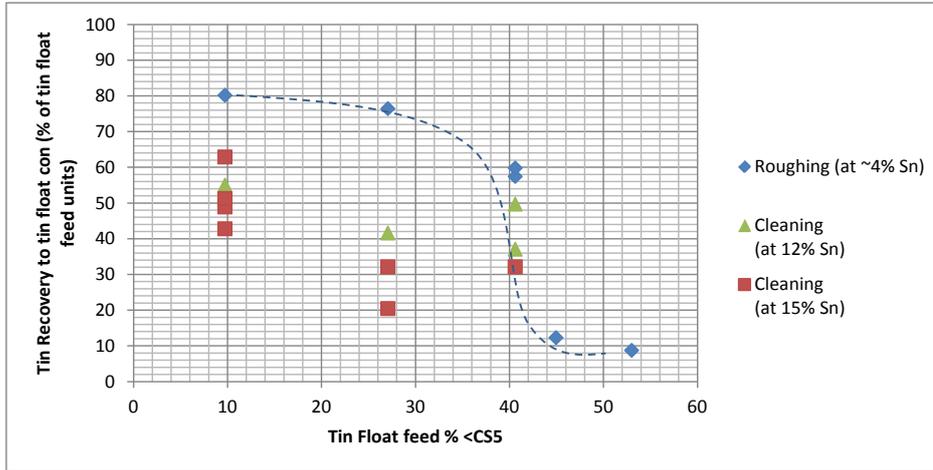
At de-slimes sizes $<4 \mu\text{m}$ tin flotation response is extremely poor.

Generally there is a very clear trend of deteriorating flotation performance with decreasing de-slime size/increasing slimes content. It should be noted T67 results do not fit with the general trends observed, with T67 result impacted by sample aging effects (refer Section 11.2.1).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

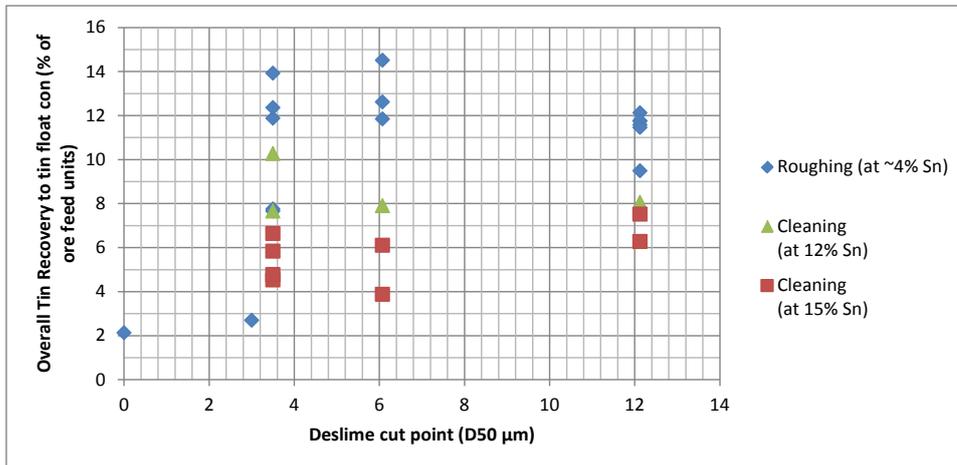
Figure 11-14 – Effect of Tin Flotation Feed slimes Content on Tin Flotation Performance



The deteriorating flotation response with decreasing de-slime size is offset to a considerable extent by increased Sn recovery to tin flotation feed at finer de-slime sizes.

This is illustrated in Figure 11-15 which shows overall tin flotation recovery from ore feed with varying de-slime size.

Figure 11-15 – Effect of De-slime size on Overall Sn Recovery to Tin Flotation Concentrate



Quite clearly the increased recovery across de-slime more than offsets poorer tin flotation performance at de-slime sizes of 4 and 6 μm. However, at de-sliming sizes ≤ ~3μm (tin flotation feed –CS5 content of >42%) overall recovery from Tin flotation is extremely poor.

Optimum de-slime cut point (D50) appears to be within the range 4 - 7μm. Given mass deportment to tin flotation feed is expected to increase considerably over this range, resulting in increased reagent consumptions (particularly SPA) and hence increased operating costs, further optimisation work is recommended.

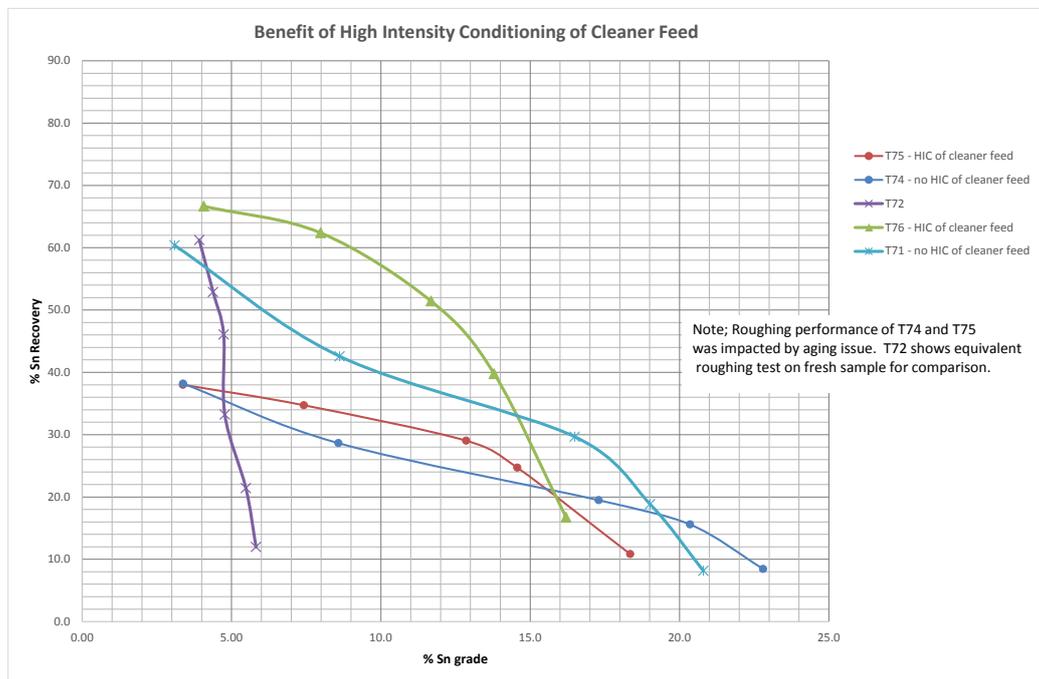


**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

In tests T74, T75, T71 and T76 use of high intensity conditioning (HIC) of rougher concentrate/cleaner feed was investigated as a means to improve response in cleaning and reduce Sn losses to cleaner 1 tails.

Clearly HIC gave a significantly improved cleaner response, with significantly reduced Sn losses to cleaner 1 tails.

Figure 11-16



Due to the small scale of the tin flotation tests meaningful measurement of specific power input to both the HIC stages (sulfide scavenger feed and cleaner feed) was not possible. Therefore, it is recommended further work be completed to better quantify HIC power requirements.

11.2.1 Sample Aging Issue

The later tin flotation results highlighted some issues with unexpected variability in flotation response. This was identified as an issue due to tin flotation feed sample “aging” through handling and storage during the laboratory routine (this is an artefact of the laboratory testing routine and not expected to be an issue at full scale).



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-17 Test T76 Sulfide Scavenger Tails Filter Cake showing visible flakes of brown aging product



Figure 11-17 shows the filter cake from T76 following the high intensity conditioning of the sulfide scavenger feed (stage immediately prior to the tin float). In the photo is shown pieces of cake which have been turned over, which have brown flaky material on them. On closer inspection these are clearly an iron compound (iron hydroxide/ iron hydroxysulfate) which has re-precipitated to produce agglomerates of particles held together by the iron compound. This is clear evidence of the sample aging/going off; it is assumed the sulfides present have oxidised releasing some iron and acid. The iron is then expected to re-precipitate as iron hydroxides and/or hydroxysulfates (such as jarosites). It is expected the iron which has precipitated on any mineral surfaces is likely of more concern than the actual agglomerates seen in T76.

Table 26 compares the dates of when the various de-sliming tests were done and when the float tests were completed to show the time elapsed between these and comparable tin floats. It appears the more obvious 'fliers'; T67 (compares with T64), T65 (compares with T62), T74 and T75 (compares with T71) have considerable time elapsed between the de-slime run and the tin float test, and the 'comparable test'. The 'aging' effect seems consistent in affect; with slowed cassiterite rate and reduced selectivity, with the tests having the largest elapsed times showing the most impact on performance.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 26 – Time Elapsed Between De-slime Test and Tin Flotation Test

Date of deslime test	Date of float test	Time elapsed (days) from deslime to float test	Time elapsed (days) from 'comparable test'	Tin Flotation Test No.	Feed material			Deslime mass recovery to u/f	Sulfide scav.				Tin float					Tin Flotation Response			
					Deslime cut point (D50) µm	Produced from test no.	% <CSS (<8 µm)		H ₂ SO ₄ g/t	SSF g/t	Water change	SIPX g/t	H ₂ SO ₄ g/t	SSF g/t	Na ₂ SO ₃ g/t	SPA7080 g/t	MIBC g/t	Roughing		Cleaning	
																		Grade (% Sn)	Recovery (% Sn)	Grade (% Sn)	Recovery (% Sn)
24/11/2014	24/11/2014	0	0	T58	12.1	UF from T56	9.7	39.3	401	200	yes	50	180	200	301	401	99	4.0	80.2	9.0	62.9
24/11/2014	24/11/2014	0	0	T59	12.1	UF from T56	9.7	39.3	440	200	yes	50	200	200	0	400	119	4.0	79.0	9.0	48.9
24/11/2014	02/12/14	8	1	T60	12.1	UF from T56	9.7	39.3	399	200	yes	50	100	200	299	299	99	4.0	62.7		
24/11/2014	01/12/14	7	1	T61	12.1	UF from T56	9.7	39.3	298	199	no	50	0	199	298	398	98	4.0	64.7		
24/11/2014	02/12/14	8	3	T62	12.1	UF from T56	9.7	39.3	400	200	yes	50	180	200	300	400	79	4.0	80.1	12.0	55.0
24/11/2014	05/12/14	11	3	T65	12.1	UF from T56	9.7	39.3	199	199	yes	50	100	199	299	398	79	4.0	78.2	15.0	51.3
3/12/2014	04/12/14	1		T64	6.1	UF from T63	27.1	61.8	397	199	yes	50	179	199	298	397	88	4.0	76.4		
3/12/2014	15/12/14	12	11	T67	6.1	UF from T63	27.1	61.8	498	200	yes	50	120	200	300	399	99	4.0	62.3	15.0	32.1
3/12/2014	20/3/2015	89	88	T79	6.1	UF from T63	27.1	61.8	1010	202	yes	50	242	303	404	656	130	4.0	66.4	12.0	41.6
22/01/2015	23/01/2015	1		T71	4	UF from T70	40.6	79.9	592	197	yes	49	197	197	296	395	88	4.0	57.5	12.0	37.0
22/01/2015	28/01/2015	6	5	T72	4	UF from T70	40.6	79.9	394	197	yes	49	177	197	296	394	88	4.0	59.8		
22/01/2015	11/02/15	20	19	T74	4	UF from T70	40.6	79.9	596	199	yes	50	199	199	298	397	79	4.0	37.1		
22/01/2015	11/02/15	20	19	T75	4	UF from T70	40.6	79.9	595	198	yes	50	198	298	397	496	79	4.0	37.5	15.0	21.9
22/01/2015	19/2/15	28	27	T76	4	UF from T70	40.6	79.9	1203	200	yes	50	241	301	401	601	129	4.0	67.3	12.0	49.7
13/01/2015	13/01/15	0		T68	3	LC Cyc 11-31-40 Fine Tails + O/F. +CS6	45.0	81.7	783	196	yes	49	176	196	294	392	97	3.9	12.3		
13/01/2015	13/01/15	0	0	T68	0	LC Cyc 11-31-40 Fine Tails + O/F	53.0	100.0	298	198	yes	50	298	198	298	397	88	3.4	8.7		

This aging issue is thought to have particularly impacted the results achieved in tests T67, T74, T75 and T79 with roughing response being significantly poorer than that seen in earlier comparable tests.

The impact of this was mitigated to some extent in T76 (which was essentially a repeat of T75) and T79 with a modified roughing procedure. In these tests the rougher concentrate was filtered to give a better estimate of mass recovery and the rougher stage continued until a target damp weight of cake (rather than froth) was reached.

It should be noted the majority of tests completed have followed expected trends and are not thought to be particularly impacted by this issue.

In future work it is strongly recommended to review sample handling procedures to minimise opportunity for oxidation, and that all tin flotation feed materials be kept in cold storage until immediately prior to use.

11.2.2 Estimated Closed Circuit Tin Flotation Performance

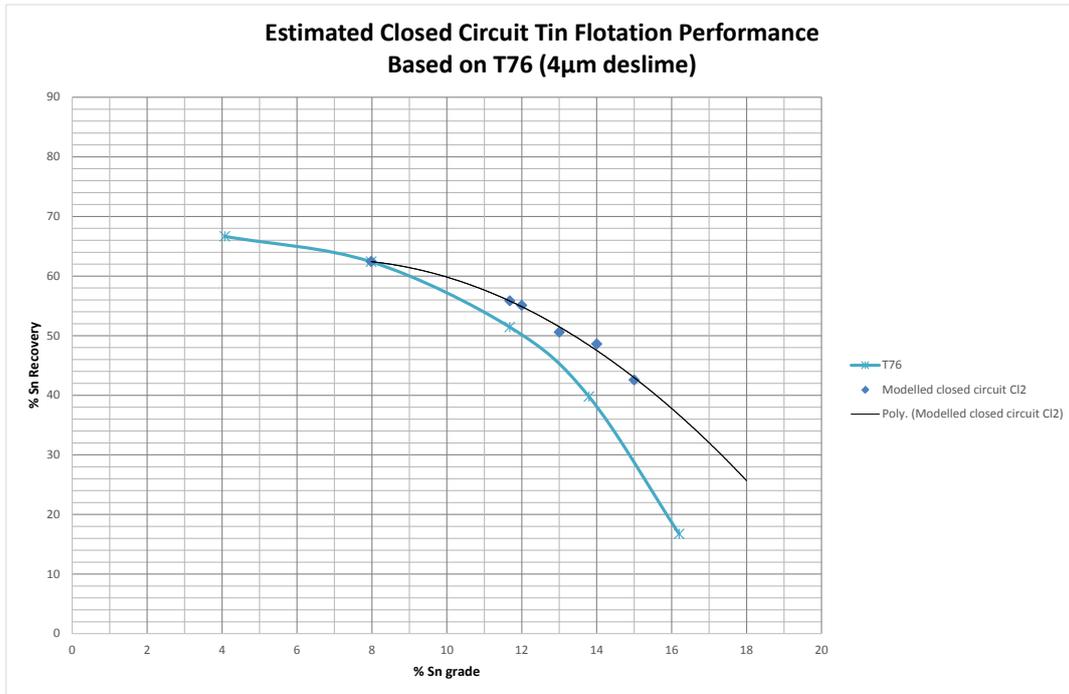
Due to restrictions in the quantity of tin flotation feed sample available conducting locked cycle tin flotation tests to estimate closed circuit cleaning performance was not practical. Therefore, in order to estimate closed circuit cleaning performance the tin flotation circuit was modelled utilising Metsim based on the batch test results seen in test T76.

Results are summarised in Figure 11-18, with the solid blue line showing the batch test result achieved in T76, while the black line and blue diamonds show the modelling outcome. Given the considerable amount of tin units contained in the cleaner 2 tailings from the batch tests (11% in T76), considerable uplift in tin flotation recovery is expected with the recycle of cleaner 2 tailings to cleaner 1 feed.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Figure 11-18



11.2.3 Tin Flotation Concentrate Composition

Tin flotation concentrate produced under the optimised flotation conditions is summarised in Table 27 for a range of Sn grades.

Table 27 – Tin Flotation Concentrate Composition (from T76)

Assay	Units	Tin Flotation Concentrate			
		15.0	14.0	13.0	12.0
Sn	%	15.0	14.0	13.0	12.0
Fe	%	23.8	24.3	24.8	25.3
As	%	0.12	0.12	0.12	0.12
Mn	%	0.31	0.32	0.33	0.34
CaO	%	0.30	0.31	0.32	0.32
MgO	%	1.71	1.75	1.80	1.87
Al ₂ O ₃	%	3.98	4.04	4.16	4.28
SiO ₂	%	14.8	15.3	15.8	16.3
S	%	2.11	2.09	2.12	2.16
CO ₃	%	10.6	11.1	11.5	12.0

“Low” and “Medium” Grade composites of cleaner concentrates were put together from cleaner concentrate products from tests T62 to T79 for more detailed analysis and leaching. Table 28 shows ICP scan results for these composites, with QXRD results shown in Table 29.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 28 – ICP Analysis of “Low” and “Medium” Grade Cleaner Concentrate

Sample	Ag	Al	As	Ba	Be	Bi	Ca	Cd	Ce	Co	Cr	Cs	Cu	Fe	Ga	Ge	Hf	In	K	La	Li	Mg	Mn	Mo
	ppm	%	ppm	ppm	ppm	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm	%	ppm	ppm	ppm	%	ppm	ppm	%	ppm	ppm	
CL2 Conc Low Grade Comp	3.65	1.95	932	60	10.2	53.1	0.24	0.42	31.3	9.1	206	10.7	350	26	17.8	0.76	2.5	5.7	0.23	15.6	24.8	1.09	3080	9.8
CL2 Conc Medium Grade Comp	3.81	1.6	973	70	13.35	77.4	0.79	<0.02	41.9	7.7	181	9.36	276	23.9	15.6	0.91	2.3	5.35	0.19	18.1	20.4	0.95	2840	8.51

Sample	Na	Nb	Ni	P	Pb	Rb	Re	S	Sb	Sc	Se	Sr	Ta	Te	Th	Ti	Tl	U	V	W	Y	Zn	Zr
	%	ppm	ppm	ppm	ppm	ppm	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm	ppm
CL2 Conc Low Grade Comp	0.06	60.3	56.7	830	1220	48	0.007	1.91	23.7	14	3	41.5	3.08	0.08	5.9	2.2	0.76	4	131	197.5	13.8	572	107
CL2 Conc Medium Grade Comp	0.05	63.9	55.5	3310	1270	40.6	0.005	2.74	22.4	13	3	101	3.23	0.08	7	2.08	0.64	4	127	226	23	485	197.6

Table 29 – QXRD Analysis of “Low” and “Medium” Grade Cleaner Concentrate

CL2 CONC LOW GRADE COMP	10.4% Sn	CL2 CONC MEDIUM GRADE COMP	14.9% Sn
Phase	Weight%	Phase	Weight%
Siderite	37.1	Siderite	34.2
Cassiterite	13.1	Cassiterite	18.9
Quartz	11.7	Rutile	12
Rutile	11.5	Quartz	10.2
Magnetite	7.5	Magnetite	9.1
Chlorite	4.6	Pyrite	2.9
Pyrite	3.9	Anatase	2.6
Dravite/tourmaline	3.1	Apatite	2.4
Anatase	2.8	Chlorite	2.1
Microcline	1.4	Dravite/tourmaline	1.9
Diaspore?	1.4	Diaspore?	1.6
Muscovite	1.2	Microcline	1.3
Apatite	0.6	Muscovite	0.7
Calcite	0	Calcite	0
Dolomite	0	Dolomite	0
Actinolite/tremolite	0	Actinolite	0

Siderite is by far the most significant diluent present in the tin flotation concentrates, with significant levels of quartz, rutile and magnetite also present. Given the quantity of siderite present the tin flotation concentrate is expected to upgrade significantly in concentrate leaching.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

11.3 Key Outcomes

- The various tin flotation testing completed has highlighted that silica is not particularly problematic from a selectivity perspective, with silica levels in concentrate being in-line with those expected due to entrainment.
- Tin flotation testwork has highlighted the criticality of appropriate de-slime and rejection of sulfur via the sulfide scavenger flotation circuit to achieving acceptable tin flotation performance;
 - A target sulfur grade in tin flotation feed post sulfide scavenging of less than ~0.7% S is recommended
 - Optimum de-slime cut point is within the range 4 - 7µm
 - At de-slimes sizes <4 µm tin flotation response is extremely poor
- Optimisation of the De-slime cut point has allowed minimisation of combine slimes and tin flotation tailings losses.
- Fundamentally poor selectivity against siderite remains the major challenge within the tin flotation circuit. From this perspective the testwork has demonstrated;
 - selectivity against siderite is significantly improved at low SPA dose rates (i.e. high dosages are detrimental to selectivity)
 - the usefulness of high intensity conditioning both of tin flotation feed and cleaner feed in improving selectivity
 - limiting mass pull within roughing reduces siderite deportment to the cleaner circuit to manageable levels
- Tin flotation test work has robustly demonstrated commercially meaningful tin flotation concentrate grades can be achieved at acceptable recoveries.

Expected Tin Float reagent consumptions (including sulfide scavenging) based on dose rates observed in the testwork are summarised in Table 30.

Table 30 - Expected Tin Float Reagent Consumptions (including sulfide scavenging)

pH	~5
Sulfuric Acid	600 g/t
PAX/SIPX	50 g/t
SSF	500 g/t
SPA	500 g/t
Na ₂ SO ₃	400 g/t
Frother (MIBC)	90 g/t

It should be noted that in the testwork SIPX was used in the sulfide scavenger. However, to maintain commonality with the sulfide flotation and sulfide dressing flotation circuits it is suggested PAX be used in place of SIPX. This is not expected to have any detrimental performance impacts.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

12 CONCENTRATE LEACHING

Full concentrate leach test results are contained in Appendix 10.

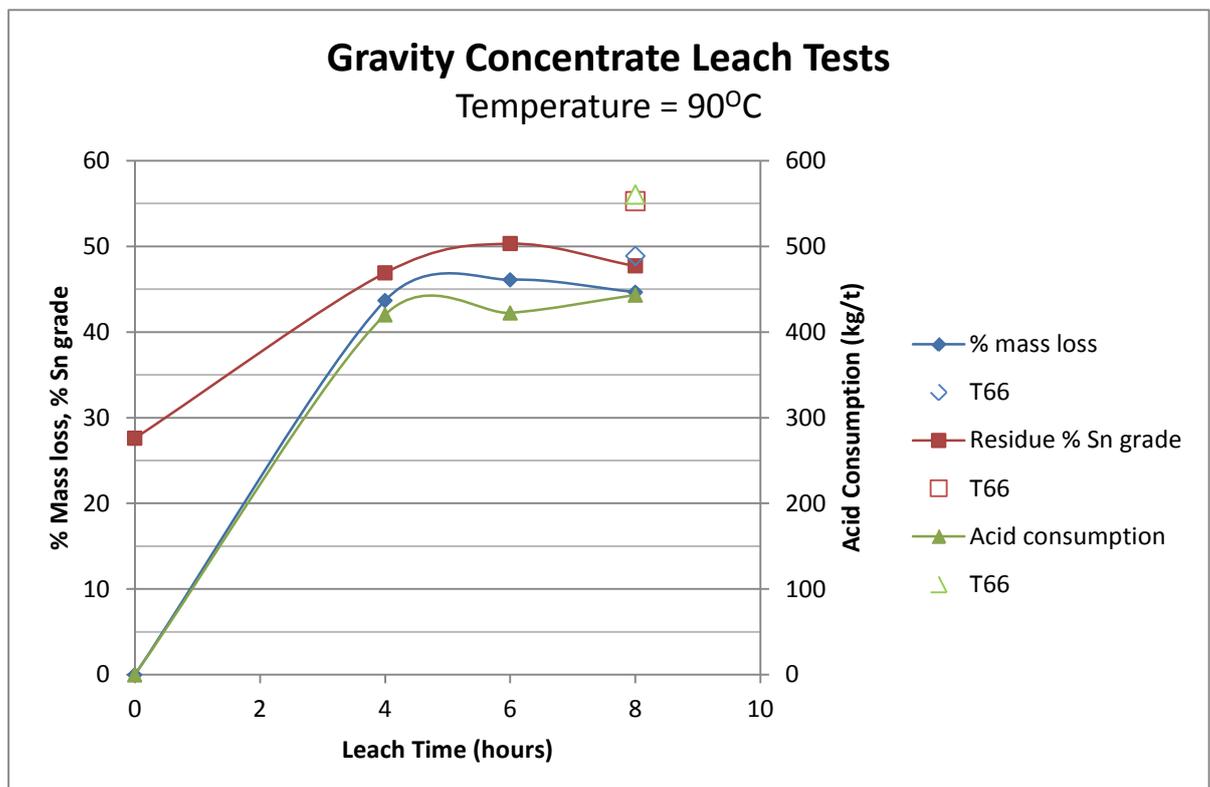
Concentrate leach tests were carried out on both the gravity concentrate produced from gravity concentrate dressing testwork and on two composites of tin flotation cleaner concentrate produced from tin flotation testing.

Aims of the concentrate leach testwork were to:

- Better quantify required concentrate leach residence time.
- Confirm achievable Sn upgrade, extents of leaching of other species, and expected acid consumption of both the gravity and tin flotation concentrates across the concentrate leach circuit.
- Produce final concentrate samples for detailed analysis including multi-element ICP scans and QXRD (refer Section 10.4 for final gravity concentrate and Section 11.2.3 for final tin flotation concentrate analysis).

Figure 12-1 shows plots of mass loss, final leach residue Sn grade and acid consumption versus leach time at 90°C for concentrate leach tests carried out on the dressed gravity concentrate.

Figure 12-1





**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

The concentrate leach is expected to operate at a temperature of ~90 to 97°C due to the large heat of dilution associated with the required acid input.

At a temperature of 90°C the concentrate leach is nearing completion by 4 hours. However, at 4 hours residues still contained some carbonate. Hence a total residence time of 8 hours is recommended to ensure complete leaching.

For the gravity concentrate acid consumption was in the range 440 to 560 kg/t after 8 hours of leaching. Actual acid consumption is expected to be highly dependent on feed concentrate composition. A residual free acid of ~20-25 g/l at the end of the leach is recommended to ensure leaching reaches completion.

Table 31 shows results for concentrate leach test T66 conducted on the dressed gravity concentrate produced under the final optimised concentrate dressing conditions, while Table 32 shows results of duplicate assays of the final gravity concentrate produced, along with the unleached concentrate for comparison.

Table 31 – Final Gravity Concentrate: Concentrate Leach Results (T66)

Acid consumption = 560 kg/t, leach time = 8 hours, Leach temperature = 90°C

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(g/L)	Rec (%)												
Start Liquor	0.8	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0
Final Liquor	0.8	0.008	0.0	74.30	91.3	0.01	4.0	3.91	95.1	0.72	35.8	4.95	82.7	2.77	35.0

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Start Solids	300.0	28.80		21.00		0.10		1.10		1.20		2.60		2.70	
Final Residue	153.4	55.25	100.0	3.82	8.7	0.13	96.0	0.11	4.9	0.70	64.2	0.56	17.3	2.79	65.0

Calc Feed	300.0	28.25		22.50		0.07		1.14		0.56		1.66		2.19	
Assay Feed		28.80		21.00		0.10		1.10		1.20		2.60		2.70	

Table 32 – “Final Gravity Concentrate” Analysis (post leaching)

Results of Duplicate Assays for T66 Residue Solids

	Sn	Fe	As	S	SiO ₂	Mn	CaO	MgO	Al ₂ O ₃
	%	%	%	%	%	%	%	%	%
T66 End Leach Res A	54.4	3.8	0.13	1.13	13.45	0.11	0.7	0.56	2.84
T66 End Leach Res B	56.1	3.83	0.13	1.16	12.8	0.11	0.71	0.56	2.73
T66 Leach Feed	28.8	21.0	0.1	0.7	7.0	1.1	1.2	2.6	2.7

Aside from the carbonates present a substantial portion of the Al₂O₃ present has also leached.

Table 33 and Table 34 show results for concentrate leach tests carried out on “Medium” and “Low” grade tin flotation cleaner concentrate samples.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 33 –“Medium” Grade Cleaner Concentrate: Concentrate Leach Results

Acid consumption = 480 kg/t, leach time = 8 hours, Leach temperature = 90°C

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Final Residue	2.8384	28.10	100.0	4.12	7.5	0.05	71.6	0.03	4.3	0.07	5.2	0.49	19.6	4.29	70.4
Calc Feed	6.0086	13.27		25.80		0.03		0.33		0.64		1.18		2.88	

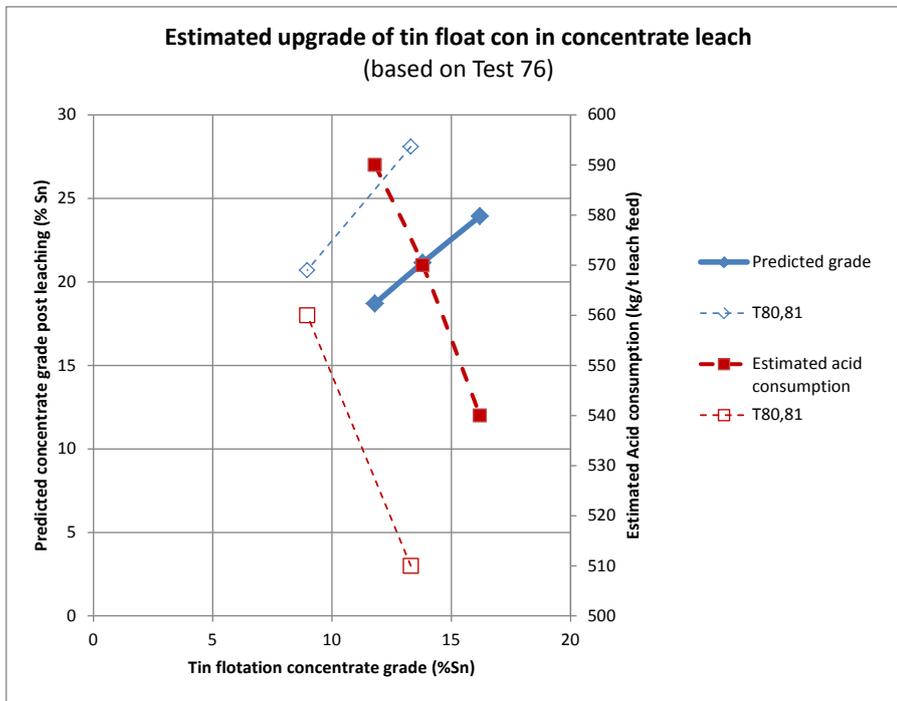
Table 34 –“Low” Grade Cleaner Concentrate: Concentrate Leach Results

Acid consumption = 528 kg/t, leach time = 8 hours, Leach temperature = 90°C

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Final Residue	2.5996	20.70	100.0	4.30	6.6	0.05	18.1	0.01	1.3	0.08	11.7	0.57	18.8	5.26	69.8
Calc Feed	6.0086	8.96		28.28		0.12		0.34		0.30		1.31		3.26	

Both the medium and low grade concentrates upgraded extremely well, more than doubling in Sn grade. The upgrade seen was much higher than expected based on previous modelling of expected concentrate leach performance of tin flotation concentrates. A comparison of model expectations and the actual test outcomes is shown in Figure 12-2.

Figure 12-2 Comparison of Concentrate Leach Model and Leach Test Outcomes



Given the significant under estimation of the upgrade of tin flotation concentrate and over estimation of acid consumption it is recommended to revise the previous concentrate leach model to better reflect expected performance on tin flotation concentrates.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

13 TAILINGS CHARACTERISTICS

The tailings streams produced from the circuit and their relative tonnages assuming a ROM treatment rate of 600,000 t/y are shown in Table 35.

Table 35 – Tailings Streams

Tailings Stream	Tonnage (t/y)⁽¹⁾
Final Sulfide Concentrate	164,400
Fine Gravity Tailings	118,400
Slime Tailings	62,200
Tin Flotation Tailings	242,000

Notes: 1. Assumes 600,000 t/y ROM treated

Head assays, size distributions and size by size assays and metal distributions of these are shown in Table 36, Table 37, Table 38 and Table 39 respectively.

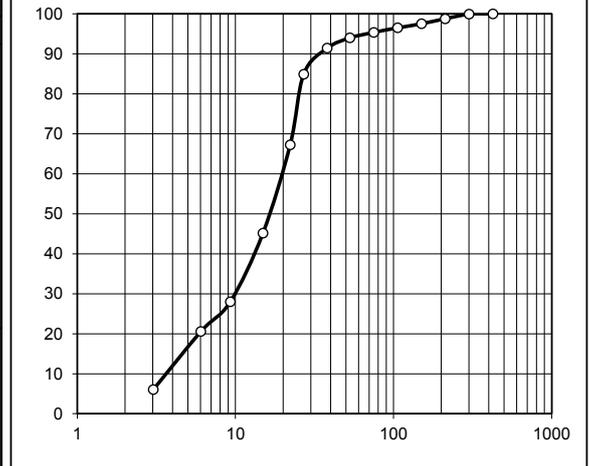
In addition to the above stream a minor amount, ~4,000 t/y, of magnetite concentrate will also be produced as an additional final tailings stream from the gravity concentrate dressing circuit.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 36 – Final Sulfide Concentrate

Product Sized Comb Clnr C1-C3		SIZE um	WEIGHTS			
			g	(%)	%PASS	
P80		850	0.00	0.00	100.0	
		600	0.00	0.00	100.0	
		425	0.00	0.00	100.0	
		300	0.21	0.09	99.9	
		212	2.54	1.12	98.8	
		150	2.88	1.27	97.5	
		106	2.29	1.01	96.5	
		75	2.57	1.14	95.4	
		53	3.12	1.38	94.0	
		26	38	5.84	2.58	91.4
		CYCLOSIZER	CS1	27	14.71	6.50
FLOW 185	CS2	22	40.08	17.70	67.2	
TEMP 21	CS3	15	49.97	22.07	45.1	
SG 3.50	CS4	9	38.84	17.15	28.0	
MINS 20	CS5	6	16.79	7.42	20.6	
CENTRIFUGE	CS6	3	32.90	14.53	6.0	
		SUB	13.68	6.04	0.0	
		TOTAL	226.42	100.0		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	4.63	0.09	4.69	42.90	4.87	0.34	4.30	40.90	4.74	1.85	4.74	0.02	5.19
CS1	10.45	0.07	8.23	44.10	11.29	0.55	15.71	44.30	11.58	0.92	5.32	0.01	5.86
CS2	17.70	0.07	13.94	43.60	18.90	0.45	21.77	46.00	20.37	0.72	7.05	0.01	9.92
CS3	22.07	0.08	19.86	42.50	22.97	0.38	22.91	39.80	21.97	1.12	13.67	0.01	12.37
CS4	17.15	0.08	15.44	41.30	17.35	0.35	16.40	41.50	17.81	1.06	10.05	0.01	9.61
CS5	7.42	0.08	6.67	41.00	7.45	0.28	5.67	33.70	6.25	1.11	4.55	0.01	4.16
CS6	14.53	0.12	19.61	38.70	13.77	0.25	9.93	38.60	14.03	2.62	21.05	0.04	32.57
<CS6	6.04	0.17	11.55	23.00	3.40	0.20	3.30	21.50	3.25	10.05	33.57	0.06	20.32
CALC	100.0	0.09	100.00	40.83	100.00	0.37	100.00	39.98	100.00	1.81	100.00	0.02	100.00
ASSAY		0.07		41.20		0.38		42.10		1.58		0.02	

ANALYSES

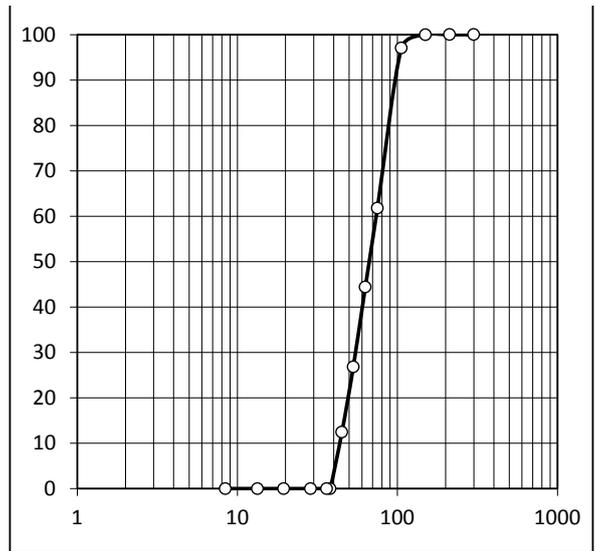
SIZE um	WT %	CaO		MgO		Al2O3		CO3		C-organic		C-inorganic	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	4.63	0.16	7.91	0.34	4.33	0.48	1.81	0.34	4.71	0.18	4.00	0.16	5.98
CS1	10.45	0.04	4.46	0.29	8.34	0.29	2.47	0.17	5.32	0.08	4.01	0.09	7.59
CS2	17.70	0.02	3.78	0.32	15.58	0.20	2.89	0.20	10.60	0.07	5.95	0.12	17.14
CS3	22.07	0.03	7.07	0.32	19.42	0.29	5.22	0.24	15.85	0.10	10.59	0.14	24.93
CS4	17.15	0.03	5.49	0.31	14.63	0.24	3.36	0.24	12.32	0.12	9.88	0.12	16.61
CS5	7.42	0.05	3.96	0.30	6.12	0.26	1.57	0.25	5.55	0.15	5.34	0.10	5.98
CS6	14.53	0.06	9.30	0.47	18.78	0.80	9.48	0.53	23.05	0.39	27.19	0.14	16.41
<CS6	6.04	0.90	58.03	0.77	12.80	14.85	73.19	1.25	22.60	1.14	33.05	0.11	5.36
CALC	100.0	0.09	100.00	0.36	100.00	1.23	100.00	0.33	100.00	0.21	100.00	0.12	100.00
ASSAY		0.02		0.37		0.48		0.28		0.15		0.13	



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 37 – Fine Gravity Tailings

LC01 Cyc6 -106 FGT		SIZE um	WEIGHTS			
			gm	(%)	%PASS	
p80		850	0.00	0.00	100.0	
		600	0.00	0.00	100.0	
		425	0.00	0.00	100.0	
		300	0.00	0.00	100.0	
		212	0.00	0.00	100.0	
		150	0.02	0.03	100.0	
		106	1.91	2.91	97.1	
	91		75	23.19	35.30	61.8
			63	11.41	17.37	44.4
			53	11.55	17.58	26.8
		45	9.45	14.39	12.4	
		38	8.16	12.42	0.0	
CYCLOSIZER	CS1	36		0.00	0.0	
FLOW 185	CS2	29		0.00	0.0	
TEMP 21	CS3	19		0.00	0.0	
SG 2.60	CS4	13		0.00	0.0	
MINS 20	CS5	8		0.00	0.0	
SUB			0.00	0.00	0.0	
TOTAL			65.69	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	38.24	0.23	39.7	12.05	36.0	0.06	40.2	0.77	33.0	57.40	38.7	0.26	32.7
63	17.37	0.22	17.3	12.55	17.0	0.05	15.2	0.90	17.5	57.20	17.5	0.29	16.6
53	17.58	0.22	17.5	12.70	17.5	0.06	18.5	0.91	17.9	57.50	17.8	0.31	17.9
45	14.39	0.22	14.3	13.75	15.5	0.06	15.1	1.06	17.1	55.90	14.2	0.35	16.5
38	12.42	0.20	11.2	14.45	14.0	0.05	10.9	1.04	14.5	53.80	11.8	0.40	16.3
26													
12													
8													
CALC	100.00	0.22	100.0	12.79	100.0	0.06	100.0	0.89	100.0	56.72	100.0	0.30	100.0
ASSAY													

ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
75	38.24	0.92	36.9	3.62	39.4	8.82	39.9				
63	17.37	0.93	16.9	3.47	17.2	8.46	17.4				
53	17.58	0.92	17.0	3.38	16.9	8.29	17.2				
45	14.39	1.01	15.2	3.47	14.2	8.13	13.8				
38	12.42	1.07	13.9	3.48	12.3	7.98	11.7				
26	0.00										
12	0.00										
8	0.00										
CALC	100.00	0.95	100.0	3.51	100.0	8.46	100.0				
ASSAY											

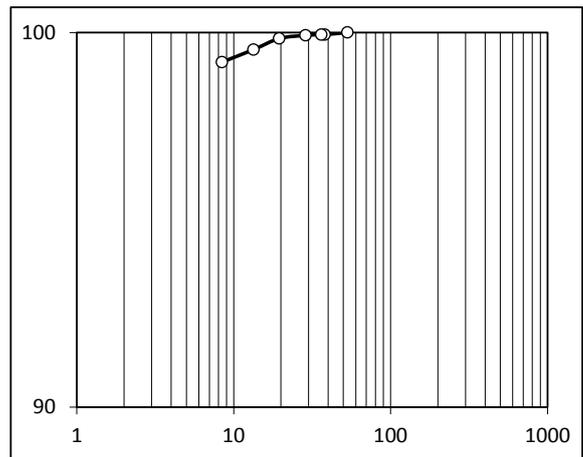


**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 38 – Slime Tails

	% Sn	% Fe	% SiO ₂	% S	% CaO
Slime Tails	0.46	21.7	38.4	1.01	0.82

Cyclone Overflow T70		SIZE um	WEIGHTS		
			gm	(%)	%PASS
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	0.00	0.00	100.0
		106	0.00	0.00	100.0
		75	0.00	0.00	100.0
		53	0.00	0.00	100.0
		38	0.06	0.06	99.9
CYCLOSIZER		36	0.00	0.00	99.9
FLOW	185	29	0.02	0.02	99.9
TEMP	21	19	0.09	0.09	99.8
SG	2.60	13	0.31	0.30	99.5
MINS	20	8	0.35	0.33	99.2
		SUB	104.20	99.21	0.0
		TOTAL	105.03	100.00	

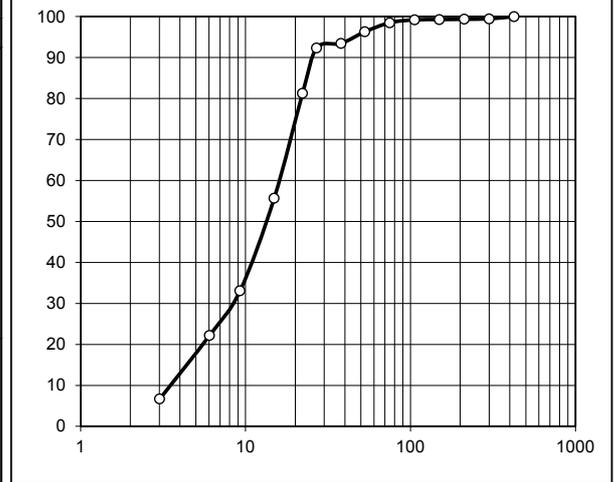




**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 39 – Tin Flotation Tails

Product Sized		SIZE um	WEIGHTS		
Ro Tail			g	(%)	%PASS
P80		850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.70	0.54	99.5
		212	0.14	0.11	99.3
		150	0.10	0.08	99.3
		106	0.10	0.08	99.2
		75	0.89	0.69	98.5
		53	2.84	2.21	96.3
		22	38	3.65	2.84
CYCLOSIZER	CS1	27	1.45	1.13	92.3
FLOW 185	CS2	22	14.23	11.06	81.3
TEMP 21	CS3	15	32.95	25.61	55.7
SG 3.50	CS4	9	29.01	22.55	33.1
MINS 20	CS5	6	14.08	10.94	22.2
CENTRIFUGE	CS6	3	19.88	15.45	6.7
		SUB	8.63	6.71	0.0
		TOTAL	128.65	100.0	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
CS1	7.67	0.41	12.84	17.65	7.03	0.05	7.38	0.77	14.55	49.20	8.78	0.53	6.03
CS2	11.06	0.44	19.87	25.30	14.53	0.05	10.63	0.48	13.08	30.00	7.72	1.11	18.21
CS3	25.61	0.26	27.18	18.80	25.00	0.05	24.62	0.28	17.66	45.40	27.05	0.72	27.35
CS4	22.55	0.20	18.41	18.45	21.60	0.05	21.68	0.20	11.11	45.60	23.92	0.67	22.41
CS5	10.94	0.18	8.04	18.60	10.57	0.05	10.52	0.21	5.66	44.20	11.26	0.64	10.39
CS6	15.45	0.16	10.09	18.85	15.12	0.05	14.85	0.45	17.13	41.60	14.96	0.52	11.92
<CS6	6.71	0.13	3.56	17.65	6.15	0.08	10.32	1.26	20.82	40.40	6.31	0.37	3.68
CALC	100.0	0.24	100.00	19.26	100.00	0.05	100.00	0.41	100.00	42.98	100.00	0.67	100.00
ASSAY		0.24		19.30		0.05		0.33		42.90		0.69	

ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3		CO3		C-organic		C-inorganic	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
CS1	7.67	0.89	5.61	3.43	6.91	7.05	6.63	2.02	5.56	0.14	6.55	1.88	5.50
CS2	11.06	1.34	12.18	3.47	10.08	6.41	8.70	4.36	17.30	0.11	7.41	4.25	17.92
CS3	25.61	1.13	23.78	3.37	22.67	7.01	22.02	2.94	27.02	0.11	17.17	2.83	27.63
CS4	22.55	1.15	21.31	3.69	21.85	7.43	20.55	2.83	22.90	0.11	15.12	2.72	23.38
CS5	10.94	1.15	10.34	3.96	11.38	8.21	11.02	2.87	11.27	0.11	7.34	2.76	11.52
CS6	15.45	1.01	12.83	4.70	19.07	10.80	20.47	2.23	12.36	0.15	14.13	2.08	12.25
<CS6	6.71	2.53	13.95	4.56	8.03	12.90	10.61	1.49	3.59	0.79	32.29	0.70	1.79
CALC	100.0	1.22	100.00	3.81	100.00	8.15	100.00	2.79	100.00	0.16	100.00	2.62	100.00
ASSAY		1.12		3.87		8.23		2.80		0.11		2.69	



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

14 CONCLUSIONS

The Severn metallurgical testing program has focused on the optimisation of the process flowsheet utilising a large “global” composite sample representing the typical Severn mineralogy, composition and tin grades. This has provided a number of important improvements to metallurgical performance, and flowsheet simplifications, in addition to generating more robust information with respect to optimum process design criteria and processing conditions.

Key outcomes of the program include:

- Elimination of the heavy media separation circuit

Based on the analysis completed heavy media separation detracts value from the Heemskirk project when the treatment of the same ROM (grade and tonnages of ore) is considered. That is, HMS detracts value when considered from a processing only perspective. On this basis inclusion of HMS in the Heemskirk flowsheet is not recommended.

- Coarser primary grind; grind size optimisation test work has demonstrated a significantly coarser primary grind size (P80 = 250 µm) is more optimum than that considered in the PFS (P80 = 130 µm). This provides the following benefits;
 - reduced tin losses due to reduced fines production
 - reduction in primary grind operating and capital costs, and overall comminution energy requirements

Significantly, the percentage of tin passing 30 µm (below which size gravity recovery is relatively poor) is estimated to decrease from ~43% passing 30 µm at a primary grind size of 130 µm (as assumed in the PFS), to only ~30% passing 30 µm at a primary grind size of 240 µm. This is equivalent to ~30% reduction in fine tin generation, and is a key contributor to the improved gravity recovery achieved.

- Optimisation of the sulfide flotation circuit has led to a significant reduction in tin losses to the final sulphide concentrate tailings stream. This, together with the elimination of the heavy media circuit has increased the amount of tin available for recovery within the gravity and tin flotation circuits.
- Heavy regrind within the sulfide flotation circuit along with use of guar are key to achieving very low Sn losses in this circuit.
- Optimisation of the gravity circuit configuration, combine with upstream flowsheet improvements, has led to ~10% improvement in tin recovery via gravity.
- Improvements with the concentrate dressing circuit have led to improved gravity concentrate quality and clearly demonstrated a high quality concentrate, low in penalty elements, can be readily produced.
- The various tin flotation testing completed has highlighted that silica is not particularly problematic from a selectivity perspective, with silica levels in concentrate being in-line with



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

those expected due to entrainment. This allows the elimination of the silica flotation circuit (considered in the PFS) and provides a simplification to the overall process flowsheet.

- Tin flotation testwork has highlighted the criticality of appropriate de-slime and rejection of sulfur via the sulfide scavenger flotation circuit to achieving acceptable tin flotation performance.
 - A target sulfur grade in tin flotation feed post sulfide scavenging of less than ~0.7% S is recommended.
 - Optimum de-slime cut point is within the range 4 - 7µm.
 - At de-slimes sizes <4 µm, or <CS5 “slimes” content of >43%, tin flotation response is extremely poor.
- Optimisation of the De-slime cut point has allowed minimisation of combine slimes and tin flotation tailings losses.
- Fundamentally poor selectivity against siderite remains the major challenge within the tin flotation circuit. From this perspective the testwork has demonstrated;
 - selectivity against siderite is significantly improved at low SPA dose rates (i.e. high dosages are detrimental to selectivity)
 - the usefulness of high intensity conditioning both of tin flotation feed and cleaner feed in improving selectivity
 - limiting mass pull within roughing reduces siderite department to the cleaner circuit to manageable levels
- Tin flotation test work has robustly demonstrated commercially meaningful tin flotation concentrate grades can be achieved at acceptable recoveries.
- Concentrate leaching performance on tin flotation concentrates was significantly better than expected, providing greater Sn upgrade with reduced acid consumption than previously estimated.
- Concentrate leaching provides a robust, tin loss free means of significantly upgrading Sn grade of both the gravity concentrate and tin flotation concentrate, as siderite forms the major diluent present in both of these concentrates.

In particular leaching of the gravity concentrate upgrades this sufficiently to allow significant dilution with relatively low grade tin flotation concentrate, allowing overall Sn recoveries to be maximised.

Based on the outcomes of the optimisation program overall tin recovery is estimated at 79.5% at a final concentrate grade of 45% Sn.

14.1 Overall Metallurgical Performance

A series of overall circuit tin balances based on the outcomes of optimisation program are contained in Appendix 14. In these two cases have been considered;

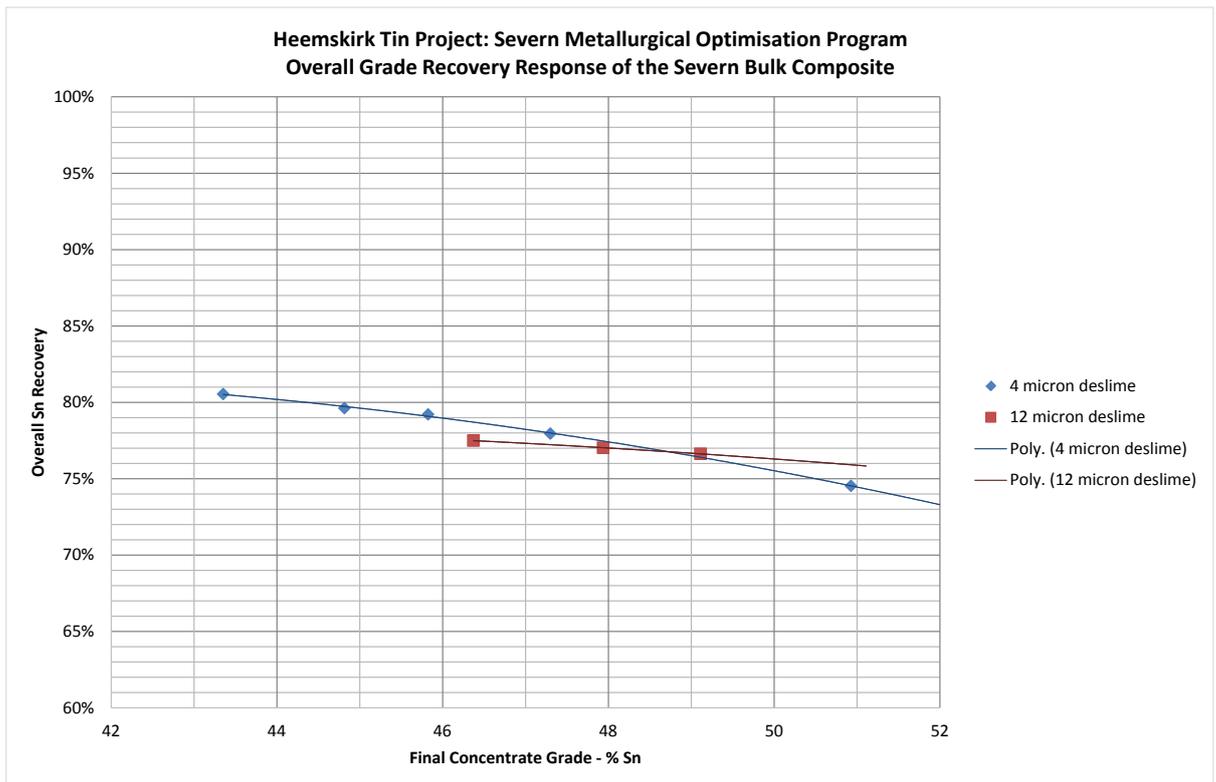
1. 4 µm cut point (D50) in de-slime ahead of tin flotation
2. 12 µm cut point (D50) in de-slime ahead of tin flotation



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

In both cases a variety of tin flotation concentrate grades have been considered to allow the generation of an overall grade recovery response curve across the entire circuit, as shown in Figure 14-1.

Figure 14-1

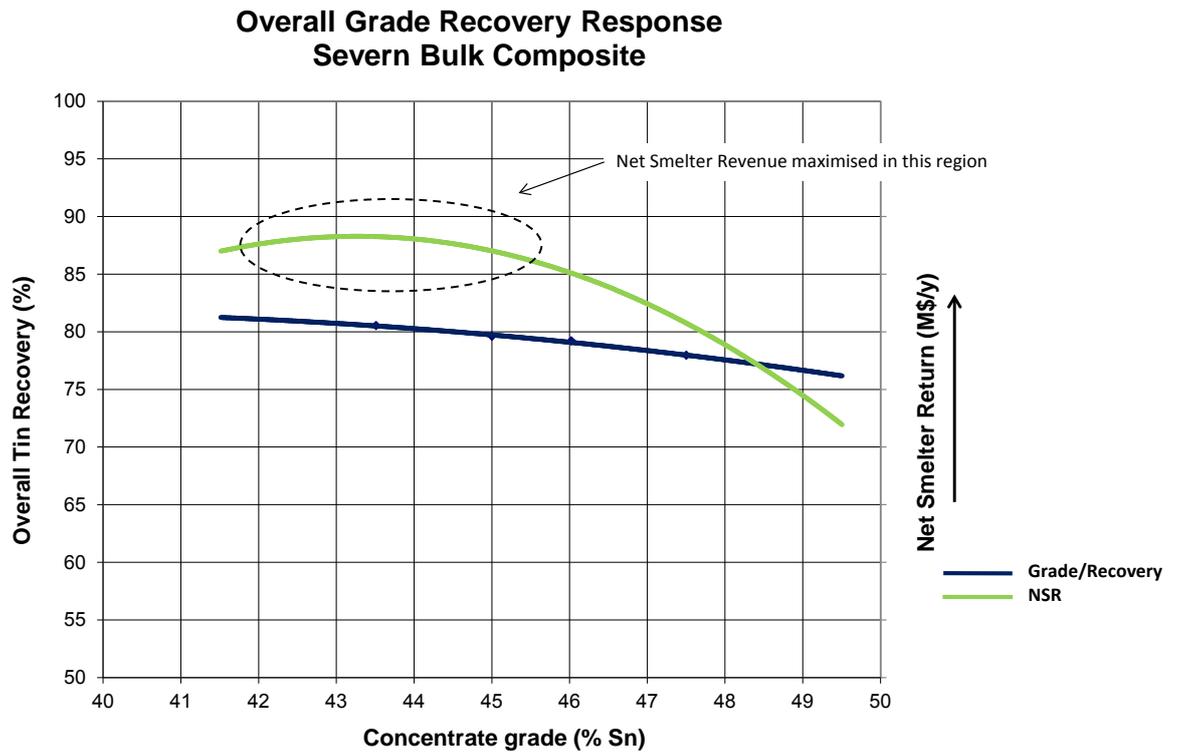


Due to the significantly flatter tin flotation grade recovery response achieved at the coarser de-slime cut point the overall grade recovery response is also relatively flat when compared to the finer cut point. However, at lower concentrate grades, less than ~48% Sn, it is expected de-sliming at the finer size will provide improved overall Sn recovery.



STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Figure 14-2



Net Smelter Return (NSR) analysis based on typical tin concentrate treatment and refining charges and penalty rates, at a range of grade recovery points has shown NSR is maximised at final concentrate tin grades in the low to mid-forties (refer Figure 14-2). As such targeting the finer de-slime size is recommended.

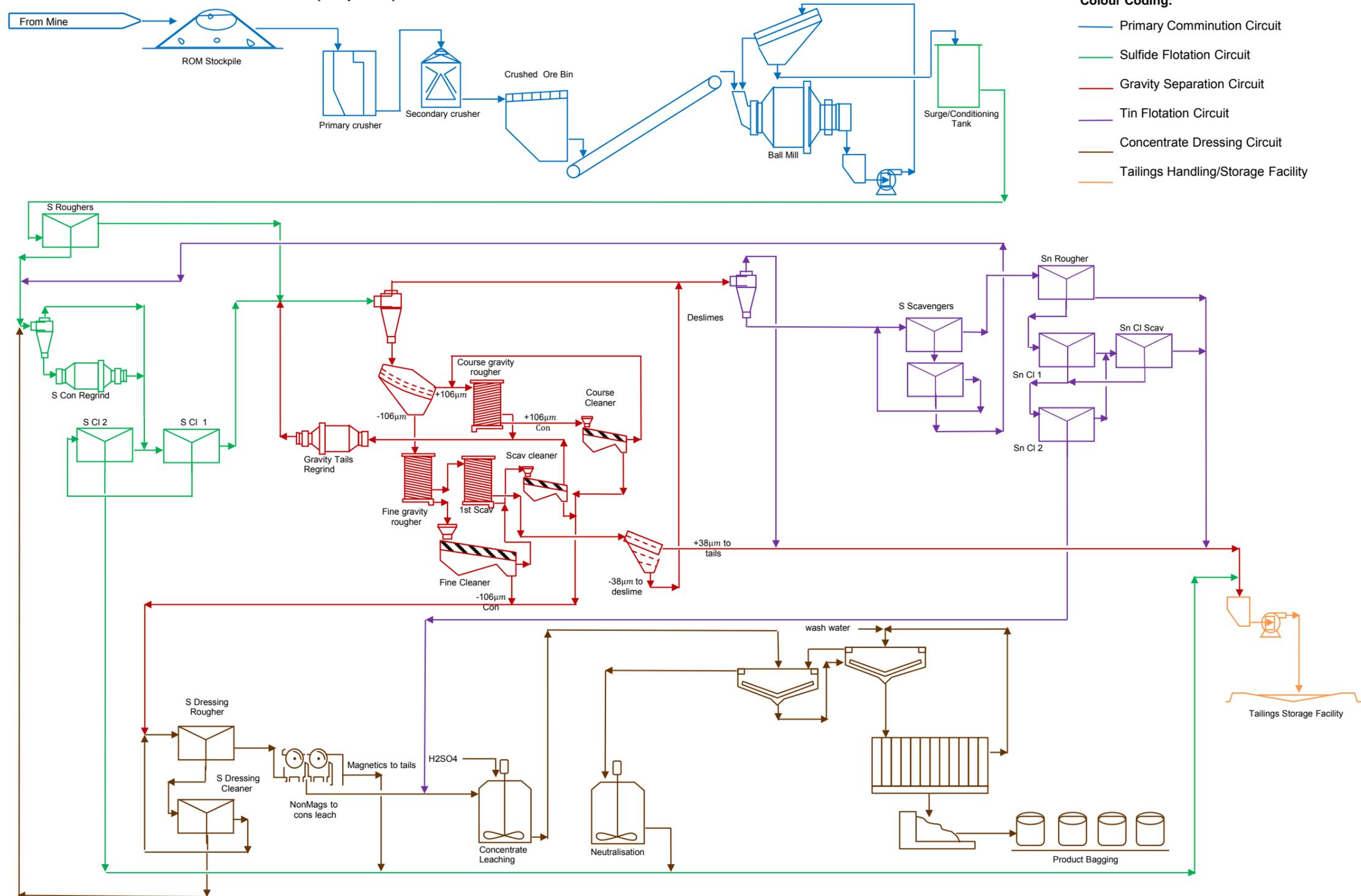


15 PROPOSED PROCESS FLOWSHEET

A simplified version of the optimised process flowsheet which incorporates the various improvements and simplifications arising out of the testwork program is shown in Figure 15-1.



Figure 15-1 OPTIMISED PROCESS FLOWSHEET (simplified)





15.1 Major design criteria

The major recommended process design criteria arising from the overall testwork program are summarised in Table 40.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 40 – Major Design Criteria

Item	Description	Units	Nominal
1.0 Primary Grinding			
	Target Grind Size (P80)	µm	250
2.0 Sulfide Flotation			
	Circuit configuration		Rougher plus R/G plus 2 stage cleaning with open circuit cleaner 1 tails
	Conditioning		
	Number of conditioning stages		1
	Laboratory Conditioning Time (per stage)	minutes	5
	Pulp density	t/m ³	1.33
	% solids	%	36
	Rougher flotation		
	Laboratory Flotation Time	minutes	20
	Feed density	t/m ³	1.33
	% solids	%	36
	Solids SG		3.2
	Regrind		
	Mill type		sand mill
	specific energy input	kWh/t	20
	Target regrind size (P80)	µm	25
	1st Cleaner flotation		
	Cleaner tail destination		final sulfide tails
	Laboratory Flotation Time	minutes	12
	Pulp density	t/m ³	1.20
	% solids	%	22
	Solids SG		4.0
	2nd Cleaner flotation		
	Cleaner tail destination		Regrind feed
	Laboratory Flotation Time	minutes	12
	Pulp density	t/m ³	1.20
	% solids	%	22
	Solids SG		4.2
3.0 Gravity			
	Primary gravity cyclone cut point (D50)		20
	Primary Gravity Screen cut point (D50)		106
	Target regrind size (P80)	µm	52
	Fine Gravity Tails Screen Cut Point (D50)		38-40
	Mass recovery to O/S ("Fine gravity tails")	%	55%
4.0 Gravity Concentrate Dressing			
4.1 Sulfide dressing flotation			
	Circuit configuration		Rougher plus 1 stage closed circuit cleaner
	Conditioning		
	Type		std
	Number of conditioning stages		2
	Laboratory Conditioning Time (per stage)	minutes	2
	% solids	%	30
	Sulfide dressing - Rougher flotation		
	Laboratory Flotation Time	minutes	15
	Feed density	t/m ³	1.30
	% solids	%	30
	Solids SG		4.3
	Sulfide dressing - 1st Cleaner flotation		
	Laboratory Flotation Time	minutes	12.0
	Pulp density	t/m ³	1.18
	% solids	%	20
	Solids SG		4.5
4.2 Dressing Magnetic Separation			
	Circuit configuration		Rougher plus regrind and cleaner
	Mass recovery to mags	%	25%
	Mags regrind mill type		ball
	Target regrind size (P80)	µm	34



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Item	Description	Units	Nominal
5.0 Tin Flotation			
De-slime			
	De-slime cut point (D50)	µm	4
Conditioning			
	Type		HIC
	Number of conditioning stages		2
	Laboratory Conditioning Time (per stage)	minutes	5
	HIC energy	kWh/t	TBC
Sulfide Scavenger - Rougher flotation			
	Laboratory Flotation Time	minutes	7.5
	Feed density	t/m ³	1.35
	% solids	%	38
	Solids SG		3.2
Sulfide Scavenger - 1st Cleaner flotation			
	Cleaner tail destination		sulfide scavenger rougher feed
	Laboratory Flotation Time	minutes	3.0
	Pulp density	t/m ³	1.18
	% solids	%	20
	Solids SG		4.0
	Concentrate destination		sulfide regrind circuit
Sn Rougher flotation			
	Circuit configuration		Rougher plus plus 2 stage cleaning with open circuit cleaner 1 tails
	Laboratory Flotation Time	minutes	18
	Feed density	t/m ³	1.30
	% solids	%	34
	Solids SG		3.2
Cleaner Feed Conditioning			
	Type		HIC
	Number of conditioning stages		2
	Laboratory Conditioning Time (per stage)	minutes	5
	Pulp density	t/m ³	1.1
	% solids	%	13
	Solids SG		3.5
	HIC energy	kWh/t	TBC
Sn 1st Cleaner flotation			
	Laboratory Flotation Time	minutes	8
	Pulp density	t/m ³	1.10
	% solids	%	13
	Solids SG		3.5
Sn 2nd Cleaner flotation			
	Laboratory Flotation Time	minutes	8
	Pulp density	t/m ³	1.10
	% solids	%	13
	Solids SG		3.5
6.0 Concentrate leach			
	Leach temperature	°C	90
	Pulp density	t/m ³	1.93
	% solids	%	60
	Solids SG		5.0
	retention time	h	8.0

15.2 Key changes from PFS Process Flowsheet

Key changes to the process flowsheet arising out of the optimisation program compared to the PFS flowsheet are summarised below:

- Elimination of the heavy media separation circuit
- Coarser primary grind; grind size optimization testwork has demonstrated a significantly coarser primary grind size is more optimum than that considered in the PFS.
- Finer Sulfide regrind, utilising sand milling rather than ball milling has led to a significant reduction in tin losses to the final sulfide concentrate tailings stream.



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

- Optimisation of the gravity circuit configuration, combine with upstream flowsheet improvements, has led to ~10% improvement in tin recovery via gravity.
- Introduction of a magnetic separation in the gravity concentrate dressing circuit
- Elimination of the silica flotation circuit
- High intensity conditioning (HIC) in tin flotation; both of sulfide scavenger feed and rougher concentrate
- Leaching of combine gravity and flotation concentrates

Table 41 shows a comparison of the tin deportment across the circuit assumed in the PFS and the Severn Optimisation Program Outcomes.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Table 41 – Comparison of Tin Department Assumed in PFS and Severn Optimisation Program Outcomes

Process Product and Tail		Assumed PFS Performance	Severn Optimisation program Outcome	Change from PFS Performance
Ore Grade	% Sn	1.06	1.00	0.06
1. Ore Feed (product)	% Sn	100	100	0.0
2. HMS Floats (tail)	% Sn	-1.5	0	1.5
3. Final Sulfide Conc (tail)	% Sn	-10.1	-2.6	7.5
Sn Recovery to Gravity Circuit Feed (product)	% Sn	88.4	97.4	9.0
4. Gravity Conc (product)	% Sn	63.9	69.1	5.2
5. Gravity Tail	% Sn	-2.6	-3.8	-1.2
6. Slime Tail	% Sn	-1.3	-3.7	-2.4
7. Tin Flotation Conc (product)	% Sn	8.5	10.4	1.9
8. Tin Flotation Tail	% Sn	-12.1	-10.2	1.9
9. Overall Recovery (product)	% Sn	72.4	79.5	7.1
10. Overall Loss (tail)	% Sn	-27.6	-20.4	7.2
Final Tin Concentrate Grade	% Sn	50.8	45.0	5.8

Notably significant reduction in tin losses to the HMS Floats, Final Sulfide Concentrate and Tin Flotation Tailings streams have been achieved. In particular the reduction in losses ahead of the primary tin recovery circuits (gravity and tin flotation), via HMS Floats and Final Sulfide Concentrate have improved tin recovery into the feed of these, with tin department to gravity circuit feed now at 97.4%, up 9% from the PFS.

Tin recovery into both gravity and tin flotation concentrates has also improved to give an overall recovery of 79.5%, an improvement of 7.1% compared to the PFS performance.

Final concentrate grade is slightly reduced compared to the PFS. However, this is more than offset by the increase in overall recovery, resulting in a significant increase in net smelter return compared to the PFS.



**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

16 RECOMMENDED FURTHER WORK

The current metallurgical testing program has focused on the Severn deposit which forms approximately 60% of the overall tin resource for the Heemskirk Tin Project. As yet, the same rigorous approach to metallurgical testing and optimisation has not been applied to the Upper Queen Hill, Lower Queen Hill and Montana deposits due to limited availability of suitable samples. However, it is expected that many of the learnings and process improvements from the Severn program will be translatable to these deposits, particularly improvements achieved with respect primary grinding, sulfide flotation, gravity and dressing circuit configuration, and tin flotation.

In outline the recommended further work with respect to the metallurgical development of the project include:

1. Testing of the other major ore sources

Detailed testing building on the learnings from Severn of the other major ore sources including the Upper Queen Hill, Lower Queen Hill and Montana deposits is planned to be under taken once sample availability permits.

2. Pilot testing, larger scale batch testing and other testwork necessary to support the DFS

In addition to further definition of process design criteria and variability testing this will need to include some larger scale testing such as piloting and/or large scale batch testing, vendor testing for equipment sizing purposes, and potentially generation of larger sample quantities for work such as tailings characterisation, production of concentrate samples, etc.

3. Further variability testing (to be completed as part of DFS)

Ore variability testing will be required on all major ore types, and on the various blends reflecting mining schedule and treatment ratios.

16.1 Specific issues requiring further definition

Gravity Separation:

- Larger scale testing utilising spirals and industrial type tables is strongly recommended to better define the optimum circuit configuration and confirm achievable performance.

Tin Flotation:

- Further optimisation of de-slime cut point

It is expected de-slime cut point can be increased somewhat (to around 6 μm) from nominally 4 μm without detrimental impact on the overall recovery. This would have advantages in terms of reducing tin flotation feed tonnage and hence reagent consumption (particularly SPA).



STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

- The requirement for “water change” (impact of solution chemistry) following high intensity conditioning ahead of sulfide scavenger flotation needs further investigation to determine if this can be successfully eliminated/solution chemistry issues mitigated by other means (eg. increased SSF dose).
- Energy input requirements for high intensity conditioning stages in tin flotation

The small scale of the tin flotation tests completed made meaningful measurement of specific energy input impractical.
- Lock cycle testing to better estimate achievable closed circuit performance.



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 1 – Sample Details

South

North

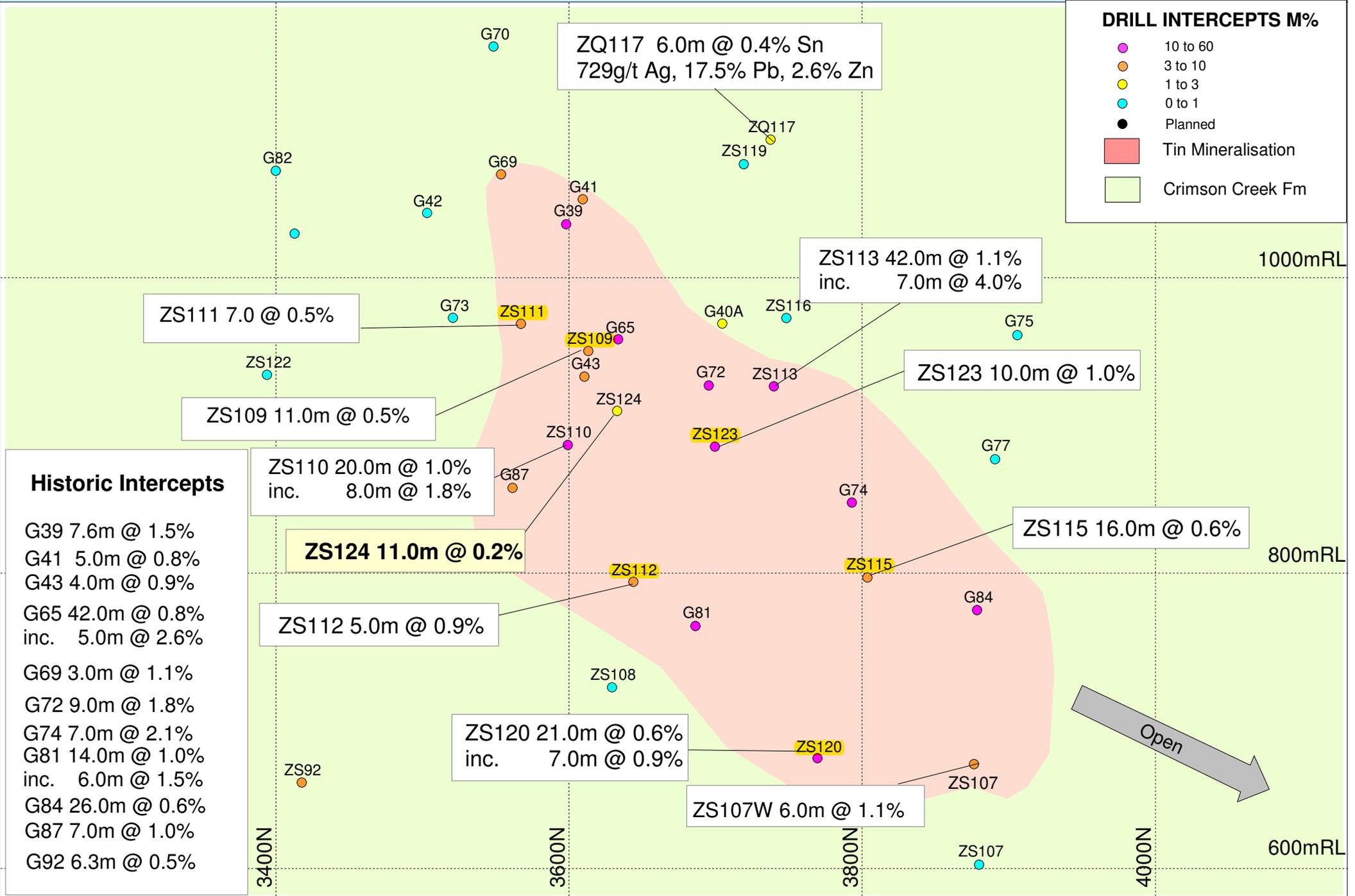
1180m RL Surface

DRILL INTERCEPTS M%

- 10 to 60
- 3 to 10
- 1 to 3
- 0 to 1
- Planned

■ Tin Mineralisation

■ Crimson Creek Fm



Historic Intercepts

- G39 7.6m @ 1.5%
- G41 5.0m @ 0.8%
- G43 4.0m @ 0.9%
- G65 42.0m @ 0.8% inc. 5.0m @ 2.6%
- G69 3.0m @ 1.1%
- G72 9.0m @ 1.8%
- G74 7.0m @ 2.1%
- G81 14.0m @ 1.0% inc. 6.0m @ 1.5%
- G84 26.0m @ 0.6%
- G87 7.0m @ 1.0%
- G92 6.3m @ 0.5%

1000mRL

800mRL

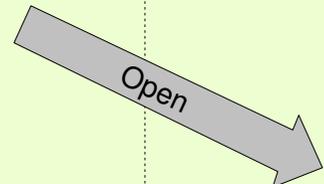
600mRL

3400N

3600N

3800N

4000N





WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 2 – Mineralogy

ALS Metallurgy

STELLAR RESOURCES LTD
Heemskirk Tin Project

Severn Bulk Composite
Testwork Mineralogy

JUNE 2014

MODA
microscopy

McArthur Ore Deposit Assessments Pty Ltd

Gary J McArthur PhD FAusIMM MMICA MSEG

Suite 6, 1st Floor, Brownell Place, 11 Wilson St (P.O. Box 1303) Burnie TAS 7320 AUSTRALIA
Tel (03) 6431 1701 Fax (03) 6431 1278 Mobile 0419 367240 email gary@modapl.com.au

ALS METALLURGY

Stellar Resources – Severn Bulk Composite Mineralogy June 2014

Method

A drillcore Bulk Composite sample from Stellar Resources' Severn Prospect was submitted for mineralogical assessment. The sample was sized into 8 fractions: +212µm, +150µm, +106µm, +75µm, +53µm, +38µm, +20µm, and +8µm) and these were mounted on three polished mounts by Australian Petrographics (Queanbeyan, NSW).

The standard MODA technique was adopted to quantify the mineralogy, using four scans.

In a first scan, for each fraction, 100 grains were selected at random and the area % of each mineral present was visually estimated. The minerals logged were: *pyrite+marcasite* (Py), *pyrrhotite* (Po), *cassiterite* (Cs), *stannite* (St), *arsenopyrite* (As), *chalcopyrite* (Cp), *sphalerite+galena* (SpGn) and *gangue* (*quartz, silicates, carbonates, etc, Ga*). This allowed calculation of an overall mineralogical composition.

In a second scan, for each fraction, 100 grains containing *pyrite* or *pyrrhotite* were selected at random and logged as per the first scan. This improved the count statistics for the Fe sulphides.

In a third scan, for each fraction, 100 grains containing *cassiterite* or *stannite* were selected at random and logged as per the first scan. This improved the count statistics for the Sn mineralisation.

In a fourth scan, for each fraction, 100 grains containing *sphalerite, galena, chalcopyrite, stannite* or *tetrahedrite* were selected at random and logged as per the first scan. This improved the count statistics for miscellaneous base metal mineralisation.

The normal liberation and association parameters were calculated.

Photomicrographs were taken of each size fraction and these were annotated using PowerPoint.

Results

Composition

The following minerals were identified, in approximate descending order:

- Gangue (*quartz, silicates, carbonate, rutile, carbonaceous matter, fluorite, talc* etc.)
- *Pyrite* (95.4% crystalline and 4.6% *melnikovite*)
- *Pyrrhotite*
- *Magnetite*
- *Sphalerite*
- *Cassiterite*
- *Marcasite*
- *Galena*
- *Arsenopyrite*
- *Chalcopyrite*
- *Goethite*
- *Hematite*
- *Stannite* (rare)
- *Tetrahedrite* (very rare)
- *Bismuthinite* (very rare)
- *Native bismuth* (very rare)

The overall composition of the Bulk Composite is summarised below:

Severn Bulk Comp Composition Vol% (from total scan)

Fraction	Wt%	Py	Po	Cs [#]	St [#]	As [#]	Cp [#]	SpGn	Ga
+212µm	12.2	11.7	0.2	0.4	0.0	0.0	0.1	0.8	86.9
+150µm	9.5	22.9	1.7	0.2	0.0	0.1	0.0	1.4	73.8
+106µm	11.6	23.0	4.6	0.2	0.0	1.0	0.0	1.1	70.1
+75µm	9.9	31.4	1.2	1.0	0.0	0.1	Tr	0.0	66.3
+53µm	9.9	26.3	3.5	1.2	1.0	0.0	0.1	2.1	66.0
+38µm	7.5	26.6	9.5	0.5	0.0	0.0	0.2	2.1	61.1
+20µm	9.0	29.9	6.2	1.3	0.0	0.0	0.2	4.0	58.4
+8µm	10.6	28.3	6.7	2.0	0.0	0.0	0.0	3.0	60.1
TOTAL	80.2	24.5	3.9	0.8	0.1	0.2	0.1	1.7	68.6

Py=pyrite, Po=pyrrhotite, Cs=cassiterite, St=stannite, As=arsenopyrite, Cp=chalcopyrite, SpGn=sphalerite+galena, Ga=gangue
 # count statistics are very poor for the scarce minerals

The composition of the grains containing *pyrite* and *pyrrhotite* is summarised below:

Severn Bulk Comp Composition Vol% (from PyPo scan)

Fraction	Fe Wt%	Py	Po	Cs	St	As	Cp	SpGn	Ga
+212µm	5.1	41.4	3.8	0.3	0	0.6	Tr	0.4	53.6
+150µm	9.6	53.0	4.9	1.2	Tr	0.1	Tr	1.3	39.6
+106µm	9.4	59.4	8.2	0.5	0	0	Tr	1.0	30.9
+75µm	12.3	63.7	7.2	0	Tr	0.1	Tr	1.3	27.7
+53µm	10.8	75.7	10.5	0.4	0	0	0.2	0.1	13.2
+38µm	11.0	74.4	16.6	0.5	0	0	0.2	0	8.4
+20µm	8.5	73.9	15.7	0.1	0	0	0.7	0.1	9.6
+8µm	10.2	73.1	20.6	0	0	0	0	0	6.4
TOTAL	76.9	65.9	11.3	0.4	Tr	0.1	0.1	0.5	21.7

The composition of the grains containing *cassiterite* and *stannite* is summarised below. Note the residence of Sn sums to 99% in *cassiterite* and 1% in *stannite*.

Severn Bulk Comp Composition Vol% (from Sn scan)

Fraction	Sn Wt%	Py	Po	Cs	St	As	Cp	SpGn	Ga
+212µm	6.2	15.6	4.2	12.9	0.4	0	0.1	0.1	66.8
+150µm	8.0	19.6	2.2	23.8	0.1	0.9	0.1	0	53.4
+106µm	8.2	11.0	4.9	32.2	2.6	0	0.7	2.0	46.7
+75µm	11.6	6.1	1.6	43.2	1.8	0	1.1	0.7	45.6
+53µm	11.1	10.0	1.6	44.1	4.2	0	0.8	2.2	37.2
+38µm	12.7	3.8	3.1	64.8	4.2	Tr	0.8	1.6	21.8
+20µm	10.1	4.1	0.1	82.0	1.3	0	0.1	0.1	12.5
+8µm	12.6	1.8	0.4	87.8	2.1	0	0.4	0	7.6
TOTAL	80.5	7.9	2.1	53.2	2.3	0.1	0.6	0.9	33.1

The composition of the grains containing *sphalerite*, *galena*, *chalcopyrite*, *stannite* and *tetrahedrite* is summarised below:

Severn Bulk Comp Composition Vol% (from SpGnCpStTe scan)

Fraction	Wt%	Py	Po	As	Sp	Gn	Cp	St	Te	Cs	Mt	He	Go	Ga
+212µm	12.2	15.9	2.0	0.2	11.8	1.4	2.1	0.2	0	0.5	0.1	0	0	65.9
+150µm	9.5	18.5	Tr	0.1	23.1	5.6	2.5	0.1	0	1.7	Tr	0	0	48.4
+106µm	11.6	14.8	Tr	0.3	35.4	4.7	1.7	0.4	0	0	0	0	0	42.9
+75µm	9.9	15.7	Tr	1.9	33.6	8.9	2.5	0.2	0	1.8	0	0	0	35.4
+53µm	9.9	10.1	0.9	0	40.9	6.6	5.8	0.2	0	0.2	0	0	0	35.3
+38µm	7.5	6.0	0.2	1.5	58.0	15.6	2.6	0.1	0.1	0.8	0	0	0	15.2
+20µm	9.0	3.5	0	0.9	46.7	29.5	9.0	0.4	0	0.4	0	0	0	9.7
+8µm	10.6	1.4	0	0	56.5	33.2	3.0	0	0	0	0	0	0	6.0
TOTAL	80.2	11.1	0.4	0.6	37.0	12.6	3.5	0.2	Tr	0.6	Tr	0	0	34.0

From the scan above, the estimated base metal head grades for the Severn Bulk Composite are 0.9%Zn and 0.6%Pb.

Liberation and Association

Essential summaries of the liberation parameters for the main economic phases are:

Severn Bulk Comp Cassiterite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary+
			Py	Po	St	Cp	As	Ga	
+212µm	6.2	0	1	1	0	0	0	71	26
+150µm	8.0	17	9	0	0	0	0	41	32
+106µm	8.2	28	8	0	0	0	0	45	17
+75µm	11.6	46	2	0	0	0	0	41	11
+53µm	11.1	59	3	0	0	0	0	36	2
+38µm	12.7	66	2	1	0	1	0	25	4
+20µm	10.1	72	0	1	0	1	0	21	3
+8µm	12.6	83	1	1	0	1	0	14	0
TOTAL	80.5	52	3	1	0	0	0	34	10

Severn Bulk Comp *Cassiterite* association%

Fraction	Sn Wt%	%associated with					
		Py	Po	St	Cp	As	Ga
+212µm	6.2	21	9	2	5	0	94
+150µm	8.0	36	6	0	2	0	73
+106µm	8.2	21	4	0	0	0	62
+75µm	11.6	7	3	5	5	0	50
+53µm	11.1	5	0	0	1	0	38
+38µm	12.7	4	2	0	1	0	28
+20µm	10.1	2	1	0	2	0	24
+8µm	12.6	1	1	0	1	0	14
TOTAL	80.5	10	3	1	2	0	43

Severn Bulk Comp *Stannite* liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary
			Py	Po	Cs	Cp	As	Ga	
+212µm	6.2	0	0	0	0	0	0	0	100
+150µm	8.0	0	0	0	0	0	0	0	100
+106µm	8.2	39	0	0	0	29	0	14	18
+75µm	11.6	57	0	0	0	6	0	0	37
+53µm	11.1	24	0	0	0	22	0	1	42
+38µm	12.7	24	0	0	0	68	0	0	3
+20µm	10.1	0	4	0	0	0	0	86	10
+8µm	12.6	98	2	0	0	0	0	0	0
TOTAL	80.5	35	1	0	0	18	0	12	32

Severn Bulk Comp *Stannite* association%

Fraction	Sn Wt%	%associated with					
		Py	Po	Cs	Cp	As	Ga
+212µm	6.2	0	100	97	97	0	3
+150µm	8.0	0	0	100	62	0	100
+106µm	8.2	0	0	0	46	0	32
+75µm	11.6	11	0	12	41	0	26
+53µm	11.1	2	2	12	61	0	28
+38µm	12.7	0	0	0	70	0	3
+20µm	10.1	4	0	10	0	0	96
+8µm	12.6	2	0	0	0	0	0
TOTAL	80.5	3	8	22	44	0	34

Stannite is a rare fine-grained component, mainly hosted by *chalcopyrite*, but also *sphalerite*, *galena*, *pyrite*, *cassiterite* and gangue.

The miscellaneous base metal sulphides (*sphalerite*, *galena* and *chalcopyrite*) are common throughout, but more so in the finer fractions. *Galena* has the highest measured liberation. *Tetrahedrite* was seen only rarely, always with *galena*. *Bismuthinite* and *native bismuth* were very rare, mostly hosted by *chalcopyrite*.

Severn Bulk Comp *Sphalerite* liberation distribution%

Fraction	Wt%#	Free	Binary	Ternary	Quat.y+	%associated with							
						Py	Po	As	Gn	Cp	St	Cs	Ga
+212µm	12.2	0	25	46	29	42	8	3	46	22	0	0	83
+150µm	9.5	26	34	31	9	20	0	5	35	13	0	4	47
+106µm	11.6	25	42	25	8	30	0	0	32	18	1	0	36
+75µm	9.9	54	16	26	4	10	0	2	22	21	0	0	26
+53µm	9.9	42	35	18	5	17	10	0	18	20	1	1	21
+38µm	7.5	52	43	5	0	7	0	0	15	25	0	0	6
+20µm	9.0	60	39	1	0	0	0	0	20	17	0	0	3
+8µm	10.6	76	22	2	0	0	0	0	8	12	0	0	6
TOTAL	80.2	40	32	21	8	17	2	1	25	18	0	1	31

Zn assays were not provided, so total weight% is used

Sphalerite often exhibits “*chalcopyrite* disease”, as evidenced by the high *sphalerite-chalcopyrite* association. The *sphalerite* is quite dark, suggesting a moderate-Fe variety.

Severn Bulk Comp *Galena* liberation distribution%

Fraction	Wt%#	Free	Binary	Ternary	Quat.y+	%associated with							
						Py	Po	As	Sp	Cp	St	Cs	Ga
+212µm	12.2	0	25	33	42	50	4	1	56	8	5	0	94
+150µm	9.5	36	25	23	17	23	0	0	43	1	0	2	52
+106µm	11.6	21	40	24	15	28	0	4	42	4	0	0	53
+75µm	9.9	56	26	17	0	17	0	0	22	4	0	1	16
+53µm	9.9	60	33	6	1	7	0	0	11	0	0	0	28
+38µm	7.5	90	10	1	0	2	0	0	6	0	0	1	2
+20µm	9.0	88	8	4	0	2	0	0	4	0	0	5	4
+8µm	10.6	96	3	0	0	2	0	0	2	0	0	0	0
TOTAL	80.2	53	22	15	11	18	1	1	25	2	1	1	34

Pb assays were not provided, so total weight% is used

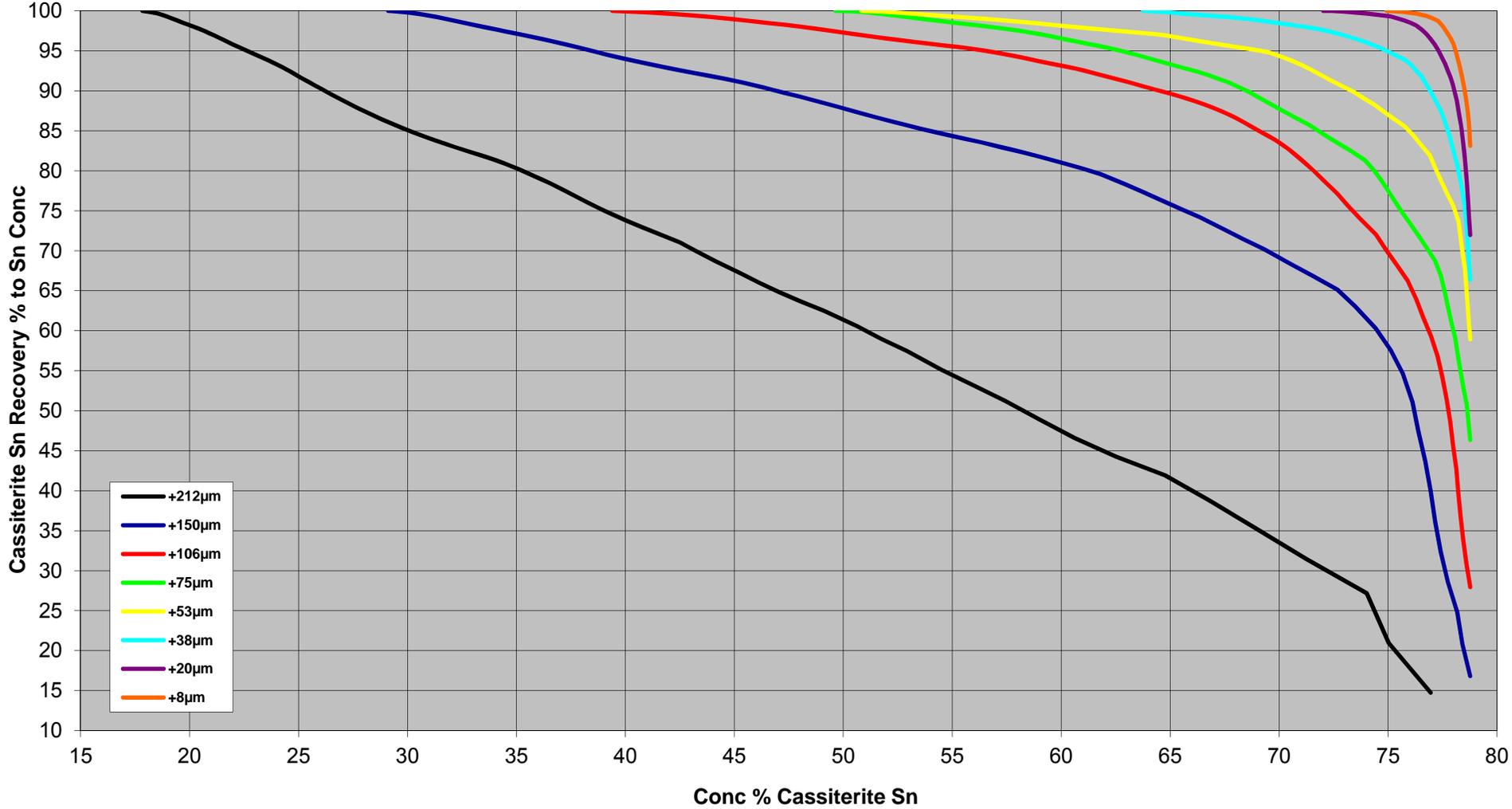
Galena is more liberated than *sphalerite*, but also occurs interstitial to *pyrite*, or as fine-grained blebs in *sphalerite* and carbonate gangue.

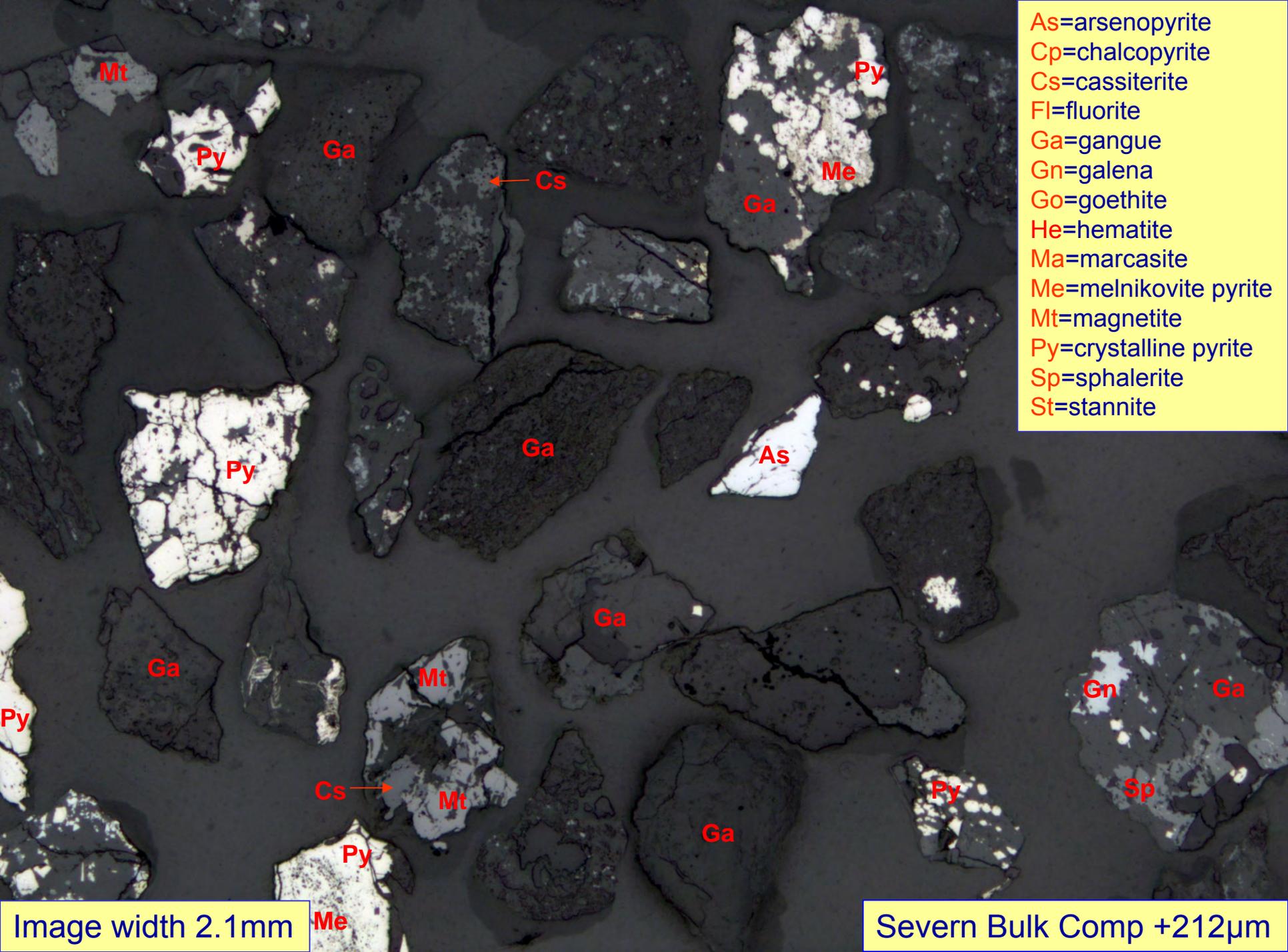
Severn Bulk Comp *Chalcopyrite* liberation distribution%

Fraction	Wt%#	Free	Binary	Ternary	Quat.y+	%associated with							
						Py	Po	As	Sp	Gn	St	Cs	Ga
+212µm	12.2	0	46	36	18	30	11	1	7	3	8	9	99
+150µm	9.5	0	39	56	4	44	2	0	2	10	6	2	98
+106µm	11.6	0	65	29	6	44	2	0	10	8	5	0	74
+75µm	9.9	40	36	8	16	12	0	6	4	2	13	15	47
+53µm	9.9	34	44	19	3	18	1	0	6	2	9	3	53
+38µm	7.5	38	49	11	2	2	4	39	11	0	2	0	18
+20µm	9.0	78	22	0	0	4	0	0	1	0	0	0	17
+8µm	10.6	66	33	0	0	0	0	0	6	0	0	0	28
TOTAL	80.2	30	42	21	7	20	3	5	6	3	6	4	57

Cu assays were not provided, so total weight% is used

Severn Bulk Composite - Cumulative Yield Curves





- As=arsenopyrite
- Cp=chalcopyrite
- Cs=cassiterite
- Fl=fluorite
- Ga=gangue
- Gn=galena
- Go=goethite
- He=hematite
- Ma=marcasite
- Me=melnikovite pyrite
- Mt=magnetite
- Py=crystalline pyrite
- Sp=sphalerite
- St=stannite

Image width 2.1mm

Severn Bulk Comp +212µm

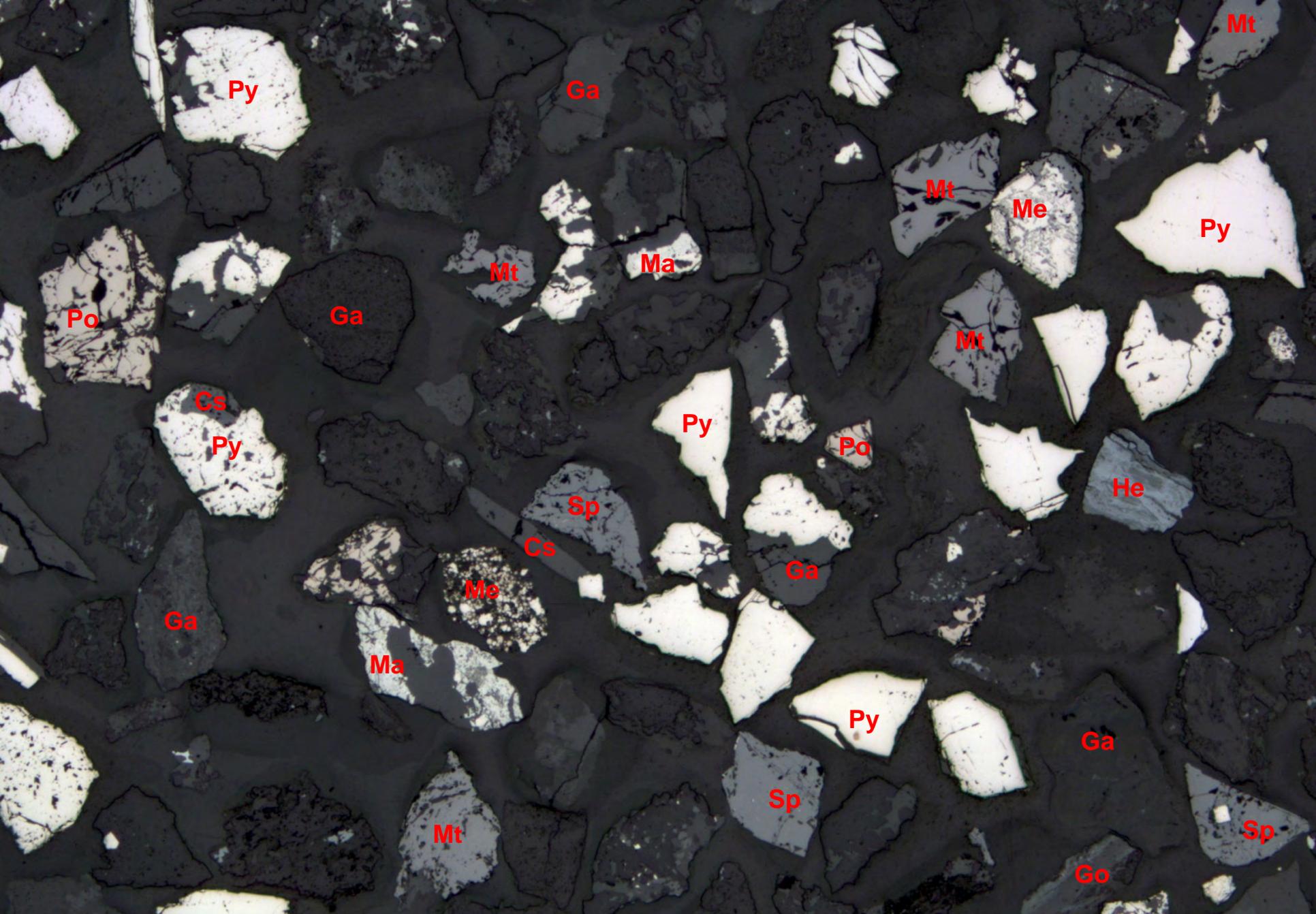
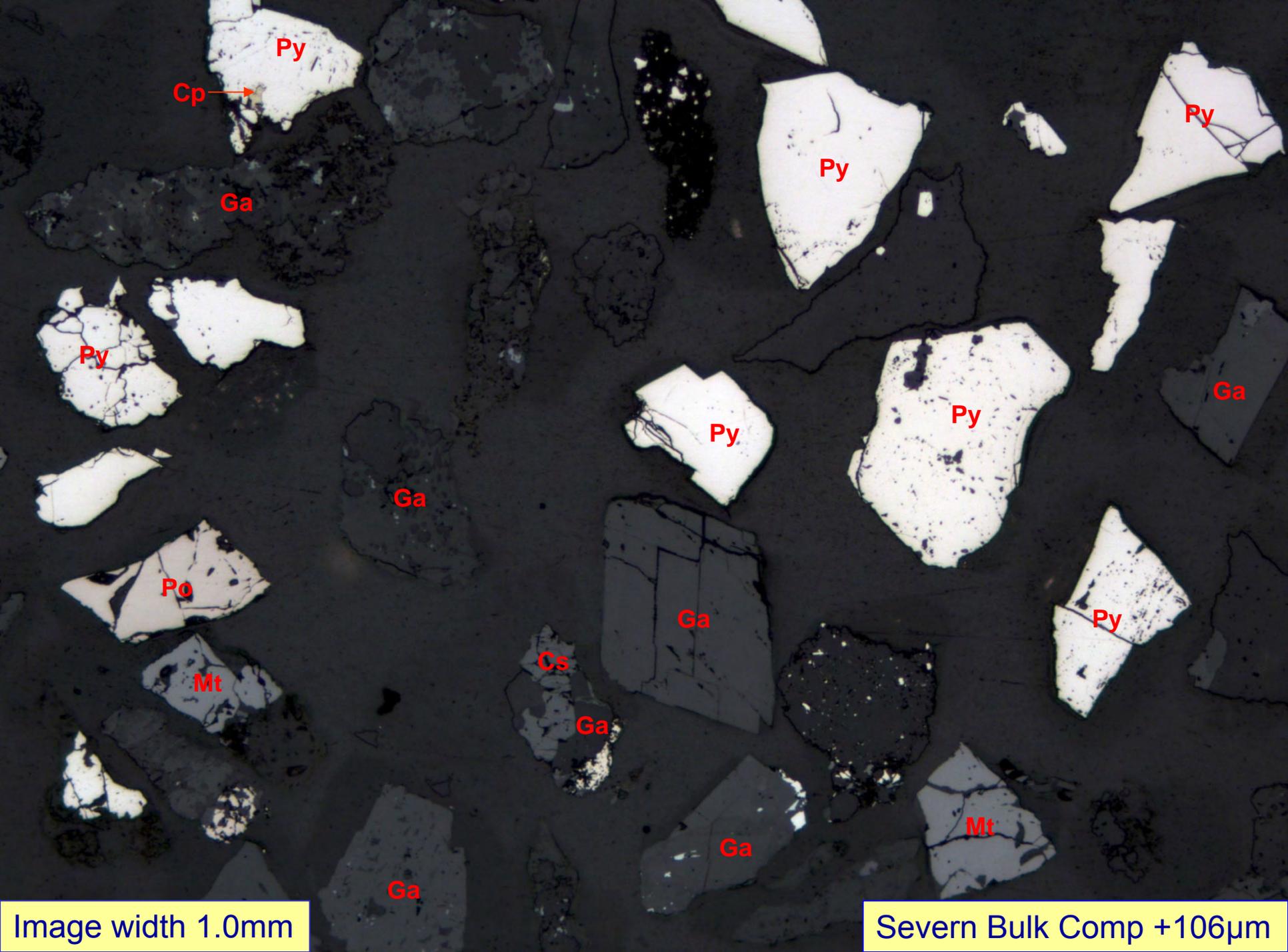


Image width 2.1mm

Severn Bulk Comp +150µm



Cp

Py

Ga

Py

Py

Py

Ga

Py

Py

Ga

Po

Ga

Py

Mt

Cs

Ga

Ga

Mt

Ga

Image width 1.0mm

Severn Bulk Comp +106µm

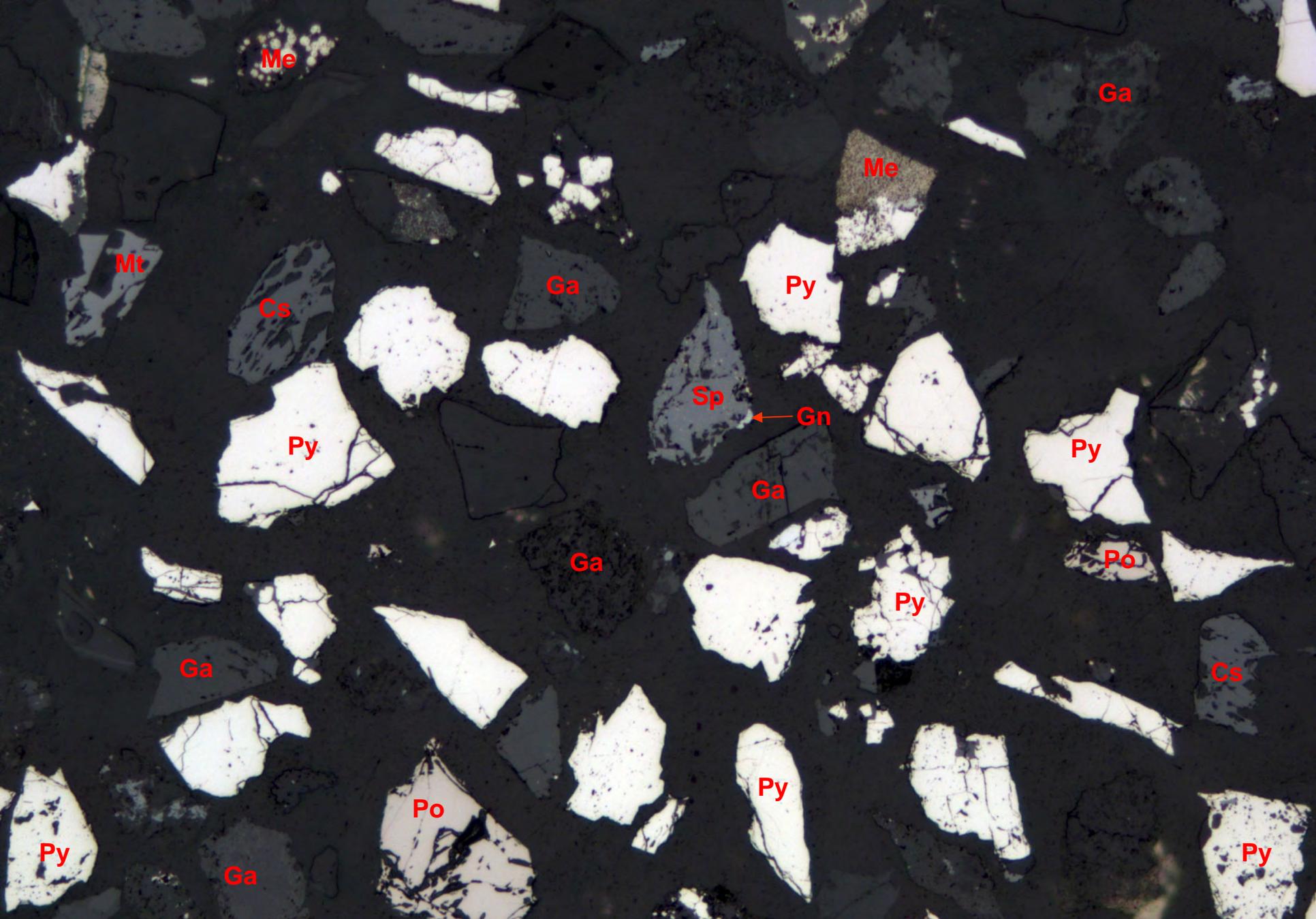
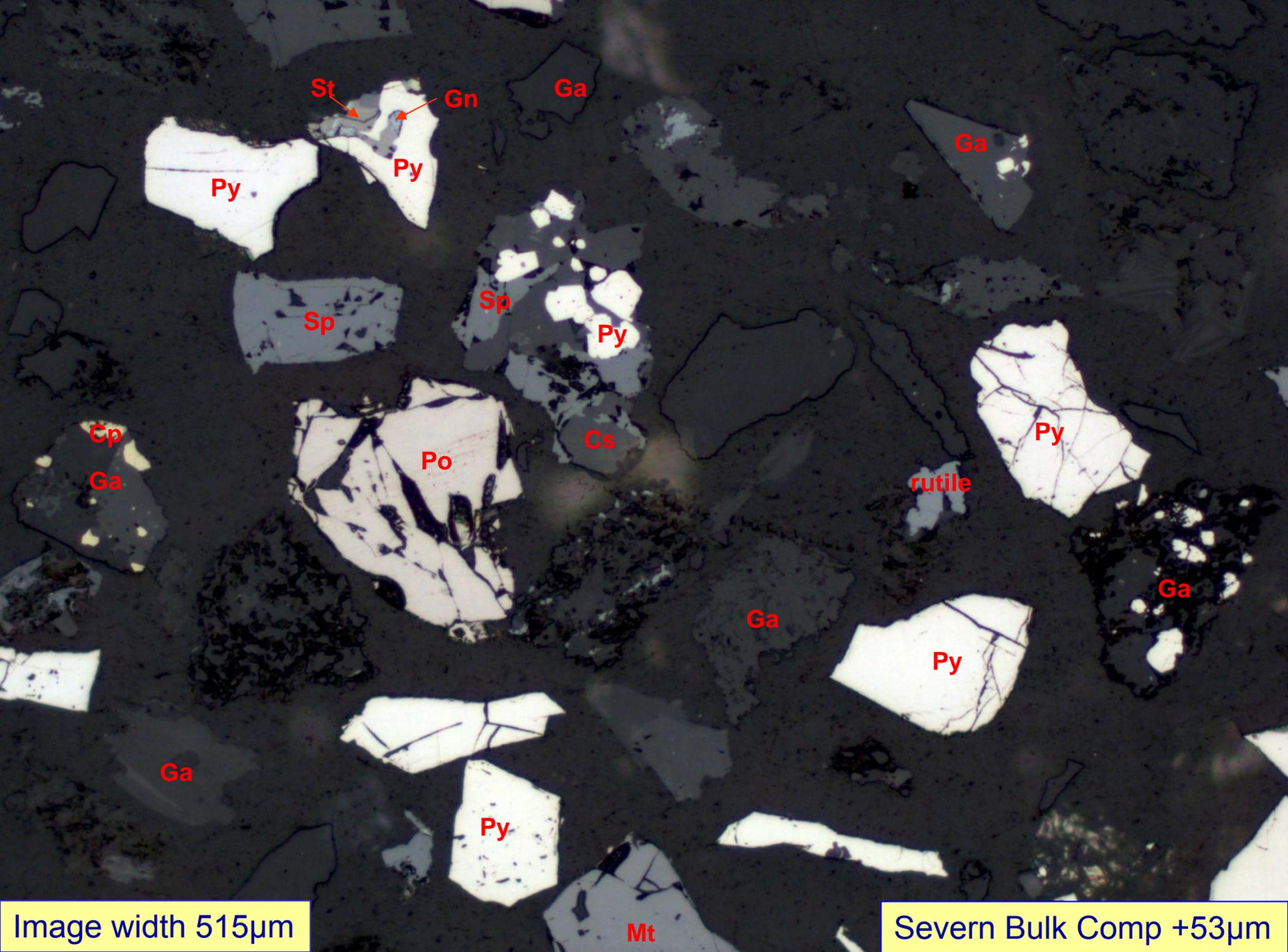


Image width 1.0mm

Poor polish

Severn Bulk Comp +75µm



St

Gn

Ga

Ga

Py

Py

Sp

Sp

Py

Cp

Ga

Po

Cs

Py

rutile

Ga

Ga

Py

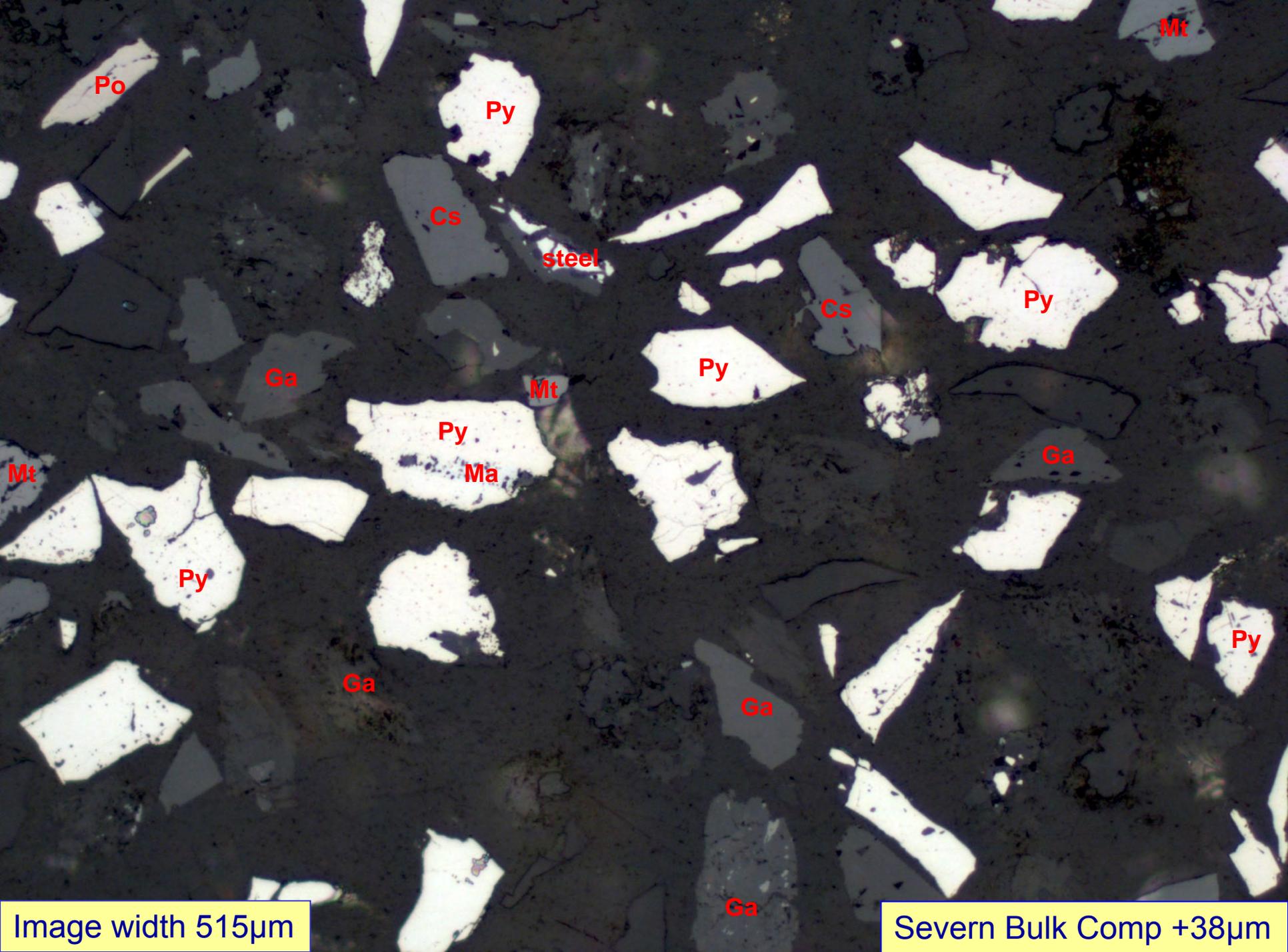
Ga

Py

Mt

Image width 515µm

Severn Bulk Comp +53µm



Po

Py

Cs

steel

Cs

Py

Ga

Py

Mt

Py

Ma

Ga

Py

Py

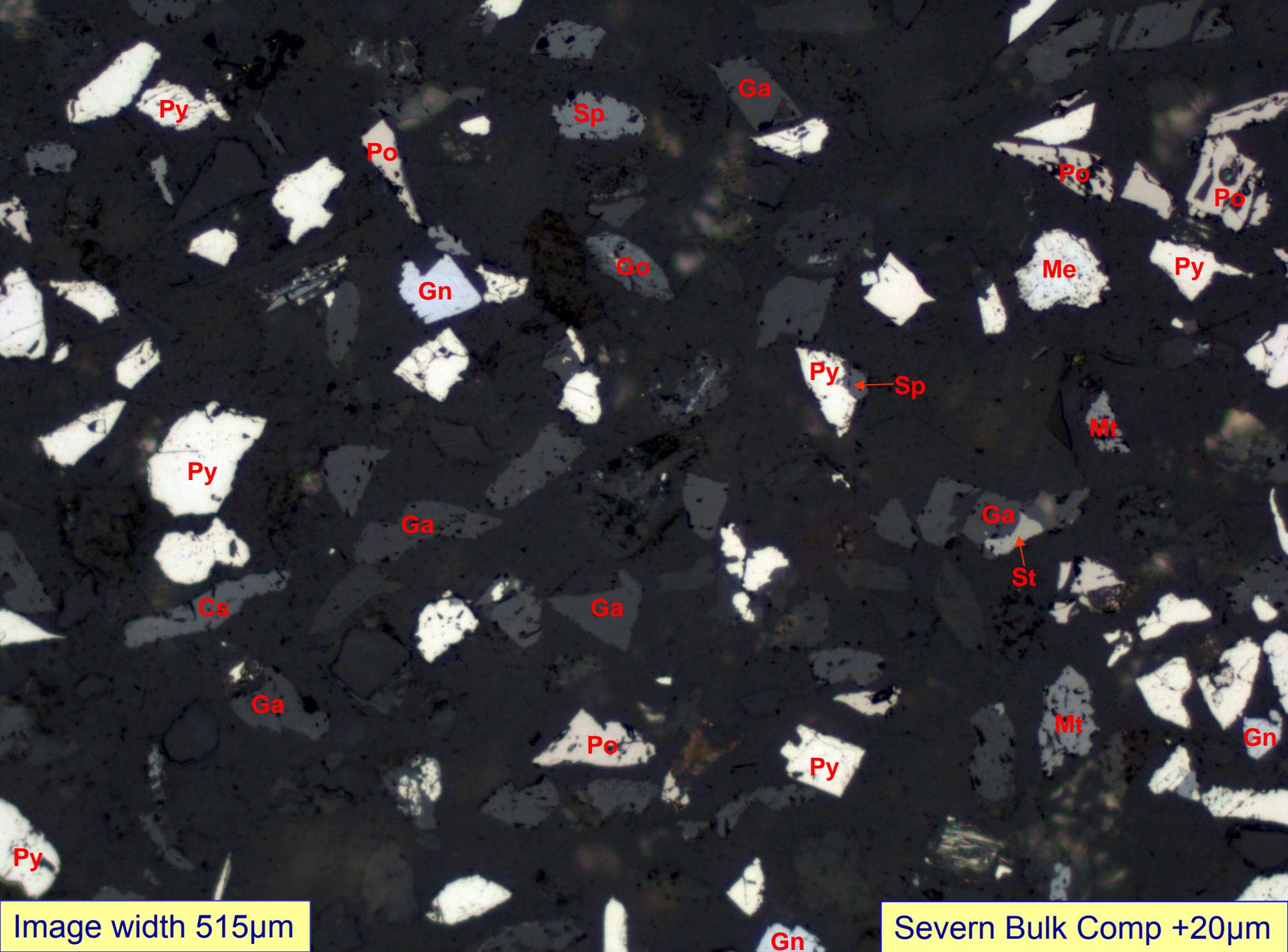
Ga

Ga

Ga

Image width 515µm

Severn Bulk Comp +38µm



Py

Po

Sp

Ga

Po

Po

Gn

Go

Me

Py

Py

Sp

Mt

Py

Ga

Ga

St

Cs

Ga

Ga

Po

Py

Mt

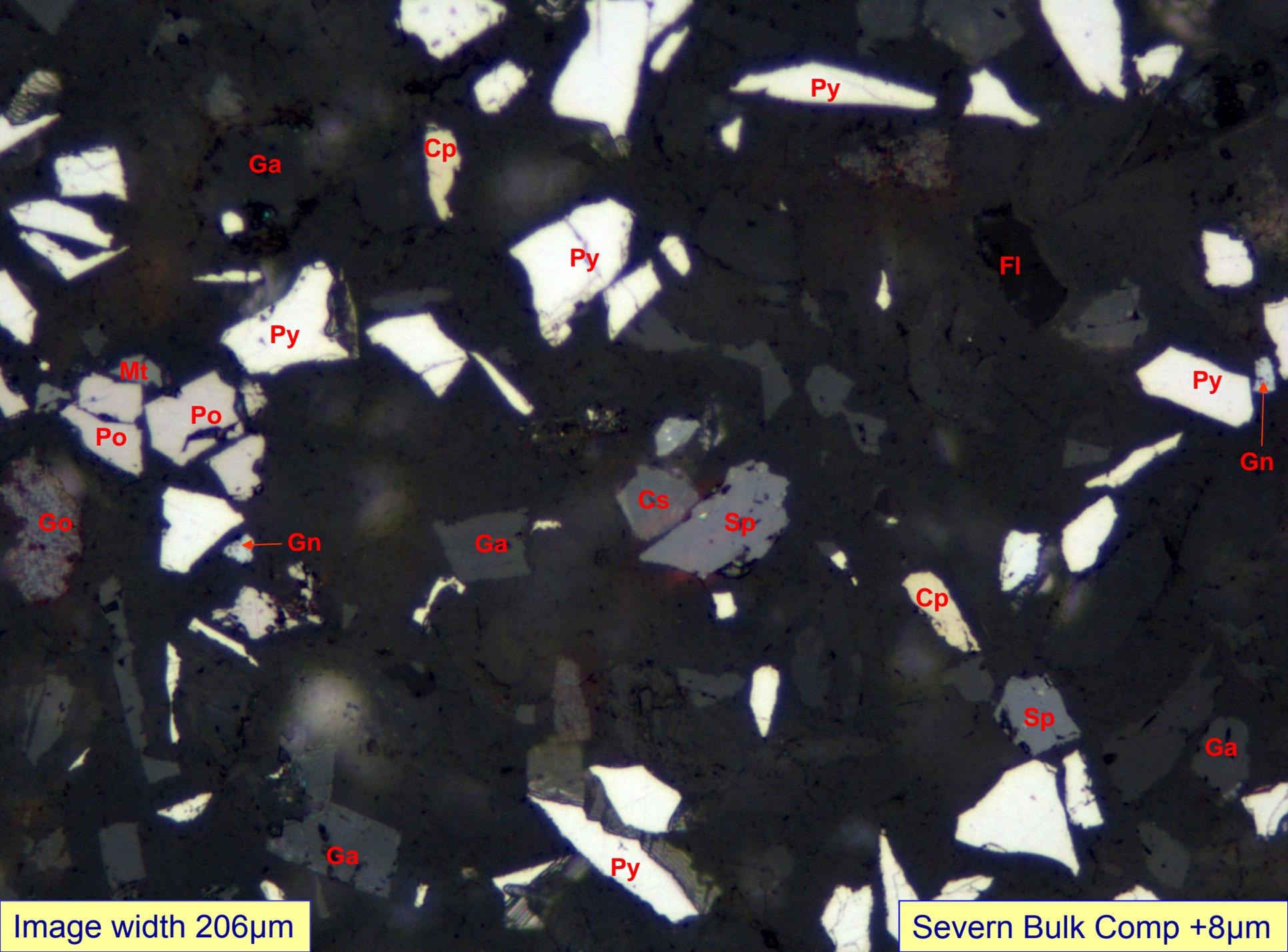
Gn

Py

Gn

Image width 515µm

Severn Bulk Comp +20µm



Py

Ga

Cp

Py

Fl

Py

Py

Mt

Po

Po

Gn

Go

Gn

Ga

Cs

Sp

Cp

Sp

Ga

Ga

Py

Image width 206µm

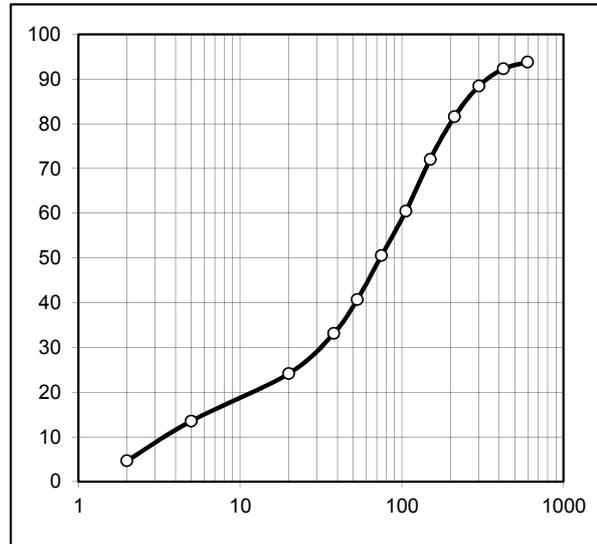
Severn Bulk Comp +8µm



BURNIE LABORATORY
 SIZE ANALYSIS REPORT SHEET WITH CS6

PROJECT	T0879
SAMPLE	SBC GROUND HEAD
DATE	260514
TECHNICIAN	MS

SBC GROUND HEAD		SIZE um	WEIGHTS		
			gm	(%)	%PASS
P80	202	600	15.00	6.23	93.8
		425	3.63	1.51	92.3
		300	9.22	3.83	88.4
		212	16.45	6.84	81.6
		150	22.96	9.54	72.0
		106	27.89	11.59	60.4
		75	23.86	9.92	50.5
		53	23.73	9.86	40.7
		38	18.09	7.52	33.1
		20	21.65	9.00	24.1
MINS 20	CS5	5	25.49	10.60	13.6
CENTRIFUGE	CS6	2	21.35	8.87	4.7
		SUB	11.26	4.68	0.0
		TOTAL	240.6	100.0	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mount Number
		%	dist	%	dist	%	dist	%	dist	%	dist	
600	6.23	0.97	6.2	21.30	5.1	0.17	3.7	9.85	4.1	40.40	8.7	
212	12.18	0.64	8.0	20.40	9.6	0.15	6.3	9.41	7.7	40.80	17.1	879064
150	9.54	0.84	8.2	25.60	9.4	0.25	8.2	15.35	9.8	32.30	10.6	879065
106	11.59	0.98	11.6	27.50	12.3	0.31	12.4	17.80	13.8	28.90	11.5	879066
75	9.92	1.10	11.1	28.30	10.8	0.34	11.6	18.60	12.3	26.80	9.1	879067
53	9.86	1.26	12.7	28.90	11.0	0.35	11.9	19.65	13.0	25.30	8.6	879068
38	7.52	1.31	10.1	29.50	8.5	0.38	9.9	19.50	9.8	24.20	6.3	879069
20	9.00	1.37	12.6	29.50	10.2	0.35	10.9	18.40	11.1	23.40	7.2	879070
8	10.60	1.40	15.1	29.80	12.1	0.35	12.8	18.15	12.9	21.30	7.8	879071
2	8.87	0.43	3.9	23.10	7.9	0.16	4.9	7.67	4.6	31.30	9.5	
CAL <2	4.68	0.13	0.6	17.49	3.1	0.46	7.5	3.26	1.0	22.77	3.7	
ASSAY	100.0	0.98	100.0	26.00	100.0	0.29	100.0	14.95	100.0	29.10	100.0	

SIZE um	WT %	MnO		CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist	%	dist
600	6.23	0.21	4.0	0.56	5.2	2.63	6.3	7.93	8.2
212	12.18	0.27	10.0	0.59	10.7	3.03	14.1	7.36	14.8
150	9.54	0.32	9.3	0.64	9.1	2.56	9.3	5.62	8.9
106	11.59	0.33	11.6	0.63	10.9	2.35	10.4	5.03	9.7
75	9.92	0.33	9.9	0.67	9.9	2.21	8.4	4.73	7.8
53	9.86	0.34	10.2	0.65	9.6	2.12	8.0	4.36	7.1
38	7.52	0.34	7.7	0.69	7.7	2.13	6.1	4.30	5.4
20	9.00	0.35	9.5	0.74	9.9	2.32	8.0	4.76	7.1
8	10.60	0.37	11.9	0.80	12.7	2.35	9.5	4.62	8.1
2	8.87	0.32	8.6	0.78	10.3	3.87	13.1	9.68	14.2
CAL <2	4.68	0.52	7.4	0.56	3.9	3.86	6.9	11.33	8.8
ASSAY	100.0	0.33	100.0	0.67	100.0	2.62	100.0	6.04	100.0

Mineral species logged:
Py-pyrite Po-pyrrhotite Cs-cassiterite
St-stannite As-arsenopyrite
Cp-chalcopyrite SpGn-sphalerite/galena Ga-gangue

Sum of the weight fractions
for the sizes examined

All sizings combined **73% of sample**
Average composition - all grains

Total number of
grains logged

Mineral content
as area %

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
19.3	0.6	18.5	0.8	0.0	2.0	0.8	58.0	300
84	0	90	0	29	0	97	48	

Average area % per
grain when present

Assays calculated from
mineral area % using
theoretical compositions

	SG	Sn	S	As	Fe	Cu
Calc'd	5.29	57.1	4.8	0.5	5.8	0.02
Actual		55.2	8.9	0.39	8.3	

Sizing assay
if provided

% of mineral
fully liberated

% of mineral in grains
with 3 minerals present

% of grains
with this mineral

	Py	Po	Cs	St	Cp	As	Ga
Mono	49	0	63	0	0	42	72
Binary	50	0	34	0	0	33	26
Ternary	0	0	2	0	0	21	2
Quat.y+	0	0	0	0	0	4	0
% Grains	12	0	69	0	0	3	52

% of mineral in grains
with 2 minerals present

% of mineral in grains
with >3 minerals present

Average number of
minerals per grain

e.g. 95% of all
binary Cs occurs
with Ga

	Py	Po	Cs	St	Cp	As	Ga
Py		0	19	0	0	0	81
Po	0		0	0	0	0	0
Cs	0	0		0	0	4	95
St	0	0	0		0	0	0
Cp	0	0	0	0		0	0
As	4	0	7	0	0		89
Ga	13	0	86	0	0	0	

These rows do not
sum to 100% because
of fully liberated and
multi-mineral grains

	Py	Po	Cs	St	Cp	As	Ga
Py		0	10	0	0	0	41
Po	0		0	0	0	0	0
Cs	2	0		0	0	2	35
St	0	0	0		0	0	0
Cp	0	0	0	0		0	0
As	12	0	15	8	6		50
Ga	3	0	25	0	0	2	

e.g. 2% of all Cs
occurs with As
but 15% of all As
occurs with Cs

e.g. while 63% of Cs
is fully liberated,
2% occurs as binaries
with As and 33% with
Ga. 2% occurs with 2
other minerals

	Free	Binary						Tern	Quat	
		Py	Po	Cs	St	Cp	As			Ga
Py	49		0	9	0	0	0	41	0	0
Po	0	0		0	0	0	0	0	0	0
Cs	63	0	0		0	0	2	33	2	0
St	0	0	0	0		0	0	0	0	0
Cp	0	0	0	0	0		0	0	0	0
As	42	1	0	2	0	0		30	21	4
Ga	72	3	0	23	0	0	0		2	0

These rows will
sum to 100%
(unless binary SpGn
occurs or unless
minor rounding
errors occur)



PARTICLE MINERALOGY REPORT

GJMcA 13.6.14

**Severn Bulk Comp
June 2014**

C +106µm 12 % by weight

D +75µm 10 % by weight

A +212µm 12 % by weight

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
11.7	0.2	0.4	0.0	0.0	0.1	0.8	86.9	100
48	22	13	18	0	3	16	92	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
22.9	1.7	0.2	0.0	0.1	0.0	1.4	73.8	100
61	35	24	4	10	0	34	84	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
23.0	4.6	0.2	0.0	1.0	0.0	1.1	70.1	100
70	48	35	37	100	0	52	88	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
31.4	1.2	1.0	0.0	0.1	0.0	0.0	66.3	100
72	45	45	17	8	1	0	88	

ASSAYS

	SG	Sn	S	As	Fe	Cu
Calc'd	3.35	0.60	9.8	0.00	21.8	0.04
Actual		0.64	9.4		20.4	

ASSAYS

	SG	Sn	S	As	Fe	Cu
Calc'd	3.59	0.26	18.4	0.08	26.9	0.00
Actual		0.84	15.4		25.6	

ASSAYS

	SG	Sn	S	As	Fe	Cu
Calc'd	3.67	0.34	19.8	0.77	28.7	0.00
Actual		0.98	17.5		27.5	

ASSAYS

	SG	Sn	S	As	Fe	Cu
Calc'd	3.76	1.45	23.0	0.06	29.5	0.01
Actual		1.10	18.6		28.3	

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	46	53	0	0	0	0	76
Binary	47	40	74	0	56	0	19
Ternary	6	6	21	3	0	0	3
Quat.y+	1	1	5	97	44	0	1
#Grains	25	4	4	0	3	0	94

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	49	62	17	0	0	0	77
Binary	47	36	51	0	0	100	19
Ternary	2	2	30	37	0	0	4
Quat.y+	2	0	2	62	0	0	0
#Grains	35	5	3	0	0	1	88

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	67	73	28	39	0	100	78
Binary	32	16	55	43	0	0	16
Ternary	1	11	16	18	0	0	5
Quat.y+	0	0	1	0	0	0	0
#Grains	35	8	5	0	0	1	80

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	74	70	46	57	0	0	81
Binary	22	24	43	6	0	0	16
Ternary	3	5	6	26	67	100	2
Quat.y+	1	1	5	11	33	0	1
#Grains	41	5	1	0	2	1	75

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	9	0	0	0	91
Po	0		0	0	0	0	100
Cs	2	2		0	0	0	96
St	0	0	0		0	0	0
Cp	0	0	0	0		0	100
As	0	0	0	0	0		0
Ga	62	11	16	0	6	0	

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	8	0	0	4	88
Po	0		0	0	0	0	100
Cs	18	0		0	0	1	81
St	0	0	0		0	0	0
Cp	0	0	0	0		0	0
As	0	0	0	0	0		100
Ga	64	17	7	0	0	6	

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	9	0	0	0	91
Po	0		0	0	0	0	100
Cs	14	1		0	0	0	81
St	0	0	0		68	0	32
Cp	0	0	0	0		0	0
As	0	0	0	0	0		0
Ga	64	20	8	0	0	0	

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	0	0	0	0	100
Po	0		0	0	0	0	100
Cs	4	0		0	0	0	95
St	0	0	0		100	0	0
Cp	0	0	0	0		0	0
As	0	0	0	0	0		0
Ga	74	26	0	0	0	0	

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		4	4	0	0	2	50
Po	5		0	0	0	1	47
Cs	21	9		2	5	0	94
St	0	100	97		97	0	3
Cp	44	0	0	0		0	100
As	0	0	0	0	0		0
Ga	14	4	4	0	2	0	

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		2	5	0	0	2	45
Po	0		0	2	0	0	38
Cs	36	6		0	2	0	73
St	0	0	100		62	0	100
Cp	0	0	0	0		0	0
As	0	0	0	0	0		100
Ga	16	3	3	0	0	1	

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	4	0	0	0	30
Po	11		0	0	0	0	27
Cs	21	4		0	0	0	62
St	0	0	0		46	0	32
Cp	0	0	0	0		0	0
As	0	0	0	0	0		0
Ga	16	5	5	0	0	0	

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		3	0	0	2	1	26
Po	5		0	0	1	0	30
Cs	7	3		5	5	0	50
St	11	0	12		41	0	26
Cp	100	33	0	0		0	100
As	100	0	0	0	0		100
Ga	14	5	0	0	2	1	

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat	
	Py	Po	Cs	St	Cp	As	Ga			
Py	46			4	0	0	0	43	6	1
Po	53	0		0	0	0	0	40	6	1
Cs	0	1	1		0	0	0	71	21	5
St	0	0	0	0		0	0	0	3	97
Cp	0	0	0	0	0		0	56	0	44
As	0	0	0	0	0		0	0	0	0
Ga	76	12	2	3	0	1	0		3	1

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat	
	Py	Po	Cs	St	Cp	As	Ga			
Py	49			4	0	0	2	42	2	2
Po	62	0		0	0	0	0	36	2	0
Cs	17	9	0		0	0	0	41	30	2
St	0	0	0	0		0	0	0	37	62
Cp	0	0	0	0	0		0	0	0	0
As	0	0	0	0	0		100	0	0	0
Ga	77	12	3	1	0	0	1		4	0

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat	
	Py	Po	Cs	St	Cp	As	Ga			
Py	67			3	0	0	0	29	1	0
Po	73	0		0	0	0	0	16	11	0
Cs	28	8	0		0	0	0	45	16	1
St	39	0	0	0		29	0	14	18	0
Cp	0	0	0	0	0		0	0	0	0
As	100	0	0	0	0		0	0	0	0
Ga	78	10	3	1	0	0	0		5	0

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat	
	Py	Po	Cs	St	Cp	As	Ga			
Py	74			0	0	0	0	22	3	1
Po	70	0		0	0	0	0	24	5	1
Cs	46	2	0		0	0	0	41	6	5
St	57	0	0	0		6	0	0	26	11
Cp	0	0	0	0	0		0	0	67	33
As	0	0	0	0	0		0	0	100	0
Ga	81	12	4	0	0	0	0		2	1



PARTICLE MINERALOGY REPORT

**Severn Bulk Comp
June 2014**

GJMcA 17.6.14

G +20µm 9 % by weight

H +8µm 11 % by weight

E +53µm 10 % by weight

F +38µm 8 % by weight

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
26.3	3.5	1.2	1.0	0.0	0.1	2.1	66.0	100
86	81	48	38	0	4	68	90	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
26.6	9.5	0.5	0.0	0.0	0.2	2.1	61.1	100
91	92	69	70	0	11	52	93	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
29.9	6.2	1.3	0.0	0.0	0.2	4.0	58.4	100
91	78	85	33	0	6	80	94	

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
28.3	6.7	2.0	0.0	0.0	0.0	3.0	60.1	100
94	93	91	68	0	0	100	98	

ASSAYS

Calc'd	SG	Sn	S	As	Fe	Cu
3.75	1.98	21.6	0.00	28.3	0.36	
Actual	1.26	19.7		28.9		

ASSAYS

Calc'd	SG	Sn	S	As	Fe	Cu
3.81	0.71	24.1	0.00	31.7	0.08	
Actual	1.31	19.5		29.5		

ASSAYS

Calc'd	SG	Sn	S	As	Fe	Cu
3.88	1.82	25.0	0.00	30.4	0.07	
Actual	1.37	18.4		29.5		

ASSAYS

Calc'd	SG	Sn	S	As	Fe	Cu
3.87	2.81	23.8	0.00	30.0	0.00	
Actual	1.40	18.2		29.8		

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	70	67	59	24	0	0	88
Binary	30	28	39	34	62	0	10
Ternary	0	0	1	26	37	0	1
Quat.y+	0	5	1	16	0	0	1
#Grains	34	4	4	1	2	0	73

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	85	91	66	24	0	0	90
Binary	15	6	29	73	9	0	9
Ternary	1	3	4	0	91	0	1
Quat.y+	0	0	0	3	0	0	0
#Grains	30	10	3	0	2	0	66

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	87	76	72	0	0	0	89
Binary	13	20	25	90	100	0	10
Ternary	1	4	3	10	0	0	1
Quat.y+	0	0	0	0	0	0	0
#Grains	33	8	3	0	3	0	62

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	97	88	83	98	0	0	97
Binary	3	12	17	2	0	0	3
Ternary	0	0	0	0	0	0	0
Quat.y+	0	0	0	0	0	0	0
#Grains	30	7	2	0	0	0	61

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	12	0	0	0	0	84
Po	0	33	0	30	0	0	37
Cs	7	0	0	0	0	0	93
St	0	0	0	66	0	0	3
Cp	0	0	0	100	0	0	0
As	0	0	0	0	0	0	0
Ga	85	1	14	0	0	0	0

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	0	0	0	0	0	100
Po	0	0	0	0	0	0	100
Cs	7	4	0	0	4	0	84
St	0	0	0	92	0	0	0
Cp	0	0	0	0	0	0	0
As	0	0	0	0	0	0	0
Ga	49	1	17	0	0	0	0

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	0	0	0	4	0	86
Po	0	0	0	0	0	0	100
Cs	1	5	0	0	5	0	85
St	4	0	0	0	0	0	96
Cp	0	0	0	0	0	0	79
As	0	0	0	0	0	0	0
Ga	29	24	14	0	15	0	0

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	0	0	0	0	0	100
Po	0	0	0	0	0	0	100
Cs	8	4	0	0	4	0	84
St	100	0	0	0	0	0	0
Cp	0	0	0	0	0	0	0
As	0	0	0	0	0	0	0
Ga	85	15	0	0	0	0	0

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	4	0	0	0	0	25
Po	5	14	0	9	0	0	15
Cs	5	0	0	1	0	0	38
St	2	2	12	61	0	0	28
Cp	37	0	0	62	0	0	37
As	0	0	0	0	0	0	0
Ga	11	1	2	0	1	0	0

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	1	0	0	0	0	15
Po	0	3	0	3	0	0	6
Cs	4	2	0	1	0	0	28
St	0	0	0	70	0	0	3
Cp	0	91	91	0	0	0	0
As	0	0	0	0	0	0	0
Ga	5	0	2	0	0	0	0

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	0	0	0	0	0	12
Po	4	0	0	0	0	0	24
Cs	2	1	0	2	0	0	24
St	4	0	10	0	0	0	96
Cp	0	0	0	0	0	0	79
As	0	0	0	0	0	0	0
Ga	4	3	2	0	1	0	0

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py	0	0	0	0	0	0	3
Po	0	0	0	0	0	0	12
Cs	1	1	0	1	0	0	14
St	2	0	0	0	0	0	0
Cp	0	0	0	0	0	0	0
As	0	0	0	0	0	0	0
Ga	3	0	0	0	0	0	0

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat
	Py	Po	Cs	St	Cp	As	Ga		
Py	70	0	4	0	0	0	25	0	0
Po	67	0	9	0	9	0	10	0	5
Cs	59	3	0	0	0	0	36	1	1
St	24	0	0	0	22	0	1	26	16
Cp	0	0	0	0	62	0	0	37	0
As	0	0	0	0	0	0	0	0	0
Ga	88	9	0	1	0	0	0	1	1

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat
	Py	Po	Cs	St	Cp	As	Ga		
Py	85	0	0	0	0	0	15	1	0
Po	91	0	0	0	0	0	6	3	0
Cs	66	2	1	0	1	0	25	4	0
St	24	0	0	0	68	0	0	0	3
Cp	0	0	0	0	0	0	91	0	0
As	0	0	0	0	0	0	0	0	0
Ga	90	5	0	2	0	0	0	1	0

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat
	Py	Po	Cs	St	Cp	As	Ga		
Py	87	0	0	0	0	0	11	1	0
Po	76	0	0	0	0	0	20	4	0
Cs	72	0	1	0	1	0	21	3	0
St	0	4	0	0	0	0	86	10	0
Cp	0	0	0	0	0	0	79	0	0
As	0	0	0	0	0	0	0	0	0
Ga	89	3	2	1	0	1	0	1	0

DISTRIBUTION MATRIX

Free	Binary							Tern	Quat
	Py	Po	Cs	St	Cp	As	Ga		
Py	97	0	0	0	0	0	3	0	0
Po	88	0	0	0	0	0	12	0	0
Cs	83	1	1	0	1	0	14	0	0
St	98	2	0	0	0	0	0	0	0
Cp	0	0	0	0	0	0	0	0	0
As	0	0	0	0	0				

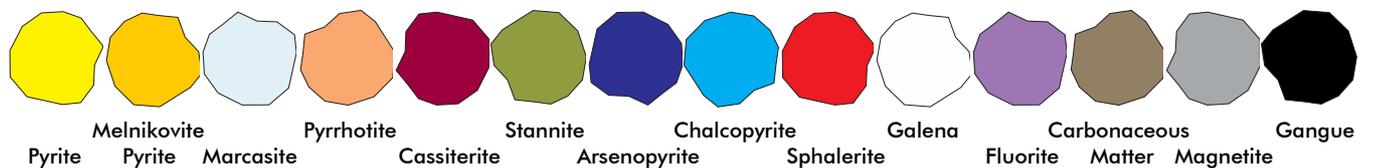
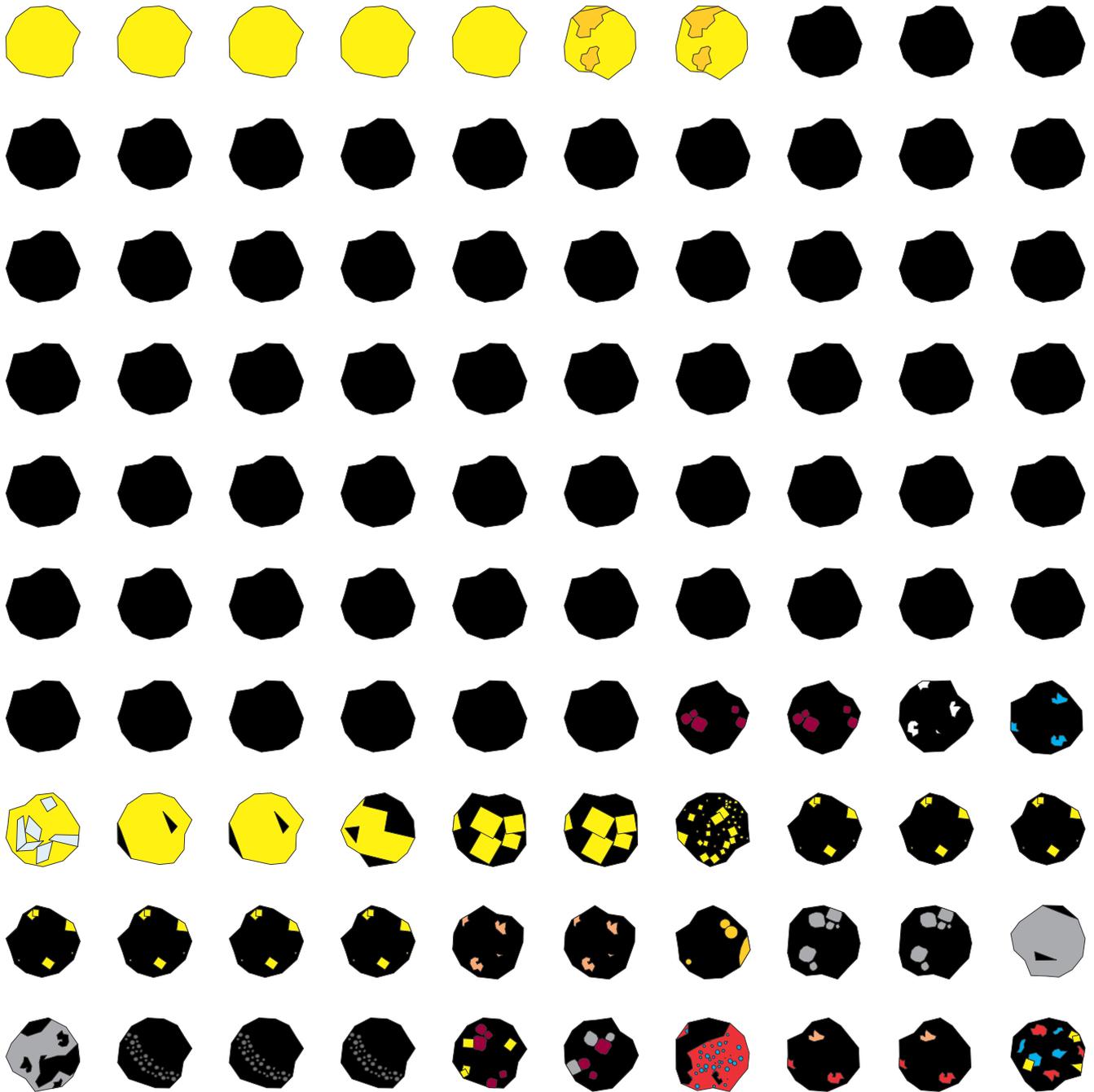
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

A +212µm

June

2014



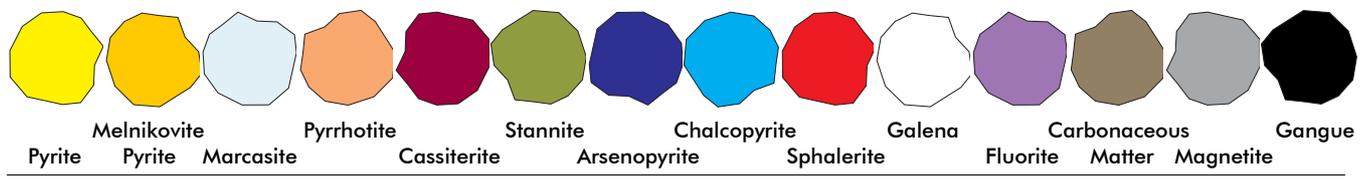
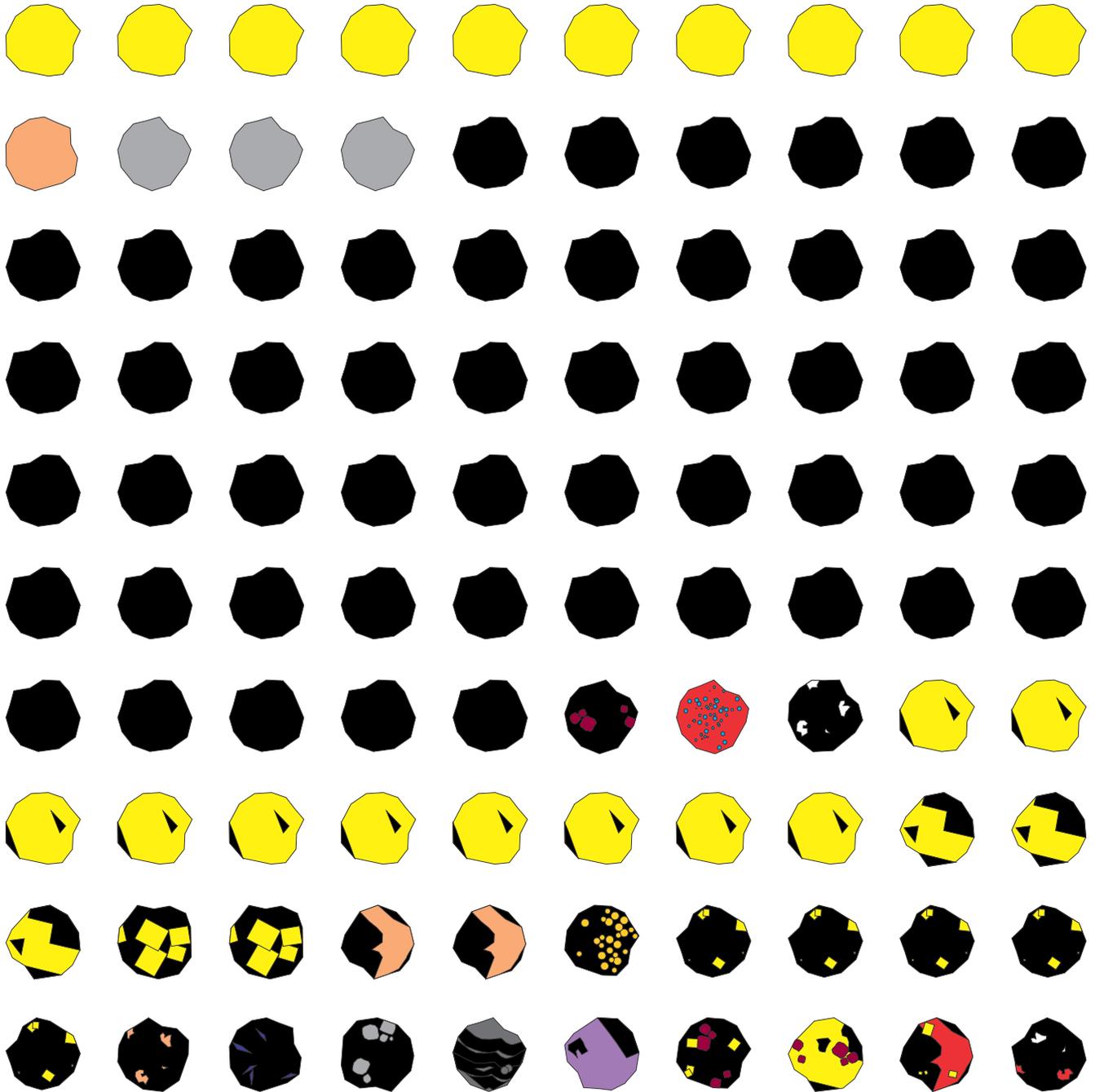
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

B + 150µm

June

2014



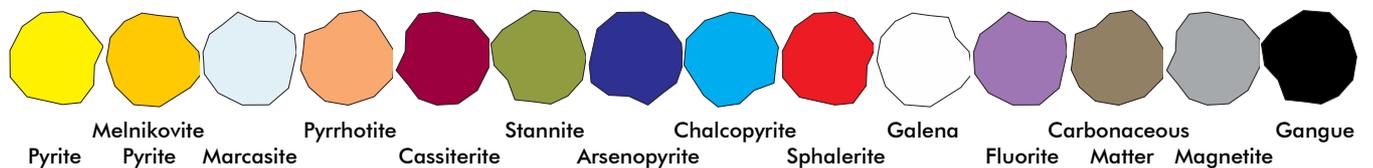
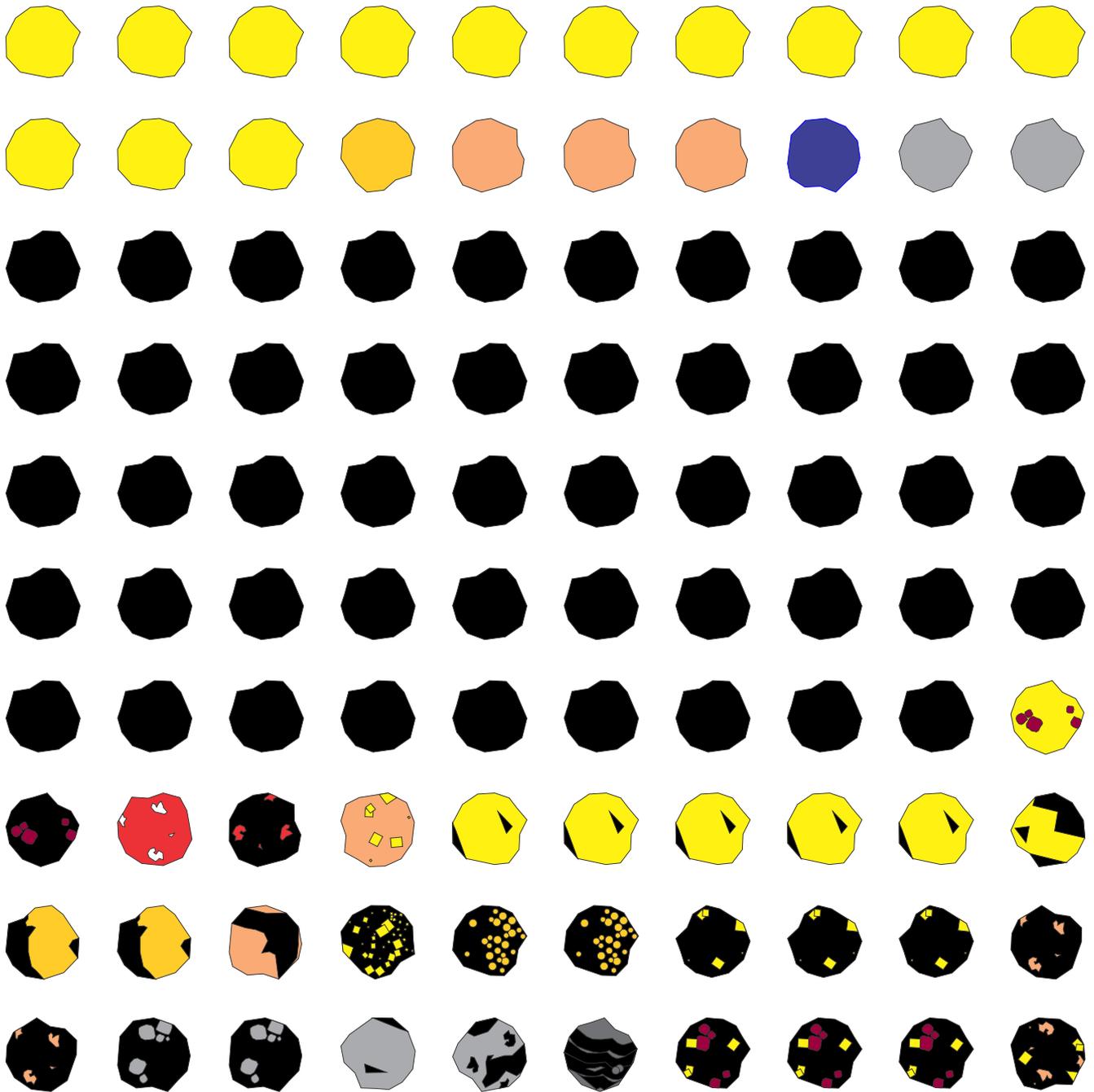
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

C + 106µm

June

2014



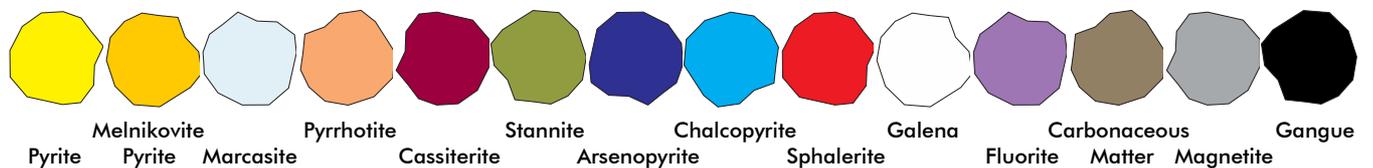
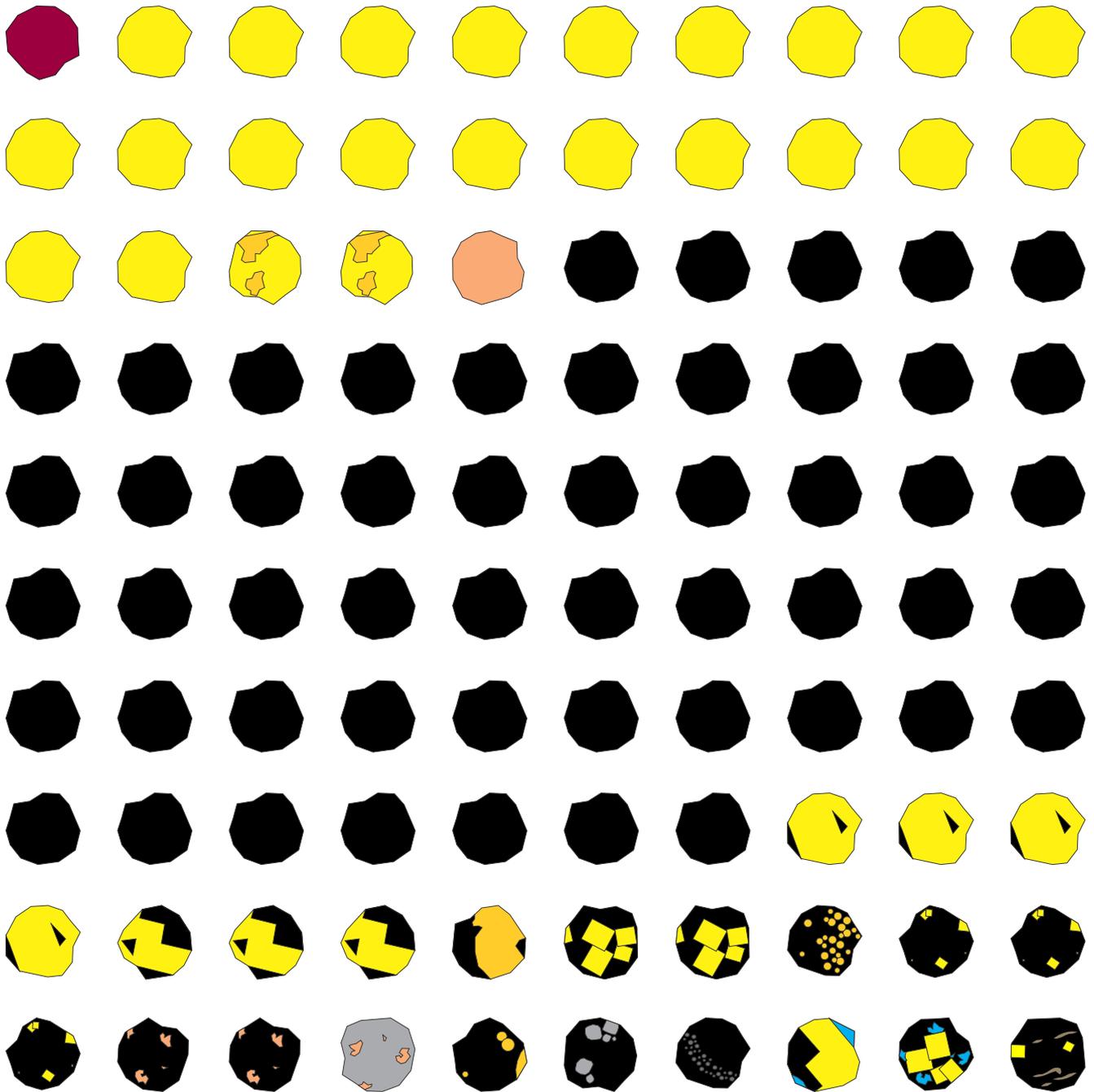
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

D +75µm

June

2014



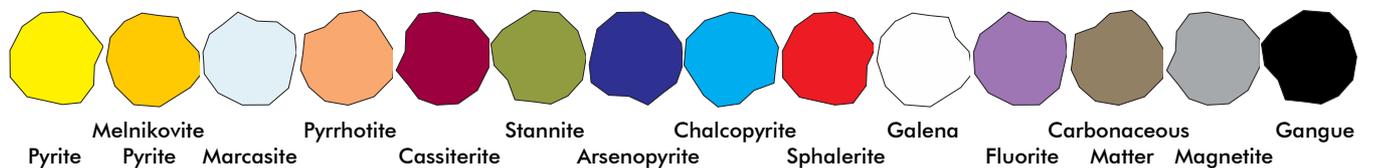
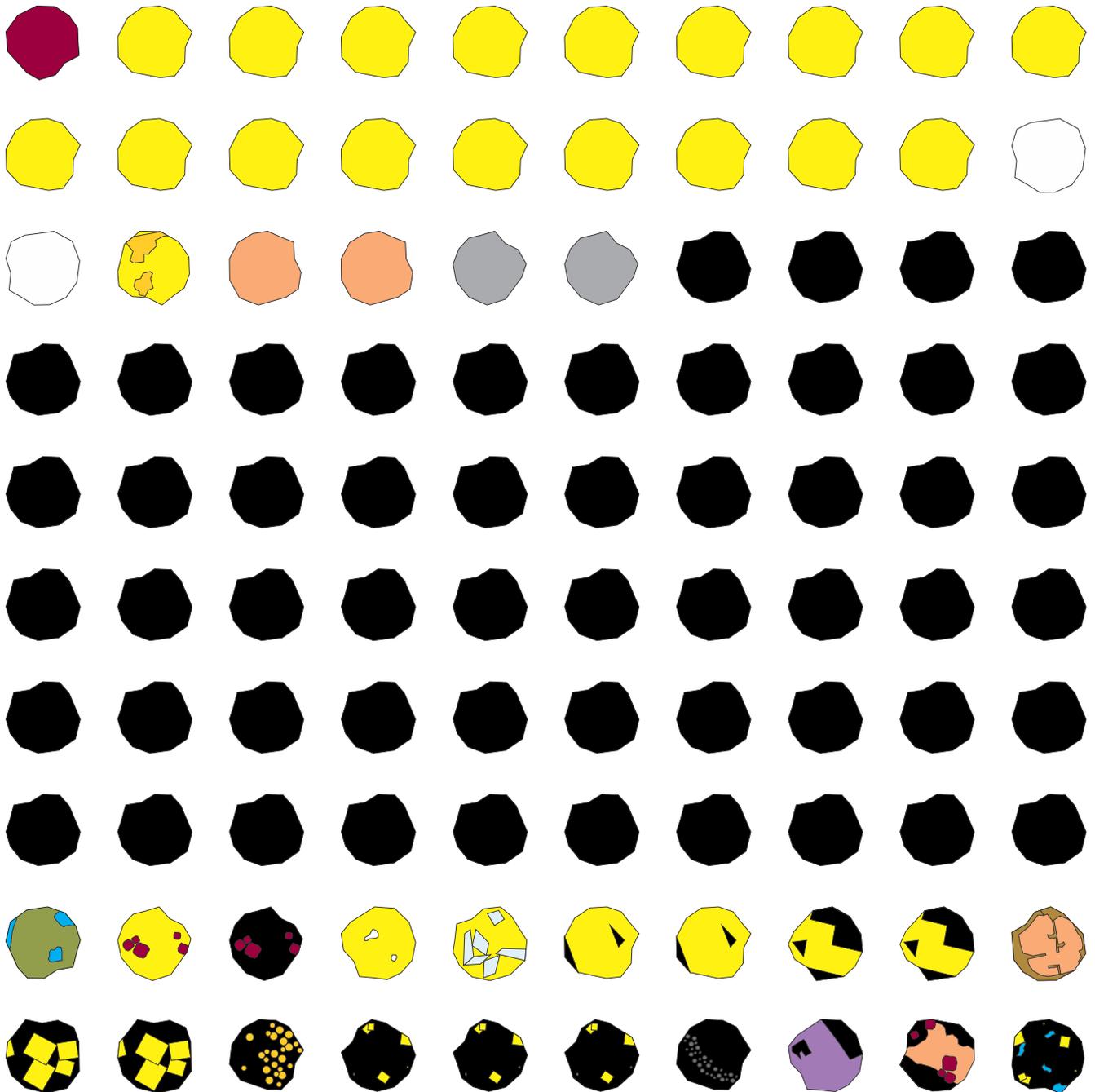
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

E +53µm

June

2014



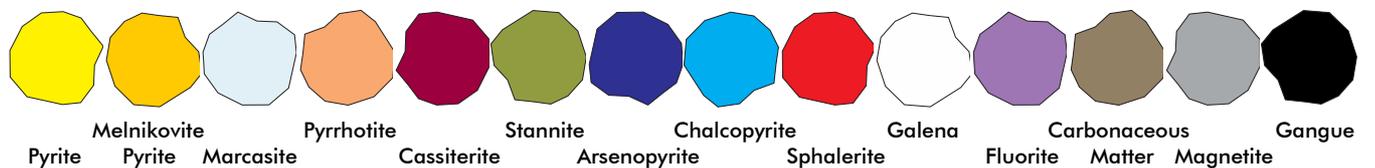
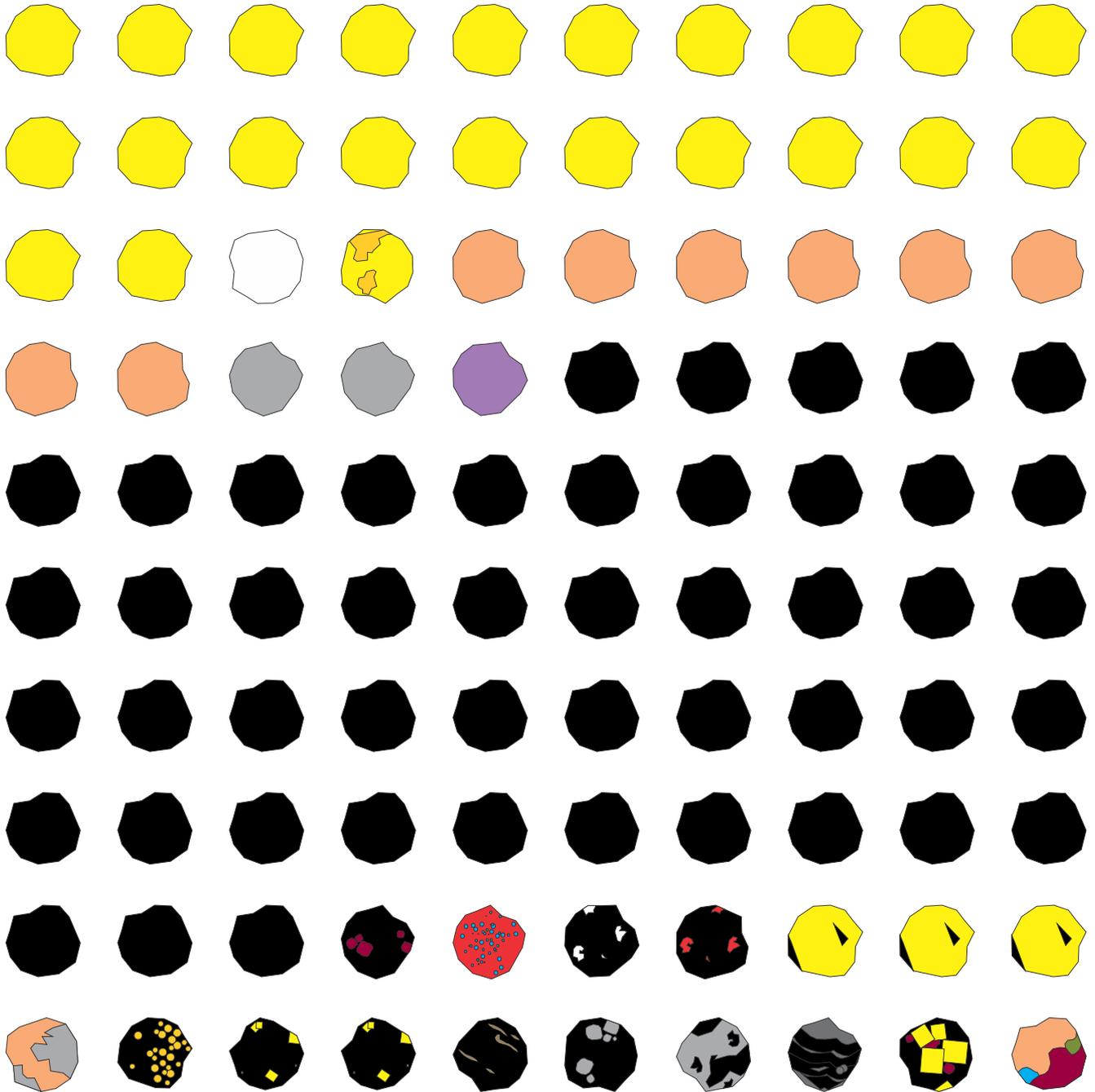
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

F +38µm

June

2014



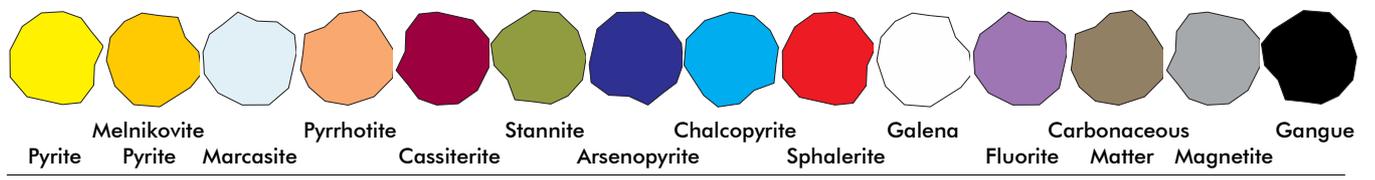
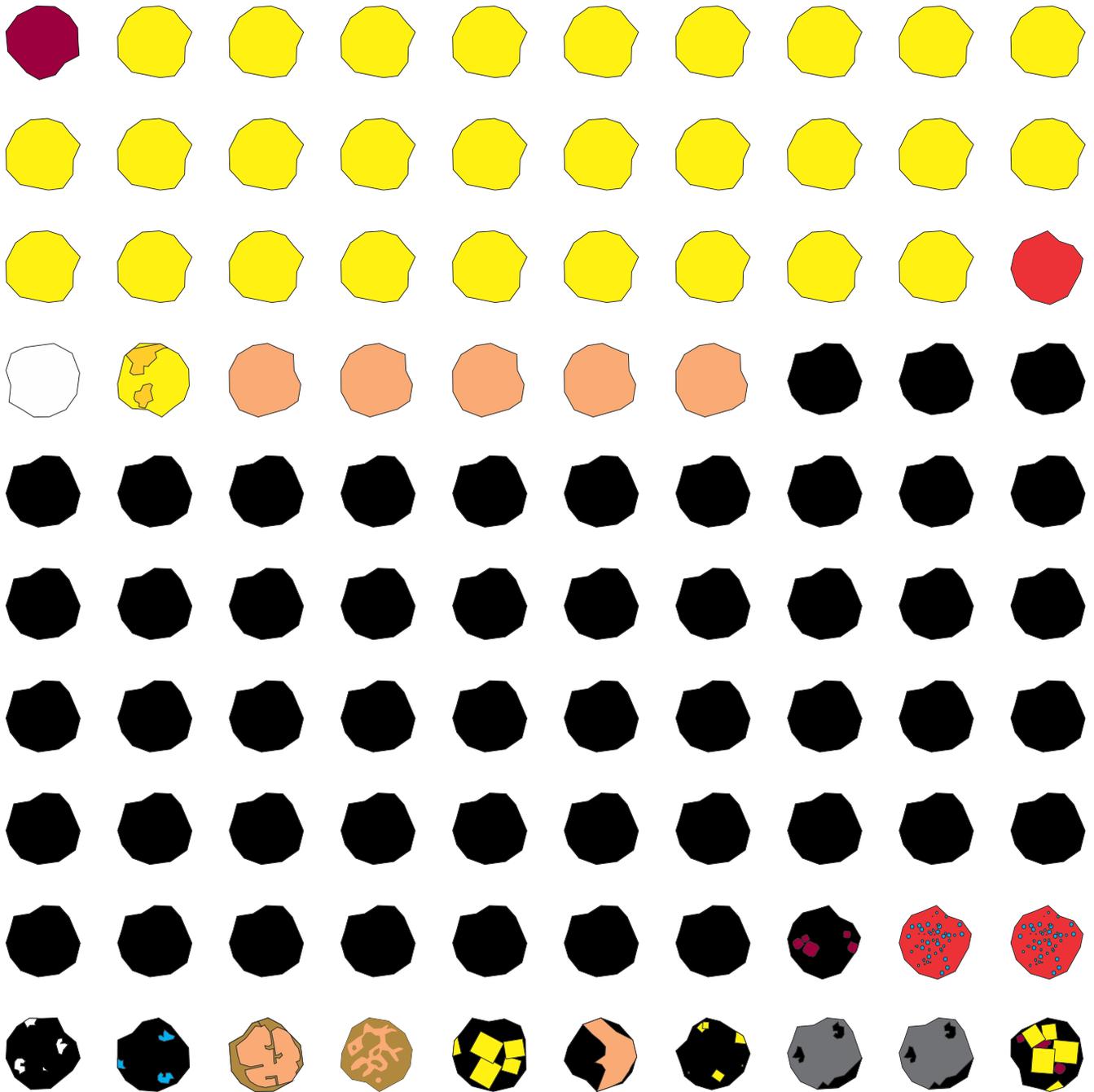
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

G +20µm

June

2014



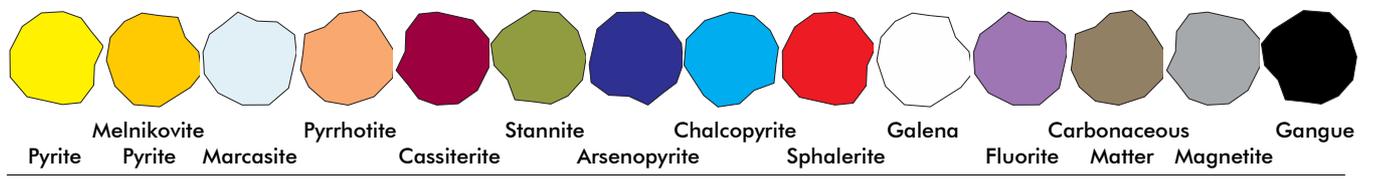
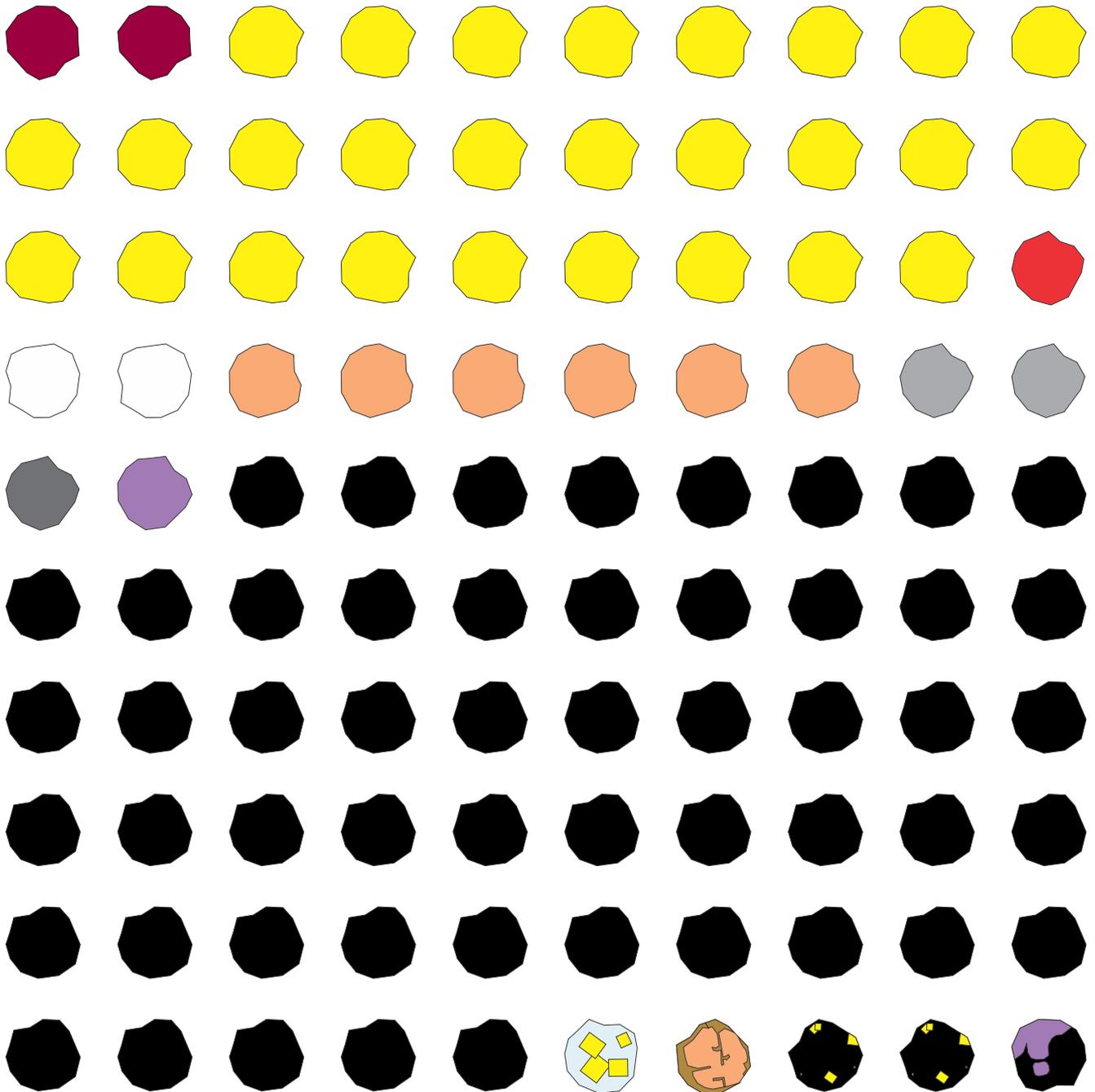
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp

H +8μm

June

2014



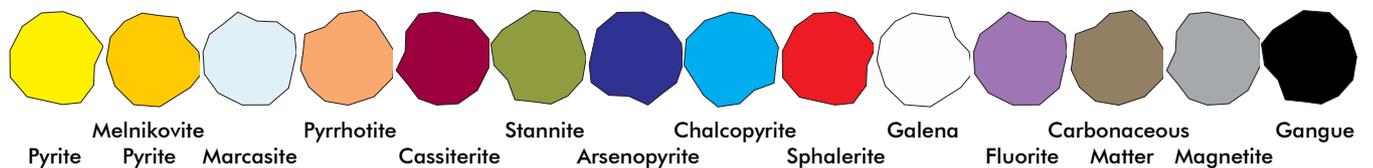
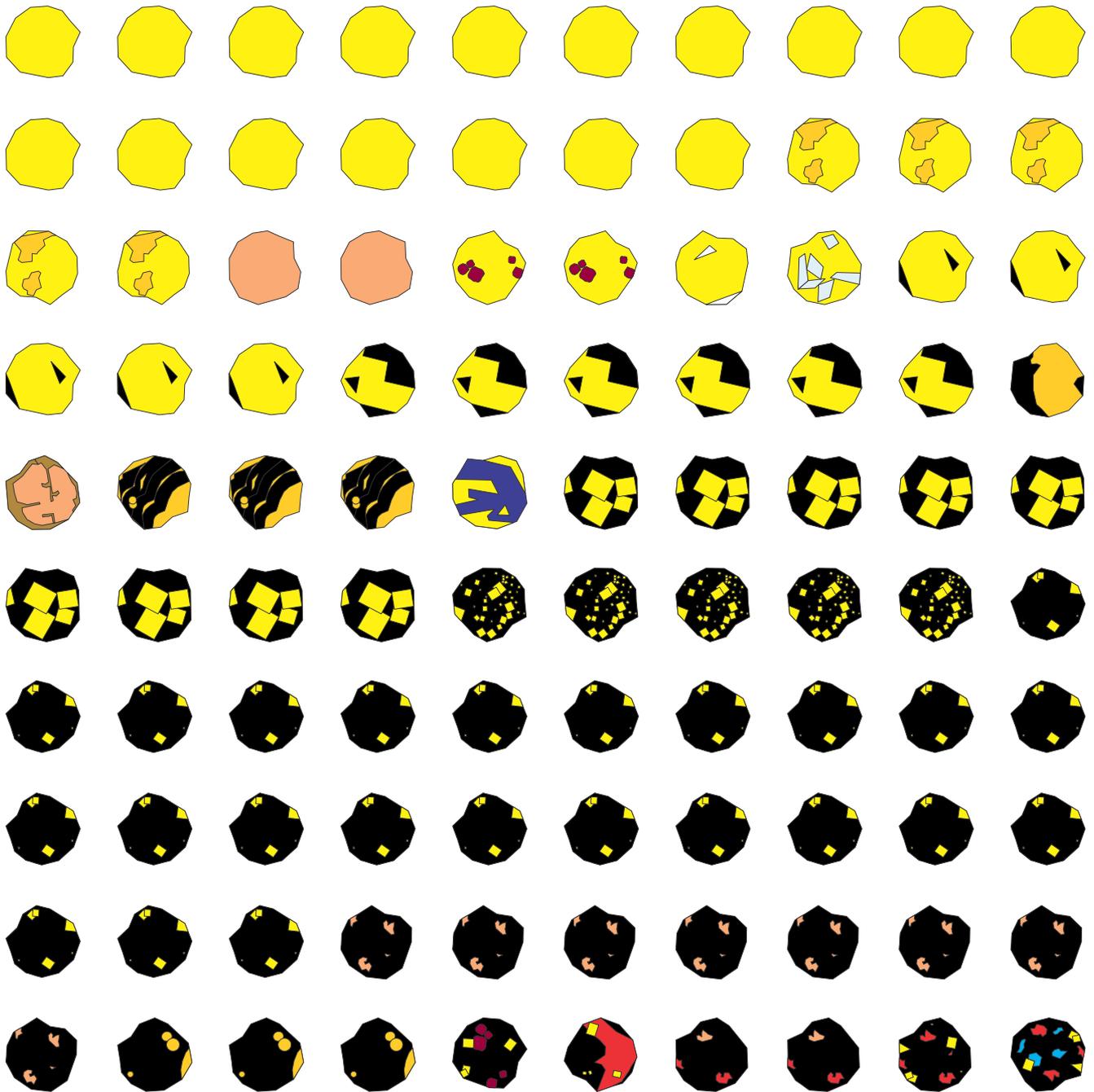
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

A +212µm

June

2014



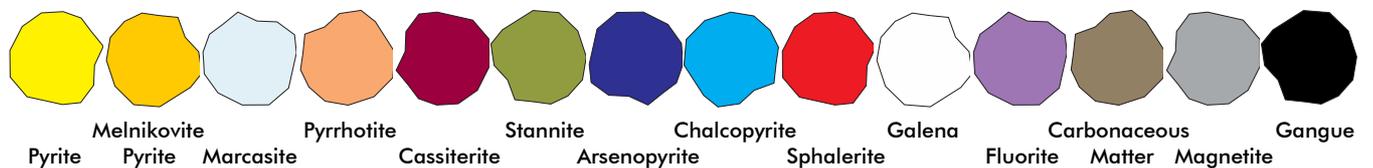
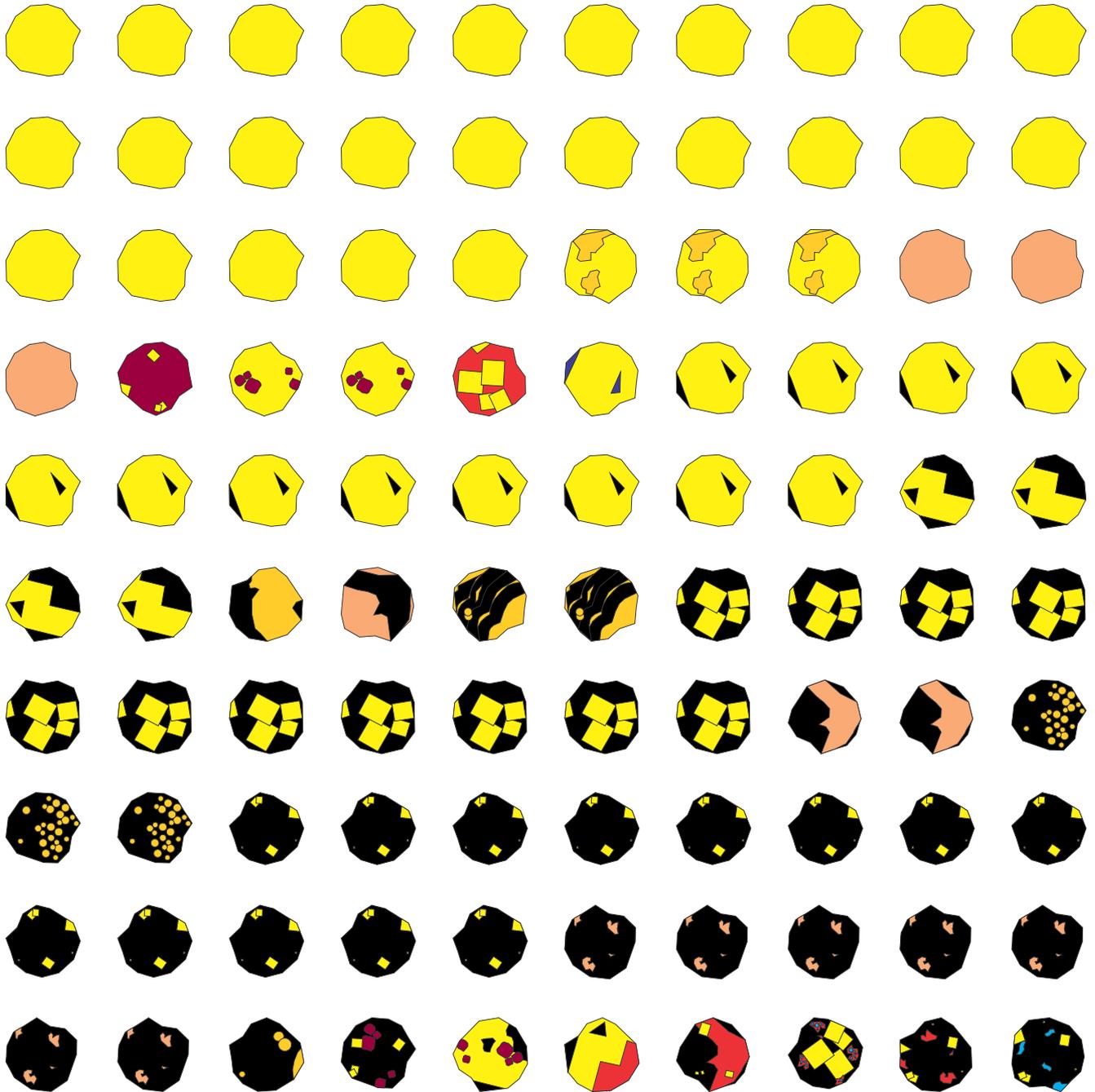
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

B + 150µm

June

2014



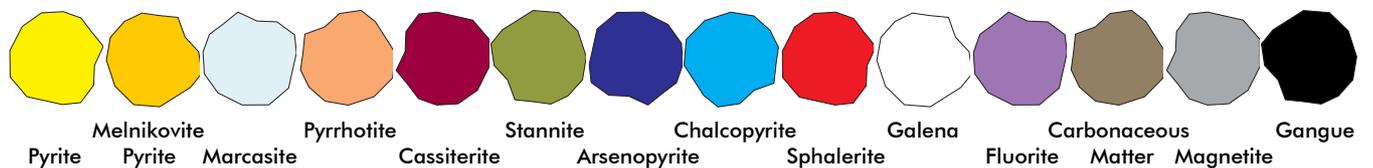
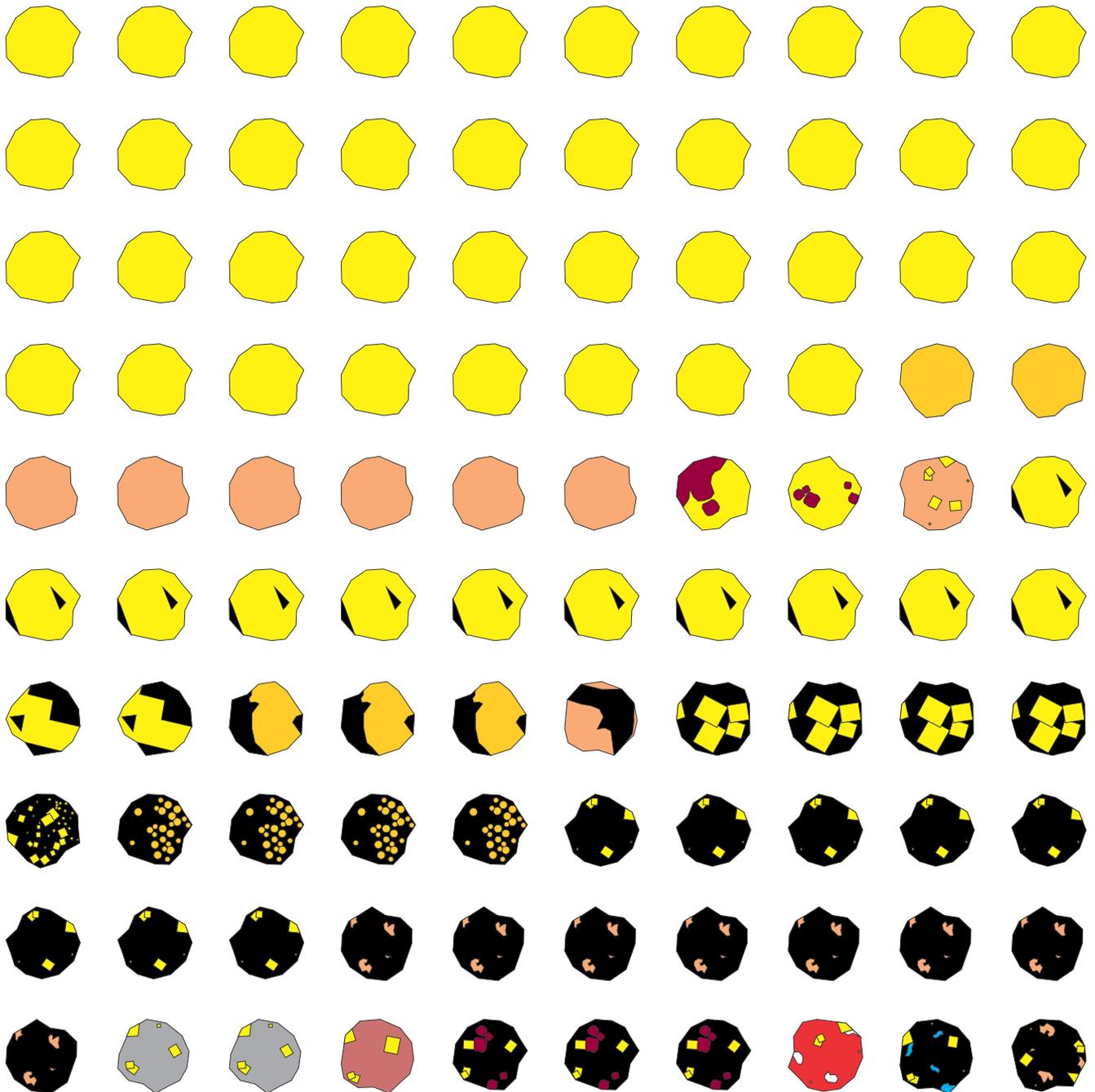
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

C + 106µm

June

2014



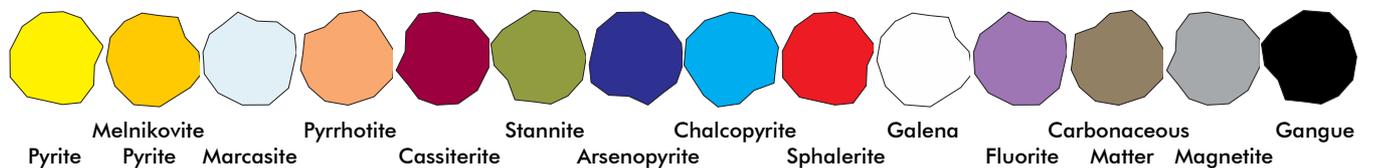
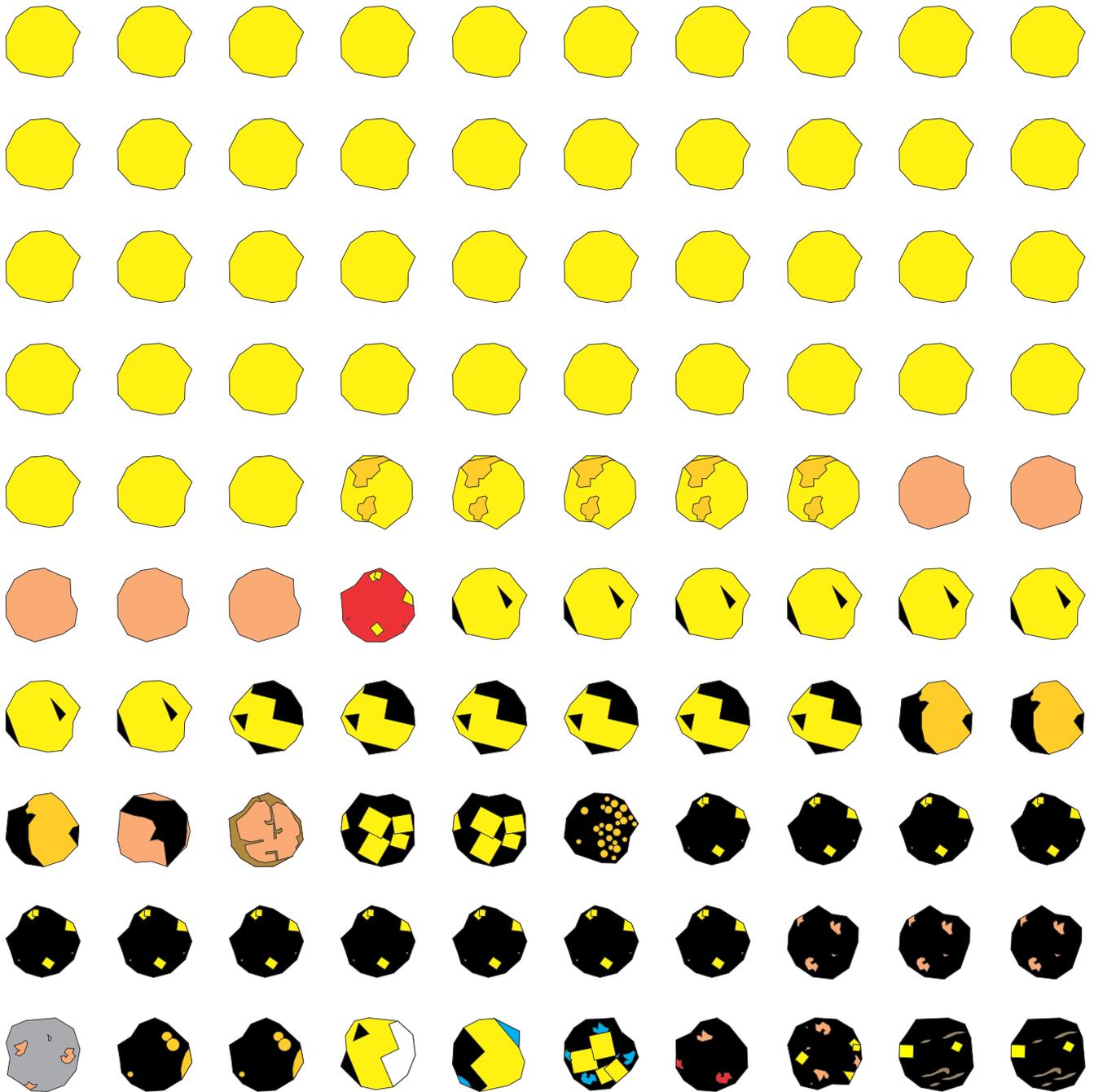
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

D +75µm

June

2014



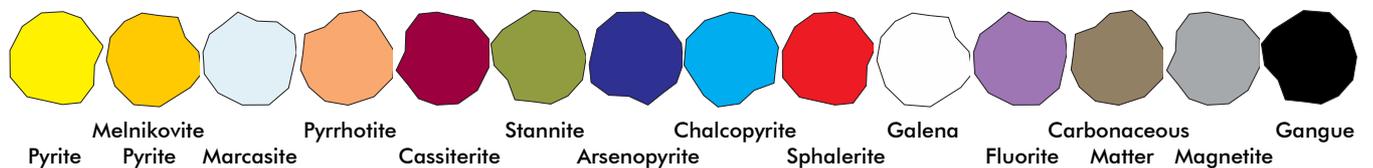
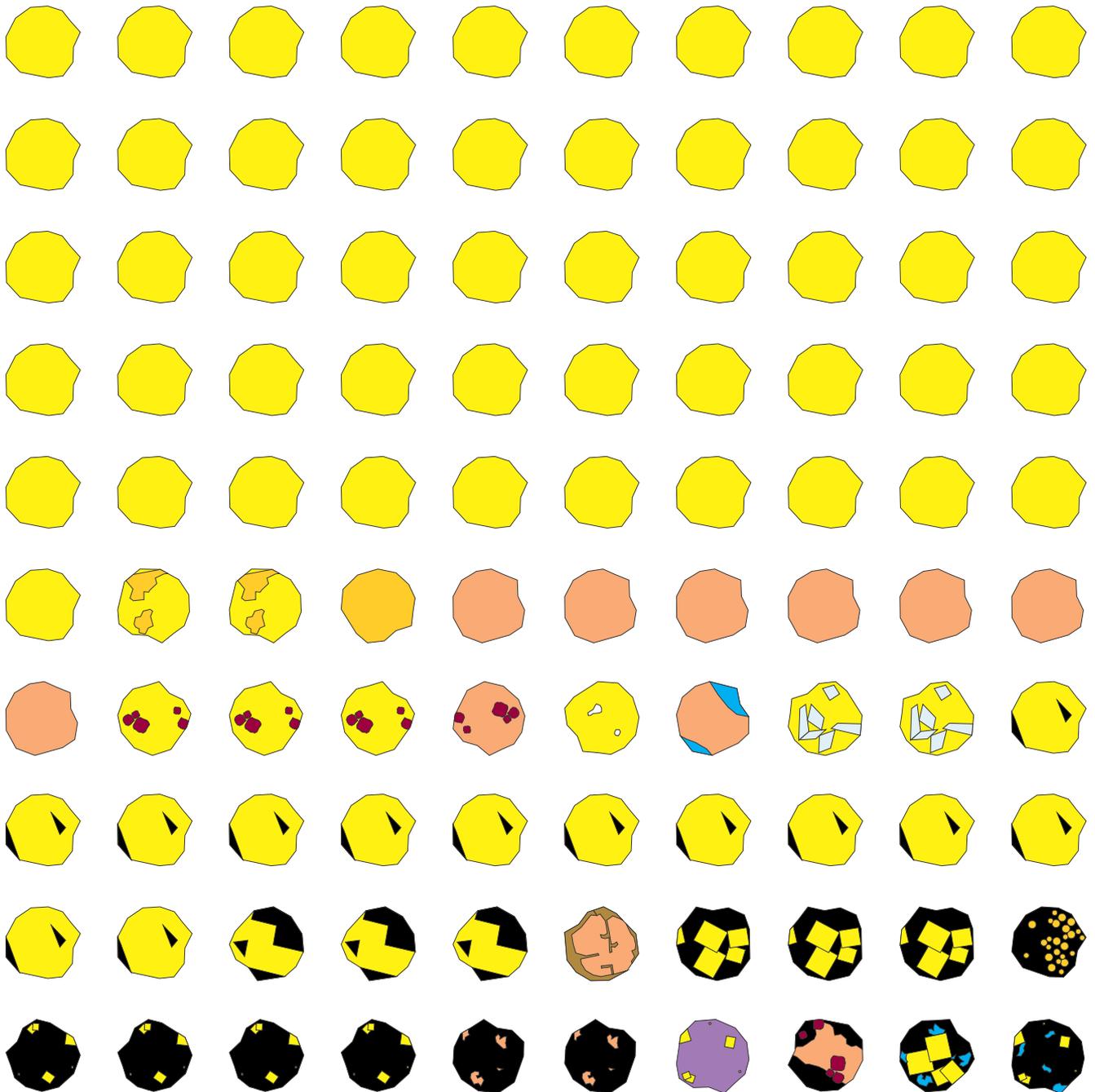
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

E +53µm

June

2014



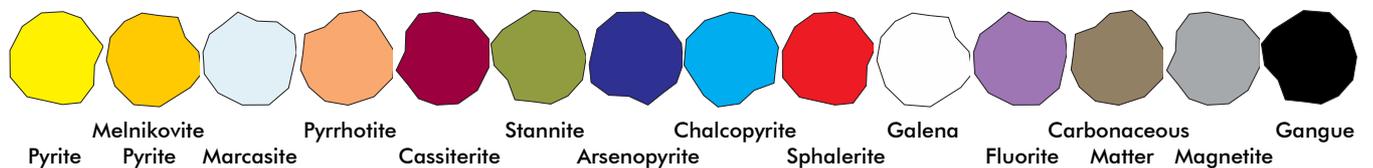
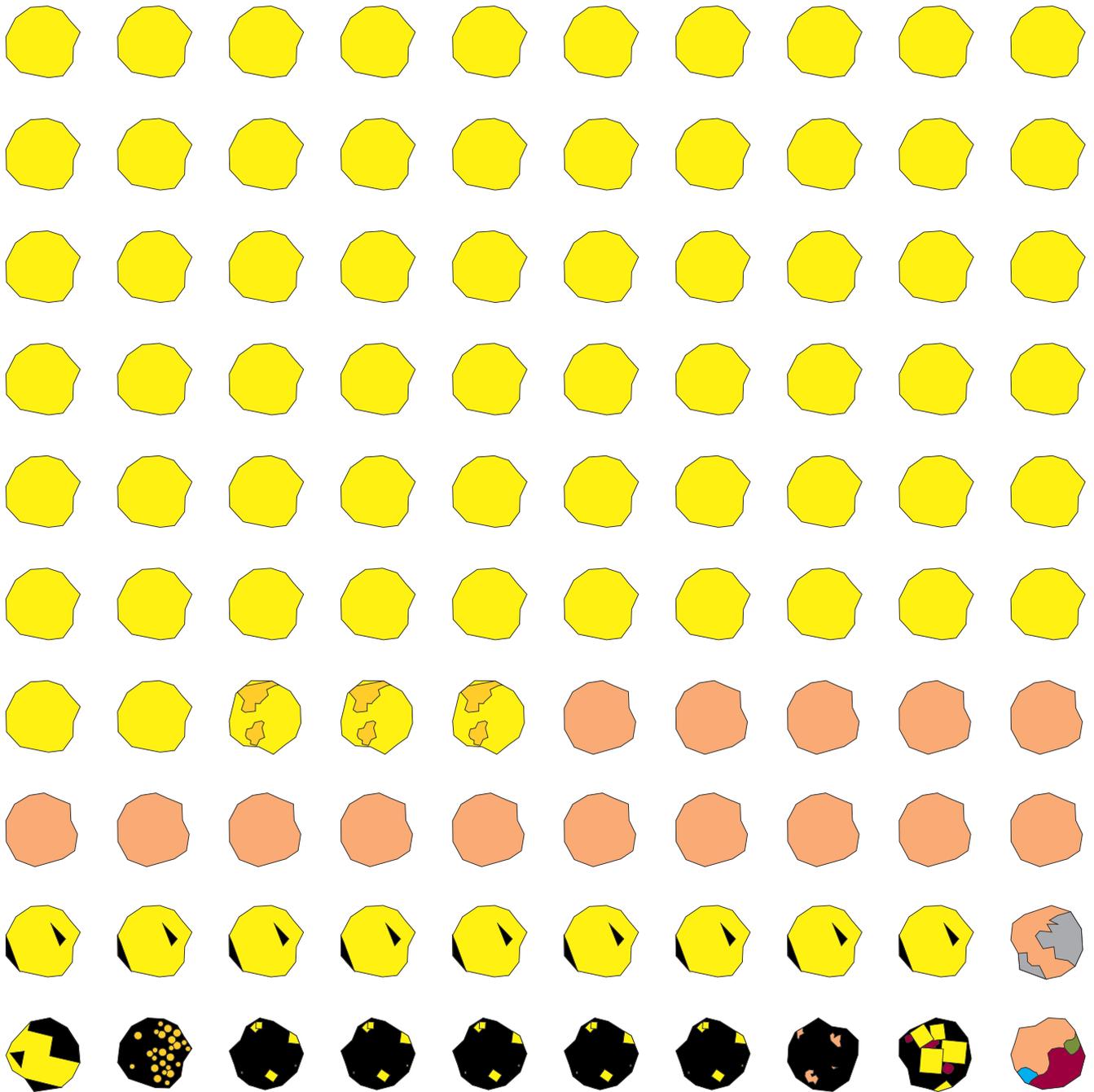
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

F +38µm

June

2014



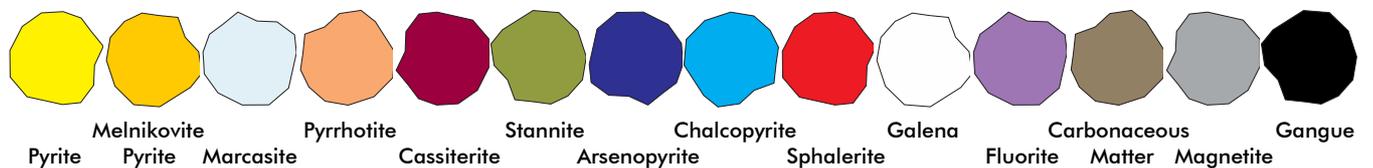
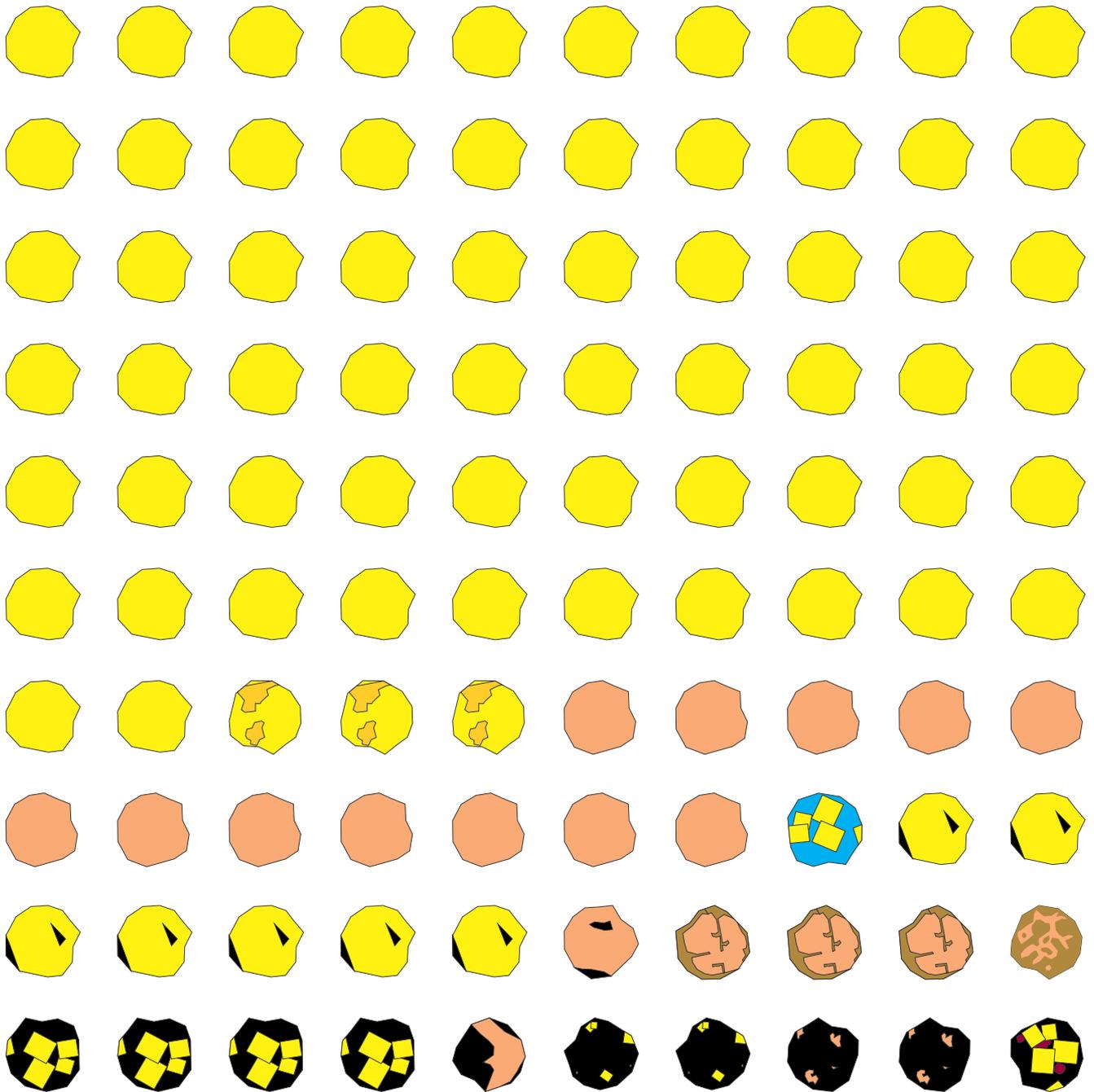
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

G +20µm

June

2014



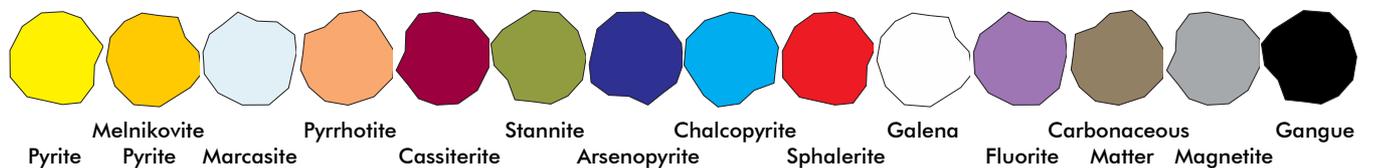
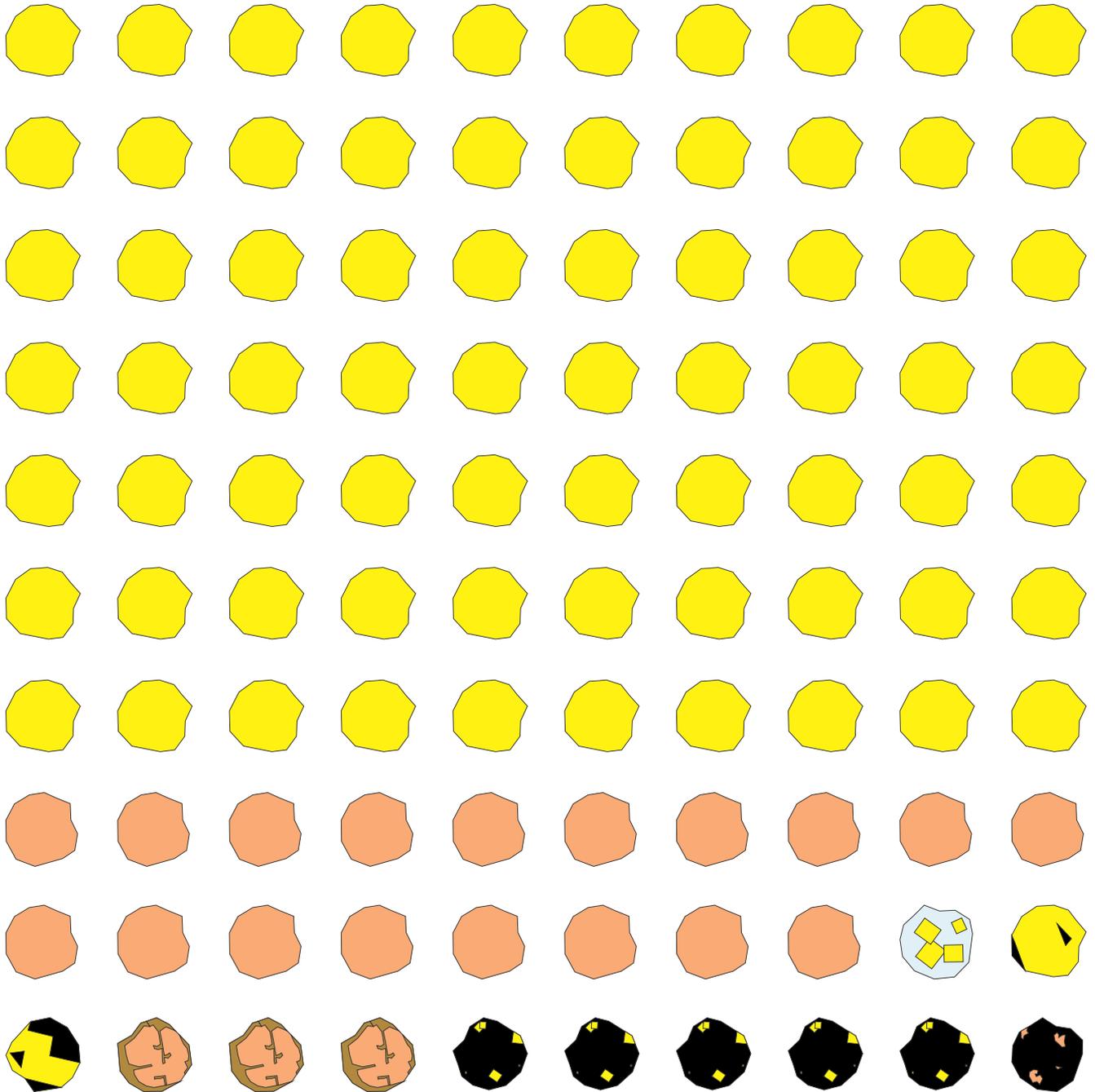
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Py/Po SCAN

H +8μm

June

2014



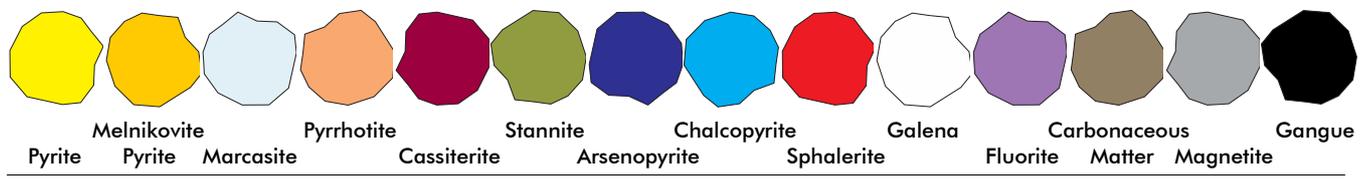
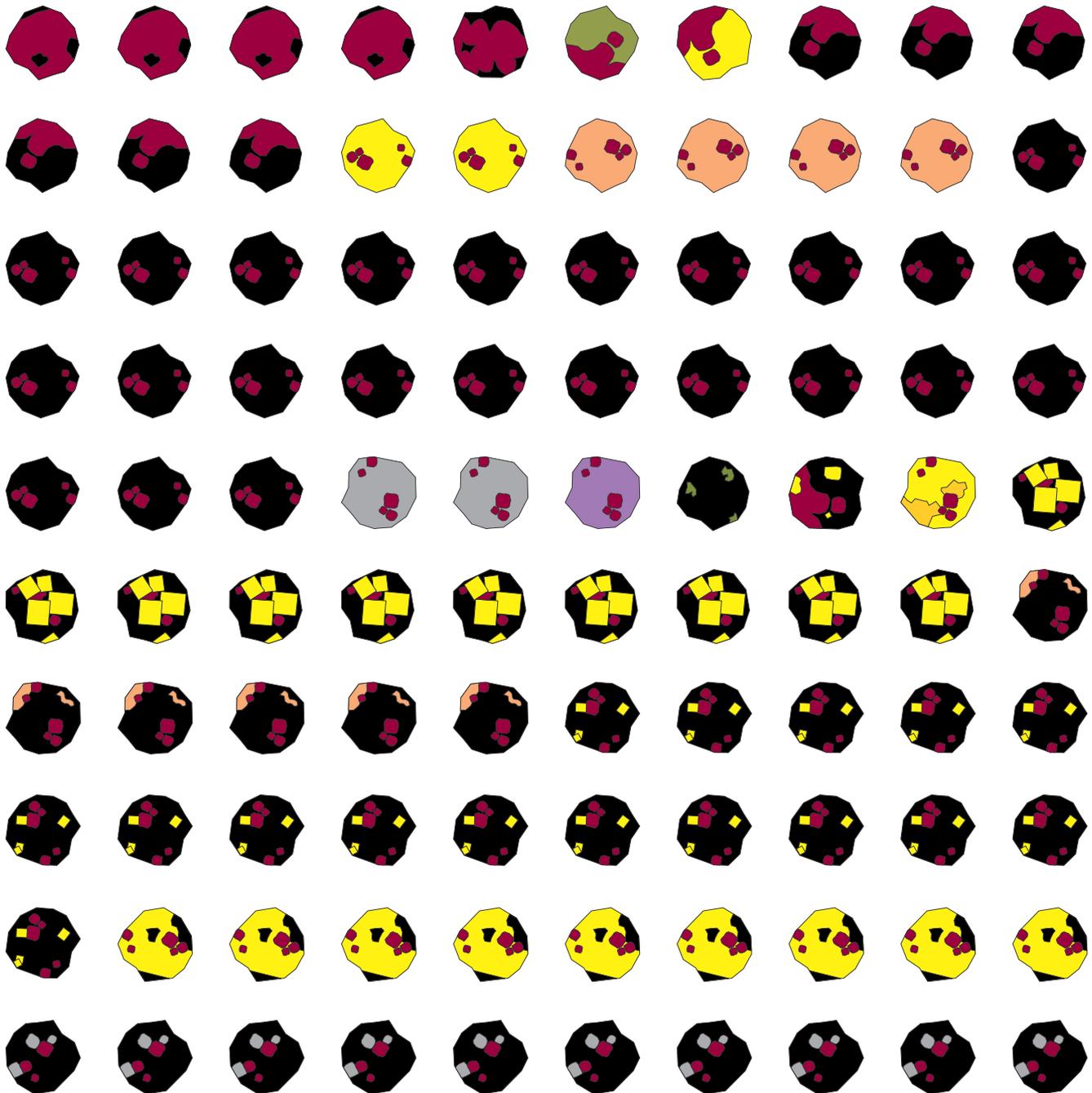
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

A +212µm

June

2014



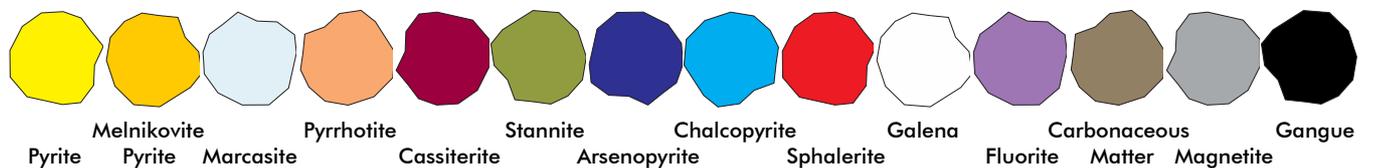
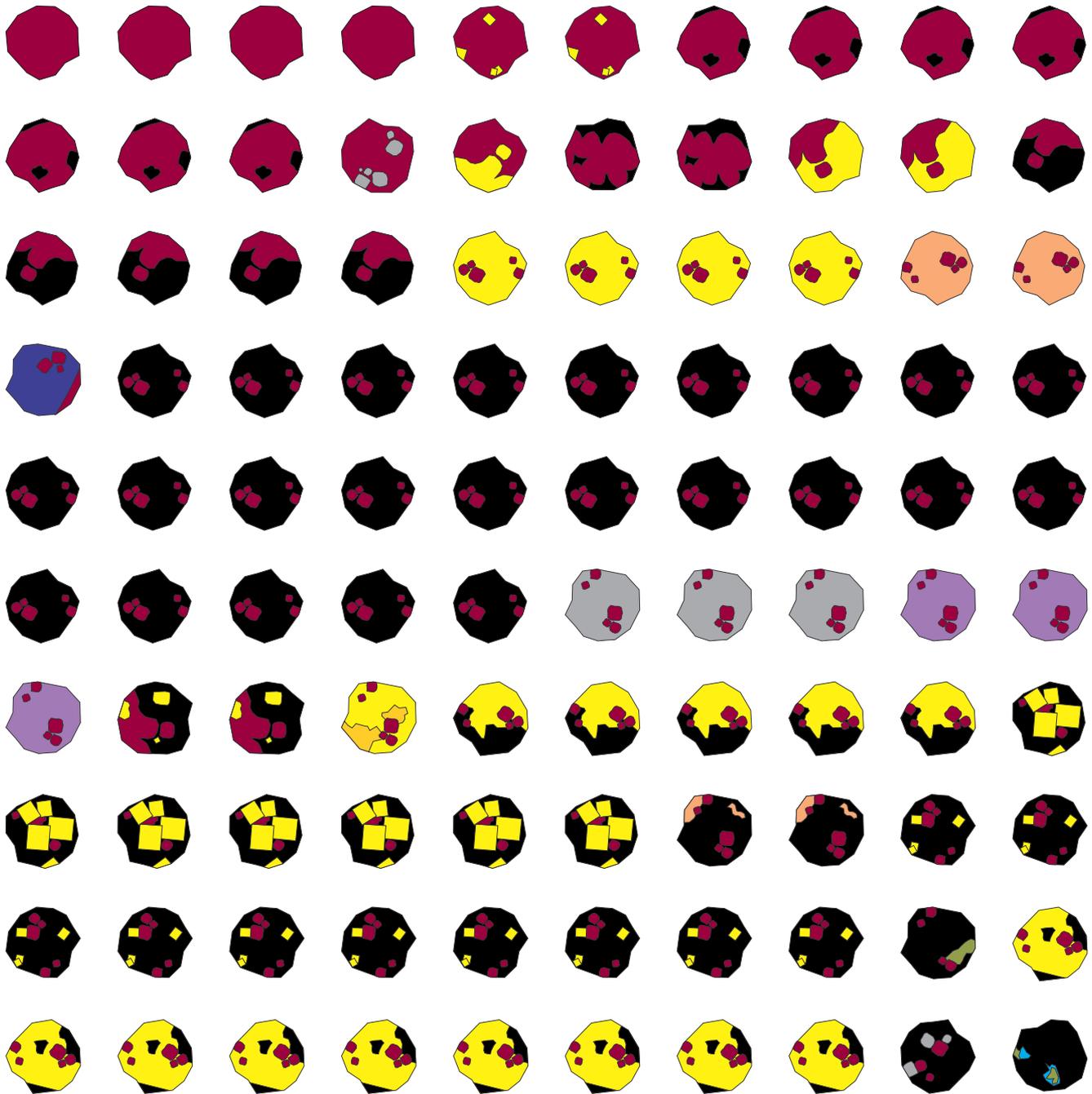
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

B + 150µm

June

2014



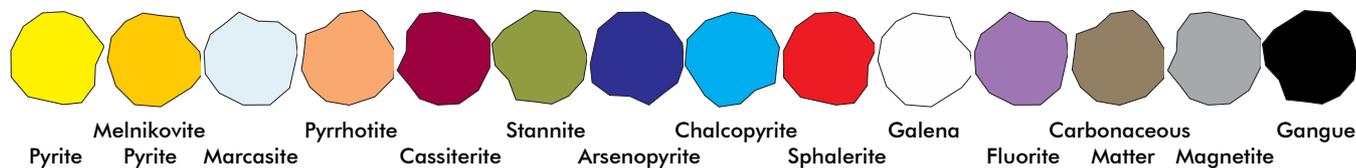
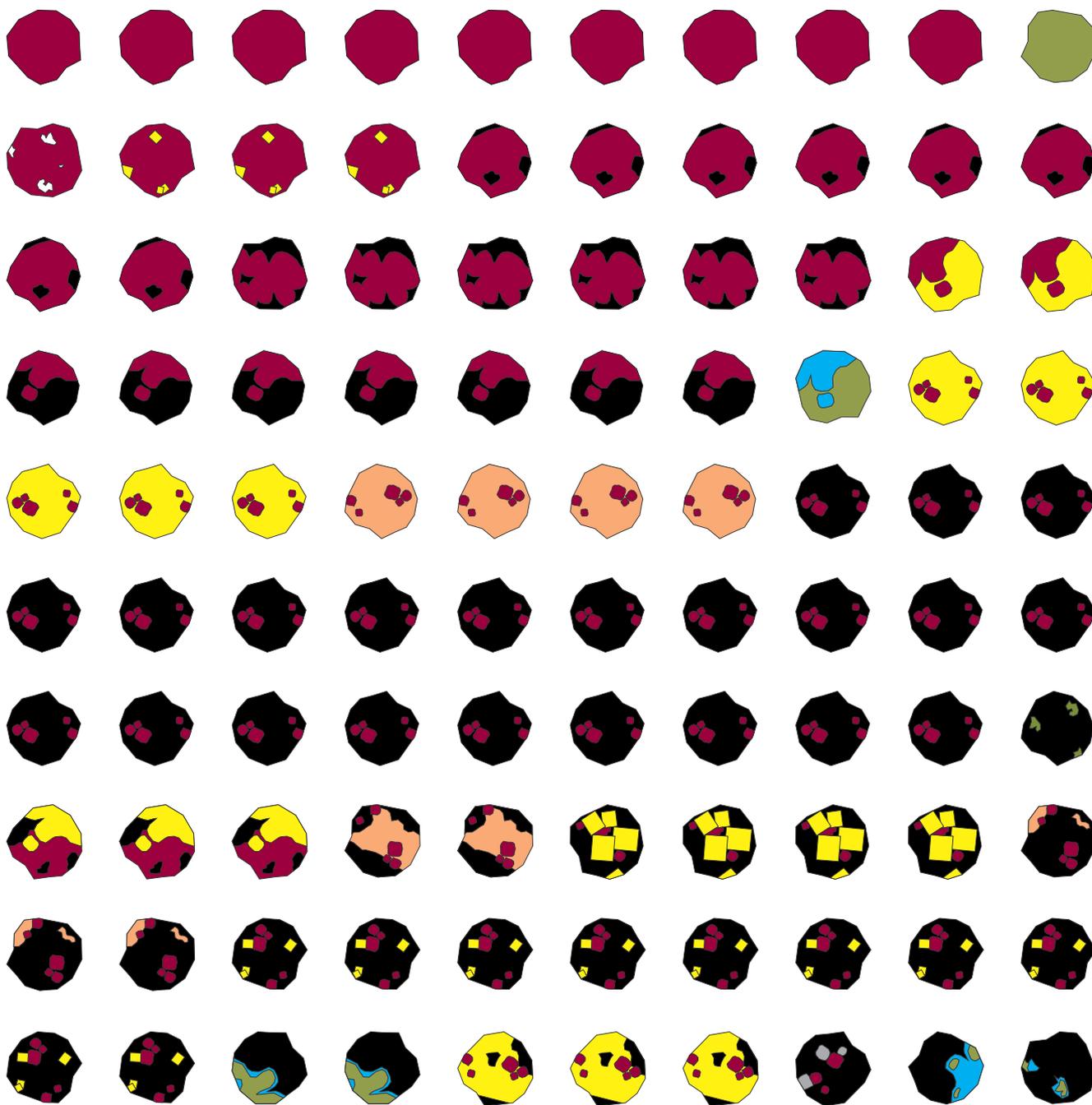
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

C + 106µm

June

2014



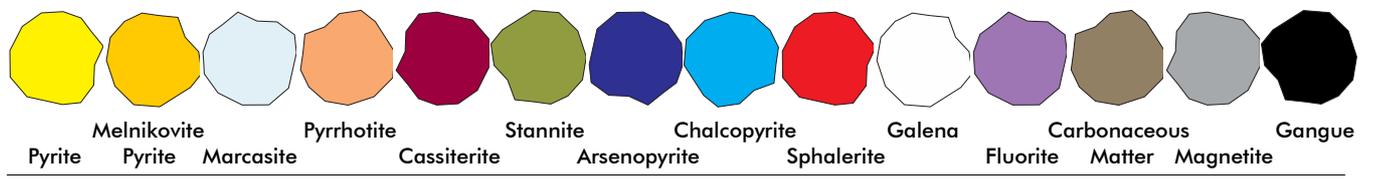
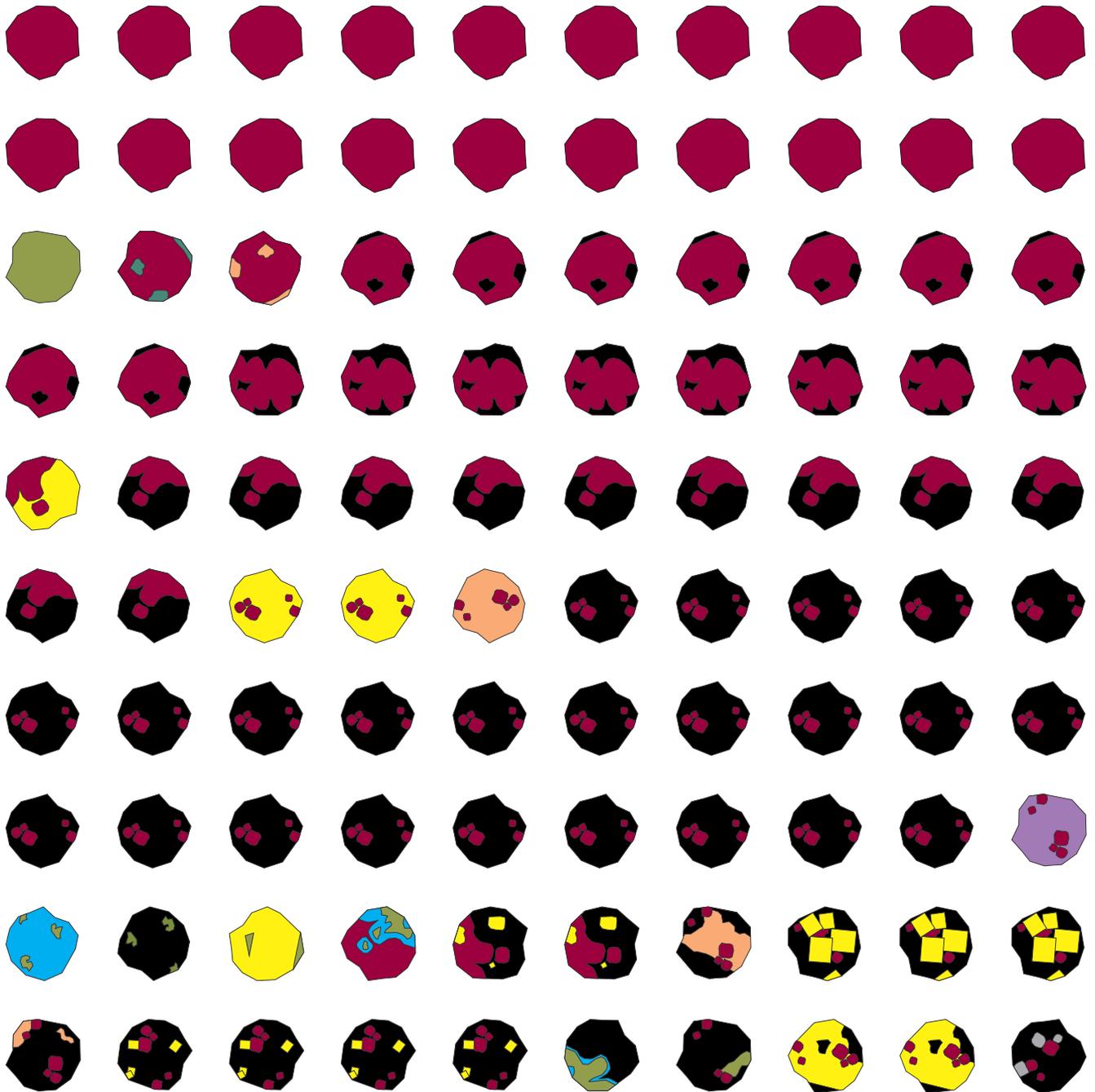
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

D +75µm

June

2014



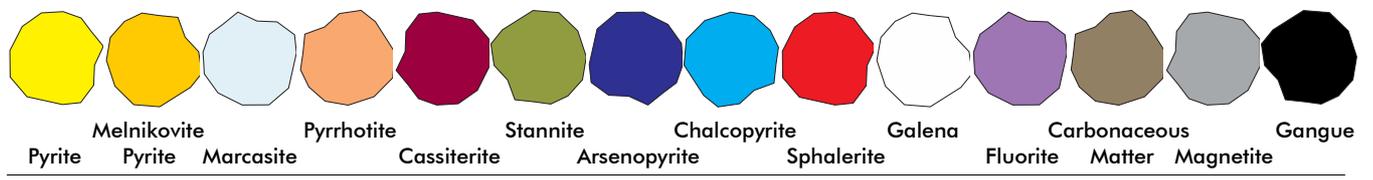
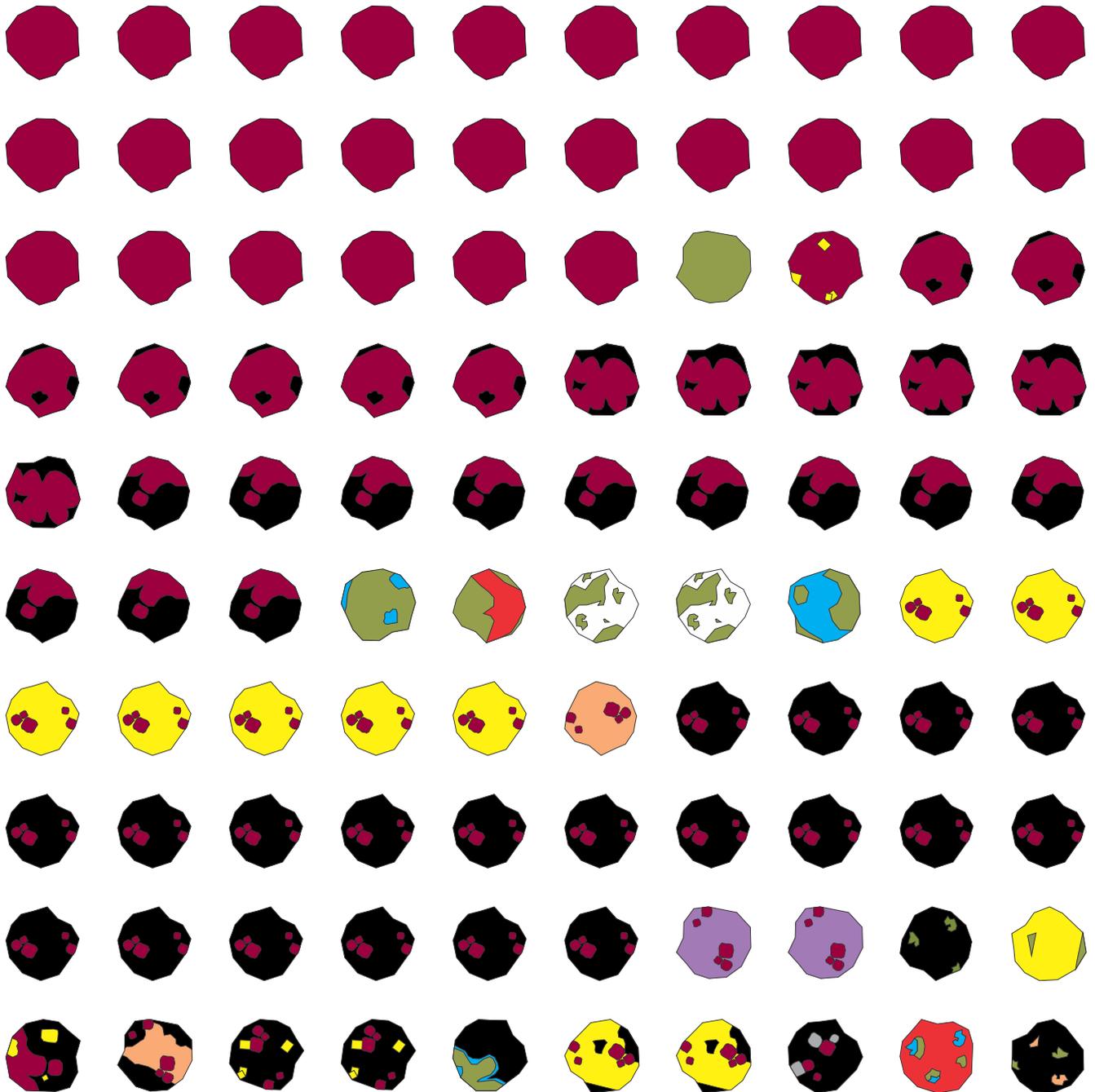
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

E +53µm

June

2014



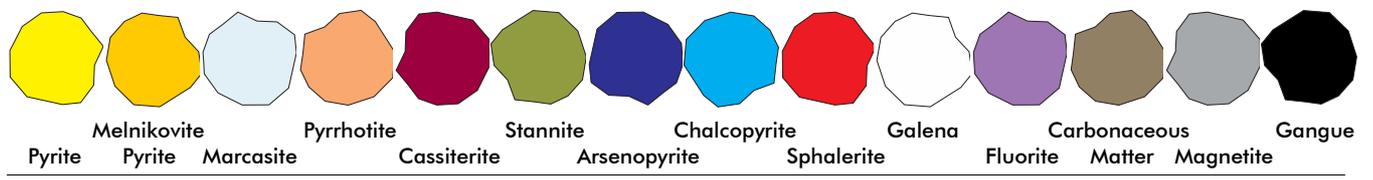
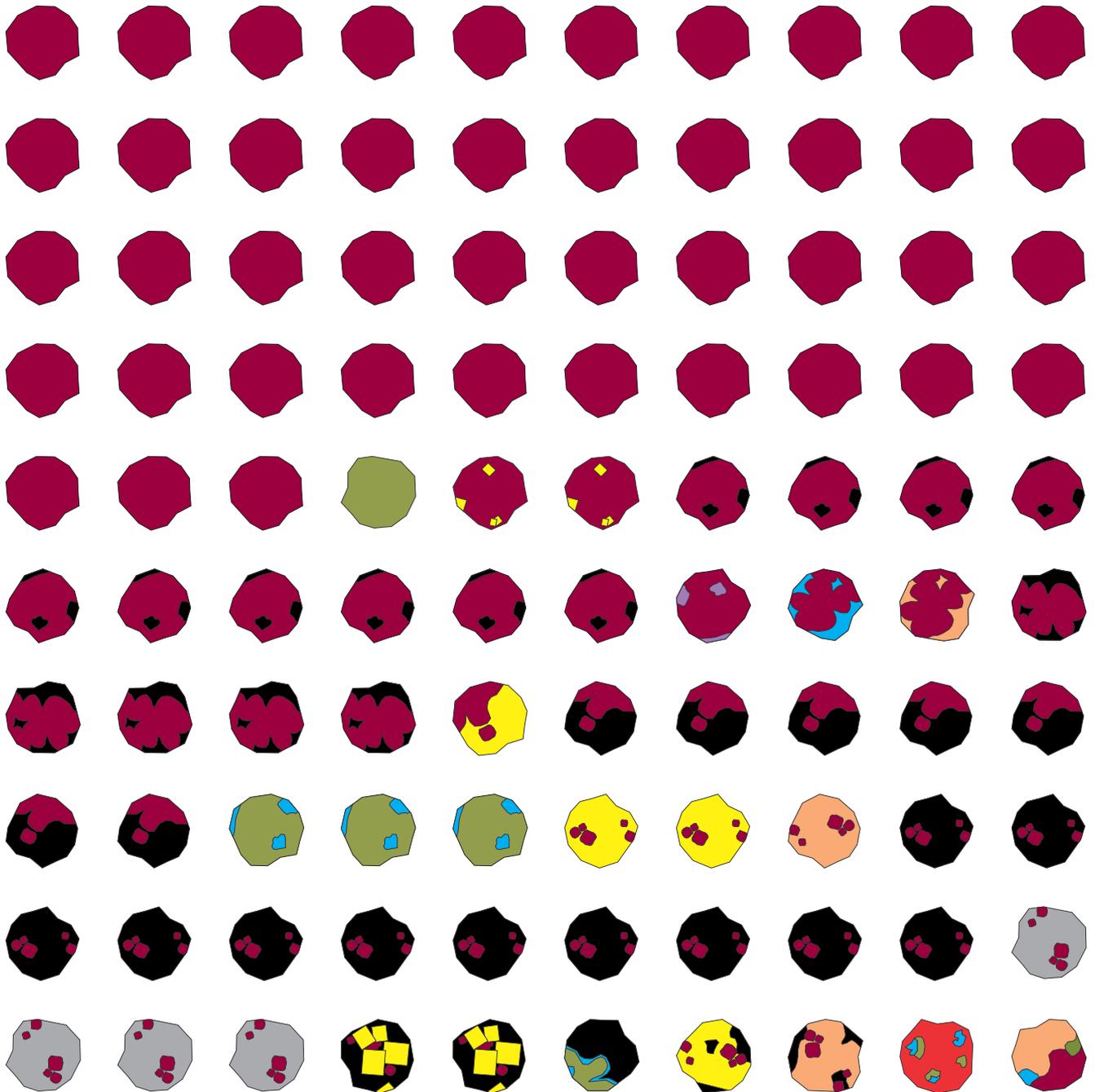
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

F +38µm

June

2014



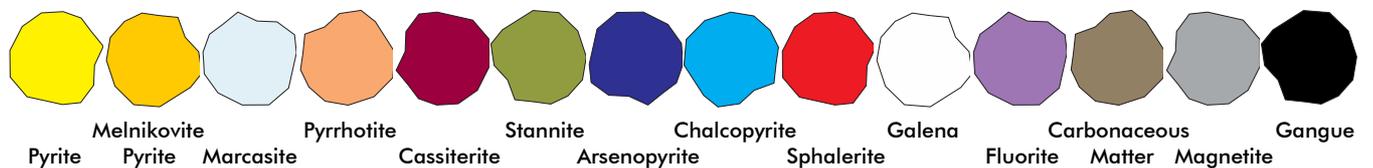
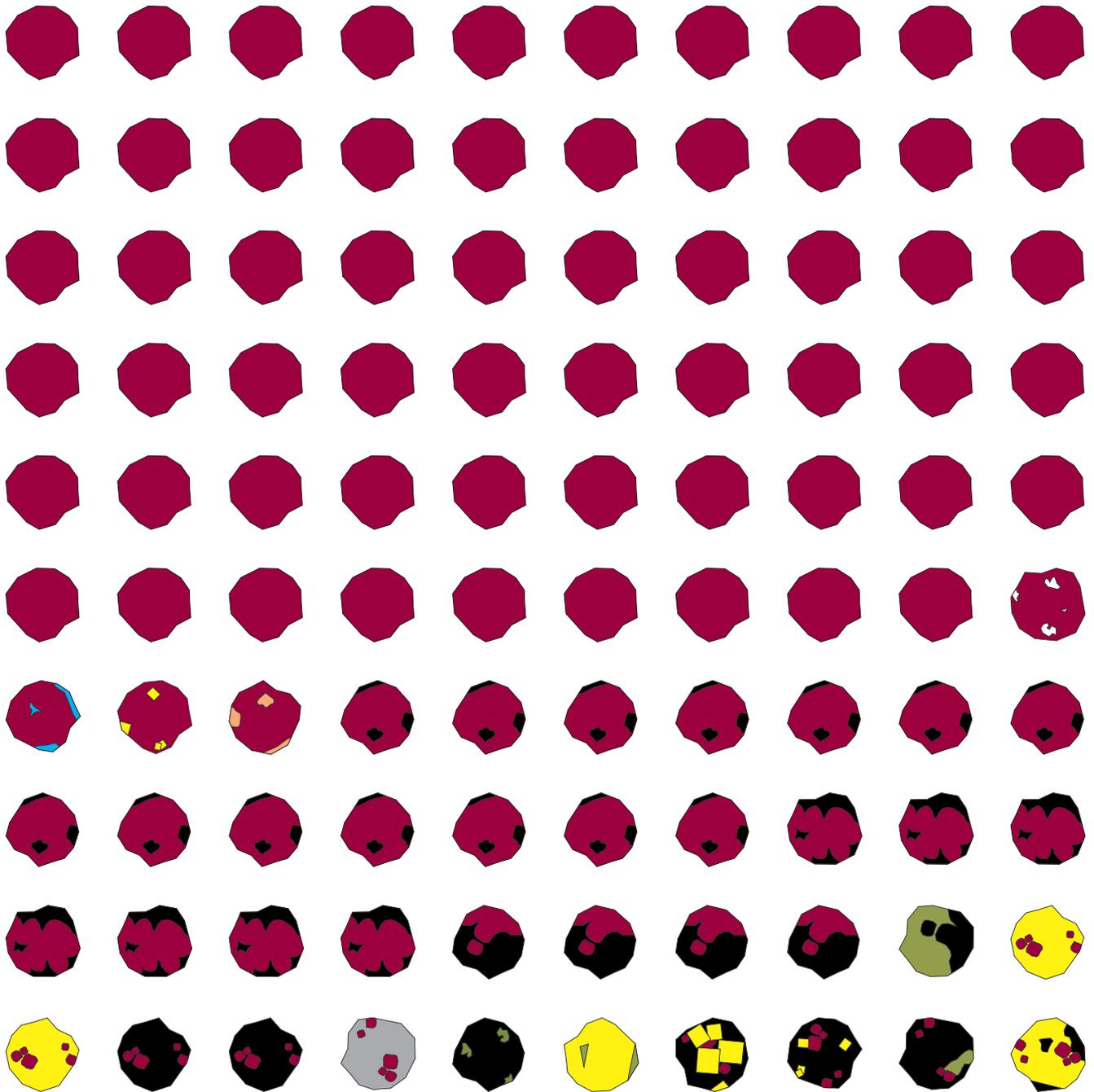
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

G +20µm

June

2014



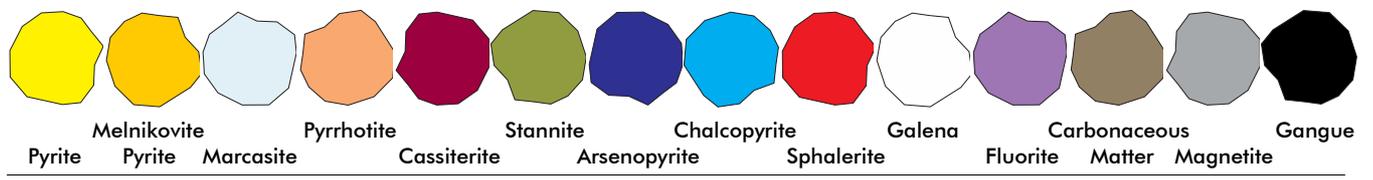
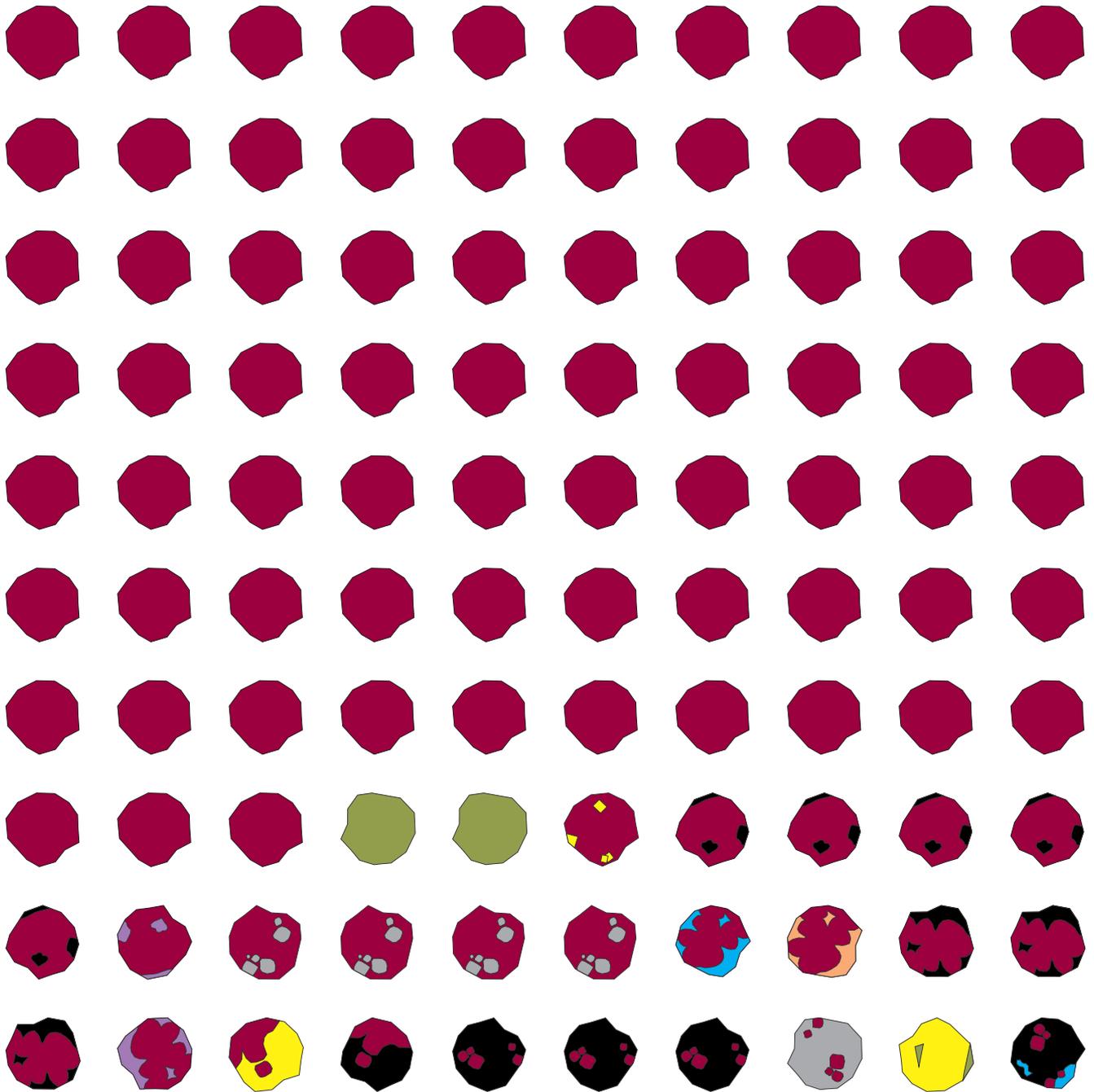
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Sn
SCAN

H +8μm

June

2014



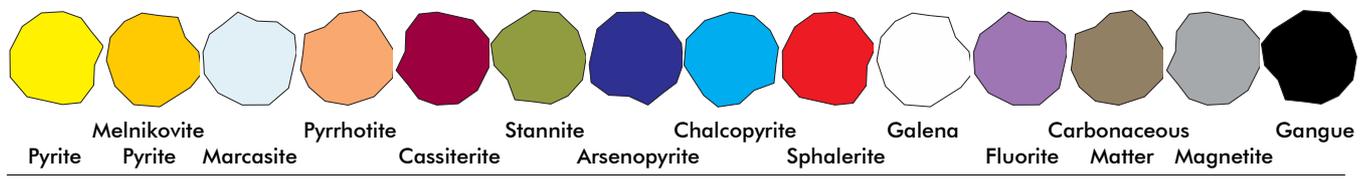
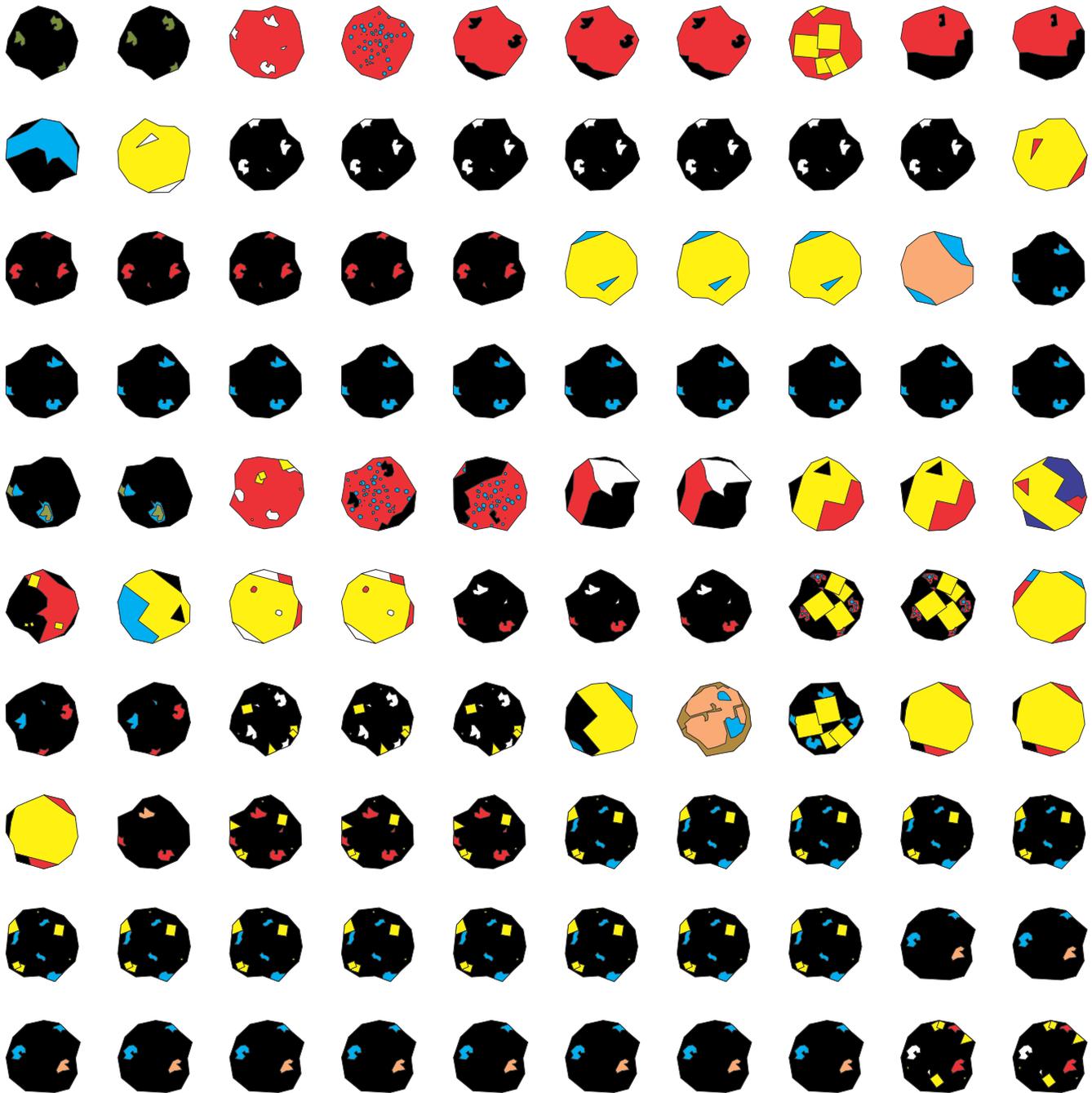
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

A +212µm

June

2014



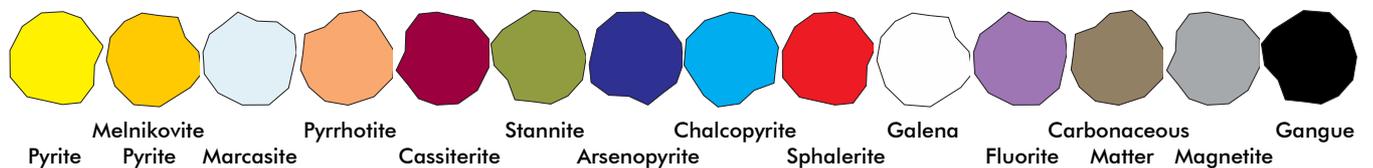
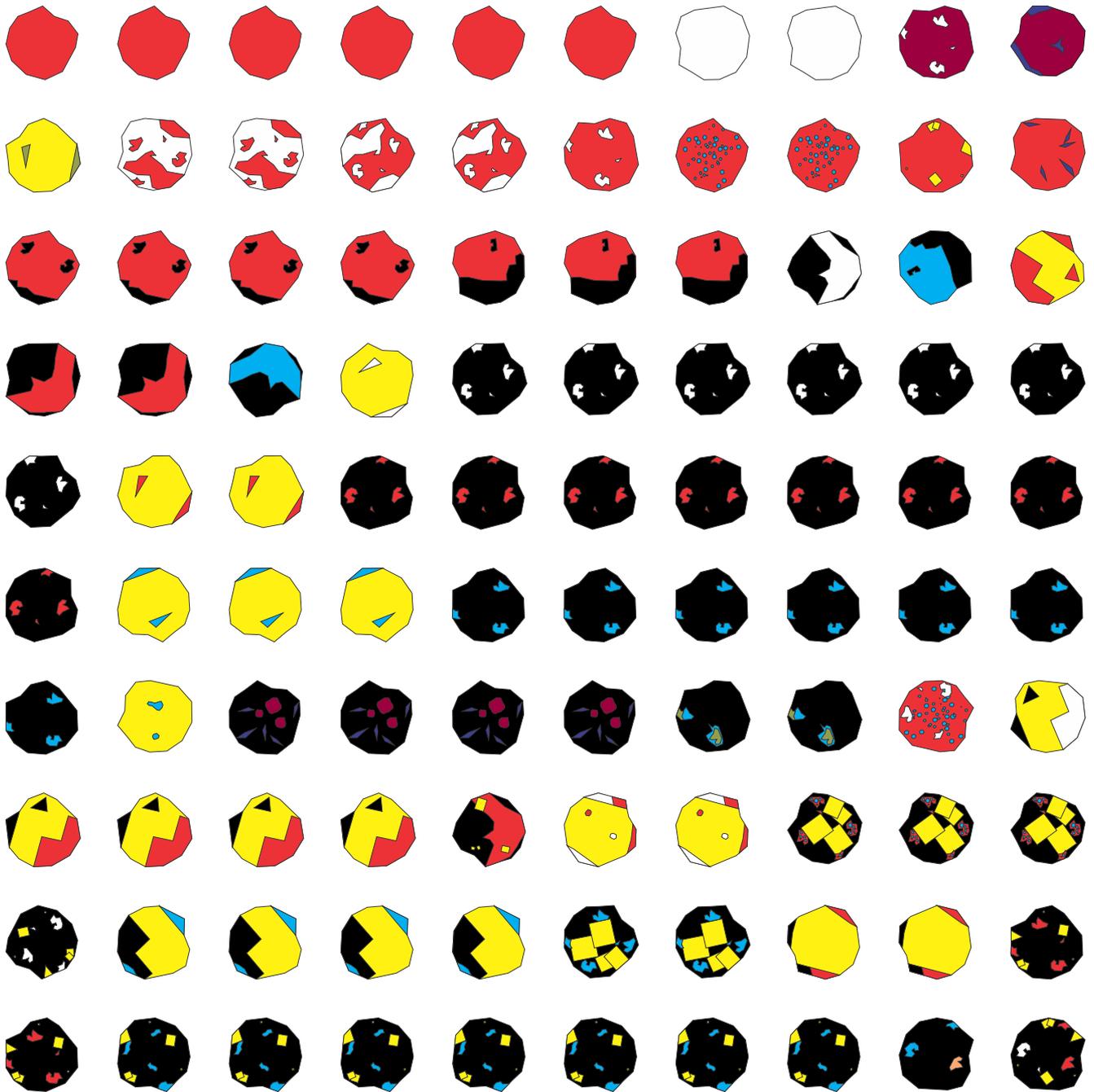
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

B + 150µm

June

2014



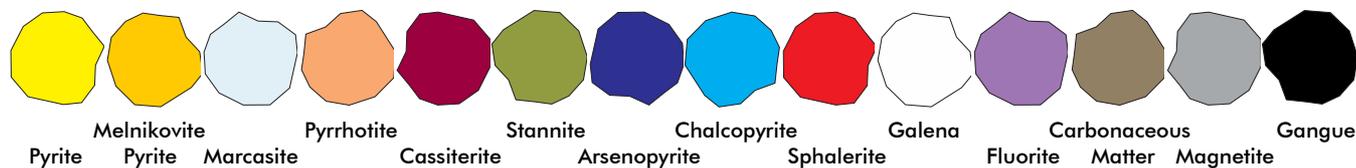
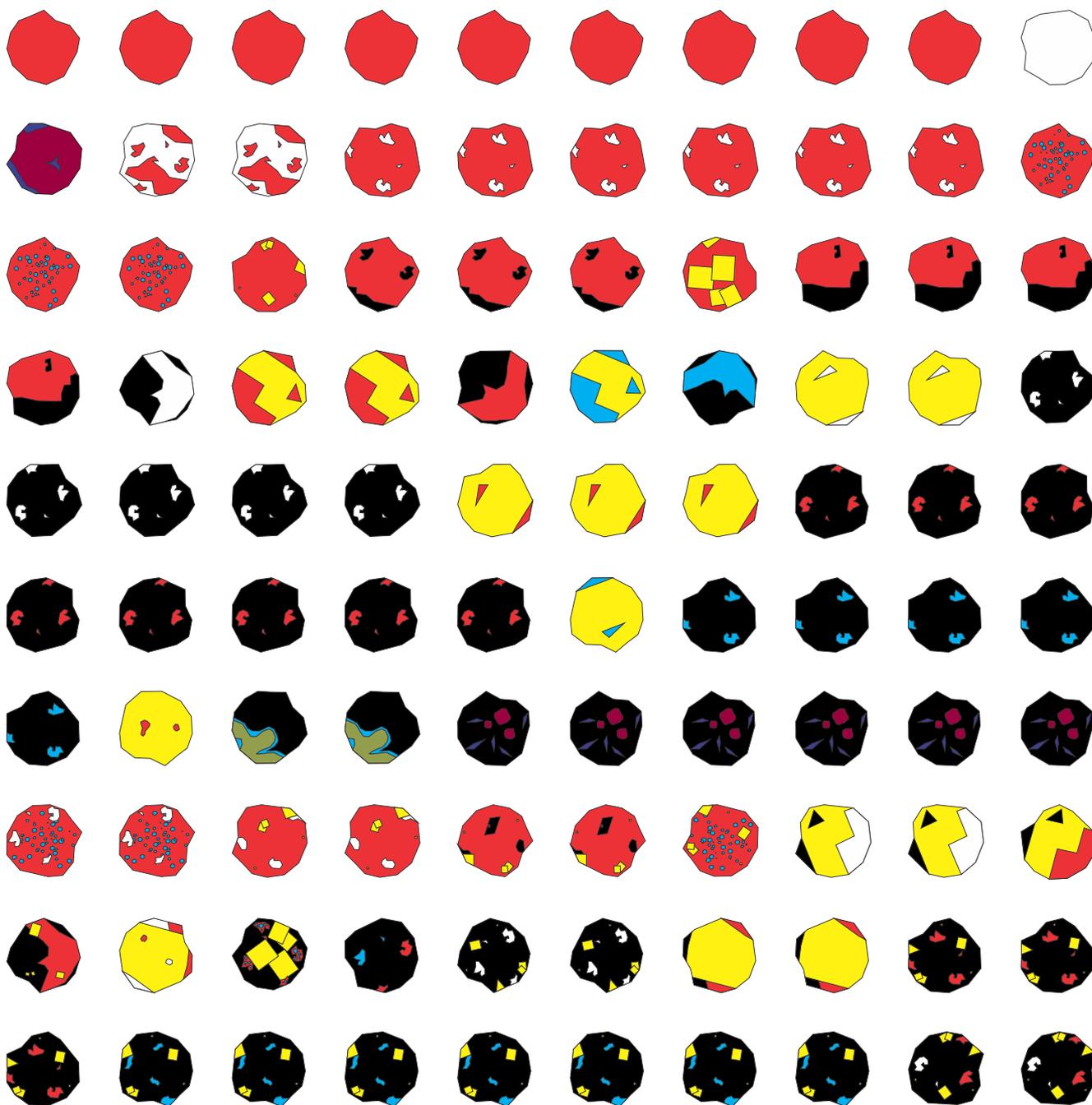
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

C + 106µm

June

2014



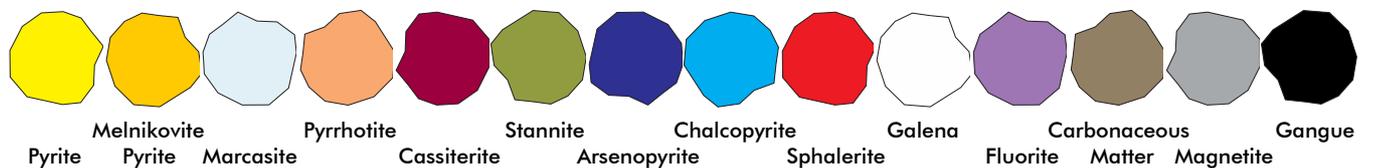
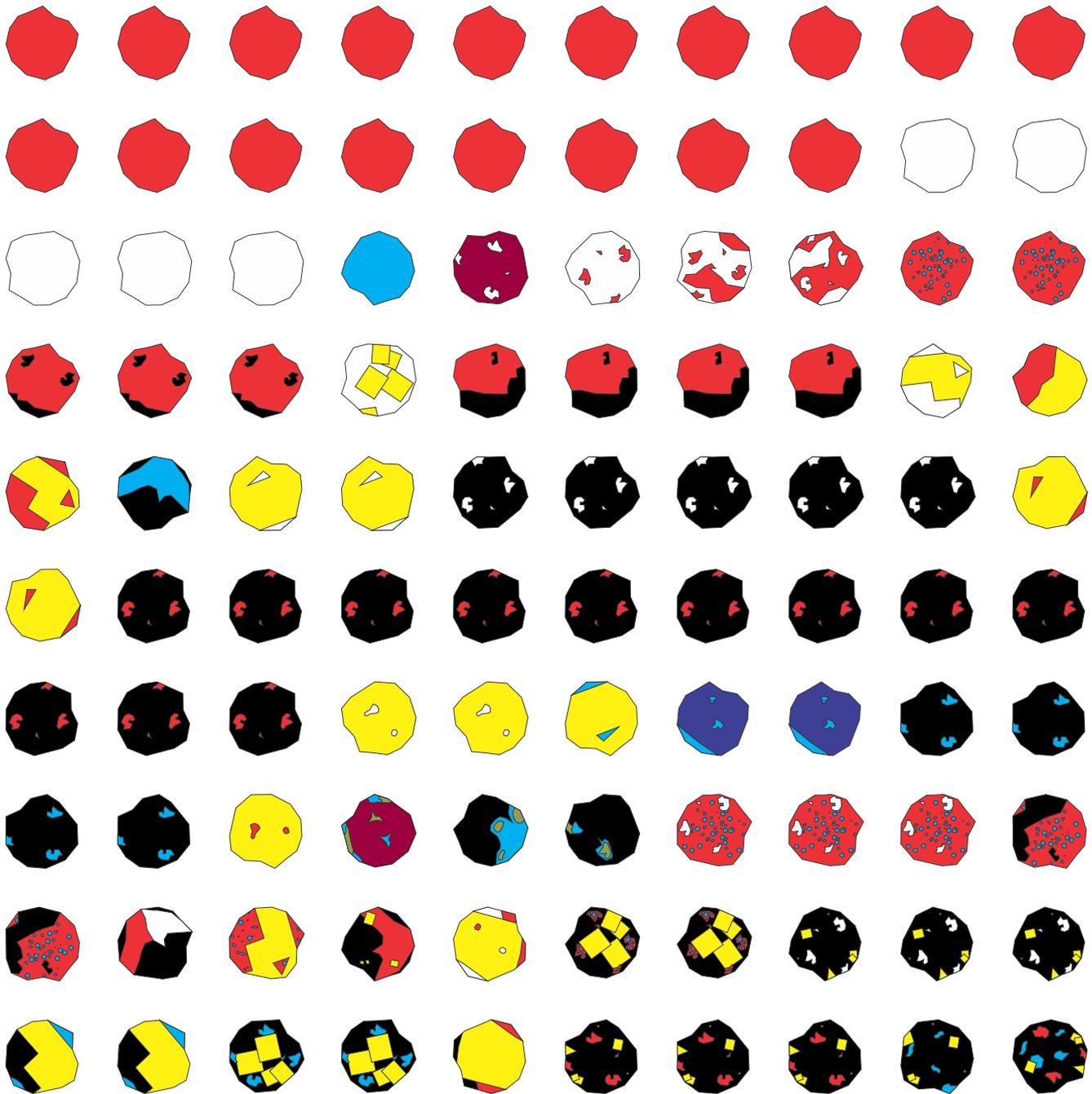
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

D +75µm

June

2014



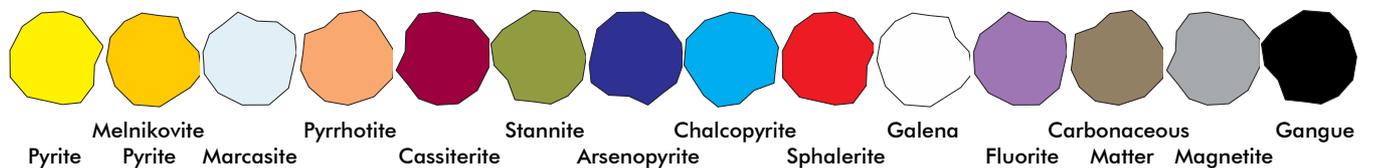
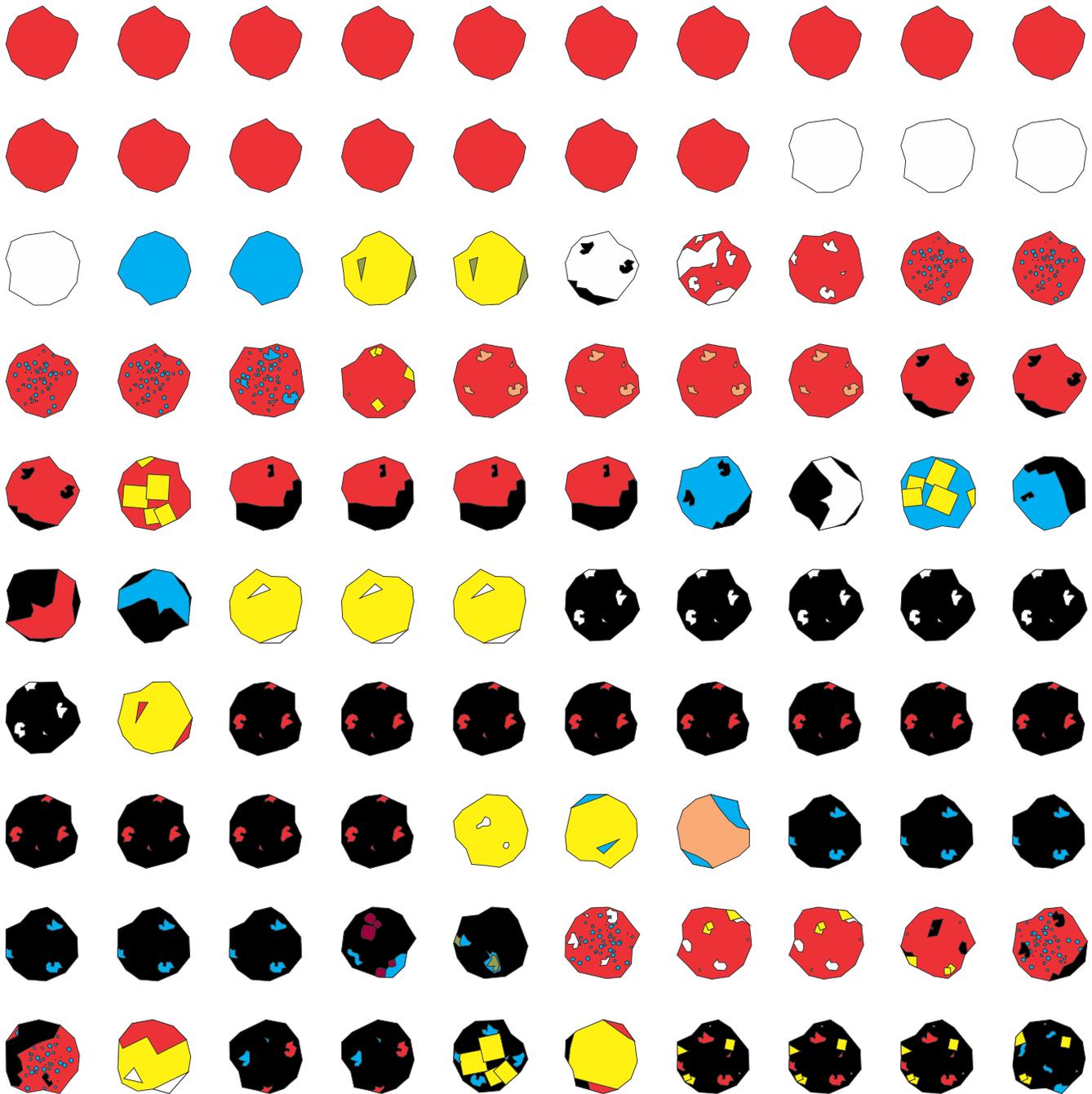
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

E +53µm

June

2014



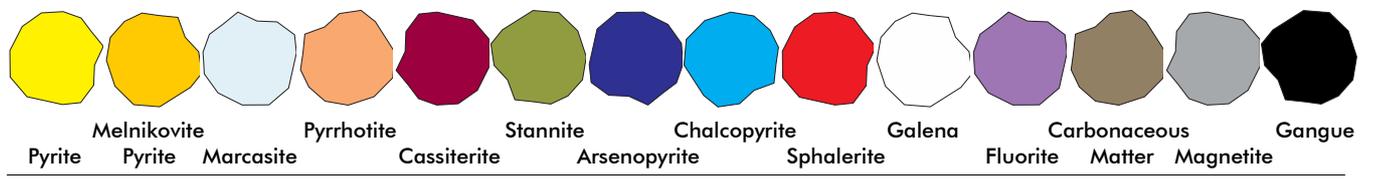
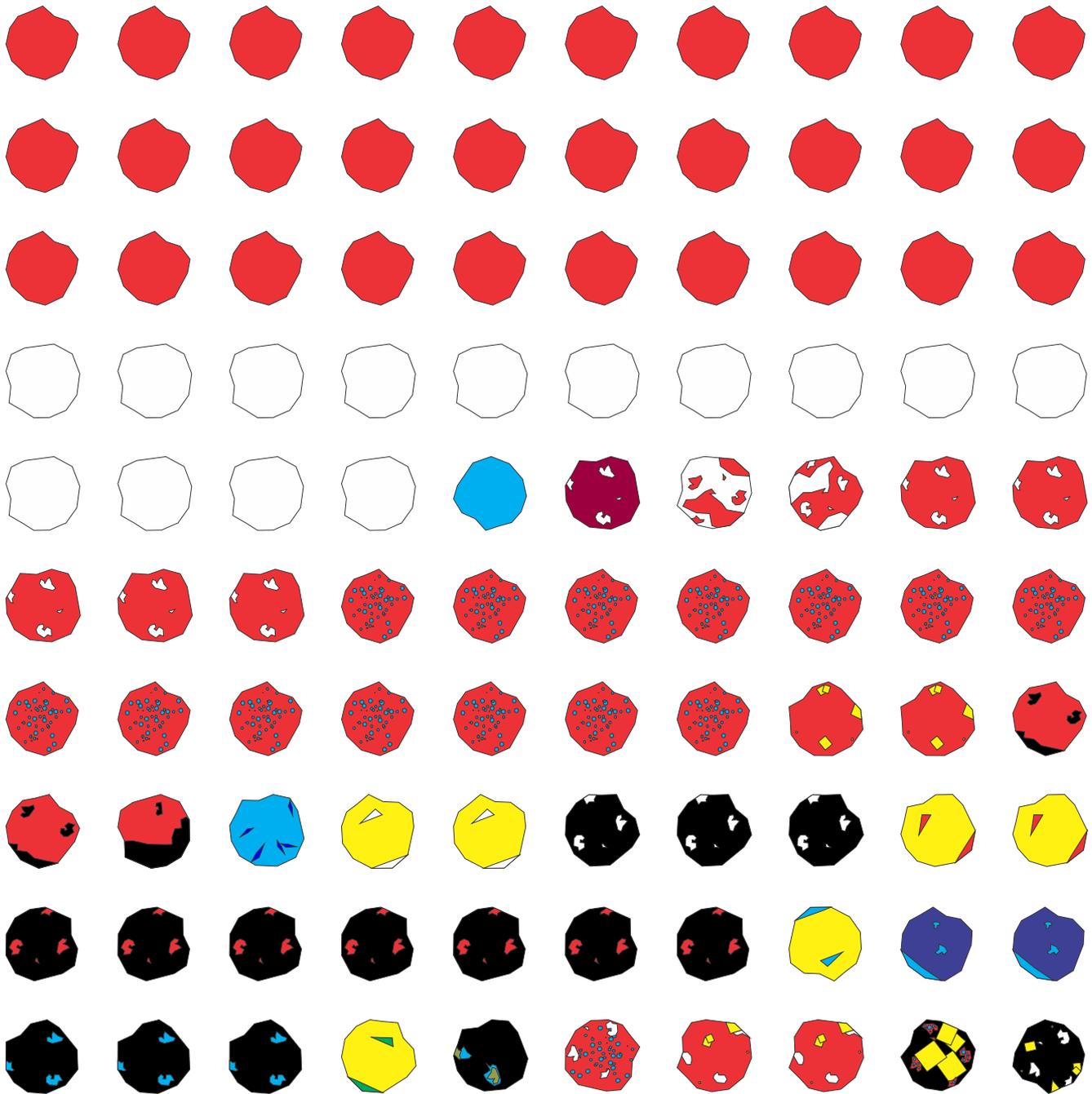
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

F +38µm

June

2014



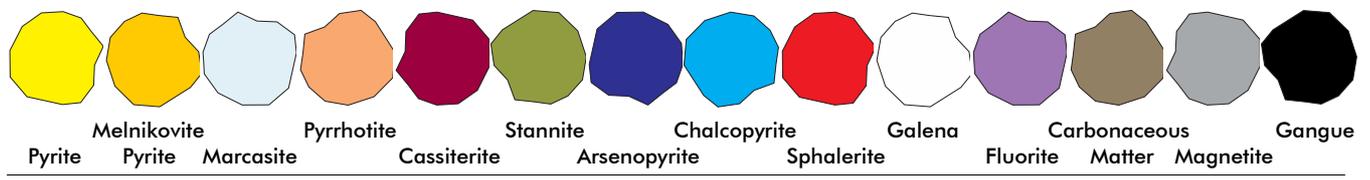
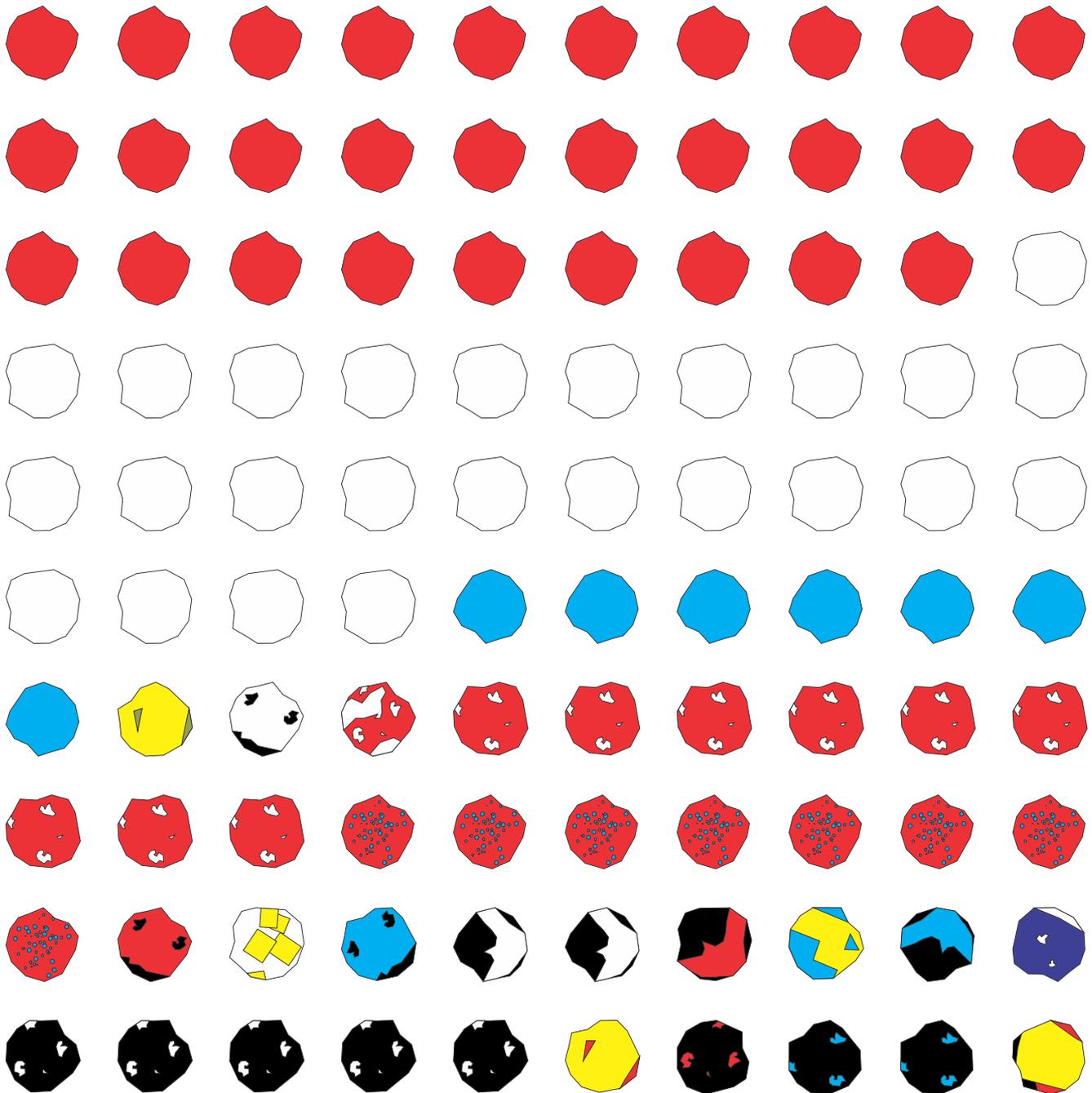
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

G +20µm

June

2014



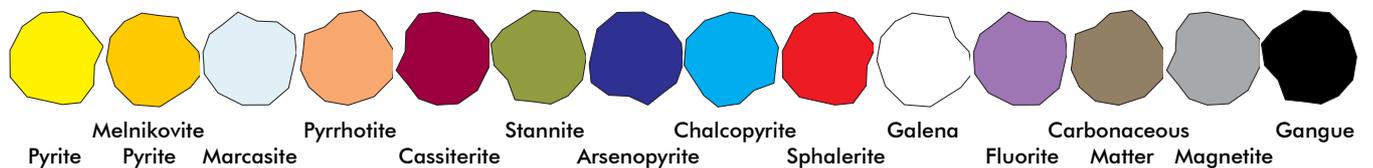
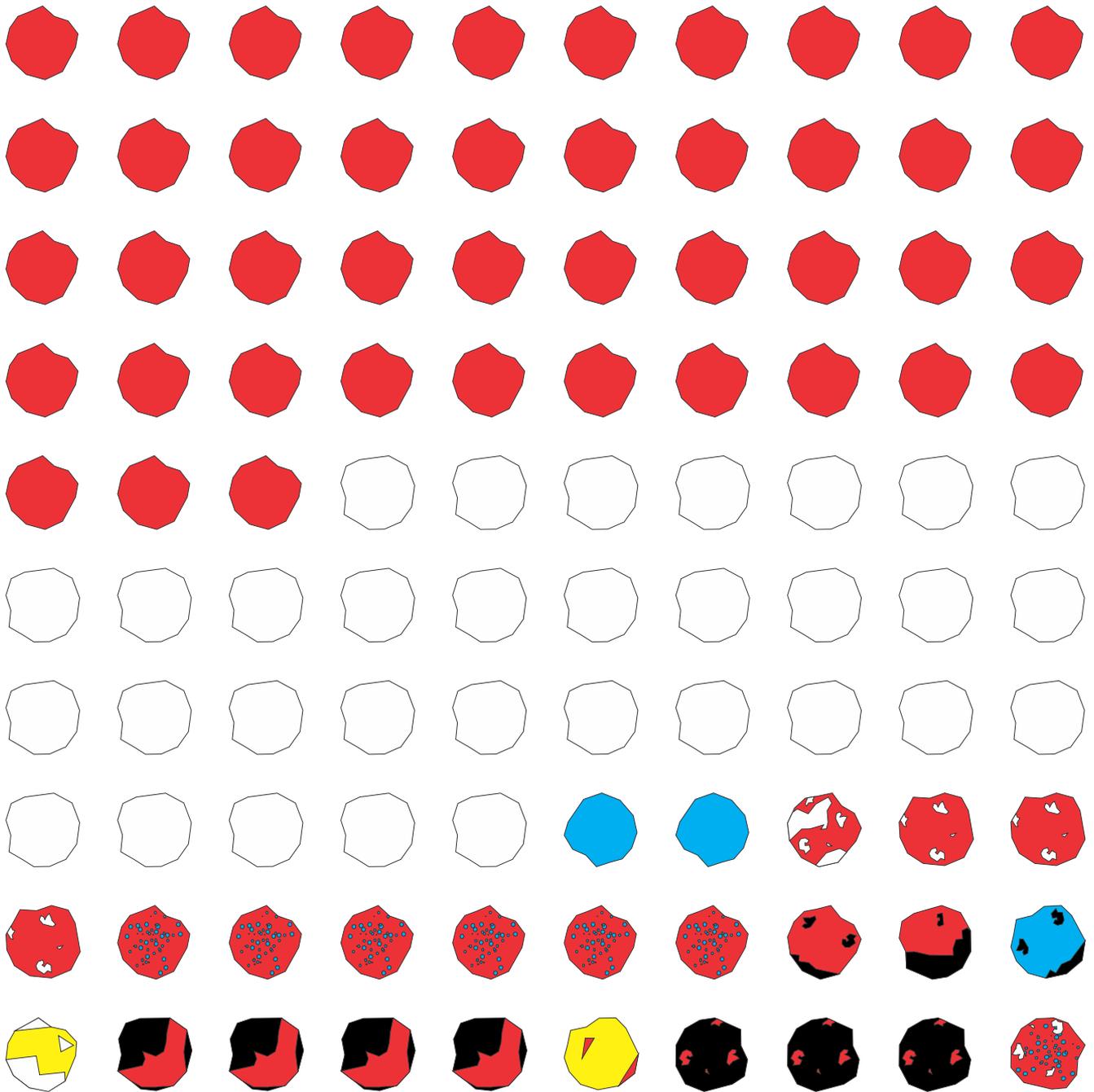
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp Non-
PyPoAs Sulphide SCAN

H +8μm

June

2014



ALS Metallurgy

STELLAR RESOURCES LTD
Heemskirk Tin Project

Severn Bulk Composite
Sulphide Tail Mineralogy

JULY 2014

MODA
microscopy

McArthur Ore Deposit Assessments Pty Ltd

Gary J McArthur PhD FAusIMM MMICA MSEG

Suite 6, 1st Floor, Brownell Place, 11 Wilson St (P.O. Box 1303) Burnie TAS 7320 AUSTRALIA
Tel (03) 6431 1701 Fax (03) 6431 1278 Mobile 0419 367240 email gary@modapl.com.au

ALS METALLURGY

Stellar Resources – Severn Bulk Composite Sulphide Tail Mineralogy July 2014

Method

A sulphide tail produced from a Bulk Composite sample from Stellar Resources' Severn Prospect was submitted for mineralogical assessment. The sample was sized into 5 fractions: +212µm, +106µm, +53µm, +20µm and +8µm and these were mounted on two polished mounts by Australian Petrographics (Queanbeyan, NSW).

The standard MODA technique was adopted to quantify the mineralogy, using two scans.

In a first scan, for each fraction, 100 grains were selected at random and the area % of each mineral present was visually estimated. The minerals logged were: *pyrite+marcasite* (Py), *pyrrhotite* (Po), *cassiterite* (Cs), *stannite* (St), *arsenopyrite* (As), *chalcopyrite* (Cp), *sphalerite+galena* (SpGn) and *gangue* (*quartz, silicates, carbonates, etc*, Ga). This allowed calculation of an overall mineralogical composition.

In a second scan, for each fraction, 100 grains containing cassiterite or stannite were selected at random and logged as per the first scan. This improved the count statistics for the Sn mineralisation.

The normal liberation and association parameters were calculated. Cumulative yield curves for *cassiterite* were calculated for each fraction.

Results

Composition

The following minerals were identified, in approximate descending order:

- *Gangue* (*quartz, silicates, carbonate, rutile, carbonaceous matter, fluorite, talc* etc.)
- *Magnetite* (preferentially represented in the +106µm fraction)
- *Pyrite* (78% crystalline and 22% *melnikovite*)
- *Cassiterite*
- *Pyrrhotite*
- *Sphalerite*
- *Marcasite*
- *Galena*
- *Arsenopyrite*
- *Chalcopyrite*
- *Goethite*
- *Hematite*
- *Stannite* (rare)
- *Native bismuth* (very rare)

The overall composition of the Sulphide Tail is summarised below:

Severn Bulk Comp Sulphide Tail Composition Vol% (from total scan)

Fraction	Wt%	Py	Po	Cs [#]	St [#]	As [#]	Cp [#]	SpGn [#]	Ga
+212µm	26.1	2.3	0.5	0.3	Tr	0	Tr	0.5	96.5
+106µm	17.4	5.1	0.4	1.9	Tr	0	0	0.1	92.5
+53µm	12.8	2.5	1.1	2.0	Tr	1.0	0	0	93.4
+20µm	12.7	2.8	1.0	0.1	Tr	0	0	0	96.2
+8µm	10.0	4.4	0	2.3	0	0	0	1.0	92.3
TOTAL	79.0	3.3	0.6	1.1	Tr	0.2	Tr	0.3	94.5

Py=pyrite, Po=pyrrhotite, Cs=cassiterite, St=stannite, As=arsenopyrite, Cp=chalcopyrite, SpGn=sphalerite+galena, Ga=gangue
count statistics are very poor for the scarce minerals

The composition of the grains containing *cassiterite* and *stannite* is summarised below. Note the residence of Sn sums to >99.9% in *cassiterite* and <0.1% in *stannite*.

Severn Bulk Comp Sulphide Tail Composition Vol% (from Sn scan)

Fraction	Sn Wt%	Py	Po	Cs	St	As	Cp	SpGn	Ga
+212µm	13.3	6.1	1.8	11.3	0.1	0	Tr	0.1	80.6
+106µm	17.8	4.8	0.5	29.5	0.3	Tr	0.2	Tr	64.7
+53µm	16.7	0.2	1.0	48.0	0.1	Tr	0.3	Tr	50.4
+20µm	21.2	Tr	0.3	74.6	Tr	0	0.1	0	25.0
+8µm	17.9	0.9	1.0	86.9	0	0	0	0	11.2
TOTAL	86.9	2.1	0.8	53.1	0.1	Tr	0.1	Tr	43.7

Liberation and Association

Essential summaries of the liberation parameters *cassiterite* are:

Severn Bulk Comp Sulphide Tail Cassiterite liberation distribution%

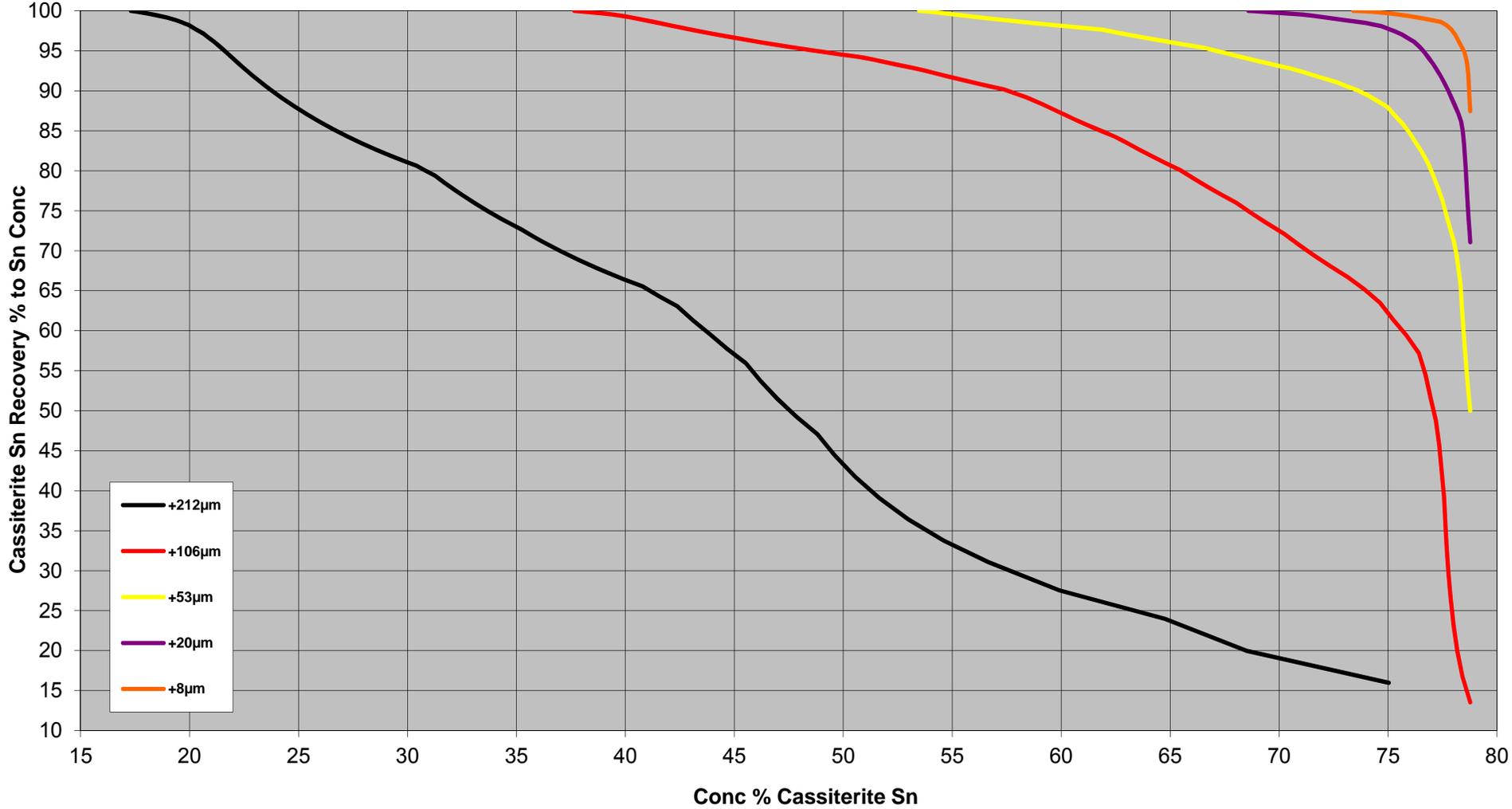
Fraction	Sn Wt%	Free	Binary with						Ternary+
			Py	Po	St	Cp	As	Ga	
+212µm	13.3	0	0	0	0	0	0	73	27
+106µm	17.8	14	3	3	0	0	0	70	10
+53µm	16.7	50	0	0	0	0	0	47	2
+20µm	21.2	71	0	0	0	1	0	27	1
+8µm	17.9	87	0	1	0	0	0	10	1
TOTAL	86.9	48	1	1	0	0	0	43	7

Severn Bulk Comp Sulphide Tail Cassiterite association%

Fraction	Sn Wt%	%associated with					
		Py	Po	St	Cp	As	Ga
+212µm	13.3	18	16	0	1	0	100
+106µm	17.8	12	5	0	1	0	80
+53µm	16.7	0	1	0	2	2	50
+20µm	21.2	0	0	0	1	0	28
+8µm	17.9	0	2	0	0	0	11
TOTAL	86.9	5	4	0	1	0	50

Stannite is a rare fine-grained component, mainly hosted by *chalcopyrite*, but also *sphalerite*, *pyrite*, *cassiterite* and gangue.

Severn Bulk Composite - Sulphide Flotation Tail Cumulative Yield Curves

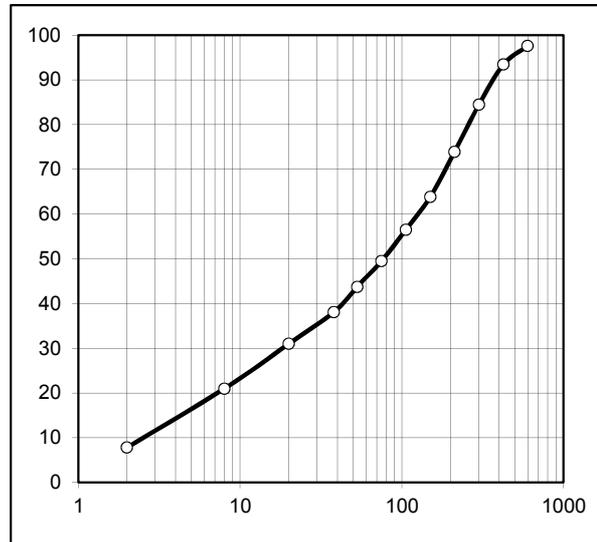




BURNIE LABORATORY
 SIZE ANALYSIS REPORT SHEET WITH CS6

PROJECT	T0879
SAMPLE	SBC Sulphide Tails
DATE	70614
TECHNICIAN	MS

SBC Sulphide Tails	SIZE um	WEIGHTS			
		gm	(%)	%PASS	
P80	600	4.32	2.44	97.6	
	425	7.34	4.15	93.4	
	300	15.89	8.99	84.4	
	263	18.62	10.54	73.9	
	150	17.83	10.09	63.8	
	106	12.92	7.31	56.5	
	75	12.33	6.98	49.5	
	53	10.21	5.78	43.7	
	38	10.02	5.67	38.1	
	20	12.48	7.06	31.0	
MINS 20	CS5	8	17.75	10.04	21.0
CENTRIFUGE	CS6	2	23.24	13.15	7.8
	SUB	13.79	7.80	0.0	
	TOTAL	176.7	100.0		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mount Number
		%	dist	%	dist	%	dist	%	dist	%	dist	
212	26.12	0.68	13.3	16.85	22.5	0.09	13.8	3.05	25.9	48.70	31.1	879194
106	17.40	1.37	17.8	18.40	16.4	0.08	8.2	2.45	13.8	45.60	19.4	879195
53	12.75	1.75	16.7	18.00	11.7	0.05	3.8	2.75	11.4	39.50	12.3	879196
20	12.73	2.23	21.2	21.20	13.8	0.16	12.0	2.71	11.2	39.90	12.4	879197
8	10.04	2.39	17.9	24.60	12.6	0.38	22.4	3.00	9.8	31.60	7.8	897198
2	13.15	0.51	5.0	21.70	14.6	0.25	19.3	4.16	17.8	34.70	11.2	
CAL <2	7.80	1.41	8.2	20.87	8.3	0.45	20.5	4.01	10.2	30.64	5.8	
ASSAY	100.0	1.34	100.0	19.55	100.0	0.17	100.0	3.08	100.0	40.90	100.0	

SIZE um	WT %	MnO		CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist	%	dist
212	26.12	0.44	20.2	0.84	23.1	3.76	26.5	9.05	27.7
106	17.40	0.63	19.2	1.00	18.3	3.62	17.0	7.87	16.0
53	12.75	0.61	13.6	1.01	13.6	3.01	10.4	6.34	9.5
20	12.73	0.71	15.9	1.29	17.3	3.28	11.3	6.64	9.9
8	10.04	0.78	13.7	1.20	12.7	3.27	8.9	6.28	7.4
2	13.15	0.44	10.2	0.85	11.8	4.13	14.7	10.65	16.4
CAL <2	7.80	0.53	7.2	0.40	3.3	5.32	11.2	14.50	13.2
ASSAY	100.0	0.57	100.0	0.95	100.0	3.70	100.0	8.55	100.0

Mineral species logged:
Py-pyrite Po-pyrrhotite Cs-cassiterite
St-stannite As-arsenopyrite
Cp-chalcopyrite SpGn-sphalerite/galena Ga-gangue

Sum of the weight fractions for the sizes examined

All sizings combined **73%** of sample

Average composition - all grains

Py	Po	Cs	St	As	Cp	SpGn	Ga	n
19.3	0.6	18.5	0.8	0.0	2.0	0.8	58.0	300
84	0	90	0	29	0	97	48	

Mineral content as area %

Total number of grains logged

Average area % per grain when present

Assays calculated from mineral area % using theoretical compositions

ASSAYS

	SG	Sn	S	As	Fe	Cu
Calc'd	5.29	57.1	4.8	0.5	5.8	0.02
Actual		55.2	8.9	0.39	8.3	

Sizing assay if provided

COMPOSITE PROPORTIONS

	Py	Po	Cs	St	Cp	As	Ga
Mono	49	0	63	0	0	42	72
Binary	50	0	34	0	0	33	26
Ternary	0	0	2	0	0	21	2
Quat.y+	0	0	0	0	0	4	0
% Grains	12	0	69	0	0	3	52

% of mineral fully liberated

% of mineral in grains with 3 minerals present

% of grains with this mineral

% of mineral in grains with 2 minerals present

% of mineral in grains with >3 minerals present

Average number of minerals per grain

BINARY ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	19	0	0	0	81
Po	0		0	0	0	0	0
Cs	0	0		0	0	4	95
St	0	0	0		0	0	0
Cp	0	0	0	0		0	0
As	4	0	7	0	0		89
Ga	13	0	86	0	0	0	

e.g. 95% of all binary Cs occurs with Ga

TOTAL ASSOCIATION MATRIX

	Py	Po	Cs	St	Cp	As	Ga
Py		0	10	0	0	0	41
Po	0		0	0	0	0	0
Cs	2	0		0	0	2	35
St	0	0	0		0	0	0
Cp	0	0	0	0		0	0
As	12	0	15	8	6		50
Ga	3	0	25	0	0	2	

These rows do not sum to 100% because of fully liberated and multi-mineral grains

of all

e.g. 2% of all Cs occurs with As but 15% of all As occurs with Cs

DISTRIBUTION MATRIX

	Free	Binary						Tern	Quat	
		Py	Po	Cs	St	Cp	As			Ga
Py	49		0	9	0	0	0	41	0	0
Po	0	0		0	0	0	0	0	0	0
Cs	63	0	0		0	0	2	33	2	0
St	0	0	0	0		0	0	0	0	0
Cp	0	0	0	0	0		0	0	0	0
As	42	1	0	2	0	0		30	21	4
Ga	72	3	0	23	0	0	0		2	0

e.g. while 63% of Cs is fully liberated, 2% occurs as binaries with As and 33% with Ga. 2% occurs with 2 other minerals

These rows will sum to 100% (unless binary SpGn occurs or unless minor rounding errors occur)

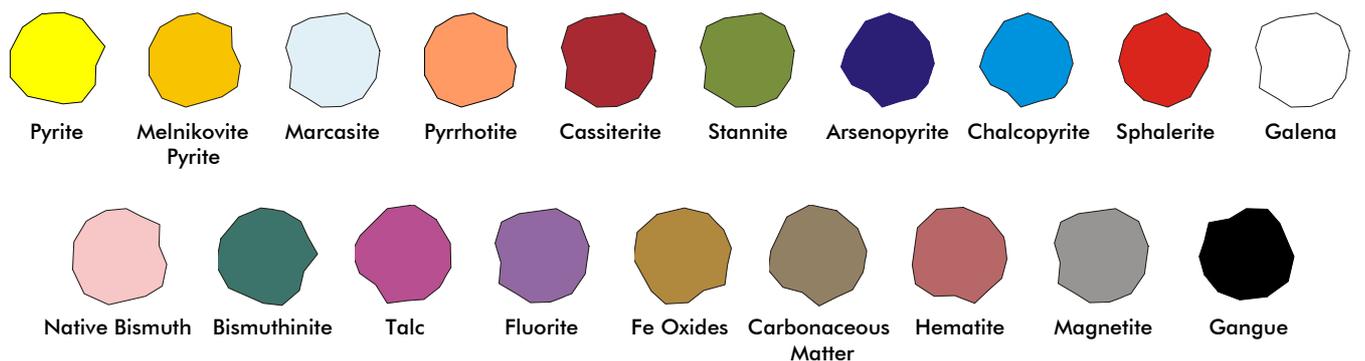
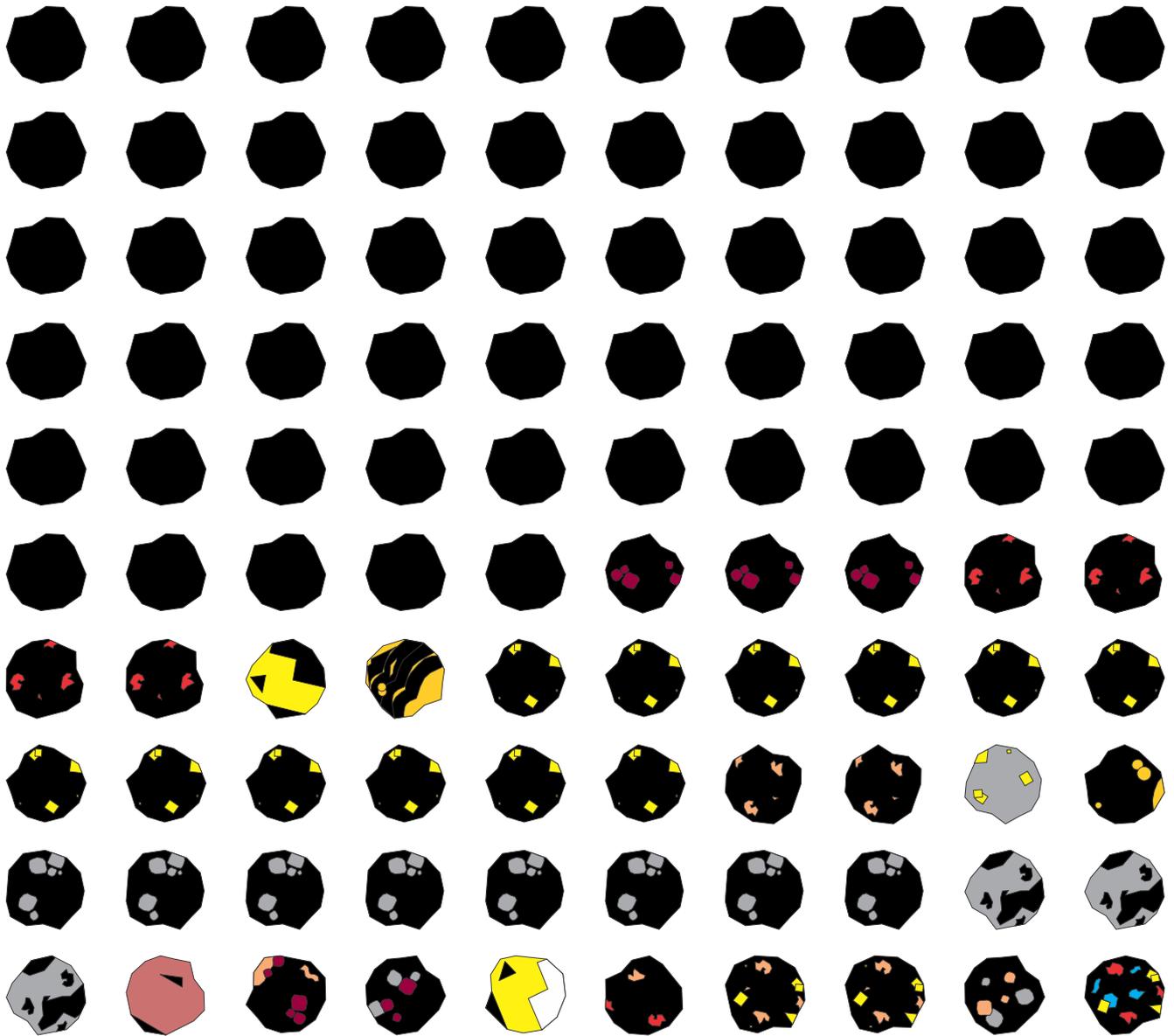
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail

A +212µm

July

2014



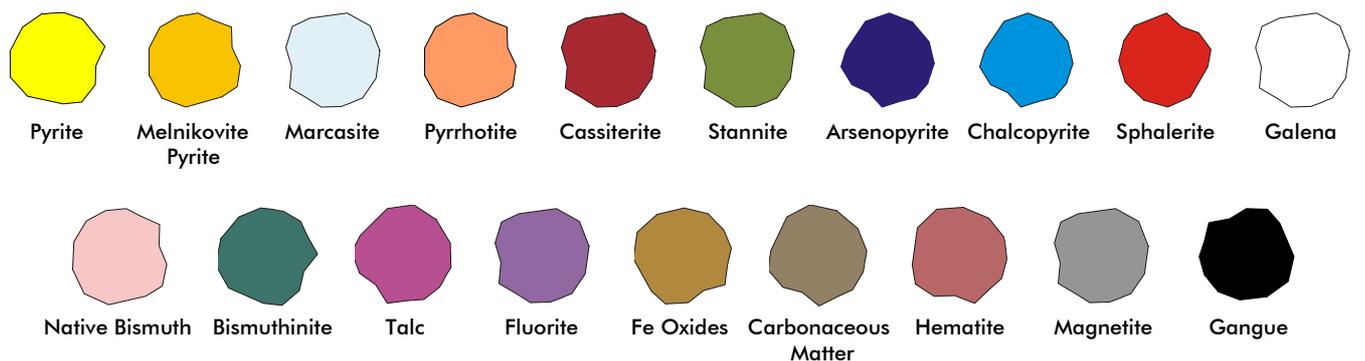
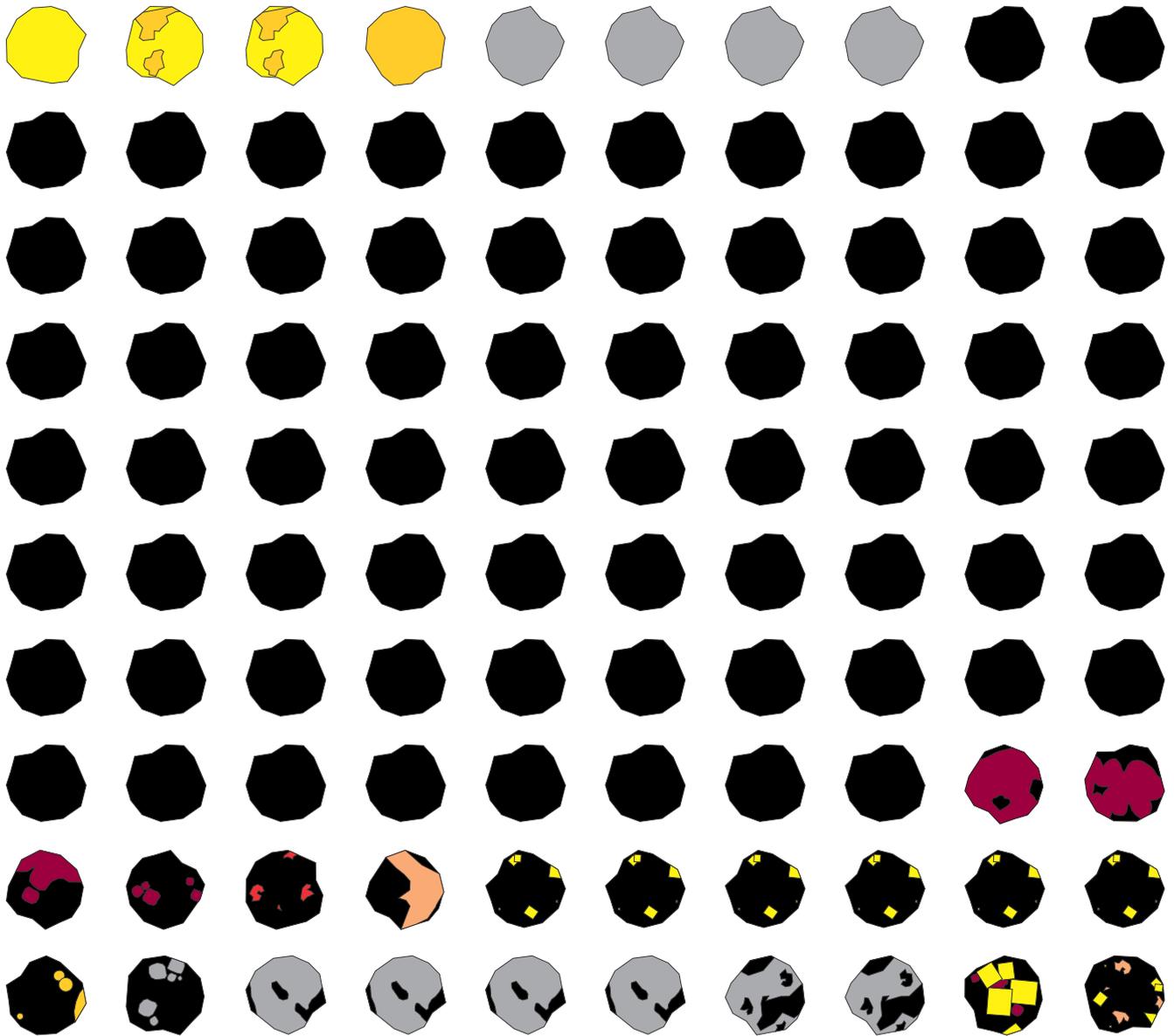
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail

B + 106µm

July

2014



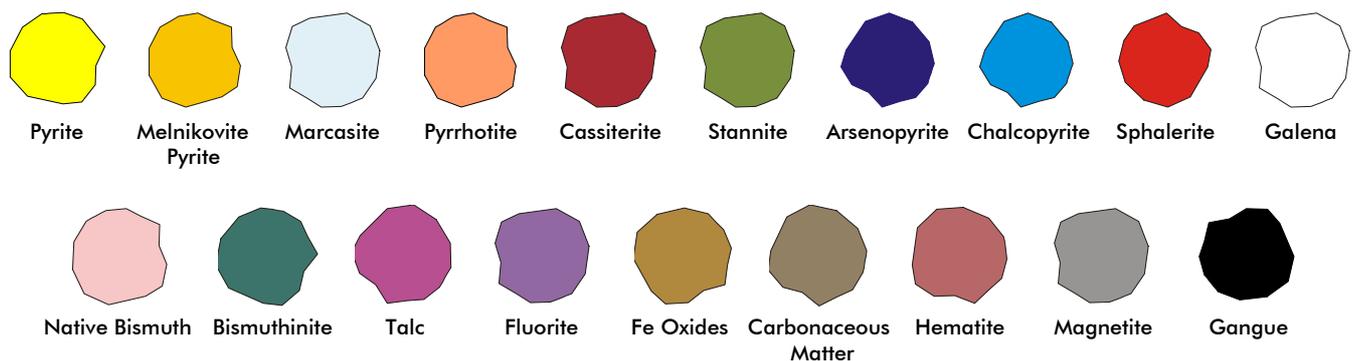
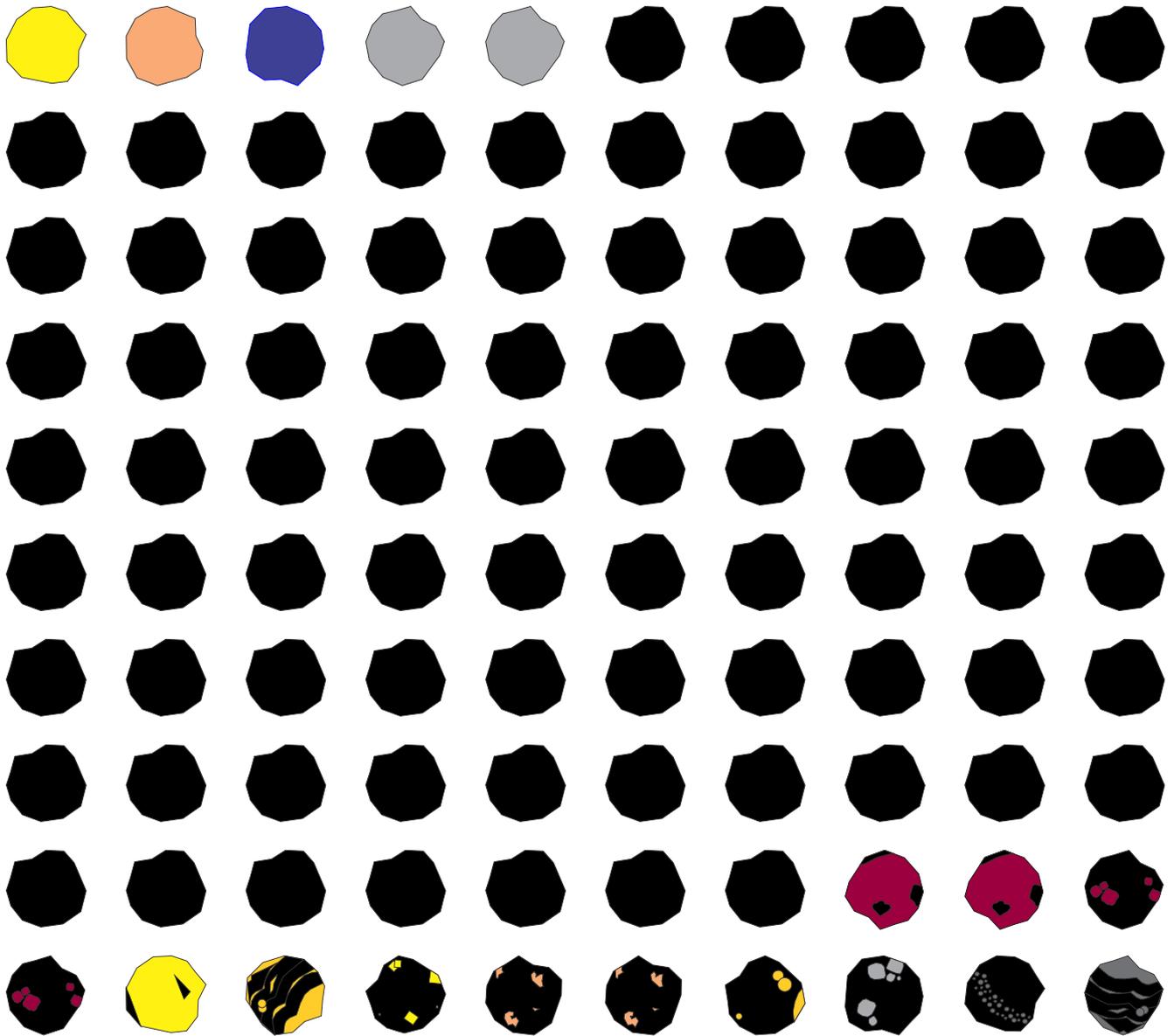
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail

C +53µm

July

2014



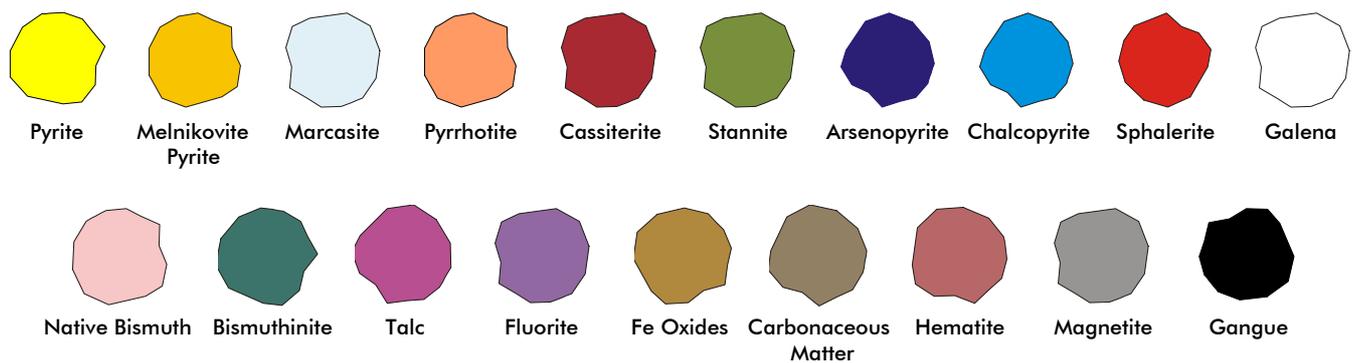
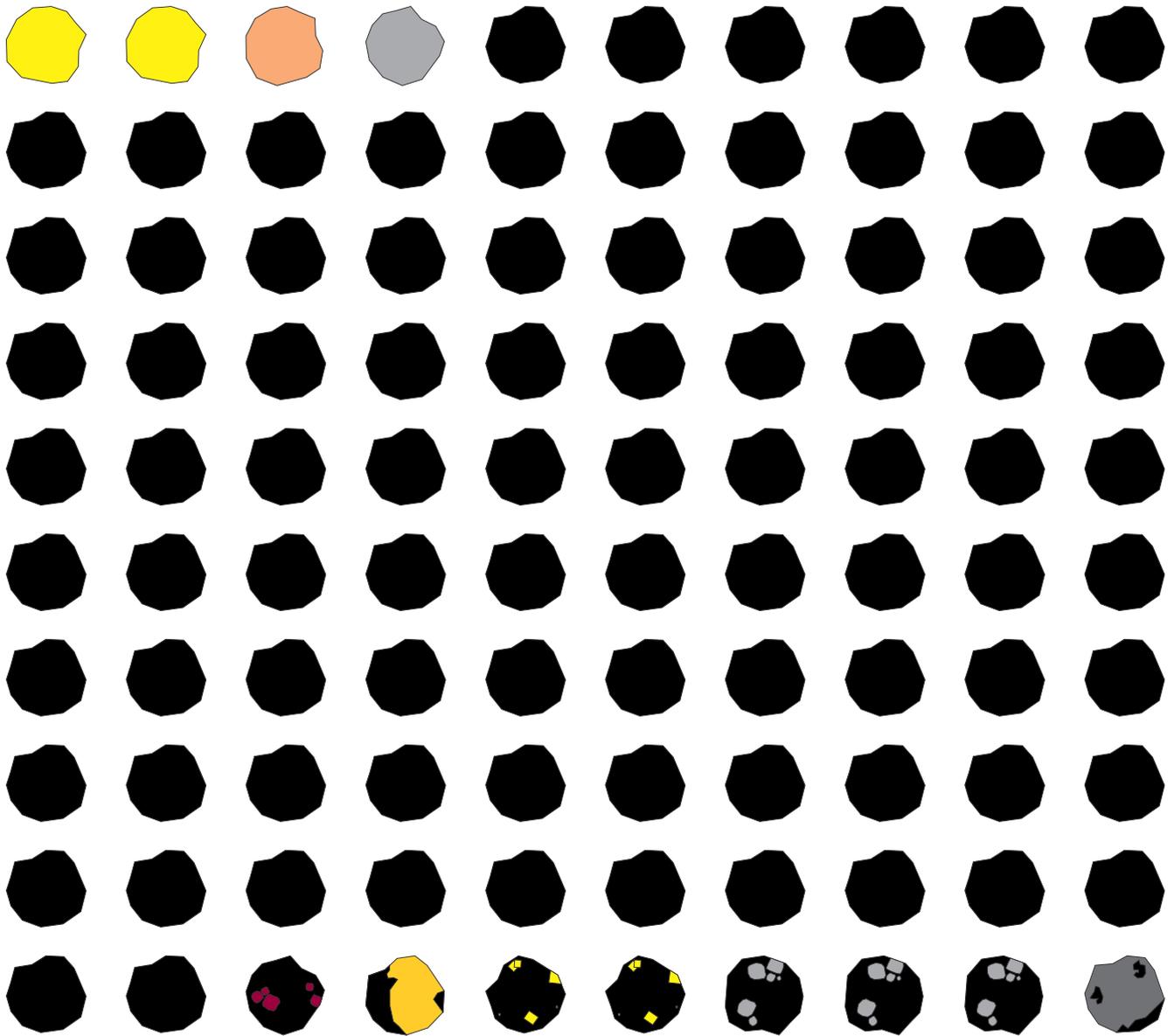
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail

D +20µm

July

2014



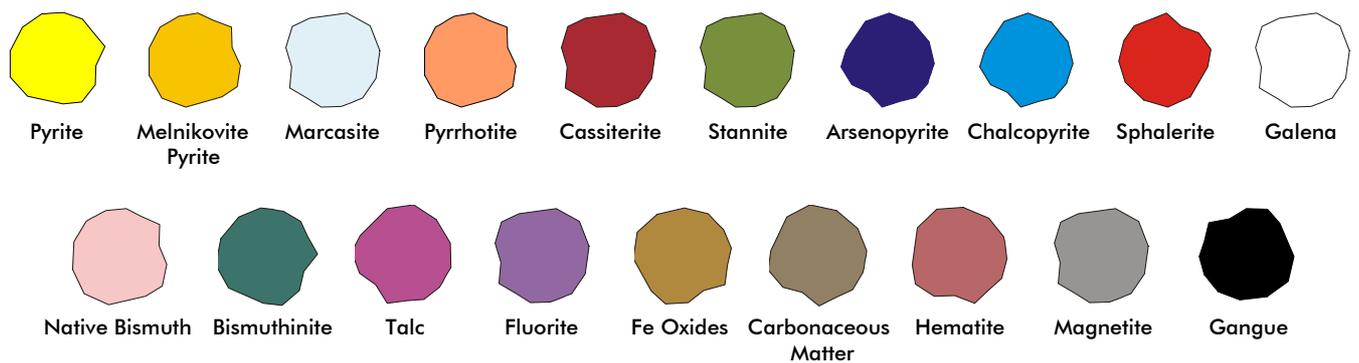
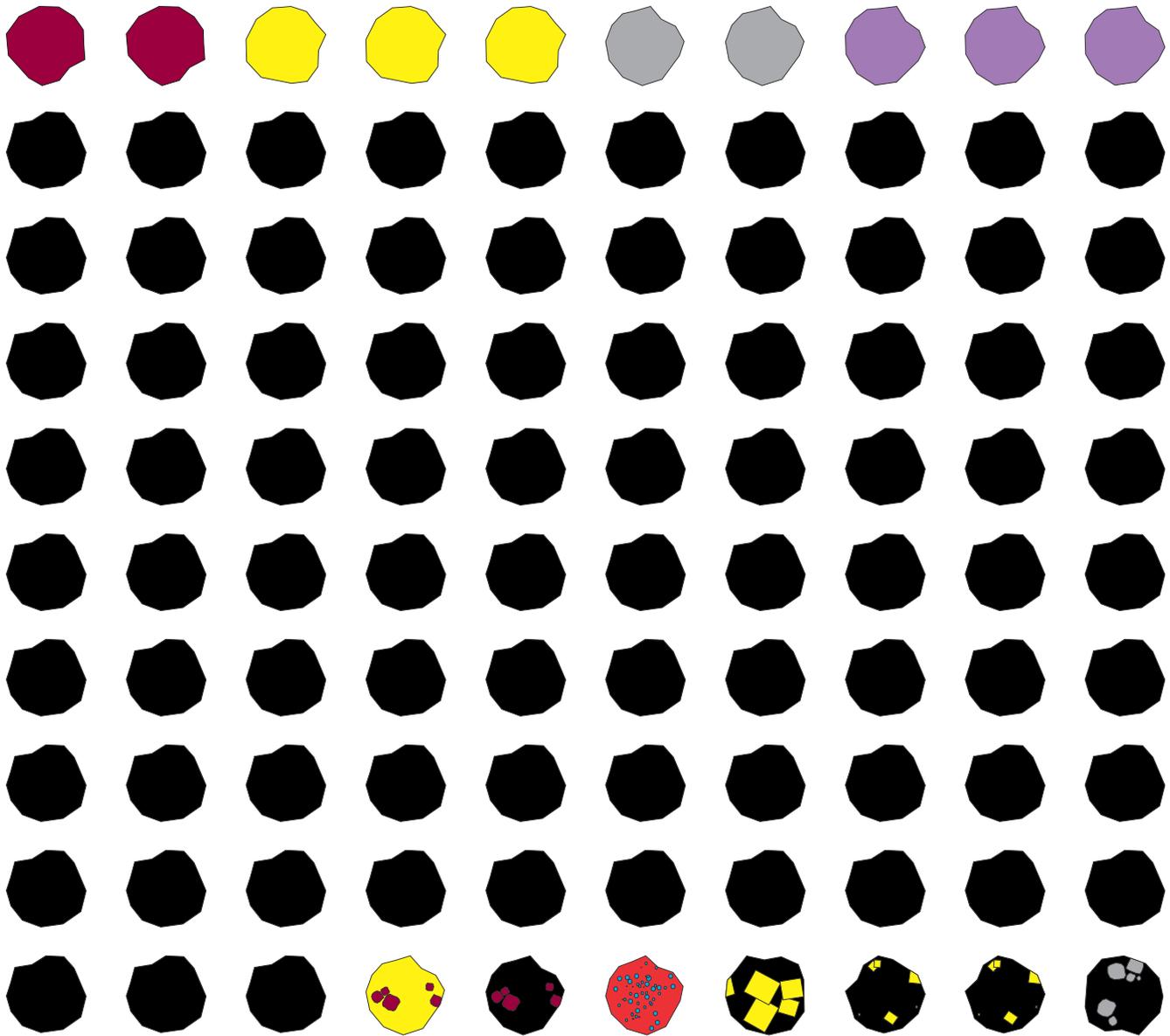
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail

E +8 μ m

July

2014



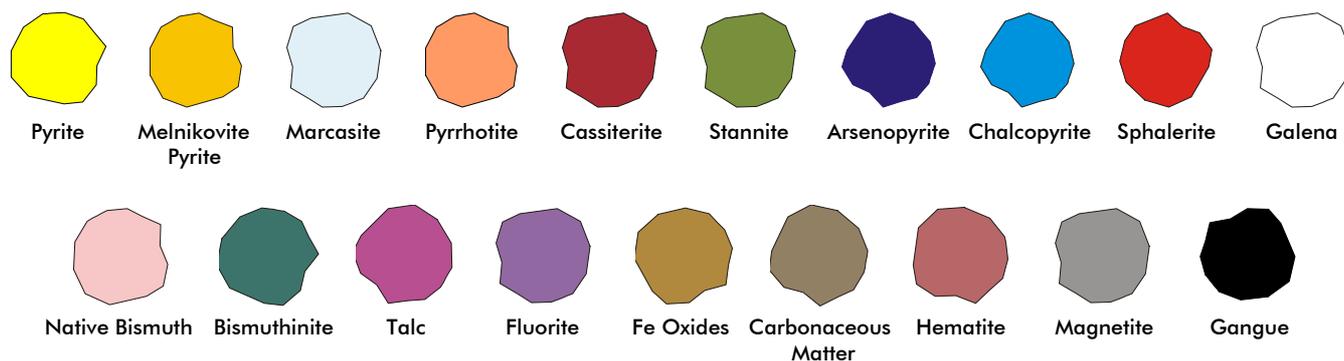
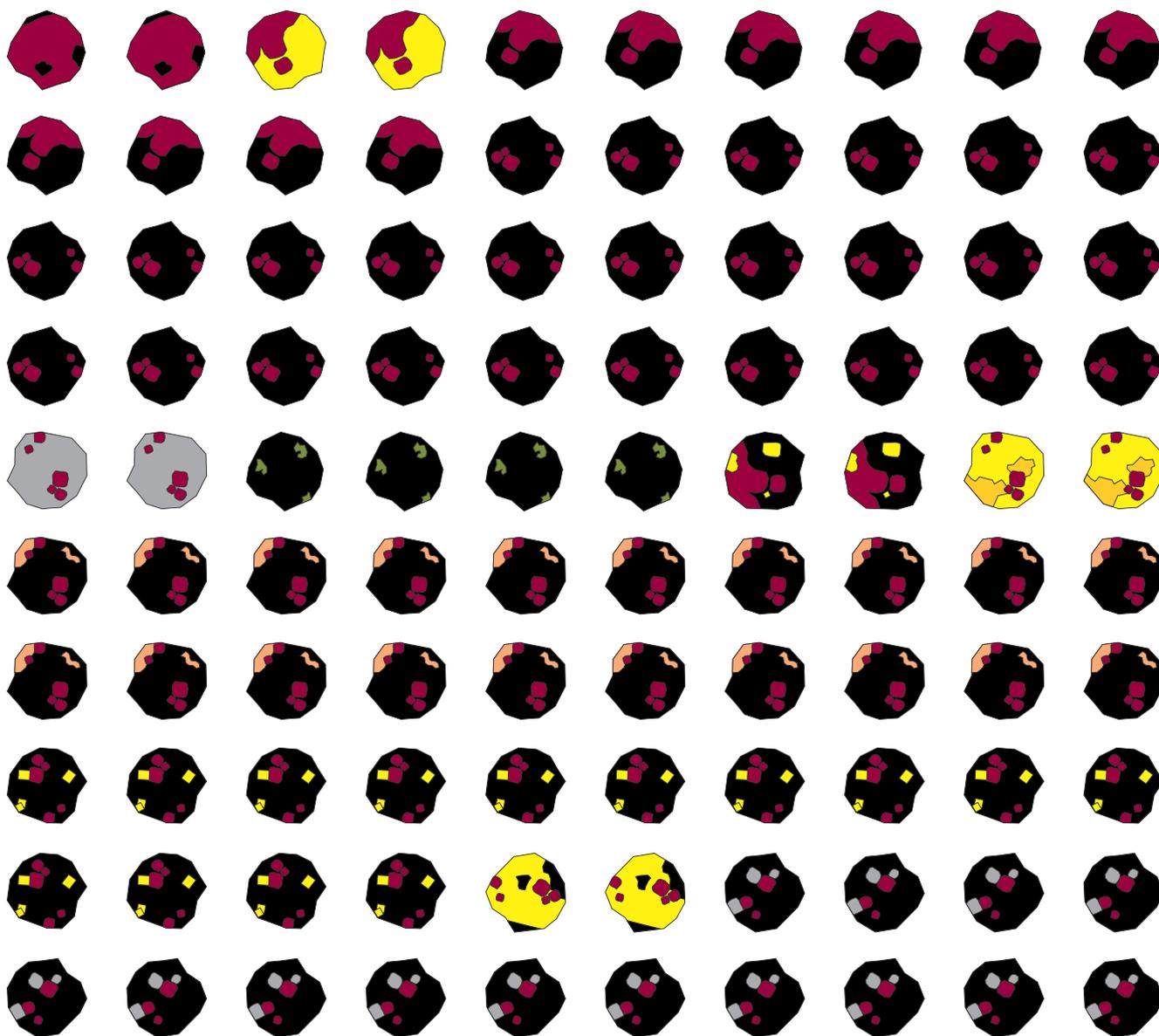
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail Sn SCAN

A +212µm

July

2014



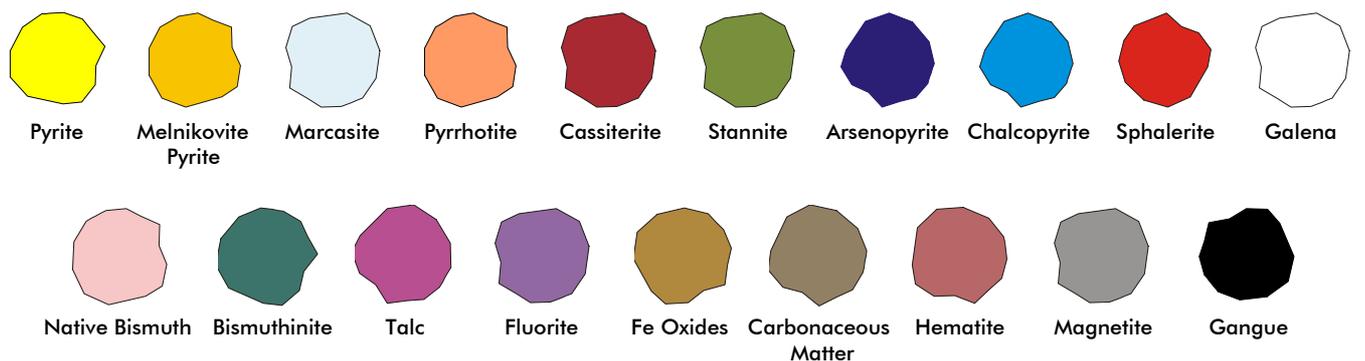
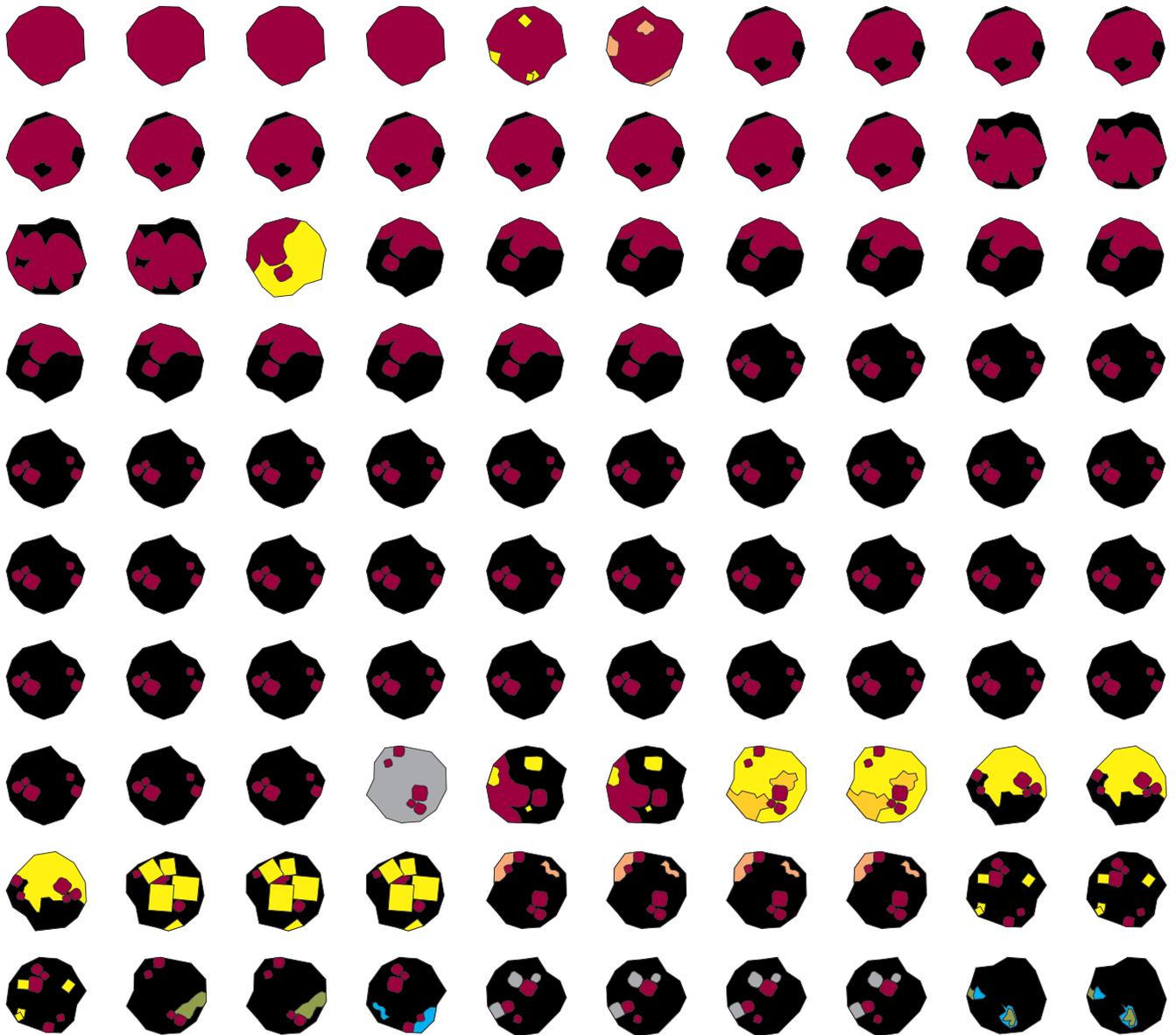
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail Sn SCAN

B + 106µm

July

2014



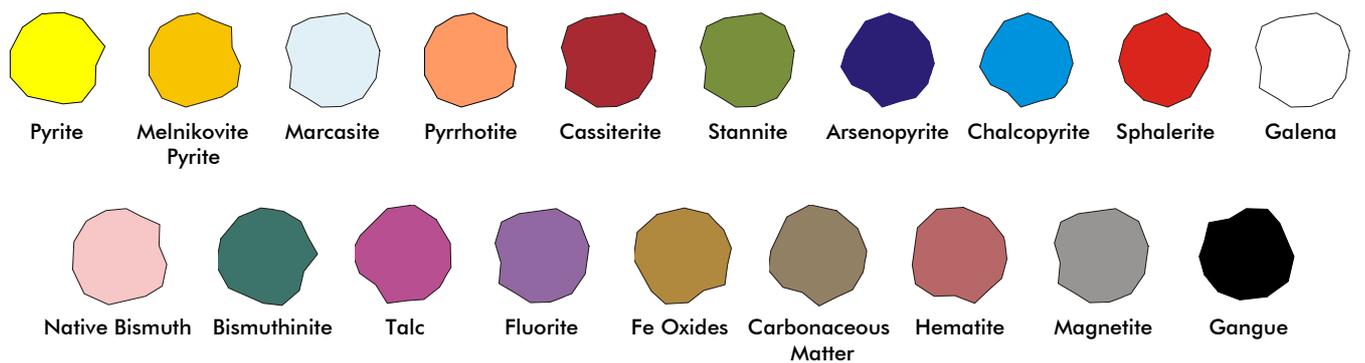
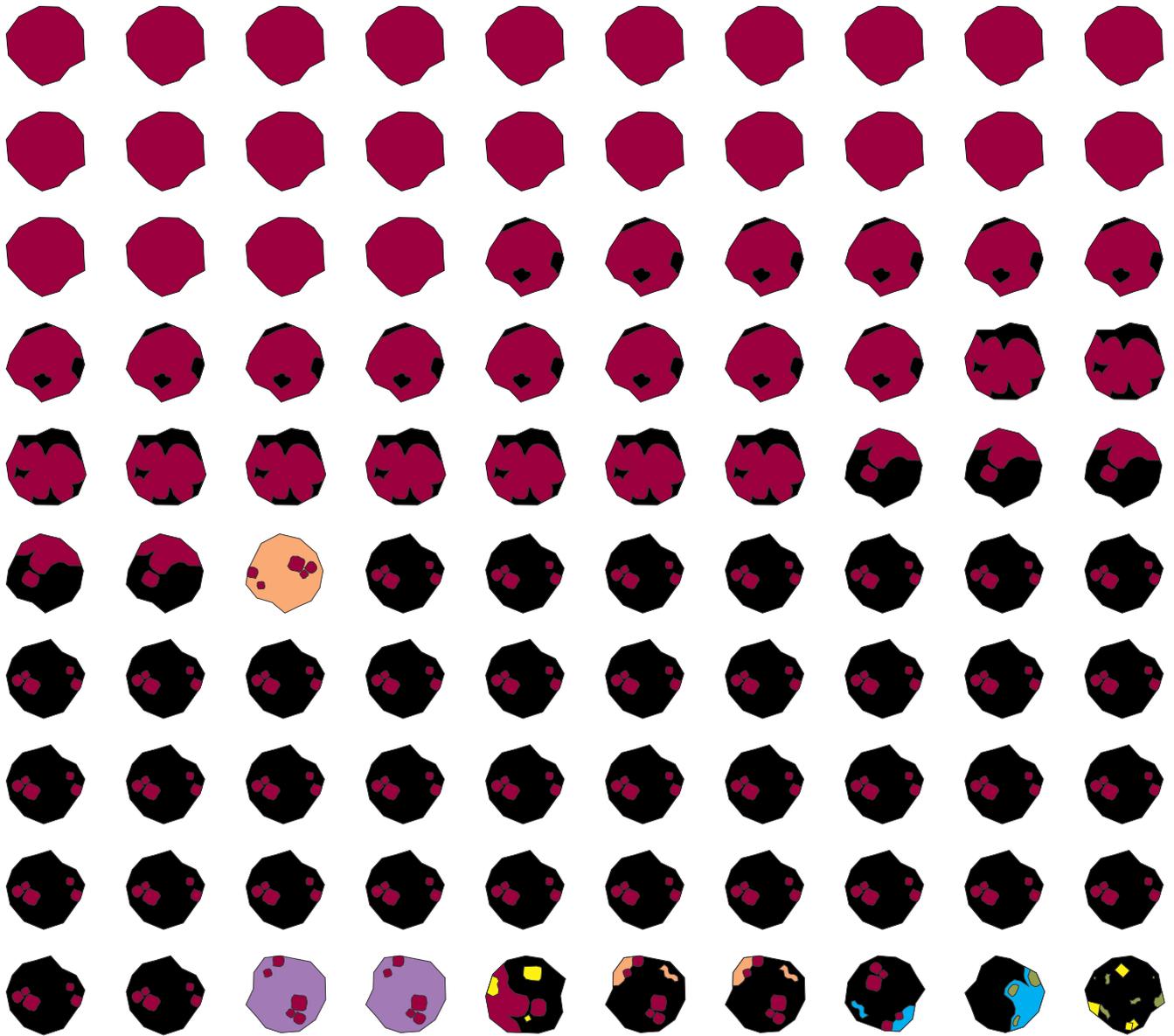
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail Sn SCAN

C +53µm

July

2014



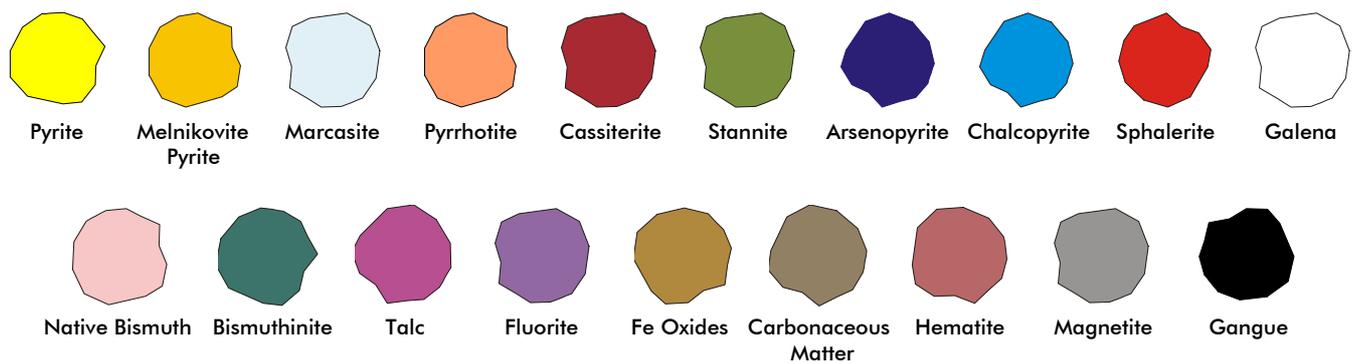
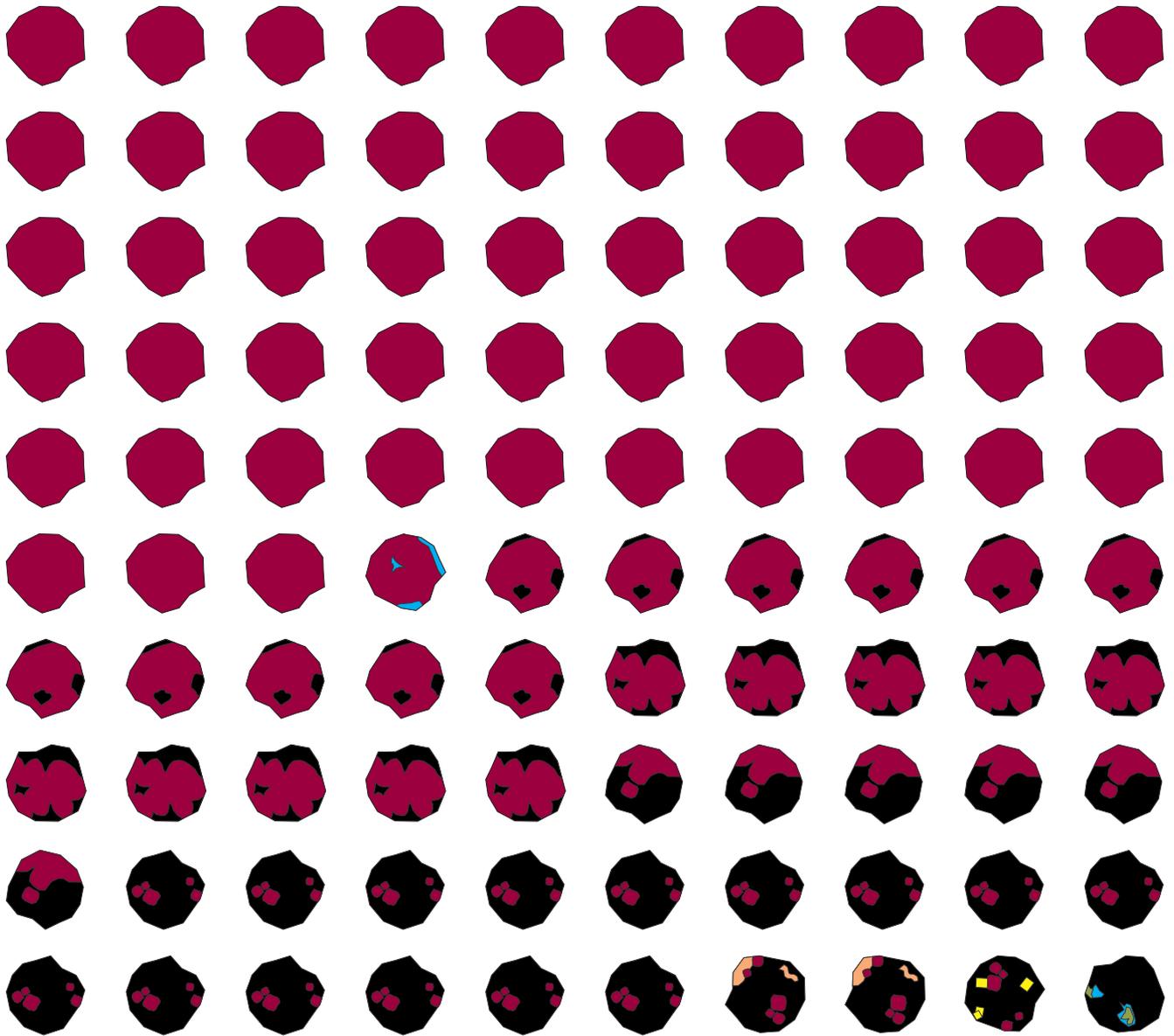
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail Sn SCAN

D +20µm

July

2014



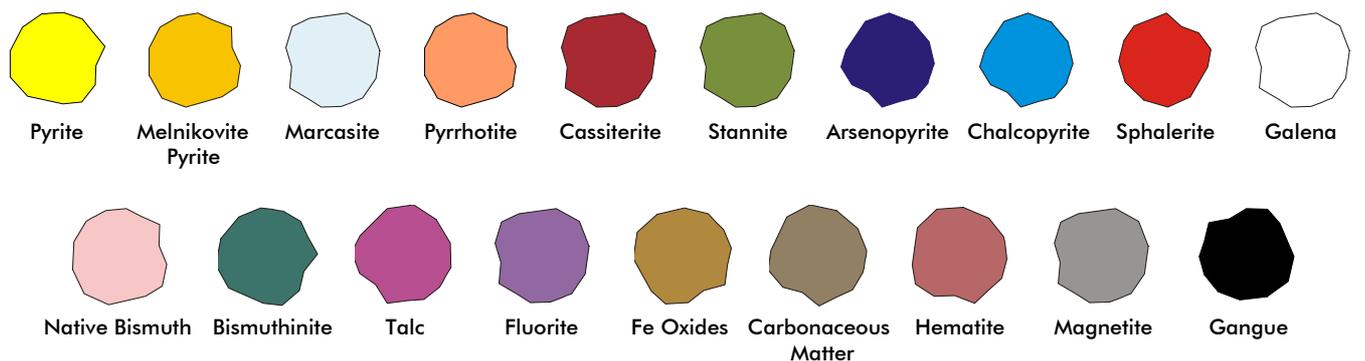
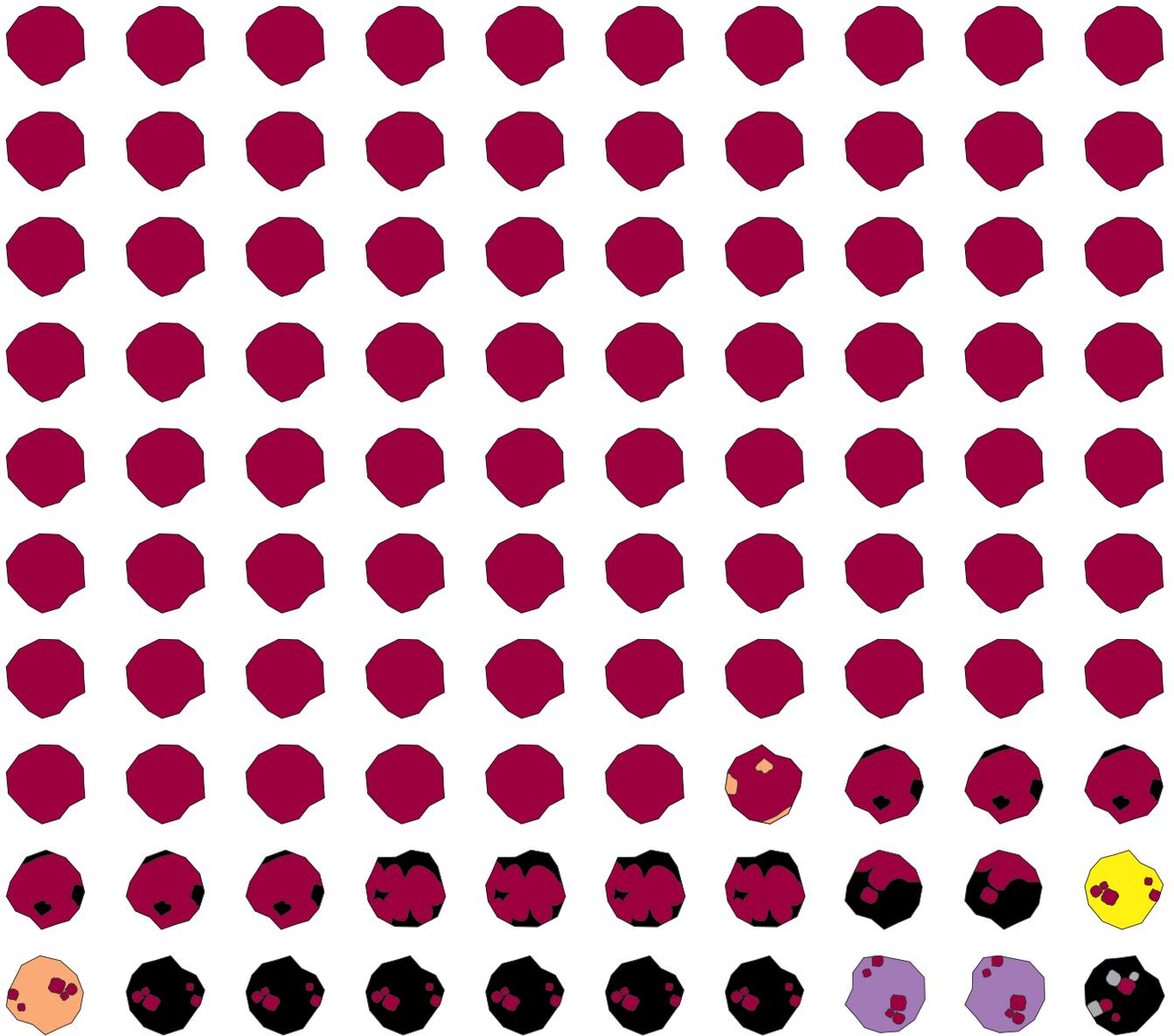
ALS Metallurgy - Heemskirk Sn Project Testwork

Severn Bulk Comp
Sulphide Tail Sn SCAN

E +8 μ m

July

2014



ALS Metallurgy

STELLAR RESOURCES LTD
Heemskirk Tin Project

Severn Bulk Composite
Sulphide Tail Siderite Mineralogy

AUGUST 2014

MODA
microscopy

McArthur Ore Deposit Assessments Pty Ltd

Gary J McArthur PhD FAusIMM MMICA MSEG

Suite 6, 1st Floor, Brownell Place, 11 Wilson St (P.O. Box 1303) Burnie TAS 7320 AUSTRALIA
Tel (03) 6431 1701 Fax (03) 6431 1278 Mobile 0419 367240 email gary@modapl.com.au

ALS METALLURGY

Stellar Resources – Severn Bulk Composite Sulphide Tail Mineralogy August 2014

Method

After a verbal request from Justin Resta (Worley Parsons metallurgical consultant for Stellar Resources), a sulphide tail produced from a Bulk Composite sample from Stellar Resources' Severn Prospect that was previously examined by MODA was re-assessed for siderite-cassiterite association. The sample was sized into 5 fractions: +212 μ m, +106 μ m, +53 μ m, +20 μ m and +8 μ m and these were mounted on two polished mounts by Australian Petrographics (Queanbeyan, NSW).

The standard MODA technique was adopted to quantify the mineralogy.

For each fraction, 100 grains containing cassiterite were selected at random and the area % of each mineral present was visually estimated. The minerals logged were: *siderite* (Sd), *quartz* (Qz), *cassiterite* (Cs), *pyrite+marcasite* (Py), *pyrrhotite* (Po), *fluorite* (Fl), other sulphides (*sphalerite, chalcopyrite, stannite, galena*; OS), and other undifferentiated *gangue* (*silicates, Fe-oxides, etc*, OG). [CAVEAT: Definitive identification of *cassiterite* in the finer fractions was difficult due to the presence of other minerals with similar optical properties].

The normal liberation and association parameters were calculated.

Results

The composition of the grains containing cassiterite is summarised below.

Severn Bulk Comp Sulphide Tail Composition Vol% (from Sn scan)

Fraction	Sn Wt%	Sd	Qz	Cs	PyMa	Po	Fl	OS	OG	Siderite fraction% of non-sulphide Ga
+212 μ m	13.3	16.1	36.6	12.9	1.2	1.0	1.4	0.2	30.8	19
+106 μ m	17.8	18.7	17.1	41.6	4.4	0.3	0.5	0.2	17.3	35
+53 μ m	16.7	16.4	9.9	54.6	2.5	0	1.0	0	15.5	38
+20 μ m	21.2	14.1	10.2	67.7	0.8	0	1.4	Tr	5.7	45
+8 μ m	17.9	7.7	1.0	88.1	0	0	1.0	0	2.3	64
TOTAL	86.9	14.5	13.7	55.7	1.8	0.2	1.1	0.1	13.1	34

Sd=siderite, Qz=quartz, Cs=cassiterite, PyMa=pyrite/marcasite, Po=pyrrhotite, Fl=fluorite, OS=other sulphides, OG=other gangue

As would be expected, the grains containing *cassiterite* in the coarser fractions are more *quartz*-rich, and the finer fractions are more *siderite*-rich.

Liberation and Association

Essential summaries of the liberation parameters for *cassiterite* are:

Severn Bulk Comp Sulphide Tail Cassiterite liberation distribution%

Fraction	Sn Wt%	Free	Binary with						Ternary+
			Sd	Qz	PyMa	Po	Fl	OG	
+212µm	13.3	0	0	11	0	0	0	18	71
+106µm	17.8	26	16	9	2	0	0	22	22
+53µm	16.7	55	6	4	2	0	0	23	10
+20µm	21.2	64	11	4	0	0	0	14	7
+8µm	17.9	92	3	2	0	0	0	3	0
TOTAL	86.9	50	8	6	1	0	0	16	19

Severn Bulk Comp Sulphide Tail Cassiterite association%

Fraction	Sn Wt%	%associated with					
		Sd	Qz	PyMa	Po	Fl	OG
+212µm	13.3	40	72	4	9	8	59
+106µm	17.8	31	17	6	2	1	37
+53µm	16.7	11	12	4	2	0	28
+20µm	21.2	14	9	0	0	0	19
+8µm	17.9	3	2	0	0	0	3
TOTAL	86.9	19	19	3	2	1	27

G.J.McArthur PhD FAusIMM MMICA MSEG
Principal Mineralogist
22.8.14



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 3 – Comminution Testwork

BOND ROD MILL CLOSED CIRCUIT GRINDABILITY : 1180 MICROMETERS

SAMPLE IDENTITY	SBC Head
CLIENT	ALS Metallurgy Burnie
PROJECT No	P0603
DATE	28-Apr

PERIOD	REVS OF MILL	WT OF 1250 mls (g)	WT OF NEW FEED (g)	WT OF O/SIZE (g)*	WT OF U/SIZE (g)*	NET WT OF U/SIZE (g)*	NET WT OF U/SIZE PER REV (g)	CIRC'TING LOAD (%)	WT OF FRESH FEED ADDED TO NEXT CYCLE (g)	WT OF U/SIZE IN FEED TO NEXT CYCLE (g)
1	200	2297.0	2297.0	1103.5	1193.5	931.3	4.657	92	1193.5	136.2
2	217	2297.0	1193.5	1094.1	1202.8	1066.6	4.915	91	1202.8	137.3
3	206	2297.0	1202.8	1085.1	1211.9	1074.6	5.216	90	1211.9	138.3
4	194	2297.0	1211.9	1125.0	1172.0	1033.7	5.328	96	1172.0	133.8
5	190	2297.0	1172.0	1134.4	1162.6	1028.8	5.415	98	1162.6	132.7
6	188	2297.0	1162.6	1146.0	1151.0	1018.3	5.416	100	1151.0	131.4
7	187	2297.0	1151.0	1148.6	1148.4	1017.0	5.438	100	1148.4	131.1

Note : * = Ex grinding mill

PRODUCT IN THE FEED	11.41 (%)
BULK DENSITY	1.8376 (t/m³)
IDEAL POTENTIAL PRODUCT	1148.5 (g)
AVERAGE EQUILIBRIUM CIRC LOAD	100 (%)
AVERAGE PRODUCT	5.427 (g/rev)
80 % PASSING FEED SIZE	8646 (µm)
80 % PASSING PRODUCT SIZE	889 (µm)

BOND ROD MILL WORK INDEX (Kilowatt hours / dry tonne) :	20.5
--	-------------



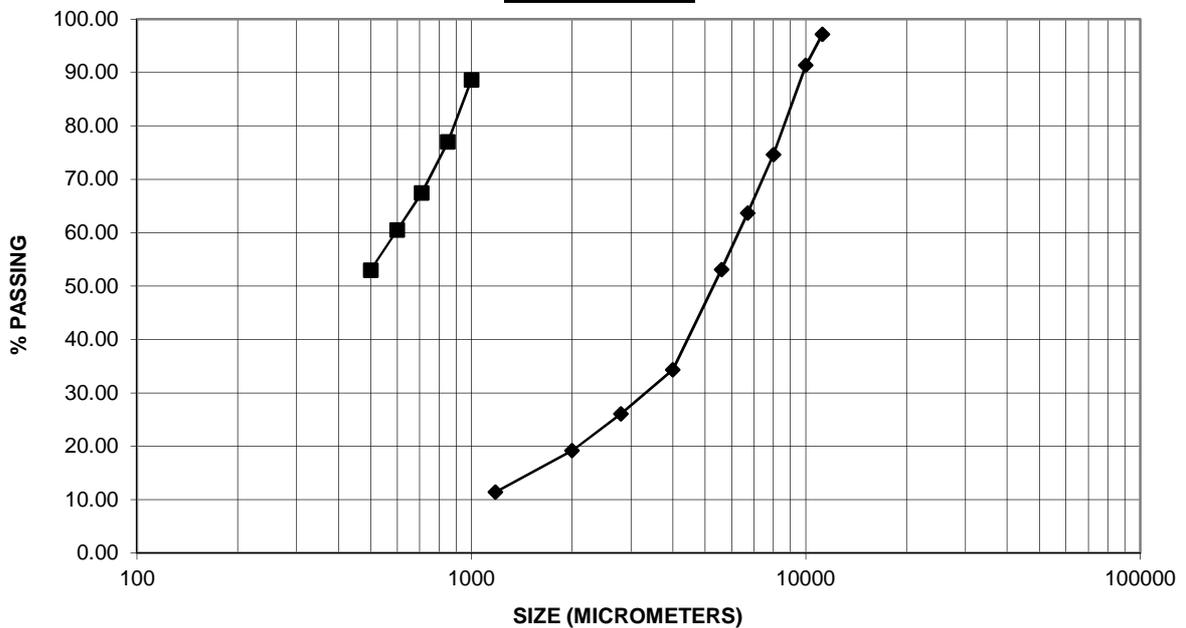
BOND ROD MILL GRINDABILITY TEST FEED AND PRODUCT SIZINGS

SBC Head
P0603

FEED TO PERIOD No. 1			
Size (mm)	Weight (g)	Retained (%)	Passing (%)
11.200	28.7	2.86	97.14
10.000	58.3	5.82	91.32
8.000	167.5	16.72	74.60
6.700	109.7	10.95	63.65
5.600	105.7	10.55	53.09
4.000	187.9	18.76	34.34
2.800	82.8	8.26	26.08
2.000	69.3	6.91	19.16
1.180	77.6	7.75	11.41
-1.180	114.4	11.41	
TOTAL	1001.8	100.00	
F 80 (µm) :		8646	

EQUILIBRIUM PRODUCTS			
Size (mm)	Weight (g)	Retained (%)	Passing (%)
1.000	130.9	11.39	88.61
0.850	133.5	11.62	76.98
0.710	109.4	9.52	67.46
0.600	79.9	6.96	60.50
0.500	86.3	7.52	52.98
-0.500	608.5	52.98	
TOTAL	1148.5	100.00	
P 80 (µm) :		889	

BOND ROD MILL GRINDABILITY : FEED & PRODUCT SIZE DISTRIBUTION



BOND BALL MILL CLOSED CIRCUIT GRINDABILITY :**212 MICROMETERS**

SAMPLE IDENTITY	SBC Head
CLIENT	ALS Metallurgy Burnie
PROJECT No	P0603
DATE	Apr-14

PERIOD	REVS OF MILL	WT OF 700 mls (g)	WT OF NEW FEED (g)	WT OF O/SIZE (g)*	WT OF U/SIZE (g)*	NET WT OF U/SIZE (g)*	NET WT OF U/SIZE PER REV (g)	CIRC'TING LOAD (%)	WT OF FRESH FEED ADDED TO NEXT CYCLE (g)	WT OF U/SIZE IN FEED TO NEXT CYCLE (g)
1	200	1224.5	1224.5	862.9	361.6	240.9	1.205	239	361.6	35.6
2	261	1224.5	361.6	867.6	356.9	321.3	1.231	243	356.9	35.2
3	256	1224.5	356.9	856.2	368.3	333.1	1.301	232	368.3	36.3
4	241	1224.5	368.3	868.9	355.6	319.3	1.325	244	355.6	35.0
5	238	1224.5	355.6	875.1	349.4	314.3	1.321	250	349.4	34.4
6	240	1224.5	349.4	874.6	349.9	315.4	1.314	250	349.9	34.5

Note : * = Ex grinding mill

PRODUCT IN THE FEED	9.86 (%)
BULK DENSITY	1.7493 (t/m³)
IDEAL POTENTIAL PRODUCT	349.9 (g)
AVERAGE EQUILIBRIUM CIRC LOAD	250 (%)
AVERAGE PRODUCT	1.318 (g/rev)
80 % PASSING FEED SIZE	2343 (µm)
80 % PASSING PRODUCT SIZE	167 (µm)

BOND BALL MILL WORK INDEX (Kilowatt hours / dry tonne) :	20.1
---	-------------



BOND BALL MILL GRINDABILITY TEST FEED AND PRODUCT SIZINGS

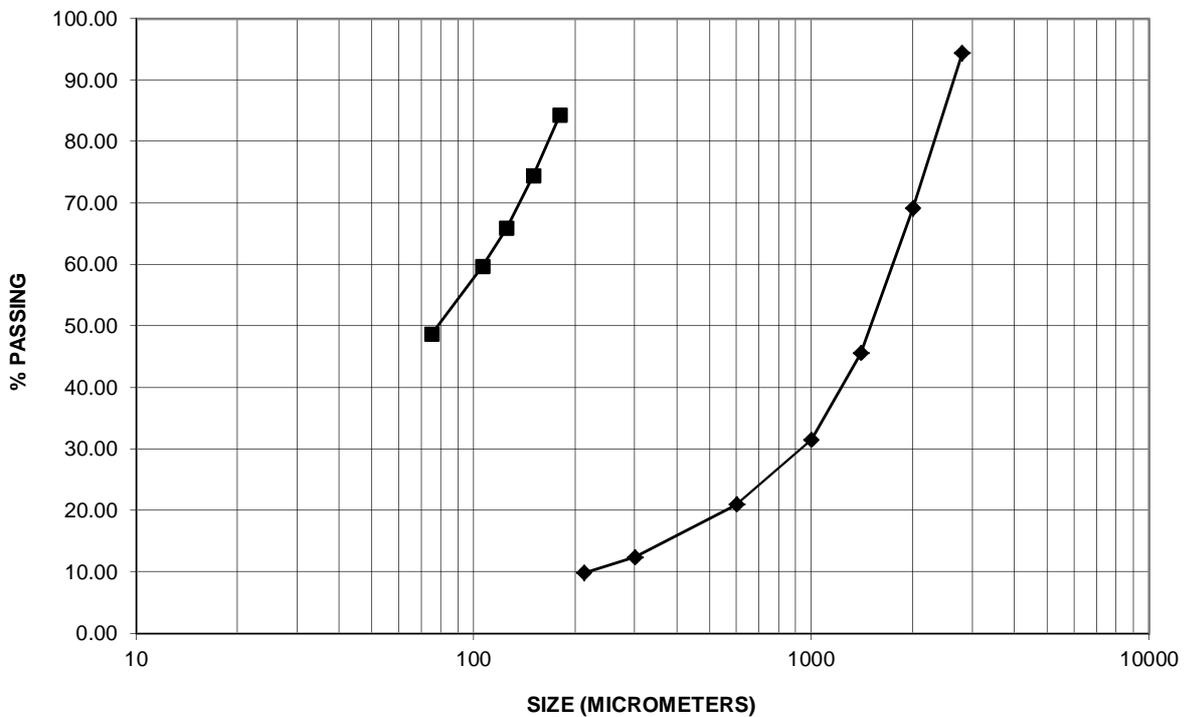
SBC Head

P0603

FEED TO PERIOD No. 1			
Size (mm)	Weight (g)	Retained (%)	Passing (%)
2.800	55.7	5.55	94.45
2.000	253.9	25.31	69.14
1.400	236.2	23.54	45.60
1.000	141.9	14.15	31.46
0.600	105.1	10.47	20.98
0.300	86.2	8.59	12.40
0.212	25.5	2.54	9.86
-0.212	98.9	9.86	
TOTAL	1003.3	100.00	
F 80 (µm) :		2343	

EQUILIBRIUM PRODUCTS			
Size (mm)	Weight (g)	Retained (%)	Passing (%)
0.180	54.6	15.61	84.39
0.150	34.7	9.93	74.46
0.125	29.7	8.50	65.96
0.106	21.9	6.26	59.70
0.075	38.3	10.97	48.74
-0.075	170.4	48.74	
TOTAL	349.6	100.00	
P 80 (µm) :		167	

BOND BALL MILL GRINDABILITY : FEED & PRODUCT SIZE DISTRIBUTION





WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 4 – Heavy Media Separation Results



BURNIE LABORATORY

HEAVY MEDIA SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	DRS01
DATE	MAY 2014
TECH	

START MATERIAL

Severn Composite SBC 9.50 to 2.35mm	
START WEIGHT (kg)	
MEDIA SG (kg/L)	2.95
FROM TEST NO	Ore

HEAVY MEDIA SEPARATION RESULTS

PRODUCT	Wt (kg)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	Al2O3 (%)	Dist (%)
DMS Sinks (> 2.95)	8365	42.98	2.31	77.0	30.00	55.5	22.40	27.6	16.95	72.0	6.20	30.2
DMS Floats (< 2.95)	6917	35.54	0.14	3.9	14.70	22.5	51.50	52.5	1.61	5.7	12.05	48.6
Fines (<2.35mm)	4180	21.48	1.15	19.2	23.80	22.0	32.40	19.9	10.55	22.4	8.69	21.2
CALC Head	19462	100.00	1.29	100.0	23.23	100.0	34.89	100.0	10.12	100.0	8.81	100.0



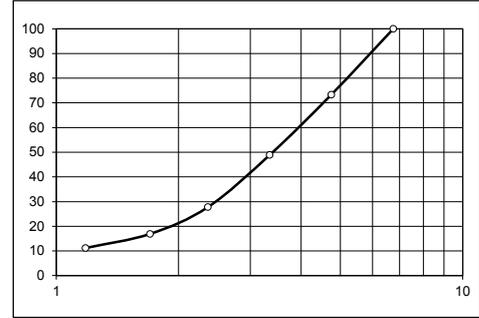
BURNIE LABORATORY: SIZE AND HEAVY LIQUID ANALYSIS

PROJECT	T0879
SAMPLE	SBC
TEST NO	T01
DATE	200514
TECHNICIAN	DK

LIQUID	hpt soln
MEASURED SG	2.95
TEMPERATURE	30
METHOD	beaker

SIZING

SIZE um	WEIGHTS		
	gm	(%)	%PASS
6.75	0.00	0.00	100.0
4.75	283.2	26.68	73.3
3.35	259.6	24.45	48.9
2.36	224.3	21.13	27.7
1.70	115.2	10.85	16.9
1.18	60.7	5.72	11.2
<1.18	118.6	11.17	0.0
TOTAL	1061.6	100.00	



SEPARATIONS

SIZE mm	WT gm	WT %	Fraction		Fraction													
			%Sn	dist	%Fe	dist	%As	dist	%S	dist	%SiO2	dist	%CaO	dist	%MgO	dist	%Al2O3	dist
Sinks+4.75	198.50	18.70	2.32	98.9	29.30	83.8	0.28	92.9	14.60	97.4	28.40	54.1	0.79	81.51	2.88	66.90	7.45	60.60
Floats+4.75	84.70	7.98	0.06	1.1	13.30	16.2	0.05	7.1	0.91	2.6	56.40	45.9	0.42	18.49	3.34	33.10	11.35	39.40
Calc 4.75 Total	283.20	26.68	1.64	100.0	24.51	100.0	0.21	100.0	10.51	100.0	36.77	100.0	0.68	100.00	3.02	100.00	8.62	100.00
Sinks+3.35	174.60	16.45	1.85	97.7	28.50	82.8	0.37	93.8	14.00	97.0	24.70	47.7	0.82	79.29	2.79	64.24	7.16	55.80
Floats+3.35	85.00	8.01	0.09	2.3	12.15	17.2	0.05	6.2	0.88	3.0	55.60	52.3	0.44	20.71	3.19	35.76	11.65	44.20
Calc 3.35 Total	259.60	24.45	1.27	100.0	23.15	100.0	0.27	100.0	9.70	100.0	34.82	100.0	0.70	100.00	2.92	100.00	8.63	100.00
Sinks+2.36	147.50	13.89	2.34	98.0	28.10	81.3	0.37	93.4	14.75	96.1	24.90	46.1	0.67	73.25	2.58	60.24	6.72	53.87
Floats+2.36	76.80	7.23	0.09	2.0	12.45	18.7	0.05	6.6	1.15	3.9	55.90	53.9	0.47	26.75	3.27	39.76	11.05	46.13
Calc 2.36 Total	224.30	21.13	1.57	100.0	22.74	100.0	0.26	100.0	10.09	100.0	35.51	100.0	0.60	100.00	2.82	100.00	8.20	100.00
Sinks+1.70	77.70	7.32	1.68	97.8	28.70	82.7	0.29	92.3	13.75	97.2	24.80	47.6	0.84	80.19	2.95	64.87	7.49	57.12
Floats+1.70	37.50	3.53	0.08	2.2	12.40	17.3	0.05	7.7	0.81	2.8	56.50	52.4	0.43	19.81	3.31	35.13	11.65	42.88
Calc 1.70 Total	115.20	10.85	1.16	100.0	23.39	100.0	0.21	100.0	9.54	100.0	35.12	100.0	0.71	100.00	3.07	100.00	8.84	100.00
Sinks+1.18	40.80	3.84	1.86	98.0	28.40	82.9	0.19	88.7	13.30	97.6	24.20	46.7	0.75	76.40	3.01	65.40	8.05	59.19
Floats+1.18	19.90	1.87	0.09	2.3	12.15	17.1	0.05	11.3	0.67	2.4	57.30	53.3	0.48	23.60	3.30	34.60	11.50	40.81
Calc +1.18 Total	60.70	5.72	1.28	100.3	23.11	100.0	0.14	100.0	9.19	100.0	34.97	100.0	0.66	100.00	3.10	100.00	9.17	100.00
Fines -1.18	118.60	11.17	1.12		24.80		0.18		8.99		33.30		0.63		3.09		8.93	
CALC FEED	1061.6	100.00	1.41		23.64		0.23		9.87		35.36		0.66		2.97		8.62	

*Number in red means less.

SUMMARY

FRACTIONS mm	Picno SG	WT %	Overall															
			%Sn	dist	%Fe	dist	%As	dist	%S	dist	%SiO2	dist	%CaO	dist	%MgO	dist	%Al2O3	dist
Sinks+4.75		18.70	2.32	30.86	29.30	23.18	0.28	23.01	14.60	27.66	28.40	15.02	0.79	22.27	2.88	18.13	7.45	16.15
Sinks+3.35		16.45	1.85	21.64	28.50	19.83	0.37	26.74	14.00	23.33	24.70	11.49	0.82	20.33	2.79	15.45	7.16	13.65
Sinks+2.36		13.89	2.34	23.13	28.10	16.52	0.37	22.59	14.75	20.76	24.90	9.78	0.67	14.03	2.58	12.07	6.72	10.83
Sinks+1.70		7.32	1.68	8.75	28.70	8.89	0.29	9.33	13.75	10.20	24.80	5.13	0.84	9.27	2.95	7.49	6.36	
Sinks+1.18		3.84	1.86	5.09	28.40	4.62	0.19	3.21	13.30	5.18	24.20	2.63	0.75	4.35	3.01	3.90	8.05	3.59
Floats+4.75		7.98	0.06	0.34	13.30	4.49	0.05	1.75	0.91	0.74	56.40	12.72	0.42	5.05	3.34	8.97	11.35	10.50
Floats+3.35		8.01	0.09	0.51	12.15	4.12	0.05	1.76	0.88	0.71	55.60	12.59	0.44	5.31	3.19	8.60	11.65	10.82
Floats+2.36		7.23	0.09	0.46	12.45	3.81	0.05	1.59	1.15	0.84	55.90	11.44	0.47	5.13	3.27	7.97	11.05	9.27
Floats+1.70		3.53	0.08	0.20	12.40	1.85	0.05	0.78	0.81	0.29	56.50	5.64	0.43	2.29	3.31	3.94	11.65	4.77
Floats+1.18		1.87	0.09	0.12	12.15	0.96	0.05	0.41	0.67	0.13	57.30	3.04	0.48	1.36	3.30	2.08	11.50	2.50
Total Sinks		60.20	2.09	89.46	28.67	73.04	0.32	84.87	14.28	87.12	25.88	44.05	0.77	70.25	2.80	56.82	7.25	50.58
Total Floats		28.63	0.08	1.64	12.58	15.23	0.05	6.29	0.93	2.71	56.12	45.43	0.44	19.14	3.27	31.56	11.40	37.86
Fines -1.18		11.17	1.12	8.90	24.80	11.72	0.18	8.84	8.99	10.17	33.30	10.52	0.63	10.61	3.09	11.62	8.93	11.57
CALC FEED		100.00	1.41	100.00	23.63	100.00	0.23	100.00	9.87	100.00	35.36	100.00	0.66	100.00	2.97	100.00	8.62	100.00



WorleyParsons

resources & energy

EcoNomics™

**STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION**

Appendix 5 – HMS Evaluation



MEMORANDUM

DATE 14 October 2014

TO Peter Blight

FROM J Resta

COPY

PROJECT 201010-00575

SUBJECT Application of HMS in the Heemskirk Flowsheet (re-issued)

DOC NO

FILE LOC

1 INTRODUCTION

The Heemskirk Tin Project Prefeasibility Study process flowsheet included heavy media separation (HMS) prior to the primary milling circuit.

Due to the variability seen in results of the heavy media and heavy liquid testwork, in some cases relatively high Sn losses and a clear lack of applicability of HMS to some ore types (lower Queen Hill in particular); a review of the merits of inclusion of HMS in the flowsheet was recommended, along with additional HMS testwork.

Inclusion of a HMS circuit provides the advantages of rejecting mass early in the circuit, leading to reduced downstream equipment sizes and potentially capital costs, and reduced downstream operating costs. However, this comes at the expense of increased circuit complexity, increased Sn losses (via the HMS floats product), and increase Sn loss opportunities (HMS introduces another tailings stream).

Taking the Heemskirk Tin Project Prefeasibility Study as a base case an assessment was completed as to the impact of removal of the HMS circuit on CAPEX, OPEX and Sn recovery. This memo details the outcomes of this assessment.

2 IMPACT OF REMOVAL OF HEAVY MEDIA SEPARATION CIRCUIT ON CAPEX, OPEX AND RECOVERY

Impacts of the removal of the heavy media circuit from the flowsheet on capital and operating costs were estimated based on the capital and operating cost estimates developed by GRES for the Heemskirk Tin Project Prefeasibility Study.

The impacts of the removal of HMS on direct capital costs were estimated on an area by area basis by factoring these based on the expected change in throughput without HMS according to the following formula (the "6 tenths rule");

$$\text{Adjusted Direct costs} = \text{Original direct cost} \times (\text{New throughput}/\text{Original throughput})^{0.6}$$



Indirect costs are calculated as a percentage of the total adjusted direct costs and summed to give the adjusted total capital estimate without HMS.

Similarly the impact on operating costs was estimated on an area by area basis by factoring these based on the expected change in throughput without HMS according to the following formula;

$$\text{Adjusted operating costs} = \text{Original operating cost} \times (\text{New throughput} / \text{Original throughput})$$

As the impacts of the removal of HMS on CAPEX and OPEX are expected to be sensitive to the mass rejection across the HMS circuit two cases were considered;

1. 23% mass rejection – as per the PFS PDC
2. 34.5% mass rejection – as per results of recent HMS testwork on the Severn bulk composite

Additionally the expected improvement in overall Sn recovery for these cases was estimated by assuming 72% downstream recovery (downstream of HMS) for those Sn units which would otherwise have been lost to the HMS floats product.

The key outcomes of this analysis are summarised in Table 1, with adjusted CAPEX and OPEX estimates for both cases considered in Appendix 1 and 2 respectively.

Table 1 – Summary: Expected Impact of Removal of Heavy Media Separation Circuit on Capital and Operating Costs

		Based on PFS PDC	Based on recent SBC HMS testwork results
Mass rejection in HMS		23.3%	35.4%
Sn loss in HMS		3.0%	3.9%
CAPEX:			
With HMS	M\$	\$80.04	\$80.04
Without HMS	M\$	\$79.17	\$81.75
Change in CAPEX	M\$	\$0.88	-\$1.70
OPEX:			
With HMS	M\$/y	\$18.86	\$18.86
Without HMS	M\$/y	\$19.26	\$20.22
Change in OPEX	M\$/y	-\$0.40	-\$1.36
Recovery Improvement necessary to offset increased in OPEX without HMS		0.3%	1.0%
Expected recovery improvement without HMS		2.2%	2.8%
Estimated improvement in net revenue without HMS	M\$/y	\$2.62	\$2.57

Table 2 shows a summary of the expected impact of removal of the heavy media circuit on metal production and “net revenue” (calculated “net revenue” is net of process plant operating costs and smelting costs, but excludes mining costs) for both of these cases.



Table 2 - Summary: Expected Impact of Removal of Heavy Media Separation Circuit on Metal Production and "Net Revenue" (excludes mining costs)

		Based on PFS PDC	Based on recent SBC HMS testwork results
Mass rejection in HMS		23.3%	35.4%
Sn loss in HMS		3.0%	3.9%
With HMS:			
ROM throughput	kt/y	600	600
ROM Grade	% Sn	1.06%	1.06%
Sn Recovery		70.0%	70.0%
Sn Production		4,452	4,452
CAPEX	\$/t Sn	\$18,000	\$18,000
OPEX	\$/t Sn	\$4,200	\$4,200
Net Smelter Return per tonne Sn	\$/t Sn	\$22,000	\$22,000
Gross Revenue (net of Smelter and Transport costs)	M\$/y	\$97.94	\$97.94
Process Plant OPEX	M\$/y	\$18.86	\$18.86
"Net Revenue" (Excluding mining costs)	M\$/y	\$79.09	\$79.09
Without HMS:			
ROM throughput	kt/y	600	600
ROM Grade	% Sn	1.06%	1.06%
Sn Recovery without HMS		72.2%	72.8%
Sn Production without HMS		4,589	4,631
CAPEX	\$/t Sn	\$17,300	\$17,700
OPEX	\$/t Sn	\$4,200	\$4,400
Net Smelter Return per tonne Sn	\$/t Sn	\$22,000	\$22,000
Gross Revenue (net of Smelter and Transport costs)	M\$/y	\$100.97	\$101.87
Process Plant OPEX	M\$/y	\$19.26	\$20.22
"Net Revenue" (Excluding mining costs)	M\$/y	\$81.71	\$81.65
Increase in Net Revenue without HMS	M\$/y	\$2.62	\$2.56

At the lower mass rejection considered, 23%, the analysis suggests removal of HMS would give a minor reduction of \$0.9 M in total CAPEX, while at 35.4% mass rejection an increase in total CAPEX of \$1.7 M was estimated. Within the accuracy of the PFS CAPEX estimate (+/- 25%) these changes are not considered significant.



In both cases considered OPEX is expected to increase with the removal of HMS due to increased throughputs, particularly in the primary grinding and gravity (particularly gravity regrind) circuits.

Assuming a mass rejection of 23%, OPEX is expected to increase by of the order of \$0.4 M /y (~\$0.70/t ROM), while at 35.4% mass rejection OPEX is expected to increase by of the order of \$1.4 M /y (~\$2.30/t).

These increases in OPEX would require an improvement in overall Sn recovery of 0.3% and 1% respectively to offset these (i.e. to remain revenue neutral). This compares with an expected increase in recovery of 2.2% and 2.8% respectively.

For both the without HMS cases CAPEX expressed in \$/t Sn falls, largely due to the increase metal output for these cases. OPEX expressed in \$/t Sn for the lower mass rejection case remains at similar level to that with HMS, and increases marginally for the higher mass rejection case. However, this increase in OPEX is more than offset due to the increase in tin production leading to an increase in overall “net revenue” of approximately \$2.6 M /y for both of the without HMS cases compared to with HMS.

3 CONCLUSIONS

- Over the range of mass rejection considered removal of HMS from the flowsheet is expected to have negligible impact on total CAPEX (within the accuracy of the estimate). However, operating costs are expected to rise with removal of HMS.
- The expected improvement in overall Sn recovery by the removal of HMS is expected to more than offset the increase in OPEX, leading to an improvement in net revenue of the order of \$2.6 M /y.
- Exclusion of HMS from the flowsheet simplifies the overall process flowsheet, and eliminates a loss opportunity (via HMS floats product) for Sn from the flowsheet.
- Previous testwork has shown HMS is not applicable to all ore types to be treated by the Heemskirk project.
- When considered from a processing only perspective HMS has no merits.

4 RECOMMENDATIONS

Based on the above analysis heavy media separation detracts value from the Heemskirk project when the treatment of the same ROM (grade and tonnages of ore) is considered. That is, HMS detracts value when considered from a processing only perspective. On this basis inclusion of HMS in the Heemskirk flowsheet is not recommended.

However, it is recommended to undertake further assessment as to whether HMS can provide any benefits in terms of mining costs and total ore reserves, before final decision is made as to the exclusion of HMS from the circuit. Key considerations in this further assessment are;

- Would inclusion of HMS allow an increase in overall ore reserves – Would a reduction in cut-off grade and average ROM grade allow reserves to be increased? Can the additional dilution be effectively rejected via HMS?
- Would inclusion of HMS allow mining costs to be reduced by adopting a less selective mining method?



- Could any mineralised waste which must be mined be converted into ore by treatment via HMS?

As HMS floats have previously been considered as a source of underground fill, consideration will also need to be given to alternative underground fill sources if HMS is removed from the circuit.



WorleyParsons

resources & energy

EcoNomicsTM

Appendix 1 – CAPEX and OPEX estimates assuming 23% mass rejection in HMS

Expected Impact of Removal of Heavy Media Separation Circuit on Capital Costs

Mass rejection in HMS **23%** ⁽⁴⁾ (as per PFS PDC)

Area	Description	GRES PFS Capital Cost (+/-25%)					Factored Capital Cost			
		Equip/Matl \$	Labour \$	Freight \$	Contingency \$	TOTAL \$	Original Throughput with HMS (kt/y)	New Throughput without HMS (kt/y)	Factor	Adjusted Costs \$
200	- PLANT SITE BULK EARTHWORKS	406,400	46,200	455	28,005	481,060	600	600	1.00	481,060
310	- CRUSHING	3,882,601	1,252,014	203,682	350,317	5,688,613	600	600	1.00	5,688,613
320	- ORE STORAGE	1,397,894	1,067,330	61,947	166,525	2,693,697	600	600	1.00	2,693,697
325	- HEAVY MEDIA SEPARATION	2,502,243	566,604	67,540	209,910	3,346,297	600	0	0.00	0
330	- GRINDING AND CLASSIFICATION	2,824,521	1,037,197	242,675	251,326	4,355,718	460	600	1.17	5,107,995
331	- SULPHIDE FLOTATION ⁽⁵⁾	3,722,954	775,663	151,794	260,195	4,910,606				
	Roughing					1,636,869	460	600	1.17	1,919,573
	Regrind & cleaning					3,273,737	600	600	1.00	3,273,737
350	- COARSE GRAVITY	859,903	273,160	23,518	70,413	1,226,995	460	600	1.17	1,438,910
351	- SULPHIDE DRESSING FLOTATION	645,287	178,506	28,026	45,223	897,042	600	600	1.00	897,042
352	- GRAVITY REGRIND & CLASSIFICATION	1,971,471	718,330	116,172	148,629	2,954,602	460	600	1.17	3,464,892
353	- FINE GRAVITY	700,831	249,173	32,962	60,811	1,043,776	600	600	1.00	1,043,776
354	- SULPHIDE SCAVENGER FLOTATION	636,829	270,039	27,307	51,752	985,927	460	600	1.17	1,156,207
355	- SILICA FLOTATION	860,888	310,195	42,994	69,252	1,283,330	460	600	1.17	1,504,974
356	- TIN FLOTATION	2,307,913	522,646	55,346	174,528	3,060,433	460	600	1.17	3,589,001
357	- CONCENTRATE ACID LEACHING	502,100	166,988	13,194	42,350	724,632	600	600	1.00	724,632
358	- TIN CONCENTRATE HANDLING AND FILTRATION	971,281	244,774	22,906	75,853	1,314,814	600	600	1.00	1,314,814
360	- REAGENTS	1,771,260	639,626	50,707	139,243	2,600,836	600	600	1.00	2,600,836
370	- POWER AND RETICULATION	5,645,930	2,708,343	114,296	503,643	8,972,213	600	600	1.00	8,972,213
390	- WATER SUPPLY	613,179	281,625	18,961	57,603	971,368	600	600	1.00	971,368
400	- TAILINGS	1,880,583	567,789	74,034	152,753	2,675,160	600	600	1.00	2,675,160
411	- FUEL FARM	292,119	55,806	6,670	22,954	377,550	600	600	1.00	377,550
420	- COMPRESSED AIR	446,899	57,070	11,327	28,121	543,417	600	600	1.00	543,417
490	- SITE BUILDINGS	581,010	242,279	47,363	50,012	920,664	600	600	1.00	920,664
495	- MOBILE PLANT & EQUIPMENT	1,755,000	7,768	70,525	91,859	1,925,152	600	600	1.00	1,925,152
499	- PLANT PIPING	2,064,532	2,262,628	9,373	294,385	4,630,918	600	600	1.00	4,630,918
804	- CONSTRUCTION EQUIPMENT	1,404,509	899,545	80,800	148,896	2,533,750	600	600	1.00	2,533,750
Total Direct Costs		40,648,138	15,401,299	1,574,574	3,494,558	61,118,570				60,449,952
Indirect Costs										
500	- ENGINEERING	107,500	13,139,963	0	671,623	13,919,086	23%			13,766,815
510	- COMMISSIONING	51,560	904,207	0	49,288	1,005,056	2%			994,061
600	- PRELIMINARIES AND GENERAL	2,096,131	74,820	116,878	114,391	2,402,221	4%			2,375,941
700	- OWNERS COSTS	1,598,636	0	0	0	1,598,636	3%			1,581,147
Total Indirect Costs		3,853,827	14,118,990	116,878	835,303	18,924,997	31%			18,717,965
TOTAL CAPITAL ESTIMATE		44,501,965	29,520,289	1,691,452	4,329,861	80,043,567				79,167,917
CHANGE IN TOTAL CAPITAL ESTIMATE										\$875,650

Notes;

- Only costs for areas 325, 330, 331 (roughing only), 350, 352, 355 and 356 (highlighted in red) are expected to be impacted by the removal of HMS from the circuit. Costs for other areas are not expected to be impacted within the accuracy of the estimate.
- Adjusted Direct costs = Original direct cost x (New throughput/Original throughput)^{0.6}
- Indirect costs are calculated as a percentage of the total direct costs
- Based on GR PFS PDC
- Sulphide flotation costs are assumed to be split 1/3 roughing and 2/3 cleaning plus regrind.

Expected Impact of Removal of Heavy Media Separation Circuit on Operating Costs

Mass rejection in HMS

23% ⁽⁵⁾

(as per PFS PDC)

GRES PFS OPEX (+/-25%)		Severn Factored OPEX					
AREA	Description	Queen Hill (\$/y)	Severn (\$/y)	Original Throughput with HMS (kt/y)	New Throughput without HMS (kt/y)	Factor	Adjusted Operating Costs (\$/y)
310	- CRUSHING & SCREENING	1,464,254	1,464,254	600	600	1.00	1,464,254
320	- FINE ORE STORAGE	174,567	174,567	600	600	1.00	174,567
325	- HEAVY MEDIA SEPARATION (HMS)	1,001,435	957,347	600	0	0.00	0
330	- GRINDING AND CLASSIFICATION	2,423,864	2,423,864	460	600	1.30	3,161,012
331	- SULPHIDE FLOAT & REGRIND	2,392,313	1,617,679	460	600	1.10	1,779,447
350	- COARSE GRAVITY	126,078	123,962	460	600	1.30	161,661
351	- SULPHIDE DRESSING FLOTATION	157,703	97,368	600	600	1.00	97,368
353	- GRAVITY REGRIND & CLASSIFICATION	680,187	713,443	460	600	1.30	930,416
354	- FINE GRAVITY	174,389	174,389	600	600	1.00	174,389
355	- TIN FLOAT DESLIME	155,810	155,810	460	600	1.30	203,195
356	- TIN SULPHIDE PRE FLOTATION	346,202	198,573	460	600	1.30	258,963
357	- TIN SILICA FLOAT	359,167	326,558	460	600	1.30	425,871
360	- TIN FLOTATION & CONCENTRATE HANDLING	1,961,786	1,267,385	600	600	1.00	1,267,385
370	- TIN CONCENTRATE ACID LEACHING	2,622,986	1,392,420	600	600	1.00	1,392,420
380	- REAGENTS	297,120	297,120	600	600	1.00	297,120
390	- WATER SUPPLY	96,533	96,533	600	600	1.00	96,533
400	- TAILINGS	260,004	298,739	600	600	1.00	298,739
420	- AIR SERVICES	171,992	171,992	600	600	1.00	171,992
490	- SITE BUILDINGS	50,548	50,548	600	600	1.00	50,548
499	- PLANT PIPING	211,678	211,678	600	600	1.00	211,678
410	- POWER AND RETICULATION	317,837	317,837	600	600	1.00	317,837
	Workshop	205,230	205,230	600	600	1.00	205,230
	Laboratory	230,710	230,710	600	600	1.00	230,710
	Administration	606,988	606,988	600	600	1.00	606,988
	Management & Services	773,500	773,500	600	600	1.00	773,500
	Production Labour	2,892,500	2,892,500	600	600	1.00	2,892,500
	Maintenance Labour	1,614,600	1,614,600	600	600	1.00	1,614,600
	Total	21,769,983	18,855,595				19,258,924
	\$/Tonne Treated	36.28	31.43				32.10
CHANGE IN OPEX ESTIMATE							
	Total						-\$403,329
	\$/Tonne Treated						-\$0.67
Recovery Improvement necessary to offset increased in OPEX without HMS							
	Net payment/% Sn recovery ⁽¹⁾			AU\$/y/% Sn recovery			\$1,400,000
	Recovery Improvement necessary to offset increased in OPEX without HMS						0.3%
	Expected recovery improvement without HMS⁽⁴⁾						2.2%

Notes;

1. Average value based on Net Smelter Return analysis
2. Only costs for areas 325, 330, 331, 350, 353, 355, 356, 357 and 380 (highlighted in red) are expected to be impacted by the removal of HMS from the circuit. Costs for other areas are not expected to be impacted within the accuracy of the estimate.
3. Adjusted operating costs = Original operating cost x (New throughput/Original throughput)
4. Expected recovery improvement is based on GR PFS PDC which showed 3.0% Sn loss to floats for Severn. Expected recovery improvement = 3.0% x 72% downstream Sn recovery = 2.2%
5. Based on GR PFS PDC



WorleyParsons

resources & energy

EcoNomicsTM

Appendix 2 – CAPEX and OPEX estimates assuming 34.5% mass rejection in HMS

Expected Impact of Removal of Heavy Media Separation Circuit on Capital Costs

Mass rejection in HMS **35.4%** ⁽⁴⁾ (as per recent HMS testwork)

Area	Description	GRES PFS Capital Cost (+/-25%)					Factored Capital Cost			
		Equip/Matl \$	Labour \$	Freight \$	Contingency \$	TOTAL \$	Original Throughput with HMS (kt/y)	New Throughput without HMS (kt/y)	Factor	Adjusted Costs \$
200	- PLANT SITE BULK EARTHWORKS	406,400	46,200	455	28,005	481,060	600	600	1.00	481,060
310	- CRUSHING	3,882,601	1,252,014	203,682	350,317	5,688,613	600	600	1.00	5,688,613
320	- ORE STORAGE	1,397,894	1,067,330	61,947	166,525	2,693,697	600	600	1.00	2,693,697
325	- HEAVY MEDIA SEPARATION	2,502,243	566,604	67,540	209,910	3,346,297	600	0	0.00	0
330	- GRINDING AND CLASSIFICATION	2,824,521	1,037,197	242,675	251,326	4,355,718	388	600	1.30	5,661,353
331	- SULPHIDE FLOTATION ⁽⁵⁾	3,722,954	775,663	151,794	260,195	4,910,606				
	Roughing					1,636,869	388	600	1.30	2,127,523
	Regrind & cleaning					3,273,737	600	600	1.00	3,273,737
350	- COARSE GRAVITY	859,903	273,160	23,518	70,413	1,226,995	388	600	1.30	1,594,789
351	- SULPHIDE DRESSING FLOTATION	645,287	178,506	28,026	45,223	897,042	600	600	1.00	897,042
352	- GRAVITY REGRIND & CLASSIFICATION	1,971,471	718,330	116,172	148,629	2,954,602	388	600	1.30	3,840,250
353	- FINE GRAVITY	700,831	249,173	32,962	60,811	1,043,776	600	600	1.00	1,043,776
354	- SULPHIDE SCAVENGER FLOTATION	636,829	270,039	27,307	51,752	985,927	388	600	1.30	1,281,461
355	- SILICA FLOTATION	860,888	310,195	42,994	69,252	1,283,330	388	600	1.30	1,668,011
356	- TIN FLOTATION	2,307,913	522,646	55,346	174,528	3,060,433	388	600	1.30	3,977,804
357	- CONCENTRATE ACID LEACHING	502,100	166,988	13,194	42,350	724,632	600	600	1.00	724,632
358	- TIN CONCENTRATE HANDLING AND FILTRATION	971,281	244,774	22,906	75,853	1,314,814	600	600	1.00	1,314,814
360	- REAGENTS	1,771,260	639,626	50,707	139,243	2,600,836	600	600	1.00	2,600,836
370	- POWER AND RETICULATION	5,645,930	2,708,343	114,296	503,643	8,972,213	600	600	1.00	8,972,213
390	- WATER SUPPLY	613,179	281,625	18,961	57,603	971,368	600	600	1.00	971,368
400	- TAILINGS	1,880,583	567,789	74,034	152,753	2,675,160	600	600	1.00	2,675,160
411	- FUEL FARM	292,119	55,806	6,670	22,954	377,550	600	600	1.00	377,550
420	- COMPRESSED AIR	446,899	57,070	11,327	28,121	543,417	600	600	1.00	543,417
490	- SITE BUILDINGS	581,010	242,279	47,363	50,012	920,664	600	600	1.00	920,664
495	- MOBILE PLANT & EQUIPMENT	1,755,000	7,768	70,525	91,859	1,925,152	600	600	1.00	1,925,152
499	- PLANT PIPING	2,064,532	2,262,628	9,373	294,385	4,630,918	600	600	1.00	4,630,918
804	- CONSTRUCTION EQUIPMENT	1,404,509	899,545	80,800	148,896	2,533,750	600	600	1.00	2,533,750
Total Direct Costs		40,648,138	15,401,299	1,574,574	3,494,558	61,118,570				62,419,590
Indirect Costs										
500	- ENGINEERING	107,500	13,139,963	0	671,623	13,919,086	23%			14,215,379
510	- COMMISSIONING	51,560	904,207	0	49,288	1,005,056	2%			1,026,450
600	- PRELIMINARIES AND GENERAL	2,096,131	74,820	116,878	114,391	2,402,221	4%			2,453,357
700	- OWNERS COSTS	1,598,636	0	0	0	1,598,636	3%			1,632,666
Total Indirect Costs		3,853,827	14,118,990	116,878	835,303	18,924,997	31%			19,327,852
TOTAL CAPITAL ESTIMATE		44,501,965	29,520,289	1,691,452	4,329,861	80,043,567				81,747,442
CHANGE IN TOTAL CAPITAL ESTIMATE										-\$1,703,875

Notes;

1. Only costs for areas 325, 330, 331 (roughing only), 350, 352, 355 and 356 (highlighted in red) are expected to be impacted by the removal of HMS from the circuit. Costs for other areas are not expected to be impacted within the accuracy of the estimate.

2. Adjusted Direct costs = Original direct cost x (New throughput/Original throughput)^{0.6}

3. Indirect costs are calculated as a percentage of the total direct costs

4. Based on results for ALS Metallurgy job no. T0879 test no. DRS01 which showed 35.4% mass rejection for SBC

5. Sulphide flotation costs are assumed to be split 1/3 roughing and 2/3 cleaning plus regrind.

Expected Impact of Removal of Heavy Media Separation Circuit on Operating Costs

Mass rejection in HMS

35.4% ⁽⁵⁾

(as per recent HMS testwork)

AREA	Description	GRES PFS OPEX (+/-25%)		Severn Factored OPEX			
		Queen Hill (\$/y)	Severn (\$/y)	Original Throughput with HMS (kt/y)	New Throughput without HMS (kt/y)	Factor	Adjusted Operating Costs (\$/y)
310	- CRUSHING & SCREENING	1,464,254	1,464,254	600	600	1.00	1,464,254
320	- FINE ORE STORAGE	174,567	174,567	600	600	1.00	174,567
325	- HEAVY MEDIA SEPARATION (HMS)	1,001,435	957,347	600	0	0.00	0
330	- GRINDING AND CLASSIFICATION	2,423,864	2,423,864	388	600	1.55	3,752,111
331	- SULPHIDE FLOAT & REGRIND	2,392,313	1,617,679	388	600	1.10	1,779,447
350	- COARSE GRAVITY	126,078	123,962	388	600	1.55	191,892
351	- SULPHIDE DRESSING FLOTATION	157,703	97,368	600	600	1.00	97,368
353	- GRAVITY REGRIND & CLASSIFICATION	680,187	713,443	388	600	1.55	1,104,401
354	- FINE GRAVITY	174,389	174,389	600	600	1.00	174,389
355	- TIN FLOAT DESLIME	155,810	155,810	388	600	1.55	241,192
356	- TIN SULPHIDE PRE FLOTATION	346,202	198,573	388	600	1.55	307,389
357	- TIN SILICA FLOAT	359,167	326,558	388	600	1.55	505,508
360	- TIN FLOTATION & CONCENTRATE HANDLING	1,961,786	1,267,385	600	600	1.00	1,267,385
370	- TIN CONCENTRATE ACID LEACHING	2,622,986	1,392,420	600	600	1.00	1,392,420
380	- REAGENTS	297,120	297,120	600	600	1.00	297,120
390	- WATER SUPPLY	96,533	96,533	600	600	1.00	96,533
400	- TAILINGS	260,004	298,739	600	600	1.00	298,739
420	- AIR SERVICES	171,992	171,992	600	600	1.00	171,992
490	- SITE BUILDINGS	50,548	50,548	600	600	1.00	50,548
499	- PLANT PIPING	211,678	211,678	600	600	1.00	211,678
410	- POWER AND RETICULATION	317,837	317,837	600	600	1.00	317,837
	Workshop	205,230	205,230	600	600	1.00	205,230
	Laboratory	230,710	230,710	600	600	1.00	230,710
	Administration	606,988	606,988	600	600	1.00	606,988
	Management & Services	773,500	773,500	600	600	1.00	773,500
	Production Labour	2,892,500	2,892,500	600	600	1.00	2,892,500
	Maintenance Labour	1,614,600	1,614,600	600	600	1.00	1,614,600
	Total	21,769,983	18,855,595				20,220,297
	\$/Tonne Treated	36.28	31.43				33.70
CHANGE IN OPEX ESTIMATE							
	Total						-\$1,364,702
	\$/Tonne Treated						-\$2.27
Recovery Improvement necessary to offset increased in OPEX without HMS							
	Net payment/% Sn recovery ⁽¹⁾			AU\$/y/% Sn recovery			\$1,400,000
	Recovery Improvement necessary to offset increased in OPEX without HMS						1.0%
	Expected recovery improvement without HMS⁽⁴⁾						2.8%

Notes;

1. Average value based on Net Smelter Return analysis
2. Only costs for areas 325, 330, 331, 350, 353, 355, 356 and 357 (highlighted in red) are expected to be impacted by the removal of HMS from the circuit. Costs for other areas are not expected to be impacted within the accuracy of the estimate.
3. Adjusted operating costs = Original operating cost x (New throughput/Original throughput)
4. Expected recovery improvement is based on results for ALS Metallurgy job no. T0879 test no. DRS01 which showed 3.9% Sn loss to floats for SBC. Expected recovery improvement = 3.9% x 72% downstream Sn recovery = 2.8%
5. Based on results for ALS Metallurgy job no. T0879 test no. DRS01 which showed 35.4% mass rejection for SBC



WorleyParsons

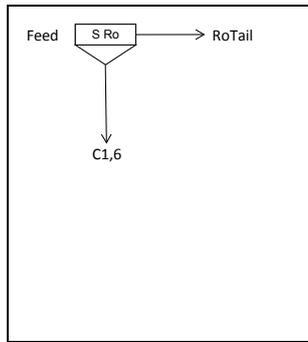
resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED
HEEMSKIRK TIN PROJECT
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 6 – Sulfide Flotation Results

Milling		Primary	Regrind
Mill	type	Long	Short
Media	type	MS ball	MS ball
Media	kg	12	0
Solids	g	2000	0
Water	g	1000	0
Time	min/sec	26	0
Speed	rpm	50	0
Lime	g	0	0
End pH	pH	6.7	0
End p80	µm	100	0



PROJECT	T0879
TEST NO	T02
DATE	220514
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 100um

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
Speed	900	W/h	kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1601						2					
Condition		50		25					2					
Condition					40				1					
Sulphide Ro C1	5.4			25		22				3-7	3.0	3	300	40
Condition		50			30				2					
Condition						7			1					
Sulphide Ro C2	5.1			50						3-8	3.0	6	350	52
Condition		50			15				2					
Condition									1					
Sulphide Ro C3	4.8					7				4-8	3.0	9	330	36
Condition		50							2					
Condition					15				1					
Sulphide Ro C4	4.7					7				4-9	3.0	12	340	45
Condition		25							2					
Condition					15				1					
Sulphide Ro C5	4.8					10				4-9	4.0	16	400	26
Condition									2					
Condition					15				2					
Sulphide Ro C6	5.0					15				4-9	4.0	20	400	15
REAGENT TOTALS (g/t)		226	1601	100	130	69								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T02 RoC1	121.0	6.1	0.29	1.7	37.5	8.7	0.30	6.7	39.8	16.0	4.62	0.9
RoC2	183.2	9.2	0.20	1.8	43.5	15.2	0.29	9.8	42.4	25.7	3.51	1.1
RoC3	118.4	5.9	0.27	1.6	39.7	9.0	0.41	8.9	38.0	14.9	6.19	1.2
RoC4	153.0	7.7	0.24	1.8	42.0	12.3	0.38	10.7	44.0	22.3	4.54	1.2
RoC5	105.4	5.3	0.51	2.7	37.4	7.5	0.79	15.3	32.0	11.2	12.8	2.3
RoC6	58.6	2.9	0.76	2.2	31.1	3.5	2.38	25.6	18.9	3.7	21.5	2.1
Ro Tail	1255.8	62.9	1.41	88.1	18.4	43.9	0.10	23.1	1.50	6.2	42.7	91.1
CALC	1995.4	100.00	1.01	100.0	26.3	100.0	0.27	100.0	15.1	100.0	29.5	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T02 RoC1	121.0	6.1	0.29	1.7	37.5	8.7	0.30	6.7	39.8	16.0	4.62	0.9
RoC2	304.2	15.2	0.24	3.6	41.1	23.8	0.29	16.4	41.4	41.7	3.95	2.0
RoC3	422.6	21.2	0.25	5.2	40.7	32.8	0.33	25.3	40.4	56.6	4.58	3.3
RoC4	575.6	28.8	0.24	7.0	41.1	45.1	0.34	36.0	41.4	78.9	4.57	4.5
RoC5	681.0	34.1	0.29	9.7	40.5	52.6	0.41	51.3	39.9	90.1	5.83	6.8
RoC6	739.6	37.1	0.32	11.9	39.7	56.1	0.57	76.9	38.3	93.8	7.08	8.9
FEED	1995.4	100.0	1.01	100.0	26.3	100.0	0.27	100.0	15.1	100.0	29.5	100.0

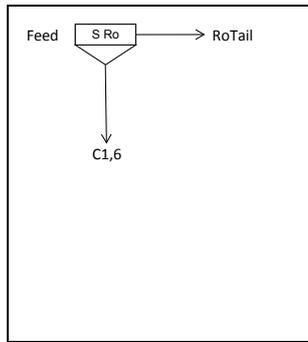
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T02 RoC1	121.0	6.1	0.13	1.2	0.79	1.8	0.96	1.0	0.07	1.3
RoC2	183.2	9.2	0.10	1.4	0.38	1.3	0.83	1.2	0.07	1.9
RoC3	118.4	5.9	0.16	1.4	0.57	1.3	1.47	1.4	0.10	1.8
RoC4	153.0	7.7	0.13	1.5	0.46	1.3	1.05	1.3	0.06	1.4
RoC5	105.4	5.3	0.33	2.6	1.13	2.2	3.04	2.6	0.14	2.2
RoC6	58.6	2.9	0.52	2.3	1.88	2.0	5.07	2.4	0.23	2.0
Ro Tail	1255.8	62.9	0.96	89.7	3.87	90.1	8.73	90.0	0.48	89.5
CALC	1995.4	100.00	0.67	100.0	2.70	100.0	6.11	100.0	0.34	100.0
ASSAY HEAD										

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T02 RoC1	121.0	6.1	0.13	1.2	0.79	1.8	0.96	1.0	0.07	1.3
RoC2	304.2	15.2	0.11	2.5	0.54	3.1	0.88	2.2	0.07	3.2
RoC3	422.6	21.2	0.13	3.9	0.55	4.3	1.05	3.6	0.08	4.9
RoC4	575.6	28.8	0.13	5.4	0.53	5.6	1.05	4.9	0.07	6.3
RoC5	681.0	34.1	0.16	8.0	0.62	7.8	1.36	7.6	0.08	8.5
RoC6	739.6	37.1	0.19	10.3	0.72	9.9	1.65	10.0	0.10	10.5
FEED	1995.4	100.0	0.67	100.0	2.70	100.0	6.11	100.0	0.34	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail	1255.8	62.9	1.41	88.1	18.4	43.9	0.10	23.1	1.50	6.2	42.7	91.1
FEED		100.0	1.01	100.0	26.3	100.0	0.27	100.0	15.1	100.0	29.5	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail	1255.8	62.9	0.96	89.7	3.87	90.1	8.73	90.0	0.48	89.5
FEED		200.0	0.67	100.0	2.70	100.0	6.11	100.0	0.34	100.0

Milling		Primary	Regrind
Mill	type	Long	Short
Media	type	MS ball	MS ball
Media	kg	12	6
Solids	g	2000	0
Water	g	1000	0
Time	min/sec	23	0
Speed	rpm	50	0
Lime	g	0	0
End pH	pH	6.72	0
End p80	µm	130	0



PROJECT	T0879
TEST NO	T03
DATE	220514
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 130µm

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
Speed	900	W/h	kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1375						4					
Condition		50		25					4					
Condition					40				1					
Sulphide Ro C1	5.4			25		22				3-7	3.0	3	350	55
Condition		50			30				2					
Condition									1					
Sulphide Ro C2	5.1			50		7				3-8	3.0	6	400	49
Condition		50			15				2					
Condition									1					
Sulphide Ro C3	4.8					7				4-8	3.0	9	340	31
Condition		50							2					
Condition									2					
Sulphide Ro C4	4.7				15					4-9	3.0	12	330	30
Condition		25							2					
Condition									1					
Sulphide Ro C5	4.8					10				4-9	4.0	16	300	25
Condition									2					
Condition									2					
Sulphide Ro C6	5.0				15					4-9	4.0	20	370	17
REAGENT TOTALS (g/t)		225	1375	100	130	69								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T03 RoC1	192.0	9.6	0.16	1.5	41.4	15.2	0.58	20.3	45.3	29.1	2.61	0.8
RoC2	194.7	9.8	0.28	2.7	41.2	15.3	0.34	12.1	41.2	26.9	4.46	1.5
RoC3	105.6	5.3	0.40	2.1	40.5	8.2	0.48	9.2	34.8	12.3	7.85	1.4
RoC4	98.0	4.9	0.37	1.8	39.3	7.4	0.49	8.7	36.6	12.0	8.48	1.4
RoC5	75.3	3.8	0.54	2.0	37.6	5.4	0.91	12.5	31.3	7.9	12.1	1.5
RoC6	61.7	3.1	0.76	2.3	32.8	3.9	1.67	18.8	20.5	4.2	19.9	2.1
Ro Tail	1268.8	63.6	1.39	87.5	18.4	44.6	0.08	18.5	1.77	7.5	42.7	91.3
CALC	1996.1	100.0	1.01	100.0	26.2	100.0	0.28	100.0	15.0	100.0	29.7	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T03 RoC1	192.0	9.6	0.16	1.5	41.4	15.2	0.58	20.3	45.3	29.1	2.61	0.8
RoC2	386.7	19.4	0.22	4.2	41.3	30.5	0.46	32.3	43.2	56.0	3.54	2.3
RoC3	492.3	24.7	0.26	6.3	41.1	38.7	0.46	41.5	41.4	68.3	4.47	3.7
RoC4	590.3	29.6	0.28	8.1	40.8	46.1	0.47	50.3	40.6	80.3	5.13	5.1
RoC5	665.6	33.3	0.31	10.1	40.5	51.5	0.52	62.8	39.6	88.2	5.91	6.6
RoC6	727.3	36.4	0.35	12.5	39.8	55.4	0.62	81.5	38.0	92.5	7.10	8.7
FEED	1996.1	100.0	1.01	100.0	26.2	100.0	0.28	100.0	15.0	100.0	29.7	100.0

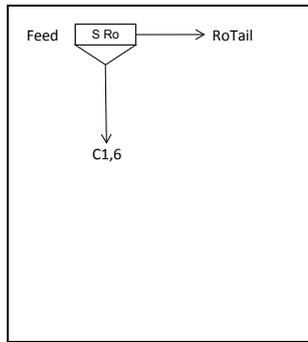
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T03 RoC1	192.0	9.6	0.08	1.1	0.34	1.2	0.63	1.0	0.04	1.2
RoC2	194.7	9.8	0.12	1.7	0.45	1.6	1.04	1.6	0.07	2.0
RoC3	105.6	5.3	0.20	1.6	0.71	1.4	1.82	1.5	0.12	1.9
RoC4	98.0	4.9	0.23	1.7	0.79	1.4	2.10	1.7	0.11	1.6
RoC5	75.3	3.8	0.32	1.8	1.13	1.6	2.92	1.8	0.15	1.7
RoC6	61.7	3.1	0.49	2.3	1.85	2.1	4.74	2.4	0.23	2.1
Ro Tail	1268.8	63.6	0.95	89.8	3.82	90.6	8.82	90.1	0.47	89.5
CALC	1996.1	100.0	0.67	100.0	2.68	100.0	6.22	100.0	0.33	100.0
ASSAY HEAD										

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T03 RoC1	192.0	9.6	0.08	1.1	0.34	1.2	0.63	1.0	0.04	1.2
RoC2	386.7	19.4	0.10	2.9	0.40	2.9	0.84	2.6	0.06	3.2
RoC3	492.3	24.7	0.12	4.5	0.46	4.3	1.05	4.2	0.07	5.1
RoC4	590.3	29.6	0.14	6.1	0.52	5.7	1.22	5.8	0.08	6.7
RoC5	665.6	33.3	0.16	7.9	0.59	7.3	1.41	7.6	0.08	8.4
RoC6	727.3	36.4	0.19	10.2	0.69	9.4	1.70	9.9	0.10	10.5
FEED	1996.1	100.0	0.67	100.0	2.68	100.0	6.22	100.0	0.33	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail	1268.8	63.6	1.39	87.5	18.4	44.6	0.08	18.5	1.77	7.5	42.7	91.3
FEED		100.0	1.01	100.0	26.2	100.0	0.28	100.0	15.0	100.0	29.7	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail	1268.8	63.6	0.95	89.8	3.82	90.6	8.82	90.1	0.47	89.5
FEED		200.0	0.67	100.0	2.68	100.0	6.22	100.0	0.33	100.0

Milling		Primary	Regrind
Mill	type	Long	Short
Media	type	MS ball	MS ball
Media	kg	12	6
Solids	g	2000	0
Water	g	1000	0
Time	min/sec	20	0
Speed	rpm	50	0
Lime	g	0	0
End pH	pH	6.69	0
End p80	µm	160	0



PROJECT	T0879
TEST NO	T04
DATE	220514
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 160um

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
Speed	900	W/h	kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1273						4					
Condition		50		25					4					
Condition					40				1					
Sulphide Ro C1	5.4			25		22				3-7	3.0	3	400	58
Condition		50			30				2					
Condition						7			1					
Sulphide Ro C2	5.1			50						3-8	3.0	6	364	45
Condition		50			15				2					
Condition						7			1					
Sulphide Ro C3	4.8									4-8	3.0	9	260	36
Condition		50			15				2					
Condition						7			2					
Sulphide Ro C4	4.7									4-9	3.0	12	310	35
Condition		25			15				2					
Condition						10			1					
Sulphide Ro C5	4.8									4-9	4.0	16	300	26
Condition					15				2					
Condition						15			2					
Sulphide Ro C6	5.0									4-9	4.0	20	300	17
REAGENT TOTALS (g/t)		225	1273	100	130	69								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T04 RoC1	232.2	11.6	0.20	2.3	41.5	18.2	0.48	20.1	44.9	34.5	3.01	1.2
RoC2	165.2	8.3	0.26	2.1	42.2	13.2	0.35	10.4	40.6	22.2	4.44	1.2
RoC3	93.8	4.7	0.36	1.7	39.7	7.0	0.60	10.2	35.2	10.9	7.13	1.1
RoC4	107.8	5.4	0.37	2.0	39.8	8.1	0.59	11.5	38.3	13.7	7.71	1.4
RoC5	79.2	4.0	0.65	2.6	36.4	5.4	1.55	22.2	27.8	7.3	13.2	1.8
RoC6	51.1	2.6	0.88	2.2	30.9	3.0	1.03	9.5	18.2	3.1	22.7	2.0
Ro Tail	1272.2	63.6	1.38	87.1	18.8	45.1	0.07	16.1	1.98	8.3	42.7	91.4
CALC	2001.5	100.0	1.01	100.0	26.5	100.0	0.28	100.0	15.1	100.0	29.7	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T04 RoC1	232.2	11.6	0.20	2.3	41.5	18.2	0.48	20.1	44.9	34.5	3.01	1.2
RoC2	397.4	19.9	0.22	4.4	41.8	31.3	0.43	30.6	43.1	56.7	3.60	2.4
RoC3	491.2	24.5	0.25	6.1	41.4	38.4	0.46	40.7	41.6	67.6	4.28	3.5
RoC4	599.0	29.9	0.27	8.1	41.1	46.5	0.48	52.2	41.0	81.3	4.90	4.9
RoC5	678.2	33.9	0.32	10.6	40.6	51.9	0.61	74.4	39.5	88.6	5.87	6.7
RoC6	729.3	36.4	0.36	12.9	39.9	54.9	0.64	83.9	38.0	91.7	7.04	8.6
FEED	2001.5	100.0	1.01	100.0	26.5	100.0	0.28	100.0	15.1	100.0	29.7	100.0

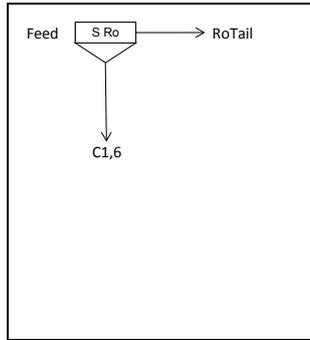
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T04 RoC1	232.2	11.6	0.09	1.5	0.35	1.5	0.68	1.2	0.05	1.7
RoC2	165.2	8.3	0.12	1.4	0.48	1.4	1.06	1.4	0.08	1.9
RoC3	93.8	4.7	0.19	1.3	0.71	1.2	1.68	1.2	0.11	1.5
RoC4	107.8	5.4	0.22	1.7	0.79	1.5	1.92	1.6	0.10	1.6
RoC5	79.2	4.0	0.37	2.1	1.28	1.8	3.13	2.0	0.18	2.1
RoC6	51.1	2.6	0.57	2.1	2.10	1.9	5.23	2.1	0.28	2.1
Ro Tail	1272.2	63.6	1.00	90.0	3.93	90.6	9.02	90.4	0.48	89.1
CALC	2001.5	100.0	0.71	100.0	2.76	100.0	6.34	100.0	0.34	100.0
ASSAY HEAD										

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T04 RoC1	232.2	11.6	0.09	1.5	0.35	1.5	0.68	1.2	0.05	1.7
RoC2	397.4	19.9	0.10	2.9	0.40	2.9	0.84	2.6	0.06	3.6
RoC3	491.2	24.5	0.12	4.1	0.46	4.1	1.00	3.9	0.07	5.1
RoC4	599.0	29.9	0.14	5.8	0.52	5.7	1.16	5.5	0.08	6.7
RoC5	678.2	33.9	0.16	7.9	0.61	7.5	1.39	7.5	0.09	8.8
RoC6	729.3	36.4	0.19	10.0	0.71	9.4	1.66	9.6	0.10	10.9
FEED	2001.5	100.0	0.71	100.0	2.76	100.0	6.34	100.0	0.34	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail	1272.2	63.6	1.38	87.1	18.8	45.1	0.07	16.1	1.98	8.3	42.7	91.4
FEED		100.0	1.01	100.0	26.5	100.0	0.28	100.0	15.1	100.0	29.7	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail	1272.2	63.6	1.00	90.0	3.93	90.6	9.02	90.4	0.48	89.1
FEED		200.0	0.71	100.0	2.76	100.0	6.34	100.0	0.34	100.0

Milling		Primary	Regrind
Mill	type	Long	Short
Media	type	MS ball	MS ball
Media	kg	12	6
Solids	g	2000	0
Water	g	1000	0
Time	min/sec	16	0
Speed	rpm	50	0
Lime	g	0	0
End pH	pH	6.73	0
End p80	µm	240	0



PROJECT	T0879
TEST NO	T05
DATE	220514
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 240um

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
Speed	900	W/h	kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1133						4					
Condition		50		25	40	22			4					
Condition									1					
Sulphide Ro C1	5.4			25						3-7	3.0	3	386	58
Condition		50			30				2					
Condition									1					
Sulphide Ro C2	5.1			50		7				3-8	3.0	6	260	52
Condition		50			15				2					
Condition									1					
Sulphide Ro C3	4.8					7								
Condition		50							2	4-8	3.0	9	60	46
Condition									2					
Sulphide Ro C4	4.7				15									
Condition		25				7			2	4-9	3.0	12	250	42
Condition									1					
Sulphide Ro C5	4.8													
Condition					15				2	4-9	4.0	16	350	36
Condition									1					
Sulphide Ro C6	5.0													
Condition					15				2	4-9	4.0	20	350	18
Condition									2					
REAGENT TOTALS (g/t)		226	1133	101	131	70								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T05 RoC1	223.0	11.2	0.19	2.1	41.1	17.5	0.35	14.0	44.4	33.9	3.02	1.1
RoC2	134.0	6.7	0.22	1.4	43.3	11.1	0.32	7.7	39.4	18.1	3.70	0.8
RoC3	27.7	1.4	0.25	0.3	39.6	2.1	0.58	2.9	38.8	3.7	4.88	0.2
RoC4	105.3	5.3	0.28	1.4	39.9	8.0	0.55	10.4	40.2	14.5	5.76	1.0
RoC5	126.3	6.3	0.52	3.2	39.8	9.6	1.29	29.3	35.7	15.4	8.33	1.8
RoC6	64.1	3.2	0.85	2.6	32.2	4.0	1.26	14.5	21.1	4.6	20.2	2.2
Ro Tail	1309.6	65.8	1.40	88.9	19.0	47.6	0.09	21.2	2.19	9.8	42.1	92.8
CALC	1990.0	100.0	1.04	100.0	26.3	100.0	0.28	100.0	14.7	100.0	29.8	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T05 RoC1	223.0	11.2	0.19	2.1	41.1	17.5	0.35	14.0	44.4	33.9	3.02	1.1
RoC2	357.0	17.9	0.20	3.5	41.9	28.7	0.34	21.7	42.5	52.0	3.28	2.0
RoC3	384.7	19.3	0.20	3.8	41.8	30.8	0.36	24.6	42.3	55.6	3.39	2.2
RoC4	490.0	24.6	0.22	5.3	41.4	38.8	0.40	35.0	41.8	70.1	3.90	3.2
RoC5	616.3	31.0	0.28	8.4	41.0	48.4	0.58	64.3	40.6	85.6	4.81	5.0
RoC6	680.4	34.2	0.34	11.1	40.2	52.4	0.64	78.8	38.7	90.2	6.26	7.2
FEED	1990.0	100.0	1.04	100.0	26.3	100.0	0.28	100.0	14.7	100.0	29.8	100.0

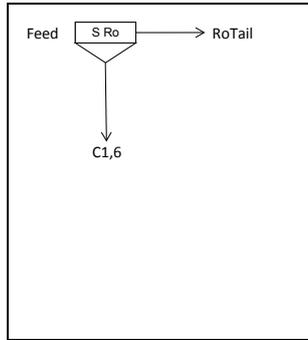
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T05 RoC1	223.0	11.2	0.09	1.4	0.37	1.5	0.70	1.2	0.05	1.6
RoC2	134.0	6.7	0.11	1.0	0.39	0.9	0.86	0.9	0.06	1.1
RoC3	27.7	1.4	0.14	0.3	0.53	0.3	1.27	0.3	0.08	0.3
RoC4	105.3	5.3	0.16	1.2	0.59	1.1	1.50	1.2	0.08	1.2
RoC5	126.3	6.3	0.23	2.1	0.79	1.8	1.93	1.9	0.12	2.2
RoC6	64.1	3.2	0.50	2.3	1.76	2.0	4.38	2.2	0.26	2.4
Ro Tail	1309.6	65.8	0.99	91.7	3.92	92.4	8.93	92.2	0.49	91.2
CALC	1990.0	100.0	0.71	100.0	2.79	100.0	6.37	100.0	0.35	100.0
ASSAY HEAD										

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T05 RoC1	223.0	11.2	0.09	1.4	0.37	1.5	0.70	1.2	0.05	1.6
RoC2	357.0	17.9	0.10	2.5	0.38	2.4	0.76	2.1	0.05	2.7
RoC3	384.7	19.3	0.10	2.7	0.39	2.7	0.80	2.4	0.06	3.0
RoC4	490.0	24.6	0.11	3.9	0.43	3.8	0.95	3.7	0.06	4.2
RoC5	616.3	31.0	0.14	6.0	0.51	5.6	1.15	5.6	0.07	6.4
RoC6	680.4	34.2	0.17	8.3	0.62	7.6	1.45	7.8	0.09	8.8
FEED	1990.0	100.0	0.71	100.0	2.79	100.0	6.37	100.0	0.35	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail	1309.6	65.8	1.40	88.9	19.0	47.6	0.09	21.2	2.19	9.8	42.1	92.8
FEED		100.0	1.04	100.0	26.3	100.0	0.28	100.0	14.7	100.0	29.8	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail	1309.6	65.8	0.99	91.7	3.92	92.4	8.93	92.2	0.49	91.2
FEED		200.0	0.71	100.0	2.79	100.0	6.37	100.0	0.35	100.0

Milling		Primary	Regrind
Mill	type	Long	Short
Media	type	MS ball	MS ball
Media	kg	12	6
Solids	g	2000	0
Water	g	1000	0
Time	min/sec	11/5/3	0
Speed	rpm	50	0
Lime	g	0	0
End pH	pH	6.75	0
End p80	µm	240	0



PROJECT	T0879
TEST NO	T06
DATE	260514
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 240um

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
Speed	900	W/h	kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1037						4					
Condition		50		25		40			4					
Condition									1					
Sulphide Ro C1	5.4			25		22				3-7	3.0	3	380	56
Condition		50				30			2					
Condition									1					
Sulphide Ro C2	5.1			50		7				3-8	3.0	6	200	48
Condition		50				15			2					
Condition									1					
Sulphide Ro C3	4.8					7				4-8	3.0	9	100	25
Condition		50							2					
Condition									2					
Sulphide Ro C4	4.8					7				4-9	3.0	12	220	37
Condition		25							2					
Condition									1					
Sulphide Ro C5	4.8					10				4-9	4.0	16	400	38
Condition									2					
Condition									2					
Sulphide Ro C6	4.8					15				4-9	4.0	20	450	23
REAGENT TOTALS (g/t)		227	1037	101	131	70								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T06 RoC1	213.9	10.8	0.18	1.9	41.0	16.7	0.34	13.3	43.8	31.0	2.89	1.1
RoC2	96.4	4.9	0.22	1.1	41.2	7.6	0.56	9.9	40.4	12.9	4.33	0.7
RoC3	25.3	1.3	0.29	0.4	39.4	1.9	0.79	3.7	35.2	2.9	8.40	0.4
RoC4	81.6	4.1	0.27	1.1	40.1	6.2	0.86	12.9	39.2	10.6	6.27	0.9
RoC5	151.9	7.7	0.40	3.0	40.6	11.8	0.79	22.0	39.5	19.8	6.61	1.7
RoC6	105.4	5.3	0.77	4.1	36.5	7.3	0.99	19.1	29.6	10.3	13.7	2.5
Ro Tail	1309.4	66.0	1.35	88.4	19.4	48.5	0.08	19.2	2.88	12.5	41.3	92.8
CALC	1983.9	100.0	1.01	100.0	26.4	100.0	0.28	100.0	15.2	100.0	29.4	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T06 RoC1	213.9	10.8	0.18	1.9	41.0	16.7	0.34	13.3	43.8	31.0	2.89	1.1
RoC2	310.3	15.6	0.19	3.0	41.1	24.3	0.41	23.2	42.7	43.9	3.34	1.8
RoC3	335.6	16.9	0.20	3.4	40.9	26.2	0.44	26.9	42.2	46.8	3.72	2.1
RoC4	417.2	21.0	0.21	4.5	40.8	32.4	0.52	39.7	41.6	57.4	4.22	3.0
RoC5	569.1	28.7	0.26	7.5	40.7	44.2	0.59	61.7	41.0	77.2	4.86	4.7
RoC6	674.5	34.0	0.34	11.6	40.1	51.5	0.65	80.8	39.2	87.5	6.23	7.2
FEED	1983.9	100.0	1.01	100.0	26.4	100.0	0.28	100.0	15.2	100.0	29.4	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T06 RoC1	213.9	10.8	0.08	1.3	0.35	1.4	0.67	1.2	0.05	1.6
RoC2	96.4	4.9	0.11	0.8	0.47	0.8	1.01	0.8	0.07	1.0
RoC3	25.3	1.3	0.21	0.4	0.88	0.4	2.10	0.4	0.11	0.4
RoC4	81.6	4.1	0.16	1.0	0.60	0.9	1.46	1.0	0.08	1.0
RoC5	151.9	7.7	0.18	2.0	0.60	1.7	1.28	1.6	0.09	2.0
RoC6	105.4	5.3	0.33	2.5	1.11	2.2	2.61	2.3	0.18	2.8
Ro Tail	1309.4	66.0	0.96	92.1	3.81	92.6	8.46	92.6	0.47	91.2
CALC	1983.9	100.0	0.69	100.0	2.72	100.0	6.03	100.0	0.34	100.0
ASSAY HEAD										

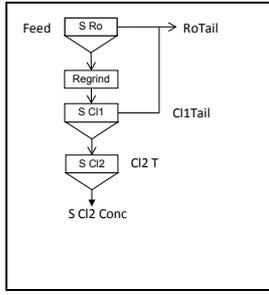
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T06 RoC1	213.9	10.8	0.08	1.3	0.35	1.4	0.67	1.2	0.05	1.6
RoC2	310.3	15.6	0.09	2.0	0.39	2.2	0.78	2.0	0.06	2.6
RoC3	335.6	16.9	0.10	2.4	0.42	2.6	0.88	2.5	0.06	3.0
RoC4	417.2	21.0	0.11	3.4	0.46	3.6	0.99	3.5	0.06	4.0
RoC5	569.1	28.7	0.13	5.4	0.50	5.2	1.07	5.1	0.07	6.0
RoC6	674.5	34.0	0.16	7.9	0.59	7.4	1.31	7.4	0.09	8.8
FEED	1983.9	100.0	0.69	100.0	2.72	100.0	6.03	100.0	0.34	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail	1309.4	66.0	1.35	88.4	19.4	48.5	0.08	19.2	2.88	12.5	41.3	92.8
FEED		100.0	1.01	100.0	26.4	100.0	0.28	100.0	15.2	100.0	29.4	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail	1309.4	66.0	0.96	92.1	3.81	92.6	8.46	92.6	0.47	91.2
FEED		200.0	0.69	100.0	2.72	100.0	6.03	100.0	0.34	100.0

Milling		Primary	Regrind
Mill type	Long	Stirred	
Media type	MS ball	Ceramic	
Media	12	2	
Solids	kg	2000	852
Water	g	1000	450
Time	min/sec	11/5/4	4
Speed	rpm	50	1200
Lime	g	0	0
End pH	pH	6.6	6.3
End p80	µm	250	26

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	38844
Cleaner	2.7	Finish	38859
0		W/h	14.48
Speed	900	kWh/t	20.0



PROJECT	T0879
TEST NO	T07
DATE	020614
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 250um
20kWh/t

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		718						2					
Condition		51		25					1					
Sulphide Ro C1	5.3				41	23			2	3-7	3.0	3.0	550	
Condition		51		25					1					
Sulphide Ro C2	5.3				31	8			2	3-8	3.0	6.0	300	
Condition		51		51					1					
Sulphide Ro C3	5.2				25	8			2	4-8	3.0	9.0	200	
Condition		51			15				1					
Sulphide Ro C4	5.3					8			2	4-9	3.0	12.0	300	
Condition		25							1					
Sulphide Ro C5	5.3				15	10			2	4-9	4.0	16.0	300	
Condition					15				1					
Sulphide Ro C6	5.3					15			2	4-9	4.0	20.0	300	
Condition									1					
Regrind	5.0		185	25					2					
Condition		102							1					
Sulphide Cl1	5.0				69	25			2	3-9	20.0	20.0	2000	
Condition			10			3			1					
Sulphide Cl2C1	4.9					5			2	2-9	3.0	3.0	400	46
Condition									1					
Sulphide Cl2C2						5			2	2-9	3.0	6.0	400	26
Condition									1					
Sulphide Cl2C3						5			2	2-9	4.0	10.0	500	12
Condition									1					
Sulphide Cl2C4						10			2	2-9	6.0	16.0	500	9
REAGENT TOTALS (g/t)		331	913	127	227	113								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T07 Cl2Con1	185.2	9.4	0.13	1.3	40.8	14.9	0.23	8.1	46.1	30.9	0.94	0.3
Cl2Con2	102.7	5.2	0.10	0.5	46.4	9.4	0.26	5.1	41.4	15.4	1.52	0.3
Cl2Con3	62.3	3.2	0.09	0.3	43.8	5.4	0.37	4.4	43.4	9.8	1.98	0.2
Cl2Con4	44.3	2.3	0.10	0.2	42.1	3.7	0.51	4.3	45.9	7.4	2.48	0.2
Cl2 Tail	54.5	2.8	0.43	1.2	34.1	3.7	0.79	8.2	29.0	5.7	14.5	1.3
Cl1 Tail	266.7	13.6	0.92	12.8	31.2	16.4	1.05	53.3	21.2	20.4	20.4	9.1
Ro Tail	1248.7	63.6	1.29	83.7	18.9	46.6	0.07	16.6	2.32	10.5	42.6	88.7
CALC	1964.4	100.0	0.98	100.0	25.8	100.0	0.27	100.0	14.1	100.0	30.5	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T07 Cl2Con1	185.2	9.4	0.13	1.3	40.8	14.9	0.23	8.1	46.1	30.9	0.94	0.3
Cl2Con2	287.9	14.7	0.12	1.8	42.8	24.3	0.24	13.2	44.4	46.2	1.15	0.6
Cl2Con3	350.2	17.8	0.11	2.1	43.0	29.7	0.26	17.6	44.2	56.0	1.30	0.8
Cl2Con4	394.5	20.1	0.11	2.3	42.9	33.4	0.29	21.9	44.4	63.4	1.43	0.9
Cl2 Tail	449.0	22.9	0.15	3.5	41.8	37.0	0.35	30.1	42.6	69.1	3.01	2.3
Cl1 Tail	715.7	36.4	0.44	16.3	37.9	53.4	0.61	83.4	34.6	89.5	9.49	11.3
FEED	1964.4	100.0	0.98	100.0	25.8	100.0	0.27	100.0	14.1	100.0	30.5	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T07 Cl2Con1	185.2	9.4	0.03	0.4	0.14	0.5	0.23	0.3	0.02	0.4
Cl2Con2	102.7	5.2	0.05	0.4	0.20	0.4	0.39	0.3	0.05	0.6
Cl2Con3	62.3	3.2	0.06	0.3	0.26	0.3	0.51	0.2	0.05	0.4
Cl2Con4	44.3	2.3	0.06	0.2	0.27	0.2	0.70	0.2	0.04	0.2
Cl2 Tail	54.5	2.8	0.32	1.2	1.39	1.4	4.14	1.8	0.22	1.4
Cl1 Tail	266.7	13.6	0.46	8.7	1.69	8.2	4.41	9.1	0.33	10.1
Ro Tail	1248.7	63.6	1.00	88.8	3.91	89.0	9.08	88.0	0.61	87.0
CALC	1964.4	100.0	0.72	100.0	2.79	100.0	6.56	100.0	0.45	100.0
ASSAY HEAD										

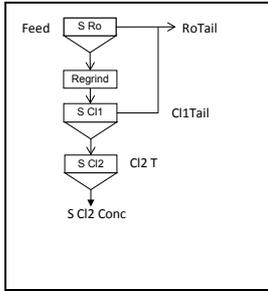
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T07 Cl2Con1	185.2	9.4	0.03	0.4	0.14	0.5	0.23	0.3	0.02	0.4
Cl2Con2	287.9	14.7	0.04	0.8	0.16	0.8	0.29	0.6	0.03	1.0
Cl2Con3	350.2	17.8	0.04	1.0	0.18	1.1	0.33	0.9	0.03	1.4
Cl2Con4	394.5	20.1	0.04	1.2	0.19	1.4	0.37	1.1	0.03	1.6
Cl2 Tail	449.0	22.9	0.08	2.5	0.33	2.7	0.83	2.9	0.06	2.9
Cl1 Tail	715.7	36.4	0.22	11.2	0.84	11.0	2.16	12.0	0.16	13.0
FEED	1964.4	100.0	0.72	100.0	2.79	100.0	6.56	100.0	0.45	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail+Cl1Tail Comb	1515.4	77.1	1.22	96.5	21.1	63.0	0.24	69.9	5.64	30.9	38.7	97.7
FEED	100.0		0.98	100.0	25.8	100.0	0.27	100.0	14.1	100.0	30.5	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail+Cl1Tail Comb	1515.4	77.1	0.90	97.5	3.52	97.3	8.26	97.1	0.56	97.1
FEED	200.0		0.72	100.0	2.79	100.0	6.56	100.0	0.45	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT	1248.7	63.6	1.29	83.7	18.9	46.6	0.07	16.6	2.32	10.5	42.6	88.7	1.00	88.8
FEED	1964.4	200.0	0.49	100.0	12.9	100.0	0.13	100.0	7.04	100.0	15.3	100.0	0.36	100.0

Milling		Primary	Regrind
Mill type	Long	Stirred	
Media type	MS ball	Ceramic	
Media	12	2	
Solids	kg	2000	842
Water	g	1000	450
Time	min/sec	11/5/4	5
Speed	rpm	50	1200
Lime	g	0	0
End pH	pH	6.75	5.9
End p80	µm	250	25



PROJECT	T0879
TEST NO	T08
DATE	030614
TECHNICIAN	MJR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 250µm
20kWh/t
CuSO4 in Regrind

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	38959
Cleaner	2.7	Finish	38973
0		W/h	14.32
Speed	900	kWh/t	20.0

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		1091						2					
Condition		51		25	40	23			1	3-7	3.0	3.0	550	
Sulphide Ro C1	5.4	51		25	30	8			2					
Condition				51	25	8			1	3-8	3.0	6.0	300	
Sulphide Ro C2	5.2	51							2					
Condition									1	4-8	3.0	9.0	200	
Sulphide Ro C3	5.0	51			15	8			2					
Condition									1	4-9	3.0	12.0	300	
Sulphide Ro C4	5.2	25			15	10			2					
Condition									1	4-9	4.0	16.0	300	
Sulphide Ro C5	5.2				15	15			2					
Condition									1	4-9	4.0	20.0	300	
Sulphide Ro C6	5.2													
Regrind				76										
Condition	5.0	101	164						2					
Condition					69	25			1					
Sulphide Cl1	5.2								2	3-9	20.0	20.0	2000	
Condition			10			3				2-9	3.0	3.0	400	49
Sulphide Cl2C1	4.8					5				2-9	3.0	6.0	400	29
Condition						5				2-9	4.0	10.0	500	15
Sulphide Cl2C2										2-9	6.0	16.0	500	10
Condition														
Sulphide Cl2C3														
Condition														
Sulphide Cl2C4														
REAGENT TOTALS (g/t)		329	1265	177	226	113								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T08 Cl2Con1	194.7	9.9	0.10	1.0	41.6	15.8	0.27	9.9	46.6	31.0	1.03	0.3
Cl2Con2	115.2	5.8	0.11	0.6	44.9	10.1	0.33	7.1	42.6	16.8	2.24	0.4
Cl2Con3	73.4	3.7	0.11	0.4	44.0	6.3	0.54	7.4	45.2	11.3	2.47	0.3
Cl2Con4	51.9	2.6	0.10	0.3	41.5	4.2	0.64	6.2	46.3	8.2	3.58	0.3
Cl2 Tail	65.5	3.3	0.45	1.5	33.5	4.3	0.82	10.1	28.4	6.4	15.3	1.7
Cl1 Tail	238.8	12.1	0.83	10.0	30.2	14.1	1.01	45.3	21.6	17.6	20.6	8.3
Ro Tail	1236.4	62.6	1.38	86.2	18.7	45.1	0.06	13.9	2.06	8.7	42.5	88.6
CALC	1975.9	100.0	1.00	100.0	25.9	100.0	0.27	100.0	14.8	100.0	30.0	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T08 Cl2Con1	194.7	9.9	0.10	1.0	41.6	15.8	0.27	9.9	46.6	31.0	1.03	0.3
Cl2Con2	309.9	15.7	0.10	1.6	42.8	26.0	0.29	17.0	45.1	47.8	1.48	0.8
Cl2Con3	383.3	19.4	0.10	2.0	43.1	32.3	0.34	24.5	45.1	59.1	1.67	1.1
Cl2Con4	435.2	22.0	0.10	2.3	42.9	36.5	0.38	30.7	45.3	67.3	1.90	1.4
Cl2 Tail	500.7	25.3	0.15	3.8	41.6	40.8	0.43	40.8	43.1	73.7	3.64	3.1
Cl1 Tail	739.5	37.4	0.37	13.8	37.9	54.9	0.62	86.1	36.1	91.3	9.12	11.4
FEED	1975.9	100.0	1.00	100.0	25.9	100.0	0.27	100.0	14.8	100.0	30.0	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T08 Cl2Con1	194.7	9.9	0.03	0.4	0.16	0.6	0.34	0.5	0.02	0.5
Cl2Con2	115.2	5.8	0.07	0.6	0.30	0.6	0.82	0.8	0.04	0.5
Cl2Con3	73.4	3.7	0.09	0.5	0.32	0.4	0.82	0.5	0.05	0.4
Cl2Con4	51.9	2.6	0.11	0.4	0.37	0.4	1.03	0.4	0.04	0.2
Cl2 Tail	65.5	3.3	0.33	1.6	1.58	1.9	4.45	2.3	0.22	1.7
Cl1 Tail	238.8	12.1	0.48	8.5	1.81	8.0	4.74	9.0	0.31	8.6
Ro Tail	1236.4	62.6	0.96	88.0	3.87	88.1	8.78	86.5	0.61	88.0
CALC	1975.9	100.0	0.68	100.0	2.75	100.0	6.35	100.0	0.43	100.0
ASSAY HEAD										

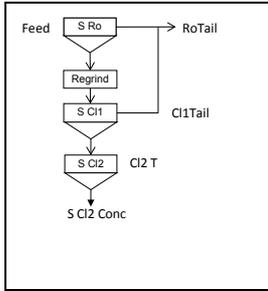
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T08 Cl2Con1	194.7	9.9	0.03	0.4	0.16	0.6	0.34	0.5	0.02	0.5
Cl2Con2	309.9	15.7	0.04	1.0	0.21	1.2	0.52	1.3	0.03	1.0
Cl2Con3	383.3	19.4	0.05	1.5	0.23	1.6	0.58	1.8	0.03	1.4
Cl2Con4	435.2	22.0	0.06	1.9	0.25	2.0	0.63	2.2	0.03	1.7
Cl2 Tail	500.7	25.3	0.10	3.5	0.42	3.9	1.13	4.5	0.06	3.3
Cl1 Tail	739.5	37.4	0.22	12.0	0.87	11.9	2.30	13.5	0.14	12.0
FEED	1975.9	100.0	0.68	100.0	2.75	100.0	6.35	100.0	0.43	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail+Cl1Tail Comb	1475.2	74.7	1.29	96.2	20.5	59.2	0.21	59.2	5.22	26.3	39.0	96.9
FEED	100.0		1.00	100.0	25.9	100.0	0.27	100.0	14.8	100.0	30.0	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail+Cl1Tail Comb	1475.2	74.7	0.88	96.5	3.54	96.1	8.13	95.5	0.56	96.7
FEED	200.0		0.68	100.0	2.75	100.0	6.35	100.0	0.43	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT	1236.4	62.6	1.38	86.2	18.7	45.1	0.06	13.9	2.06	8.7	42.5	88.6	0.96	88.0
FEED	1975.9	200.0	0.50	100.0	12.9	100.0	0.13	100.0	7.41	100.0	15.0	100.0	0.34	100.0

Milling		Primary	Regrind
Mill type	Long MS ball	Short MS ball	
Media type	12	6.0 Reg	
Media kg	2000	866	
Water g	1000	400	
Time min/sec	11/5/4	9	
Speed rpm	50	50	
Lime g	0	0	
End pH	6.75	6.75	
End p80 µm	250	67	



PROJECT	T0879
TEST NO	T09
DATE	040614
TECHNICIAN	MJR

PRODUCT FLOATED	Severn Ore Comp
	SBC

NOTES	Sulphide Rougher
	Feed P80 250um
	Ballmill Regrind

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	
Cleaner	2.7	Finish	
0		W/h	
Speed	900	kWh/t	

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		932						2					
Condition		50		25	40	22			1		3-7	3.0	550	
Sulphide Ro C1	5.4			25					2					
Condition		50			30	7			1		3-8	3.0	300	
Sulphide Ro C2	5.3			50					2					
Condition		50			25	7			1		4-8	3.0	200	
Sulphide Ro C3	5.2				15	7			2					
Condition		50							1					
Sulphide Ro C4	5.3					7			2					
Condition		25							1		4-9	3.0	300	
Sulphide Ro C5	5.3				15	10			2					
Condition									1					
Sulphide Ro C6	5.3				15	15			2					
Condition									1		4-9	4.0	300	
Regrind														
Condition	5.0		397	25	40	25			2					
Condition		100							1					
Sulphide Cl1	5.4								2		3-9	10.0	1400	
Condition			20			2								
Sulphide Cl2C1	5.2					5			2		2-9	1.5	400	61
Condition									1					
Sulphide Cl2C2						5			2		2-9	2.0	400	54
Condition									1					
Sulphide Cl2C3						5			2		2-9	3.0	300	38
Condition									1					
Sulphide Cl2C4									2		2-9	3.0	200	9
REAGENT TOTALS (g/t)		325	1348	125	180	111								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T09 Cl2Con1	244.1	12.2	0.15	1.8	42.3	19.8	0.59	25.9	46.4	38.2	1.59	0.6
Cl2Con2	217.1	10.9	0.19	2.1	42.6	17.7	0.66	25.8	45.7	33.5	1.85	0.7
Cl2Con3	115.0	5.8	0.36	2.1	41.8	9.2	0.93	19.2	36.8	14.3	5.60	1.1
Cl2Con4	17.1	0.9	0.75	0.6	32.8	1.1	1.10	3.4	24.7	1.4	18.5	0.5
Cl2 Tail	25.1	1.3	0.78	1.0	29.3	1.4	0.53	2.4	14.2	1.2	24.9	1.0
Cl1 Tail	152.1	7.6	1.33	10.1	24.4	7.1	0.37	10.1	7.22	3.7	32.7	8.3
Ro Tail	1228.2	61.4	1.35	82.4	18.6	43.7	0.06	13.2	1.86	7.7	42.8	87.7
CALC	1998.7	100.00	1.01	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.0	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T09 Cl2Con1	244.1	12.2	0.15	1.8	42.3	19.8	0.59	25.9	46.4	38.2	1.59	0.6
Cl2Con2	461.2	23.1	0.17	3.9	42.4	37.5	0.62	51.6	46.1	71.7	1.71	1.3
Cl2Con3	576.2	28.8	0.21	5.9	42.3	46.7	0.68	70.9	44.2	86.0	2.49	2.4
Cl2Con4	593.3	29.7	0.22	6.6	42.0	47.8	0.70	74.2	43.7	87.4	2.95	2.9
Cl2 Tail	618.4	30.9	0.25	7.5	41.5	49.2	0.69	76.6	42.5	88.6	3.84	4.0
Cl1 Tail	770.5	38.6	0.46	17.6	38.1	56.3	0.63	86.8	35.5	92.3	9.54	12.3
FEED	1998.7	100.0	1.01	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.0	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T09 Cl2Con1	244.1	12.2	0.07	1.2	0.15	0.7	0.31	0.6	0.05	1.4
Cl2Con2	217.1	10.9	0.07	1.1	0.17	0.7	0.38	0.7	0.04	1.0
Cl2Con3	115.0	5.8	0.17	1.4	0.47	1.0	1.08	1.0	0.12	1.6
Cl2Con4	17.1	0.9	0.43	0.5	1.18	0.4	3.10	0.4	0.30	0.6
Cl2 Tail	25.1	1.3	0.59	1.1	2.60	1.2	6.29	1.3	0.37	1.1
Cl1 Tail	152.1	7.6	0.72	8.0	2.84	7.9	6.75	8.3	0.50	8.7
Ro Tail	1228.2	61.4	0.97	86.7	3.95	88.3	8.87	87.8	0.61	85.7
CALC	1998.7	100.00	0.69	100.0	2.75	100.0	6.21	100.0	0.44	100.0
ASSAY HEAD										

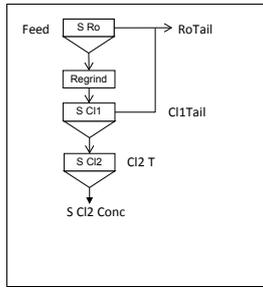
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T09 Cl2Con1	244.1	12.2	0.07	1.2	0.15	0.7	0.31	0.6	0.05	1.4
Cl2Con2	461.2	23.1	0.07	2.3	0.16	1.3	0.34	1.3	0.05	2.4
Cl2Con3	576.2	28.8	0.09	3.8	0.22	2.3	0.49	2.3	0.06	4.0
Cl2Con4	593.3	29.7	0.10	4.3	0.25	2.7	0.57	2.7	0.07	4.6
Cl2 Tail	618.4	30.9	0.12	5.4	0.34	3.9	0.80	4.0	0.08	5.6
Cl1 Tail	770.5	38.6	0.24	13.3	0.84	11.7	1.97	12.2	0.16	14.3
FEED	1998.7	100.0	0.69	100.0	2.75	100.0	6.21	100.0	0.44	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail+Cl1Tail Comb	1380.3	69.1	1.35	92.5	19.2	50.8	0.09	23.4	2.45	11.4	41.7	96.0
FEED	100.0		1.01	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.0	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail+Cl1Tail Comb	1380.3	69.1	0.94	94.6	3.83	96.1	8.64	96.0	0.60	94.4
FEED	100.0		0.69	100.0	2.75	100.0	6.21	100.0	0.44	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	1422.5	71.2	1.33	94.1	19.5	53.3	0.11	29.1	2.92	14.0	41.1	97.6	0.93	96.2
FEED	1998.7	100.0	1.01	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.0	100.0	0.00	100.0

Milling		Primary	Regrind
Mill type	Long	Short	
Media type	MS ball	MS ball	
Media kg	12	6.0 Reg	
Solids g	2000	843	
Water g	1000	400	
Time min/sec	11/5/4	12	
Speed rpm	50	50	
Lime g	0	0	
End pH	6.75	6.84	
End p80	250	54	



PROJECT	T0879
TEST NO	T10
DATE	050614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
Sulphide Rougher	
Feed P80 250um	
Ballmill Regrind	

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	0.0
Cleaner	2.7	Finish	0.0
Speed	0	W/h	0.00
	900	kWh/t	-

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		950						2					
Condition		50		25					2					
Condition	5.4			25	40	22			1	3-7	3.0	3.0	550	
Condition		50		25	30	7			2					
Condition	5.3			50	25	7			1	3-8	3.0	6.0	300	
Condition		50							2					
Condition	5.2				15	7			1	4-8	3.0	9.0	200	
Condition		50							2					
Condition	5.2				15	7			1	4-9	3.0	12.0	300	
Condition		25							2					
Condition	5.3				15	10			1	4-9	4.0	16.0	300	
Condition									2					
Condition	5.3				15	15			2	4-9	4.0	20.0	300	
Regrind														
Condition	5.0	100	686	25					2					
Condition					30	25			1					
Condition	5.6								2	3-9	15.0	15.0	1700	
Condition			24			2								
Condition	5.0					5				2-9	1.5	1.5	400	60
Condition														
Condition						5				2-9	3.0	4.5	400	51
Condition														
Condition						5				2-9	3.0	7.5	200	26
Condition														
Condition										2-9	3.0	10.5	200	9
REAGENT TOTALS (g/t)		325	1661	125	170	111								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T10 Cl2Con1	241.1	12.1	0.15	1.9	40.9	18.7	0.49	21.7	42.4	35.5	1.36	0.5
Cl2Con2	205.3	10.3	0.17	1.8	42.8	16.6	0.58	21.9	44.0	31.4	2.12	0.7
Cl2Con3	52.4	2.6	0.26	0.7	44.6	4.4	0.75	7.2	37.4	6.8	5.11	0.4
Cl2Con4	18.2	0.9	0.35	0.3	42.0	1.4	0.79	2.6	30.9	2.0	7.40	0.2
Cl2 Tail	53.9	2.7	0.50	1.4	37.0	3.8	1.06	10.5	29.6	5.5	13.1	1.2
Cl1 Tail	186.4	9.3	1.16	11.2	31.0	10.9	0.65	22.3	14.3	9.2	25.0	7.8
Ro Tail	1243.4	62.1	1.29	82.8	18.8	44.1	0.06	13.7	2.20	9.5	42.9	89.1
CALC	2000.7	100.0	0.97	100.0	26.4	100.0	0.27	100.0	14.4	100.0	29.9	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T10 Cl2Con1	241.1	12.1	0.15	1.9	40.9	18.7	0.49	21.7	42.4	35.5	1.36	0.5
Cl2Con2	446.4	22.3	0.16	3.7	41.8	35.3	0.53	43.6	43.1	66.9	1.71	1.3
Cl2Con3	498.8	24.9	0.17	4.4	42.1	39.7	0.55	50.8	42.5	73.8	2.07	1.7
Cl2Con4	517.0	25.8	0.18	4.7	42.1	41.2	0.56	53.5	42.1	75.7	2.25	1.9
Cl2 Tail	570.9	28.5	0.21	6.1	41.6	44.9	0.61	64.0	40.9	81.3	3.27	3.1
Cl1 Tail	757.3	37.9	0.44	17.2	39.0	55.9	0.62	86.3	34.4	90.5	8.62	10.9
FEED	2000.7	100.0	0.97	100.0	26.4	100.0	0.27	100.0	14.4	100.0	29.9	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T10 Cl2Con1	241.1	12.1	0.09	1.6	0.13	0.6	0.28	0.6	0.04	1.1
Cl2Con2	205.3	10.3	0.09	1.3	0.23	0.9	0.43	0.7	0.06	1.4
Cl2Con3	52.4	2.6	0.16	0.6	0.42	0.4	0.88	0.4	0.11	0.7
Cl2Con4	18.2	0.9	0.24	0.3	0.59	0.2	1.30	0.2	0.14	0.3
Cl2 Tail	53.9	2.7	0.28	1.1	1.42	1.4	3.34	1.5	0.20	1.2
Cl1 Tail	186.4	9.3	0.56	7.6	2.06	7.1	4.94	7.5	0.41	8.7
Ro Tail	1243.4	62.1	0.97	87.5	3.90	89.5	8.79	89.2	0.61	86.6
CALC	2000.7	100.0	0.69	100.0	2.71	100.0	6.13	100.0	0.44	100.0
ASSAY HEAD										

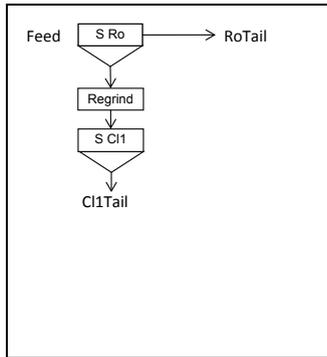
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T10 Cl2Con1	241.1	12.1	0.09	1.6	0.13	0.6	0.28	0.6	0.04	1.1
Cl2Con2	446.4	22.3	0.09	2.9	0.18	1.4	0.35	1.3	0.05	2.5
Cl2Con3	498.8	24.9	0.10	3.5	0.20	1.9	0.40	1.6	0.06	3.2
Cl2Con4	517.0	25.8	0.10	3.8	0.22	2.1	0.44	1.8	0.06	3.5
Cl2 Tail	570.9	28.5	0.12	4.9	0.33	3.5	0.71	3.3	0.07	4.7
Cl1 Tail	757.3	37.9	0.23	12.5	0.76	10.5	1.75	10.8	0.16	13.4
FEED	2000.7	100.0	0.69	100.0	2.71	100.0	6.13	100.0	0.44	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail+Cl1Tail Comb	1429.8	71.5	1.27	93.9	20.3	55.1	0.14	36.0	3.77	18.7	40.6	96.9
FEED	2000.7	100.0	0.97	100.0	26.4	100.0	0.27	100.0	14.4	100.0	29.9	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail+Cl1Tail Comb	1429.8	71.5	0.92	95.1	3.66	96.5	8.29	96.7	0.58	95.3
FEED	2000.7	100.0	0.69	100.0	2.71	100.0	6.13	100.0	0.44	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT	1243.4	62.1	1.29	82.8	18.8	44.1	0.06	13.7	2.20	9.5	42.9	89.1	0.97	87.5
FEED	2000.7	100.0	0.97	100.0	26.4	100.0	0.27	100.0	14.4	100.0	29.9	100.0	0.69	100.0

Milling		Primary	Regrind
Mill type		Long MS ball	Short MS ball
Media type		12 kg	6.0 Reg
Solids		2000 g	760 g
Water		1000 g	400 g
Time	min/sec	11/5/4	20
Speed	rpm	50	50
Lime	g	0	0
End pH	pH	6	6.3
End p80	µm	250	41



PROJECT	T0879
TEST NO	T11
DATE	100614
TECHNICIAN	BR

PRODUCT FLOATED
Severn Ore Comp
SBC

NOTES
Sulphide Rougher
Feed P80 250um
Ballmill Regrind

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	0.0
Cleaner	2.7	Finish	0.0
0		W/h	0.00
Speed	900	kWh/t	-

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		956						2					
Condition		50		25	40				2					
Condition						35			1	3-7	3.0	3.0	550	
Sulphide Ro C1	5.5			25	30				2					
Condition		50				7			1	3-8	3.0	6.0	360	
Sulphide Ro C2	5.3			50	25				2					
Condition		50				7			1	3-8	3.0	9.0	200	
Sulphide Ro C3	5.2				15				2					
Condition		50				7			1	4-8	3.0	12.0	300	
Sulphide Ro C4	5.2				15				2					
Condition		25				10			1	4-9	3.0	15.0	300	
Sulphide Ro C5	5.3				15				2					
Condition						15			1	4-9	4.0	16.0	300	
Sulphide Ro C6	5.3								2					
Condition									1	4-9	4.0	20.0	300	
Regrind														
Condition	5.0		986						2					
Condition		101		25	40				1					
Condition						25			2					
Sulphide Cl1	5.4									3-9	15.0	15.0	1700	21
REAGENT TOTALS (g/t)		327	1942	126	181	107								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST
T11 Cl1Con	358.0	18.0	0.16	2.8	40.3	28.0	0.52	35.2	43.0	54.6	3.31	2.0
Cl1 Tail	322.5	16.2	0.57	9.1	36.5	22.9	0.78	47.5	29.5	33.7	14.1	7.6
Ro Tail	1307.8	65.8	1.36	88.1	19.4	49.1	0.07	17.3	2.52	11.7	41.4	90.5
CALC	1988.3	100.0	1.02	100.0	25.9	100.0	0.27	100.0	14.2	100.0	30.1	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
T11 Cl1Con	358.0	18.0	0.16	2.8	40.3	28.0	0.52	35.2	43.0	54.6	3.31	2.0
Cl1 Tail	680.5	34.2	0.35	11.9	38.5	50.9	0.64	82.7	36.6	88.3	8.40	9.5
FEED	1988.3	100.0	1.02	100.0	25.9	100.0	0.27	100.0	14.2	100.0	30.1	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T11 Cl1Con	358.0	18.0	0.13	3.2	0.39	2.5	0.88	2.5	0.06	2.4
Cl1 Tail	322.5	16.2	0.35	7.7	1.32	7.6	3.12	7.9	0.21	7.6
Ro Tail	1307.8	65.8	1.00	89.1	3.84	89.9	8.72	89.6	0.61	89.9
CALC	1988.3	100.0	0.74	100.0	2.81	100.0	6.40	100.0	0.45	100.0
ASSAY HEAD										

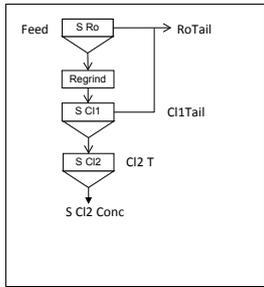
CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
T11 Cl1Con	358.0	18.0	0.13	3.2	0.39	2.5	0.88	2.5	0.06	2.4
Cl1 Tail	680.5	34.2	0.23	10.9	0.83	10.1	1.94	10.4	0.13	10.1
FEED	1988.3	100.0	0.74	100.0	2.81	100.0	6.40	100.0	0.45	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST
RoTail+Cl1Tail Comb	1630.3	82.0	1.20	97.2	22.7	72.0	0.21	64.8	7.86	45.4	36.0	98.0
FEED		100.0	1.02	100.0	25.9	100.0	0.27	100.0	14.2	100.0	30.1	100.0

CUM PRODUCTS	CUM Wt	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST
RoTail+Cl1Tail Comb	1630.3	82.0	0.87	96.8	3.34	97.5	7.61	97.5	0.53	97.6
FEED		100.0	0.74	100.0	2.81	100.0	6.40	100.0	0.45	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT	1307.8	65.8	1.36	88.1	19.4	49.1	0.07	17.3	2.52	11.7	41.4	90.5	1.00	89.1
FEED	4345.0	100.0	1.02	100.0	25.9	100.0	0.27	100.0	14.2	100.0	30.1	100.0	0.00	100.0

Milling		Primary	Regrind
Mill type	Long	Stirred	
Media type	MS ball	Ceramic	
Media kg	12		2
Solids g	2000		893
Water g	1000		450
Time min/sec	11/5/4		2
Speed rpm	50		1200
Lime g	0		0
End pH	6.4		6.15
End p80 μ m	250		37



PROJECT	T0879
TEST NO	T12
DATE	160614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
Sulphide Rougher	
Feed P80 250um	
10kWh/t	
CuSO4 in Regrind	
No Acid in Cleaners	

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	39015
Cleaner	2.7	Finish	39023
	0	W/h	7.59
Speed	900	kWh/t	10.0

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		872						2					
Condition		50		25					2					
Condition					30	22			1	3-7	3.0	3.0	550	
Sulphide Ro C1	5.4	50		25	30	7			2					
Condition									1					
Sulphide Ro C2	5.2	50		50					2	3-8	3.0	6.0	300	
Condition									1					
Sulphide Ro C3	5.3	50			25	7			2					
Condition									1					
Sulphide Ro C4	5.3	50			25	7			2	4-8	3.0	9.0	200	
Condition									1					
Sulphide Ro C5	5.3	25			15	10			2	4-9	3.0	12.0	300	
Condition									1					
Sulphide Ro C6	5.4				15	15			2	4-9	4.0	16.0	300	
Condition									1					
Regrind	6.2	101		101					1					
Condition					50	25			1					
Sulphide C1	6.2				10	7			1	3-9	4.0	4.0	800	
Condition									2					
Sulphide C1 scav1					10	7			1	3-9	4.0	8.0	400	
Condition									2					
Sulphide C1 Scav2									1	3-9	9.0	17.0	600	
Condition						2			1					
Sulphide C2C1	5.7					2			1	2-9	1.5	1.5	400	60
Condition									1					
Sulphide C2C2						5			1	2-9	2.5	4.0	400	54
Condition									1					
Sulphide C2C3					5	5			1	2-9	4.0	8.0	350	30
Condition									1					
Sulphide C2C4					10				1	2-9	5.0	13.0	350	6
REAGENT TOTALS (g/t)		327	872	201	226	124								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST	Sn Acid Sol ppm	DIST
T12 C12Con1	240.5	12.1	0.12	1.4	42.1	19.5	0.54	23.1	46.8	38.3	1.13	0.5	0.05	0.8	360	26.2
C12Con2	215.1	10.8	0.12	1.3	43.4	18.0	0.57	21.8	45.7	33.4	1.35	0.5	0.06	0.9	370	24.1
C12Con3	105.4	5.3	0.21	1.1	43.8	8.9	0.87	16.3	41.4	14.8	3.59	0.6	0.11	0.8	240	7.6
C12Con4	21.0	1.1	0.57	0.6	36.3	1.5	2.19	8.2	29.2	2.1	12.4	0.4	0.28	0.4	150	1.0
C12 Tail	33.5	1.7	0.96	1.6	27.3	1.8	0.63	3.8	11.6	1.3	27.2	1.5	0.64	1.5	120	1.2
C1 Tail	175.1	8.8	1.55	13.4	22.5	7.6	0.38	11.8	5.14	3.1	35.7	10.4	0.83	10.1	70	3.7
Ro Tail	1199.4	60.3	1.36	80.6	18.6	42.9	0.07	14.9	1.71	7.0	43.1	86.1	1.03	85.5	100	36.3
CALC	1990.0	100.0	1.02	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.2	100.0	0.73	100.0	166	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00					

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST	Sn Acid Sol ppm	DIST
T12 C12Con1	240.5	12.1	0.12	1.4	42.1	19.5	0.54	23.1	46.8	38.3	1.13	0.5	0.05	0.8	360	26.2
C12Con2	455.6	22.9	0.12	2.7	42.7	37.4	0.55	44.9	46.3	71.7	1.23	0.9	0.05	1.7	365	50.2
C12Con3	561.0	28.2	0.14	3.8	42.9	46.3	0.61	61.3	45.4	86.6	1.68	1.6	0.07	2.5	341	57.9
C12Con4	582.0	29.2	0.15	4.4	42.7	47.8	0.67	69.5	44.8	88.6	2.06	2.0	0.07	2.9	334	58.8
C12 Tail	615.5	30.9	0.20	6.0	41.8	49.5	0.67	73.2	43.0	90.0	3.43	3.5	0.10	4.4	323	60.0
C1 Tail	790.6	39.7	0.50	19.4	37.6	57.1	0.60	85.1	34.6	93.0	10.6	13.9	0.26	14.5	267	63.7
FEED	1990.0	100.0	1.02	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.2	100.0	0.73	100.0	166	100.0

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T12 C12Con1	240.5	12.1	0.17	0.7	0.29	0.6	0.02	0.6	0.26	35.9	2.36	45.9	2.78	43.6
C12Con2	215.1	10.8	0.20	0.8	0.35	0.6	0.03	0.8	0.24	29.6	1.98	34.4	2.61	36.6
C12Con3	105.4	5.3	0.37	0.7	0.73	0.6	0.06	0.7	0.14	8.5	0.71	6.0	2.11	14.5
C12Con4	21.0	1.1	1.12	0.4	2.39	0.4	0.18	0.4	0.10	1.2	0.40	0.7	0.87	1.2
C12 Tail	33.5	1.7	2.58	1.6	7.23	1.9	0.40	1.6	0.06	1.2	0.33	0.9	0.18	0.4
C1 Tail	175.1	8.8	2.79	8.9	6.86	9.6	0.53	10.8	0.03	3.0	0.17	2.4	0.11	1.3
Ro Tail	1199.4	60.3	4.00	86.9	9.03	86.3	0.61	85.2	0.03	20.6	0.10	9.7	0.03	2.3
CALC	1990.0	100.0	2.77	100.0	6.30	100.0	0.43	100.0	0.09	100.0	0.62	100.0	0.77	100.0
ASSAY HEAD														

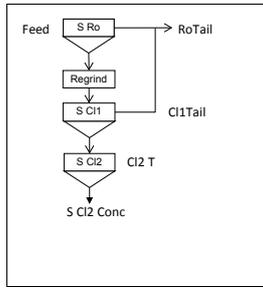
CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T12 C12Con1	240.5	12.1	0.17	0.7	0.29	0.6	0.02	0.6	0.26	35.9	2.36	45.9	2.78	43.6
C12Con2	455.6	22.9	0.18	1.5	0.32	1.2	0.02	1.3	0.25	65.5	2.18	80.3	2.70	80.3
C12Con3	561.0	28.2	0.22	2.2	0.40	1.8	0.03	2.0	0.23	74.0	1.90	86.3	2.59	94.8
C12Con4	582.0	29.2	0.25	2.7	0.47	2.2	0.04	2.5	0.23	75.2	1.85	87.0	2.53	96.0
C12 Tail	615.5	30.9	0.38	4.2	0.84	4.1	0.06	4.0	0.22	76.3	1.77	87.9	2.40	96.4
C1 Tail	790.6	39.7	0.91	13.1	2.17	13.7	0.16	14.8	0.17	79.4	1.41	90.3	1.89	97.7
FEED	1990.0	100.0	2.77	100.0	6.30	100.0	0.43	100.0	0.09	100.0	0.62	100.0	0.77	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+C11Tail Comb	1374.5	69.1	1.38	94.0	19.1	50.5	0.11	26.8	2.15	10.0	42.2	96.5	1.00	95.6
FEED	1990.0	100.0	1.02	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.2	100.0	0.73	100.0

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST	Sn Acid Sol ppm	DIST
RoTail+C11Tail Comb	1374.5	69.1	3.85	95.8	8.75	95.9	0.60	96.0	0.03	23.7	0.11	12.1	0.04	3.6	96	40.0
FEED	1990.0	100.0	2.77	100.0	6.30	100.0	0.43	100.0	0.09	100.0	0.62	100.0	0.77	100.0	166	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	1429.0	71.8	1.36	96.2	19.5	53.7	0.15	38.7	2.76	13.4	41.4	98.4	0.99	97.5
FEED	1990.0	100.0	1.02	100.0	26.1	100.0	0.28	100.0	14.8	100.0	30.2	100.0	0.73	100.0

Milling		Primary	Regrind
Mill type	Long	Stirred	
Media type	MS ball	Ceramic	
Media kg	12	2	
Solids g	2000	873	
Water g	1000	450	
Time min/sec	11/5/4	4	
Speed rpm	50	1200	
Lime g	0	0	
End pH	pH 6.45	6.1	
End p80	µm 250	25	



PROJECT	T0879
TEST NO	T13
DATE	160614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
Sulphide Rougher	
Feed P80 250um	
20kWh/t	
CuSO4 in Regrind	
No Acid in Cleaners	

Float Cell	Volume	Regrind	Power
Rougher	3.8	Start	39203
Cleaner	2.7	Finish	39218
Speed	0	W/h	14.84
	900	kWh/t	20.0

	pH	0.5 GUAR g/t	98 H2SO4 g/t	1 CuSO4 g/t	0.2 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		858						2					
Condition		50		25					2					
Sulphide Ro C1	5.5				30	22			1	3-7	3.0	3.0	550	
Condition		50		25					2					
Sulphide Ro C2	5.2				30	7			1	3-8	3.0	6.0	300	
Condition		50		50					2					
Sulphide Ro C3	5.3				25	7			1	4-8	3.0	9.0	200	
Condition		50							2					
Sulphide Ro C4	5.3				25	7			1	4-9	3.0	12.0	300	
Condition		25							2					
Sulphide Ro C5	5.4				15	10			1	4-9	4.0	16.0	300	
Condition									2					
Sulphide Ro C6	5.4				15	15			1	4-9	4.0	20.0	300	
Regrind				100										
Condition	6.2	100							1					
Sulphide C1	6.2				50	25			1	3-9	4.0	4.0	700	
Condition					10	7			1					
Sulphide C1 scav1					10	7			2	3-9	4.0	8.0	400	
Condition									1					
Sulphide C1 Scav2									2	3-9	9.0	17.0	600	
Condition	5.7					2			1	2-9	1.5	1.5	400	57
Sulphide C1C1						5			1	2-9	3.0	4.5	400	50
Condition									1					
Sulphide C1C2						5			1	2-9	5.0	9.5	350	34
Condition									1					
Sulphide C1C3						10			1	2-9	7.0	16.5	350	8
Condition									1					
Sulphide C1C4									1	2-9	7.0	16.5	350	8
REAGENT TOTALS (g/t)		325	858	200	225	126								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST	Sn Acid Sol ppm
T13 C12Con1	228.2	11.4	0.09	1.0	41.4	18.1	0.35	14.0	47.2	37.0	1.95	0.7	0.11	1.8	400
C12Con2	199.2	10.0	0.09	0.9	43.8	16.7	0.41	14.3	44.5	30.5	1.24	0.4	0.06	0.8	350
C12Con3	120.0	6.0	0.12	0.7	45.3	10.4	0.62	13.0	41.6	17.1	2.13	0.4	0.10	0.8	230
C12Con4	28.5	1.4	0.34	0.5	37.8	2.1	2.98	14.9	36.1	3.5	7.06	0.3	0.16	0.3	250
C12 Tail	29.4	1.5	0.95	1.4	27.2	1.5	1.30	6.7	11.1	1.1	26.9	1.3	0.61	1.3	120
C1 Tail	174.9	8.8	1.59	13.6	22.9	7.7	0.72	22.1	4.44	2.7	34.7	10.0	0.80	9.8	80
Ro Tail	1218.4	61.0	1.38	82.0	18.7	43.6	0.07	15.0	1.93	8.1	43.1	86.8	1.00	85.2	110
CALC	1998.6	100.0	1.03	100.0	26.2	100.0	0.29	100.0	14.6	100.0	30.3	100.0	0.72	100.0	174
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00				

CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST	Sn Acid Sol ppm
T13 C12Con1	228.2	11.4	0.09	1.0	41.4	18.1	0.35	14.0	47.2	37.0	1.95	0.7	0.11	1.8	400
C12Con2	427.4	21.4	0.09	1.9	42.5	34.8	0.38	28.3	45.9	67.5	1.62	1.1	0.09	2.6	377
C12Con3	547.4	27.4	0.10	2.6	43.1	45.2	0.43	41.4	45.0	84.6	1.73	1.6	0.09	3.4	345
C12Con4	575.9	28.8	0.11	3.1	42.9	47.2	0.56	56.3	44.5	88.1	1.99	1.9	0.09	3.7	340
C12 Tail	605.3	30.3	0.15	4.4	42.1	48.8	0.59	63.0	42.9	89.3	3.20	3.2	0.12	5.0	329
C1 Tail	780.2	39.0	0.47	18.0	37.8	56.4	0.62	85.0	34.3	91.9	10.3	13.2	0.27	14.8	273
FEED	1998.6	100.0	1.03	100.0	26.2	100.0	0.29	100.0	14.6	100.0	30.3	100.0	0.72	100.0	174

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T13 C12Con1	228.2	11.4	0.12	0.5	0.33	0.6	0.03	0.8	0.34	44.3	2.43	42.7	2.59	36.4
C12Con2	199.2	10.0	0.18	0.7	0.34	0.5	0.02	0.5	0.20	22.8	2.37	36.4	2.41	29.6
C12Con3	120.0	6.0	0.24	0.5	0.57	0.5	0.04	0.6	0.11	7.5	0.72	6.7	2.77	20.5
C12Con4	28.5	1.4	0.72	0.4	1.58	0.4	0.11	0.4	0.10	1.6	0.32	0.7	4.17	7.3
C12 Tail	29.4	1.5	2.59	1.4	7.56	1.8	0.40	1.4	0.05	0.8	0.39	0.9	0.30	0.5
C1 Tail	174.9	8.8	2.70	8.7	7.25	10.0	0.54	11.0	0.02	2.0	0.17	2.3	0.25	2.7
Ro Tail	1218.4	61.0	3.92	87.8	8.98	86.2	0.60	85.4	0.03	20.9	0.11	10.3	0.04	3.0
CALC	1998.6	100.0	2.72	100.0	6.35	100.0	0.43	100.0	0.09	100.0	0.65	100.0	0.81	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM WT	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T13 C12Con1	228.2	11.4	0.12	0.5	0.33	0.6	0.03	0.8	0.34	44.3	2.43	42.7	2.59	36.4
C12Con2	427.4	21.4	0.15	1.2	0.33	1.1	0.03	1.3	0.27	67.1	2.40	79.1	2.51	66.0
C12Con3	547.4	27.4	0.17	1.7	0.39	1.7	0.03	1.8	0.24	74.6	2.03	85.8	2.56	86.4
C12Con4	575.9	28.8	0.20	2.1	0.45	2.0	0.03	2.2	0.23	76.3	1.95	86.5	2.64	93.8
C12 Tail	605.3	30.3	0.31	3.5	0.79	3.8	0.05	3.6	0.22	77.1	1.87	87.4	2.53	94.3
C1 Tail	780.2	39.0	0.85	12.2	2.24	13.8	0.16	14.6	0.18	79.1	1.49	89.7	2.02	97.0
FEED	1998.6	100.0	2.72	100.0	6.35	100.0	0.43	100.0	0.09	100.0	0.65	100.0	0.81	100.0

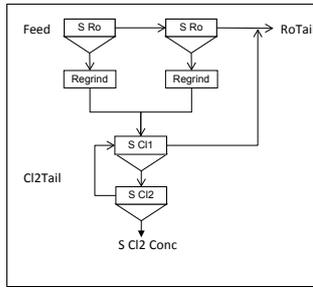
CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+C11Tail Comb	1393.3	69.7	1.41	95.6	19.2	51.2	0.15	37.0	2.25	10.7	42.0	96.8	0.97	95.0
FEED	100.0		1.03	100.0	26.2	100.0	0.29	100.0	14.6	100.0	30.3	100.0	0.72	100.0

CUM PRODUCTS	CUM WT	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST	Sn Acid Sol ppm
RoTail+C11Tail Comb	1393.3	69.7	3.77	96.5	8.76	96.2	0.59	96.4	0.03	22.9	0.12	12.6	0.07	5.7	106
FEED	100.0		2.72	100.0	6.35	100.0	0.43	100.0	0.09	100.0	0.65	100.0	0.81	100.0	

CUM PRODUCTS	CUM WT	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	1451.2	72.6	1.38	97.4	19.8	54.8	0.23	58.6	3.09	15.4	41.1	98.4	0.95	96.6
FEED	1998.6	100.0	1.03	100.0	26.2	100.0	0.29	100.0	14.6	100.0	30.3	100.0	0.72	100.0

Milling		Primary	Regrind
Mill type	Large	Stirred	
Media type	MS ball	Sand	
Media kg	40	3	
Solids kg	12	5251	
Water kg	6	3000	
Time min/sec	17.5	7	
Speed rpm	50	1000	
Lime g	0	0	
End pH	6.4	6	
End p80	250	82	

Float Cell	Volume	Regrind	Power
Rougher	30	Start	39985
Cleaner1	30	Finish	40052
Cleaner2	30	W/h	66.95
Speed	900	kWh/t	15.0



PROJECT	T0879
TEST NO	T14+T15
DATE	200614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
2*12kg Test	
Feed P80 250um	
15kWh/t	
CuSO4 in Regrind	
No Acid in Cleaners	

	pH	0.5 GUAR g/t	98 H2SO4 g/t	6 CuSO4 g/t	1.5 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		732						2					
Condition		25		25					2					
Condition					30				1		20-30	3.0	3.0	4400
Sulphide Ro C1	5.4			25		16								
Condition		12			30				2		20-30	3.0	6.0	5000
Condition				50		8			1					
Sulphide Ro C2		12			25				2		20-30	3.0	9.0	2200
Condition						4			1		20-50	3.0	12.0	2200
Sulphide Ro C3		12			25				2		20-50	3.0	15.0	2200
Condition						4			1		20-50	3.0	18.0	2200
Sulphide Ro C4		6			15				2		20-60	4.0	22.0	2600
Condition						6			1		20-60	4.0	28.0	2900
Sulphide Ro C5					15				2		20-60	4.0	32.0	2900
Condition	5.2					6								
Sulphide Ro C6				100										
Regrind									1					
Condition	5.4	25			50	6			1					
Condition					12	2			1		20-60	4.0	4.0	9000
Sulphide Cl1	5.4													
Condition					12	3			2		20-60	4.0	8.0	3000
Sulphide Cl1 scav1														
Condition									1		20-60	9.0	17.0	2600
Sulphide Cl1 Scav2														
Condition	5.6					2			1		20-30	1.5	1.5	4900
Sulphide Cl2C1						1			1		20-30	3.0	4.5	3800
Condition						2			1		20-30	3.0	6.5	3800
Sulphide Cl2C2					5						20-50	5.0	9.5	1300
Condition						2			1		20-50	5.0	11.5	1300
Sulphide Cl2C3					10						20-50	5.0	14.5	1200
Condition														
Sulphide Cl2C4														
REAGENT TOTALS (g/t)		93	732	199	229	64								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T14+15 Cl2Con1	3432.2	14.2	0.13	1.8	43.2	23.8	0.40	20.6	47.3	47.4	1.60	0.7	0.08	1.5
Cl2Con2	2628.6	10.9	0.20	2.2	42.6	17.9	0.56	22.1	42.1	32.3	2.38	0.8	0.10	1.4
Cl2Con3	813.2	3.4	0.54	1.8	38.7	5.0	1.89	23.1	31.6	7.5	9.26	1.0	0.22	1.0
Cl2Con4	231.1	1.0	1.00	0.9	32.9	1.2	2.25	7.8	23.5	1.6	19.0	0.6	0.39	0.5
Cl2 Tail	440.3	1.8	1.01	1.8	30.0	2.1	0.54	3.6	15.8	2.0	23.1	1.4	0.54	1.3
Cl1 Tail	1956.7	8.1	1.99	15.9	22.2	7.0	0.25	7.4	3.40	1.9	37.6	9.9	0.94	10.0
RoTail	14587.0	60.6	1.27	75.5	18.4	43.0	0.07	15.4	1.72	7.3	43.4	85.5	1.06	84.3
CALC	24089.0	100.0	1.01	100.0	25.9	100.0	0.28	100.0	14.2	100.0	30.7	100.0	0.76	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00			

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T14+15 Cl2Con1	3432.2	14.2	0.13	1.8	43.2	23.8	0.40	20.6	47.3	47.4	1.60	0.7	0.08	1.5
Cl2Con2	6060.8	25.2	0.16	4.0	42.9	41.7	0.47	42.8	45.0	79.7	1.94	1.6	0.09	2.9
Cl2Con3	6874.0	28.5	0.21	5.8	42.4	46.7	0.64	65.9	43.5	87.2	2.80	2.6	0.10	3.9
Cl2Con4	7105.1	29.5	0.23	6.7	42.1	48.0	0.69	73.7	42.8	88.7	3.33	3.2	0.11	4.4
Cl2 Tail	7545.4	31.3	0.28	8.5	41.4	50.1	0.68	77.3	41.2	90.8	4.48	4.6	0.14	5.7
Cl1 Tail	9502.1	39.4	0.63	24.5	37.5	57.0	0.59	84.6	33.4	92.7	11.3	14.5	0.30	15.7
FEED	24089.0	100.0	1.01	100.0	25.9	100.0	0.28	100.0	14.2	100.0	30.7	100.0	0.76	100.0

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	MnO %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T14+15 Cl2Con1	3432.2	14.2	0.13	0.7	0.36	0.8	0.02	0.7	0.21	33.2	1.70	38.1	1.04	20.0
Cl2Con2	2628.6	10.9	0.22	0.9	0.44	0.8	0.04	1.0	0.26	31.5	2.30	39.5	3.17	46.7
Cl2Con3	813.2	3.4	0.67	0.8	1.29	0.7	0.14	1.1	0.21	7.9	1.18	6.3	5.62	25.6
Cl2Con4	231.1	1.0	1.27	0.4	2.75	0.4	0.27	0.6	0.15	1.6	0.67	1.0	2.07	2.7
Cl2 Tail	440.3	1.8	2.07	1.4	5.30	1.6	0.36	1.5	0.10	2.0	0.76	2.2	1.00	2.5
Cl1 Tail	1956.7	8.1	2.60	7.8	6.27	8.2	0.61	11.6	0.04	3.6	0.27	3.4	0.24	2.6
RoTail	14587.0	60.6	3.96	88.0	9.03	87.6	0.59	83.5	0.03	20.2	0.10	9.5	0.00	0.0
CALC	24089.0	100.0	2.72	100.0	6.24	100.0	0.43	100.0	0.09	100.0	0.64	100.0	0.74	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	MnO %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T14+15 Cl2Con1	3432.2	14.2	0.13	0.7	0.36	0.8	0.02	0.7	0.21	33.2	1.70	38.1	1.04	20.0
Cl2Con2	6060.8	25.2	0.17	1.6	0.39	1.6	0.03	1.7	0.23	64.7	1.96	77.6	1.96	66.6
Cl2Con3	6874.0	28.5	0.23	2.4	0.50	2.3	0.04	2.8	0.23	72.6	1.87	83.8	2.40	92.2
Cl2Con4	7105.1	29.5	0.26	2.8	0.57	2.7	0.05	3.4	0.23	74.2	1.83	84.8	2.39	94.9
Cl2 Tail	7545.4	31.3	0.37	4.2	0.85	4.3	0.07	4.9	0.22	76.2	1.77	87.0	2.30	97.4
Cl1 Tail	9502.1	39.4	0.83	12.0	1.97	12.4	0.18	16.5	0.18	79.8	1.46	90.5	1.88	100.0
FEED	24089.0	100.0	2.72	100.0	6.24	100.0	0.43	100.0	0.09	100.0	0.64	100.0	0.74	100.0

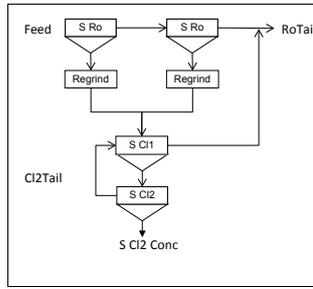
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+Cl1Tail Comb	16543.7	68.7	1.35	91.5	18.8	49.9	0.09	22.7	1.91	9.2	42.7	95.4	1.05	94.3
FEED		100.0	1.01	100.0	25.9	100.0	0.28	100.0	14.2	100.0	30.7	100.0	0.76	100.0

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	MnO %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
RoTail+Cl1Tail Comb	16543.7	68.7	3.79	95.8	8.70	95.7	0.59	95.1	0.03	23.8	0.12	13.0	0.03	2.6
FEED		100.0	2.72	100.0	6.24	100.0	0.43	100.0	0.09	100.0	0.64	100.0	0.74	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	17215.0	71.5	1.34	94.2	19.3	53.3	0.13	34.1	2.56	12.8	41.9	97.4	1.02	96.1
FEED		100.0	1.01	100.0	25.9	100.0	0.28	100.0	14.2	100.0	30.7	100.0	0.76	100.0

Milling		Primary	Regrind
Mill type	Large	Stirred	
Media type	MS ball	Sand	
Media kg	40	5	
Solids kg	12	2650	
Water kg	6	3000	
Time min/sec	17.5	9	
Speed rpm	50	1000	
Lime g	0	0	
End pH	6.4	6	
End p80	250	38	

Float Cell	Volume	Regrind	Power
Rougher	30	Start	40227
Cleaner1	30	Finish	40272
Cleaner2	30	W/h	45.06
Speed	900	kWh/t	20.0



PROJECT	T0879
TEST NO	T16+T17
DATE	250614
TECHNICIAN	MJR

PRODUCT FLOATED	Severn Ore Comp
SBC	

NOTES	2*12kg Test
Feed P80 250um	
CuSO4 in Regrind	
No Acid in Cleaners	

	pH	0.5 GUAR g/t	98 H2SO4 g/t	6 CuSO4 g/t	1.5 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		737						2					
Condition		25		25					2					
Condition					30	17			1	20-30	3.0	3.0	4400	
Sulphide Ro C1	5.4			25					2					
Condition		13			30	8			1	20-30	3.0	6.0	5000	
Sulphide Ro C2				50					2					
Condition		13			25	4			1	20-50	3.0	9.0	2200	
Sulphide Ro C3									2					
Condition		13			25	4			1	20-50	3.0	12.0	2200	
Sulphide Ro C4									2					
Condition		6			15	6			1	20-60	4.0	16.0	2600	
Sulphide Ro C5									2					
Condition	5.2				15	6			1	20-60	4.0	20.0	2900	
Sulphide Ro C6				100										
Regrind									1					
Condition	5.4	25			50	6			1					
Condition					13	2			1	20-60	5.0	5.0	9000	
Sulphide Cl1	5.4								2	20-60	5.0	10.0	3000	
Condition					13	3			1	20-60	12.0	22.0	2600	
Sulphide Cl1 scav1									1	20-30	1.5	1.5	4900	63
Condition	5.6					2			1	20-30	3.0	4.5	3800	58
Sulphide Cl2C1									1	20-50	5.0	9.5	1300	73
Condition					5	2			1	20-50	5.0	14.5	1200	26
Sulphide Cl2C2														
Condition					10									
Sulphide Cl2C3														
Condition														
Sulphide Cl2C4														
REAGENT TOTALS (g/t)		94	737	200	231	64								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T16+17 Cl2Con1	3092.7	12.9	0.08	1.0	42.2	21.2	0.36	17.3	44.7	43.3	1.00	0.4	0.04	0.7
Cl2Con2	2214.6	9.2	0.13	1.2	42.3	15.2	0.52	17.9	41.2	28.6	1.39	0.4	0.17	2.1
Cl2Con3	955.3	4.0	0.18	0.7	45.4	7.0	1.21	18.0	37.6	11.3	2.70	0.3	0.09	0.5
Cl2Con4	309.2	1.3	0.41	0.5	41.6	2.1	2.92	14.0	33.2	3.2	7.60	0.3	0.16	0.3
Cl2 Tail	459.6	1.9	1.01	2.0	31.4	2.3	1.04	7.4	16.6	2.4	20.9	1.3	0.45	1.2
Cl1 Tail	2285.4	9.5	1.62	15.6	23.0	8.5	0.36	12.8	5.29	3.8	36.1	11.2	0.74	9.6
Ro Tail	14629.0	61.1	1.28	78.9	18.3	43.6	0.06	12.5	1.62	7.4	43.5	86.0	1.03	85.5
CALC	23945.8	100.00	0.99	100.0	25.7	100.0	0.27	100.0	13.3	100.0	30.9	100.0	0.73	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00			

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T16+17 Cl2Con1	3092.7	12.9	0.08	1.0	42.2	21.2	0.36	17.3	44.7	43.3	1.00	0.4	0.04	0.7
Cl2Con2	5307.3	22.2	0.10	2.3	42.2	36.4	0.43	35.2	43.2	71.9	1.16	0.8	0.09	2.9
Cl2Con3	6262.6	26.2	0.11	3.0	42.7	43.5	0.55	53.2	42.4	83.2	1.40	1.2	0.09	3.3
Cl2Con4	6571.8	27.4	0.13	3.5	42.7	45.6	0.66	67.3	41.9	86.4	1.69	1.5	0.10	3.6
Cl2 Tail	7031.4	29.4	0.18	5.5	41.9	47.9	0.68	74.7	40.3	88.8	2.94	2.8	0.12	4.8
Cl1 Tail	9316.8	38.9	0.54	21.1	37.3	56.4	0.60	87.5	31.7	92.6	11.1	14.0	0.27	14.5
FEED	23945.8	100.0	0.99	100.0	25.7	100.0	0.27	100.0	13.3	100.0	30.9	100.0	0.73	100.0

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T16+17 Cl2Con1	3092.7	12.9	0.10	0.5	0.19	0.4	0.01	0.3	0.22	33.6	1.84	40.5	2.00	35.6
Cl2Con2	2214.6	9.2	0.14	0.5	0.28	0.4	0.02	0.4	0.29	31.7	2.33	36.7	3.48	44.3
Cl2Con3	955.3	4.0	0.31	0.5	0.51	0.3	0.04	0.4	0.16	7.6	0.78	5.3	2.38	13.1
Cl2Con4	309.2	1.3	0.73	0.3	1.26	0.3	0.10	0.3	0.13	2.0	0.52	1.1	0.95	1.7
Cl2 Tail	459.6	1.9	1.93	1.3	4.80	1.5	0.32	1.4	0.11	2.5	0.69	2.3	0.51	1.3
Cl1 Tail	2285.4	9.5	2.37	8.2	6.11	9.2	0.54	12.0	0.04	4.5	0.32	5.2	0.14	1.8
Ro Tail	14629.0	61.1	3.99	88.7	9.11	88.0	0.60	85.2	0.03	18.1	0.09	8.9	0.03	2.1
CALC	23945.8	100.00	2.75	100.0	6.33	100.0	0.43	100.0	0.08	100.0	0.59	100.0	0.73	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T16+17 Cl2Con1	3092.7	12.9	0.10	0.5	0.19	0.4	0.01	0.3	0.22	33.6	1.84	40.5	2.00	35.6
Cl2Con2	5307.3	22.2	0.12	0.9	0.23	0.8	0.01	0.7	0.25	65.4	2.04	77.2	2.62	79.9
Cl2Con3	6262.6	26.2	0.15	1.4	0.27	1.1	0.02	1.1	0.24	72.9	1.85	82.5	2.58	93.0
Cl2Con4	6571.8	27.4	0.17	1.7	0.32	1.4	0.02	1.4	0.23	74.9	1.79	83.7	2.50	94.7
Cl2 Tail	7031.4	29.4	0.29	3.1	0.61	2.8	0.04	2.8	0.22	77.4	1.72	85.9	2.37	96.1
Cl1 Tail	9316.8	38.9	0.80	11.3	1.96	12.0	0.16	14.8	0.18	81.9	1.37	91.1	1.83	97.9
FEED	23945.8	100.0	2.75	100.0	6.33	100.0	0.43	100.0	0.08	100.0	0.59	100.0	0.73	100.0

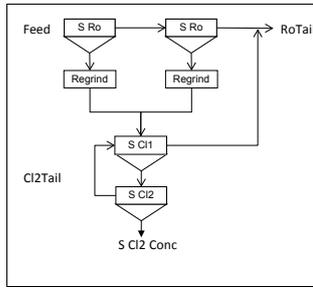
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+Cl1Tail Comb	16914.3	70.6	1.33	94.5	19.0	52.1	0.10	25.3	2.12	11.2	42.5	97.2	0.99	95.2
FEED		100.0	0.99	100.0	25.7	100.0	0.27	100.0	13.3	100.0	30.9	100.0	0.73	100.0

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
RoTail+Cl1Tail Comb	16914.3	70.6	3.77	96.9	8.70	97.2	0.59	97.2	0.03	22.6	0.12	14.1	0.04	3.9
FEED		100.0	2.75	100.0	6.33	100.0	0.43	100.0	0.08	100.0	0.59	100.0	0.73	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	17683.2	73.8	1.30	97.0	19.7	56.5	0.17	46.8	3.04	16.8	41.3	98.8	0.96	96.7
FEED		100.0	0.99	100.0	25.7	100.0	0.27	100.0	13.3	100.0	30.9	100.0	0.73	100.0

Milling		Primary	Regrind
Mill type	Large	Stirred	
Media type	MS ball	Sand	
Media kg	40	5	
Solids kg	12	2678	
Water kg	6	3000	
Time min/sec	17.5	7	
Speed rpm	50	1000	
Lime g	0	0	
End pH	6.4	6	
End p80	250	38	

Float Cell	Volume	Regrind	Power
Rougher	30	Start	40334
Cleaner1	30	Finish	40375
Cleaner2	30	W/h	40.97
Speed	900	kWh/t	18



PROJECT	T0879
TEST NO	T18+T19
DATE	270614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
2*12kg Test	
Feed P80 250um	
CuSO4 in Regrind	
No Acid in Cleaners	

	pH	0.5 GUAR g/t	98 H2SO4 g/t	6 CuSO4 g/t	1.5 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		734						2					
Condition		25		25					2					
Condition					30				1		20-30	3.0	3.0	2200
Sulphide Ro C1	5.4					16								
Condition		12		25					2					
Condition					30				1		20-30	3.0	6.0	2500
Sulphide Ro C2		12		50		8								
Condition					25				2					
Condition						4			1		20-50	3.0	9.0	1100
Sulphide Ro C3		12												
Condition					25				2					
Condition						4			1		20-50	3.0	12.0	1100
Sulphide Ro C4		6												
Condition					15				2					
Condition						6			1		20-60	4.0	16.0	1300
Sulphide Ro C5					15									
Condition	5.2					6			2		20-60	4.0	20.0	1450
Sulphide Ro C6				100										
Regrind									1					
Condition	5.4	25			50	6			1					
Condition					12	2					20-60	5.0	5.0	9000
Sulphide C1	5.4								1					
Condition					12	3					20-60	5.0	10.0	3000
Sulphide C1 scav1									2					
Condition											20-60	12.0	22.0	3000
Sulphide C1 Scav2									1					
Condition	5.6					2			1		20-30	1.5	1.5	5000
Sulphide C2C1														62
Condition						1			1		20-30	3.0	4.5	4000
Sulphide C2C2														62
Condition					5				1		20-50	5.0	9.5	2000
Sulphide C2C3						2								58
Condition					10				1		20-50	5.0	14.5	1200
Sulphide C2C4														22
REAGENT TOTALS (g/t)		94	734	200	230	64								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T18+19 CI2Con1	3109.0	12.9	0.08	1.1	42.6	21.2	0.39	17.3	47.3	42.2	0.86	0.4	0.05	0.9
CI2Con2	2463.4	10.2	0.13	1.4	42.7	16.9	0.45	15.8	44.0	31.1	1.23	0.4	0.06	0.9
CI2Con3	1158.4	4.8	0.19	1.0	43.8	8.1	1.14	18.9	38.9	12.9	2.97	0.5	0.10	0.7
CI2Con4	260.7	1.1	0.59	0.7	38.4	1.6	4.48	16.7	28.9	2.2	11.0	0.4	0.23	0.4
CI2 Tail	413.7	1.7	1.03	1.9	30.0	2.0	0.79	4.7	15.3	1.8	22.2	1.3	0.52	1.3
CI1 Tail	2081.2	8.7	1.64	14.9	23.1	7.7	0.37	11.0	4.81	2.9	35.2	10.1	0.77	9.4
Ro Tail	14549.9	60.5	1.25	79.1	18.2	42.4	0.08	15.6	1.66	6.9	43.6	87.0	1.01	86.5
CALC	24036.4	100.0	0.95	100.0	25.9	100.0	0.29	100.0	14.5	100.0	30.3	100.0	0.71	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T18+19 CI2Con1	3109.0	12.9	0.08	1.1	42.6	21.2	0.39	17.3	47.3	42.2	0.86	0.4	0.05	0.9
CI2Con2	5572.4	23.2	0.10	2.5	42.6	38.1	0.42	33.1	45.8	73.3	1.02	0.8	0.05	1.8
CI2Con3	6730.8	28.0	0.12	3.4	42.8	46.3	0.54	52.0	44.6	86.2	1.36	1.3	0.06	2.5
CI2Con4	6991.5	29.1	0.13	4.1	42.7	47.9	0.69	68.7	44.1	88.4	1.72	1.6	0.07	2.8
CI2 Tail	7405.2	30.8	0.18	6.0	42.0	49.9	0.69	73.4	42.4	90.2	2.86	2.9	0.09	4.1
CI1 Tail	9486.5	39.5	0.50	20.9	37.8	57.6	0.62	84.4	34.2	93.1	9.96	13.0	0.24	13.5
FEED	24036.4	100.0	0.95	100.0	25.9	100.0	0.29	100.0	14.5	100.0	30.3	100.0	0.71	100.0

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T18+19 CI2Con1	3109.0	12.9	0.08	0.4	0.21	0.4	0.02	0.6	0.25	38.2	2.11	41.3	1.79	29.3
CI2Con2	2463.4	10.2	0.14	0.5	0.27	0.4	0.03	0.7	0.27	32.7	2.35	36.4	3.14	40.7
CI2Con3	1158.4	4.8	0.33	0.6	0.56	0.4	0.05	0.6	0.16	9.1	0.95	6.9	3.87	23.6
CI2Con4	260.7	1.1	1.11	0.4	1.85	0.3	0.16	0.4	0.10	1.3	0.48	0.8	1.12	1.5
CI2 Tail	413.7	1.7	2.17	1.4	5.43	1.5	0.37	1.5	0.07	1.4	0.56	1.5	0.45	1.0
CI1 Tail	2081.2	8.7	2.47	7.9	6.23	8.5	0.57	11.7	0.03	3.1	0.27	3.5	0.12	1.3
Ro Tail	14549.9	60.5	3.95	88.7	9.22	88.4	0.59	84.5	0.02	14.3	0.11	9.6	0.03	2.7
CALC	24036.4	100.0	2.70	100.0	6.32	100.0	0.42	100.0	0.08	100.0	0.66	100.0	0.79	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T18+19 CI2Con1	3109.0	12.9	0.08	0.4	0.21	0.4	0.02	0.6	0.25	38.2	2.11	41.3	1.79	29.3
CI2Con2	5572.4	23.2	0.11	0.9	0.24	0.9	0.02	1.3	0.26	70.8	2.22	77.7	2.39	69.9
CI2Con3	6730.8	28.0	0.14	1.5	0.29	1.3	0.03	1.9	0.24	79.9	2.00	84.6	2.64	93.5
CI2Con4	6991.5	29.1	0.18	2.0	0.35	1.6	0.03	2.3	0.24	81.2	1.94	85.4	2.59	95.1
CI2 Tail	7405.2	30.8	0.29	3.3	0.63	3.1	0.05	3.8	0.23	82.6	1.86	86.8	2.47	96.0
CI1 Tail	9486.5	39.5	0.77	11.3	1.86	11.6	0.17	15.5	0.18	85.7	1.51	90.4	1.95	97.3
FEED	24036.4	100.0	2.70	100.0	6.32	100.0	0.42	100.0	0.08	100.0	0.66	100.0	0.79	100.0

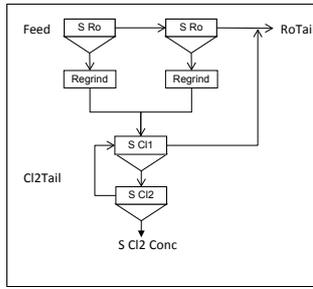
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+CI1Tail Comb	16631.1	69.2	1.30	94.0	18.8	50.1	0.11	26.6	2.06	9.8	42.6	97.1	0.98	95.9
FEED		100.0	0.95	100.0	25.9	100.0	0.29	100.0	14.5	100.0	30.3	100.0	0.71	100.0

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
RoTail+CI1Tail Comb	16631.1	69.2	3.77	96.7	8.85	96.9	0.59	96.2	0.02	17.4	0.13	13.2	0.05	4.0
FEED		100.0	2.70	100.0	6.32	100.0	0.42	100.0	0.08	100.0	0.66	100.0	0.79	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	17305.6	72.0	1.28	96.6	19.4	53.7	0.19	48.0	2.78	13.8	41.6	98.7	0.96	97.5
FEED		100.0	0.95	100.0	25.9	100.0	0.29	100.0	14.5	100.0	30.3	100.0	0.71	100.0

Milling		Primary	Regrind
Mill type	Large	Stirred	
Media type	MS ball	Sand	
Media kg	40	5	
Solids kg	12	2678	
Water kg	6	3000	
Time min/sec	17.5	7	
Speed rpm	50	1000	
Lime g	0	0	
End pH	6.4	6	
End p80	250	38	

Float Cell	Volume	Regrind	Power
Rougher	30	Start	40334
Cleaner1	30	Finish	40375
Cleaner2	30	W/h	40.97
Speed	900	kWh/t	18



PROJECT	T0879
TEST NO	T20+T21
DATE	300614
TECHNICIAN	MJR

PRODUCT FLOATED	
Severn Ore Comp	
SBC	

NOTES	
2*12kg Test	
Feed P80 250um	
CuSO4 in Regrind	
No Acid in Cleaners	

	pH	0.5 GUAR g/t	98 H2SO4 g/t	6 CuSO4 g/t	1.5 PAX g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	5.0		734						2					
Condition		25		25					2					
Condition					30	16			1	20-30	3.0	3.0	2200	
Sulphide Ro C1	5.4	12		25	30	8			2					
Condition									1	20-30	3.0	6.0	2500	
Sulphide Ro C2		12		50	25	4			2					
Condition									1	20-50	3.0	9.0	1100	
Sulphide Ro C3		12			25	4			2					
Condition									1	20-50	3.0	12.0	1100	
Sulphide Ro C4		6			15	6			2					
Condition									1	20-60	4.0	16.0	1300	
Sulphide Ro C5					15	6			2					
Condition	5.2									20-60	4.0	20.0	1450	
Sulphide Ro C6				100										
Regrind									1					
Condition	5.4	25			50	6			1					
Condition									1	20-60	5.0	5.0	9000	
Sulphide Cl1	5.4				12	2			1					
Condition									2	20-60	5.0	10.0	3000	
Sulphide Cl1 scav1					12	3								
Condition									1	20-60	12.0	22.0	3000	
Sulphide Cl1 Scav2														
Condition	5.6					2			1	20-30	1.5	1.5	5000	63
Sulphide Cl2C1						1			1					
Condition									1	20-30	3.0	4.5	4000	59
Sulphide Cl2C2						2								
Condition					5	2			1	20-50	5.0	9.5	2000	56
Sulphide Cl2C3														
Condition					10				1	20-50	5.0	14.5	1200	18
Sulphide Cl2C4														
REAGENT TOTALS (g/t)		94	734	200	230	64								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T20+21 Cl2Con1	3173.3	13.2	0.09	1.2	42.3	21.6	0.39	18.4	46.9	43.8	0.91	0.4	0.04	0.7
Cl2Con2	2371.2	9.9	0.14	1.4	42.9	16.4	0.53	18.6	43.6	30.4	1.29	0.4	0.06	0.8
Cl2Con3	1121.1	4.7	0.22	1.1	44.6	8.1	1.47	24.4	39.3	13.0	3.46	0.5	0.10	0.6
Cl2Con4	212.8	0.9	0.52	0.5	38.2	1.3	2.97	9.4	30.1	1.9	10.9	0.3	0.23	0.3
Cl2 Tail	348.3	1.4	1.08	1.6	30.0	1.7	0.91	4.7	13.7	1.4	23.5	1.1	0.54	1.1
Cl1 Tail	2055.9	8.6	1.74	15.4	22.9	7.6	0.30	9.1	4.06	2.5	35.4	10.0	0.80	9.5
Ro Tail	14759.9	61.4	1.24	78.8	18.3	43.4	0.07	15.3	1.65	7.1	43.0	87.2	1.02	86.9
CALC	24042.5	100.0	0.97	100.0	25.8	100.0	0.28	100.0	14.1	100.0	30.2	100.0	0.72	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00			

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
T20+21 Cl2Con1	3173.3	13.2	0.09	1.2	42.3	21.6	0.39	18.4	46.9	43.8	0.91	0.4	0.04	0.7
Cl2Con2	5544.5	23.1	0.11	2.7	42.6	38.0	0.45	37.0	45.5	74.2	1.07	0.8	0.05	1.6
Cl2Con3	6665.6	27.7	0.13	3.7	42.9	46.0	0.62	61.4	44.4	87.1	1.47	1.4	0.06	2.2
Cl2Con4	6878.4	28.6	0.14	4.2	42.8	47.4	0.69	70.8	44.0	89.0	1.77	1.7	0.06	2.5
Cl2 Tail	7226.7	30.1	0.19	5.8	42.1	49.0	0.70	75.5	42.5	90.4	2.81	2.8	0.09	3.6
Cl1 Tail	9282.6	38.6	0.53	21.2	37.9	56.6	0.61	84.7	34.0	92.9	10.0	12.8	0.24	13.1
FEED	24042.5	100.0	0.97	100.0	25.8	100.0	0.28	100.0	14.1	100.0	30.2	100.0	0.72	100.0

PRODUCTS	WT g	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T20+21 Cl2Con1	3173.3	13.2	0.11	0.5	0.24	0.5	0.01	0.3	0.24	37.1	2.20	45.8	2.08	36.0
Cl2Con2	2371.2	9.9	0.13	0.5	0.30	0.5	0.02	0.5	0.26	30.1	2.14	33.3	3.40	43.9
Cl2Con3	1121.1	4.7	0.37	0.6	0.68	0.5	0.06	0.7	0.17	9.3	0.87	6.4	2.62	16.0
Cl2Con4	212.8	0.9	1.27	0.4	1.97	0.3	0.15	0.3	0.11	1.1	0.47	0.7	0.40	0.5
Cl2 Tail	348.3	1.4	2.37	1.3	5.54	1.3	0.39	1.3	0.08	1.4	0.48	1.1	0.27	0.5
Cl1 Tail	2055.9	8.6	2.58	8.1	6.28	8.5	0.58	11.6	0.03	3.0	0.22	3.0	0.06	0.7
Ro Tail	14759.9	61.4	3.95	88.6	9.13	88.5	0.60	85.4	0.03	18.0	0.10	9.7	0.03	2.4
CALC	24042.5	100.0	2.73	100.0	6.33	100.0	0.43	100.0	0.09	100.0	0.63	100.0	0.76	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
T20+21 Cl2Con1	3173.3	13.2	0.11	0.5	0.24	0.5	0.01	0.3	0.24	37.1	2.20	45.8	2.08	36.0
Cl2Con2	5544.5	23.1	0.12	1.0	0.27	1.0	0.01	0.8	0.25	67.2	2.17	79.2	2.64	79.9
Cl2Con3	6665.6	27.7	0.16	1.6	0.34	1.5	0.02	1.4	0.24	76.5	1.95	85.6	2.64	95.9
Cl2Con4	6878.4	28.6	0.20	2.0	0.39	1.7	0.03	1.7	0.23	77.6	1.91	86.2	2.57	96.4
Cl2 Tail	7226.7	30.1	0.30	3.3	0.63	3.0	0.04	3.1	0.22	79.0	1.84	87.3	2.46	96.9
Cl1 Tail	9282.6	38.6	0.80	11.4	1.88	11.5	0.16	14.6	0.18	82.0	1.48	90.3	1.93	97.6
FEED	24042.5	100.0	2.73	100.0	6.33	100.0	0.43	100.0	0.09	100.0	0.63	100.0	0.76	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoTail+Cl1Tail Comb	16815.8	69.9	1.30	94.2	18.8	51.0	0.10	24.5	1.94	9.6	42.0	97.2	0.99	96.4
FEED		100.0	0.97	100.0	25.8	100.0	0.28	100.0	14.1	100.0	30.2	100.0	0.72	100.0

CUM PRODUCTS	CUM Wt	WT %	MgO %	DIST	Al2O3 %	DIST	Mn %	DIST	Cu %	DIST	Pb %	DIST	Zn %	DIST
RoTail+Cl1Tail Comb	16815.8	69.9	3.78	96.7	8.78	97.0	0.59	96.9	0.03	21.0	0.11	12.7	0.03	3.1
FEED		100.0	2.73	100.0	6.33	100.0	0.43	100.0	0.09	100.0	0.63	100.0	0.76	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	CaO %	DIST
RoT, Con4 Comb	17376.9	72.3	1.29	96.3	19.3	54.0	0.15	38.6	2.52	12.9	41.3	98.6	0.97	97.8
FEED		100.0	0.97	100.0	25.8	100.0	0.28	100.0	14.1	100.0	30.2	100.0	0.72	100.0

Calculated heads

Test	Sn %	Sn Acid Sol ppm	Fe %	As %	S %	SiO ₂ %	CaO %	MgO %	Al ₂ O ₃ %	Mn %	Cu %	Pb %	Zn %
T02	1.01		26.28	0.27	15.12	29.50	0.67	2.70	6.11	0.34			
T03	1.01		26.20	0.28	14.95	29.73	0.67	2.68	6.22	0.33			
T04	1.01		26.48	0.28	15.10	29.71	0.71	2.76	6.34	0.34			
T05	1.04		26.25	0.28	14.68	29.85	0.71	2.79	6.37	0.35			
T06	1.01		26.43	0.28	15.24	29.38	0.69	2.72	6.03	0.34			
T07	0.98		25.81	0.27	14.08	30.54	0.72	2.79	6.56	0.45			
T08	1.00		25.87	0.27	14.81	30.01	0.68	2.75	6.35	0.43			
T09	1.01		26.10	0.28	14.83	29.98	0.69	2.75	6.21	0.44			
T10	0.97		26.41	0.27	14.38	29.92	0.69	2.71	6.13	0.44			
T11	1.02		25.90	0.27	14.18	30.11	0.74	2.81	6.40	0.45			
T12	1.02	166	26.13	0.28	14.77	30.18	0.73	2.77	6.30	0.43	0.09	0.62	0.77
T13	1.03	174	26.16	0.29	14.57	30.28	0.72	2.72	6.35	0.43	0.09	0.65	0.81
T14+T15	1.01		25.90	0.28	14.23	30.71	0.76	2.72	6.24	0.43	0.09	0.64	0.74
T16+T17	0.99		25.70	0.27	13.33	30.89	0.73	2.75	6.33	0.43	0.08	0.59	0.73
T18+T19	0.95		25.94	0.29	14.50	30.33	0.71	2.70	6.32	0.42	0.08	0.66	0.79
T20+T21	0.97		25.83	0.28	14.14	30.24	0.72	2.73	6.33	0.43	0.09	0.63	0.76
Average	1.00	170	26.1	0.28	14.6	30.1	0.71	2.74	6.29	0.40	0.09	0.63	0.77

Sn %	Sn Acid Sol ppm	Fe %	As %	S %	SiO ₂ %	CaO %	MgO %	Al ₂ O ₃ %	Mn %	Cu %	Pb %	Zn %
1.00	170	26.1	0.28	14.6	30.1	0.71	2.74	6.29	0.40	0.09	0.63	0.77

TEST	Ore	Primary Grind		ROUGHER						Regrind	Regrind	Regrind	Regrind	CLEANER					RoTail	NOTES
		P80 (um)	pH	H2SO4	GUAR	CuSO4	PAX	MIBC	pH	kWh/t	Ball (min)	CuSO4	P80 (um)	H2SO4	GUAR	CuSO4	PAX	MIBC	pH	
T02	SBC	100	6.70	1601	226	100	130	69	5.4										104	Standard Rougher Float
T03	SBC	130	6.72	1375	225	100	130	69	5.4										131	Standard Rougher Float
T04	SBC	160	6.69	1273	225	100	130	69	5.4										185	Standard Rougher Float
T05	SBC	240	6.73	1133	226	100	131	70	5.4										278	Standard Rougher Float
T06	SBC	240	6.75	1037	227	101	131	70	5.4										258	Standard Rougher Float
T07	SBC	250	6.60	718	229	102	143	71	5.3	20		0	26	195	102	25	85	43	4.9	Stirred Mill Regrind (slow cleaner float response)
T08	SBC	250	6.75	1091	228	101	142	70	5.4	20		76	25	174	101	0	84	43	4.8	Stirred Mill Regrind (slow cleaner float response)
T09	SBC	250	6.80	932	225	100	140	69	5.4		8.50	0	67	417	100	25	40	42	5.2	Ball Mill Regrind (Fast cleaner float response)
T10	SBC	250	6.65	950	225	100	140	69	5.4		12.45	0	54	710	100	25	30	42	5.0	Ball Mill Regrind (Medium cleaner float response)
T11	SBC	250	6.00	956	226	101	141	82	5.5		20.00	0	41	986	101	25	40	25	5.0	Ball Mill Regrind (Medium cleaner float response)
T12	SBC	250	6.40	872	226	101	141	70	5.4	10		101	37	0	101	0	85	55	5.7	Stirred Mill Regrind (Fast cleaner float response)
T13	SBC	250	6.45	858	225	100	140	69	5.5	20		100	25	0	100	0	85	57	5.7	Stirred Mill Regrind (Fast cleaner float response)
T14/T15	SBC	250	6.40	732	68	100	139	45	5.4	15		100	82	0	25	0	90	18	5.6	
T16/T17	SBC	250	6.40	732	68	100	139	45	5.4	18		100	38	0	25	0	90	18	5.6	
T18/T19	SBC	250	6.40	732	68	100	139	45	5.4	18		100	38	0	25	0	90	18	5.6	
T20/T21	SBC	250	6.40	732	68	100	139	45	5.4	18		100	38	0	25	0	90	18	5.6	

TEST	Product	WT %	Sn %	Dist %	Fe %	Dist %	As %	Dist %	S %	Dist %	SiO2 %	Dist %	CaO %	Dist %	MgO %	Dist %	Al2O3 %	Dist %	Mn %	Dist %	Cu %	Dist %	Pb %	Dist %	Zn %	Dist %	Sn Acid Sol ppm	Dist %
T02	RoCon	37.1	0.32	11.9	39.75	56.1	0.57	76.9	38.25	93.8	7.08	8.9	0.19	10.3	0.72	9.9	1.65	10.0	0.10	10.5								
T03	RoCon	36.4	0.35	12.5	39.81	55.4	0.62	81.5	37.95	92.5	7.10	8.7	0.19	10.2	0.69	9.4	1.70	9.9	0.10	10.5								
T04	RoCon	36.4	0.36	12.9	39.88	54.9	0.64	83.9	37.98	91.7	7.04	8.6	0.19	10.0	0.71	9.4	1.66	9.6	0.10	10.9								
T05	RoCon	34.2	0.34	11.1	40.21	52.4	0.64	78.8	38.73	90.2	6.26	7.2	0.17	8.3	0.62	7.6	1.45	7.8	0.09	8.8								
T06	RoCon	34.0	0.34	11.6	40.07	51.5	0.65	80.8	39.25	87.5	6.23	7.2	0.16	7.9	0.59	7.4	1.31	7.4	0.09	8.8								
T07	Cl2Con	20.1	0.11	2.3	42.88	33.4	0.29	21.9	44.43	63.4	1.43	0.9	0.04	1.2	0.19	1.4	0.37	1.1	0.03	1.6								
T08	Cl2Con	22.0	0.10	2.3	42.87	36.5	0.38	30.7	45.27	67.3	1.90	1.4	0.06	1.9	0.25	2.0	0.63	2.2	0.03	1.7								
T09	Cl2Con	29.7	0.22	6.6	42.04	47.8	0.70	74.2	43.66	87.4	2.95	2.9	0.10	4.3	0.25	2.7	0.57	2.7	0.07	4.6								
T10	Cl2Con	25.8	0.18	4.7	42.07	41.2	0.56	53.5	42.12	75.7	2.25	1.9	0.10	3.8	0.22	2.1	0.44	1.8	0.06	3.5								
T11	Cl1Con	18.0	0.16	2.8	40.30	28.0	0.52	35.2	43.00	54.6	3.31	2.0	0.13	3.2	0.39	2.5	0.88	2.5	0.06	2.4								
T12	Cl2Con	29.2	0.15	4.4	42.68	47.8	0.67	69.5	44.78	88.6	2.06	2.0	0.07	2.9	0.25	2.7	0.47	2.2	0.04	2.5	0.23	75.2	1.85	87.0	2.53	96.0	334	58.8
T13	Cl2Con	28.8	0.11	3.1	42.86	47.2	0.56	56.3	44.55	88.1	1.99	1.9	0.09	3.7	0.20	2.1	0.45	2.0	0.03	2.2	0.23	76.3	1.95	86.5	2.64	93.8	340	56.4
T14/T15	Cl2Con	29.5	0.23	6.7	42.13	48.0	0.69	73.7	42.81	88.7	3.33	3.2	0.11	4.4	0.26	2.8	0.57	2.7	0.05	3.4	0.23	74.2	1.83	84.8	2.39	94.9		
T16/T17	Cl2Con	27.4	0.13	3.5	42.67	45.6	0.66	67.3	41.95	86.4	1.69	1.5	0.10	3.6	0.17	1.7	0.32	1.4	0.02	1.4	0.23	74.9	1.79	83.7	2.50	94.7		
T18/T19	Cl2Con	29.1	0.13	4.1	42.68	47.9	0.69	68.7	44.06	88.4	1.72	1.6	0.07	2.8	0.18	2.0	0.35	1.6	0.03	2.3	0.24	81.2	1.94	85.4	2.59	95.1		
T20/T21	Cl2Con	28.6	0.14	4.2	42.75	47.4	0.69	70.8	44.00	89.0	1.77	1.7	0.06	2.5	0.20	2.0	0.39	1.7	0.03	1.7	0.23	77.6	1.91	86.2	2.57	96.4		

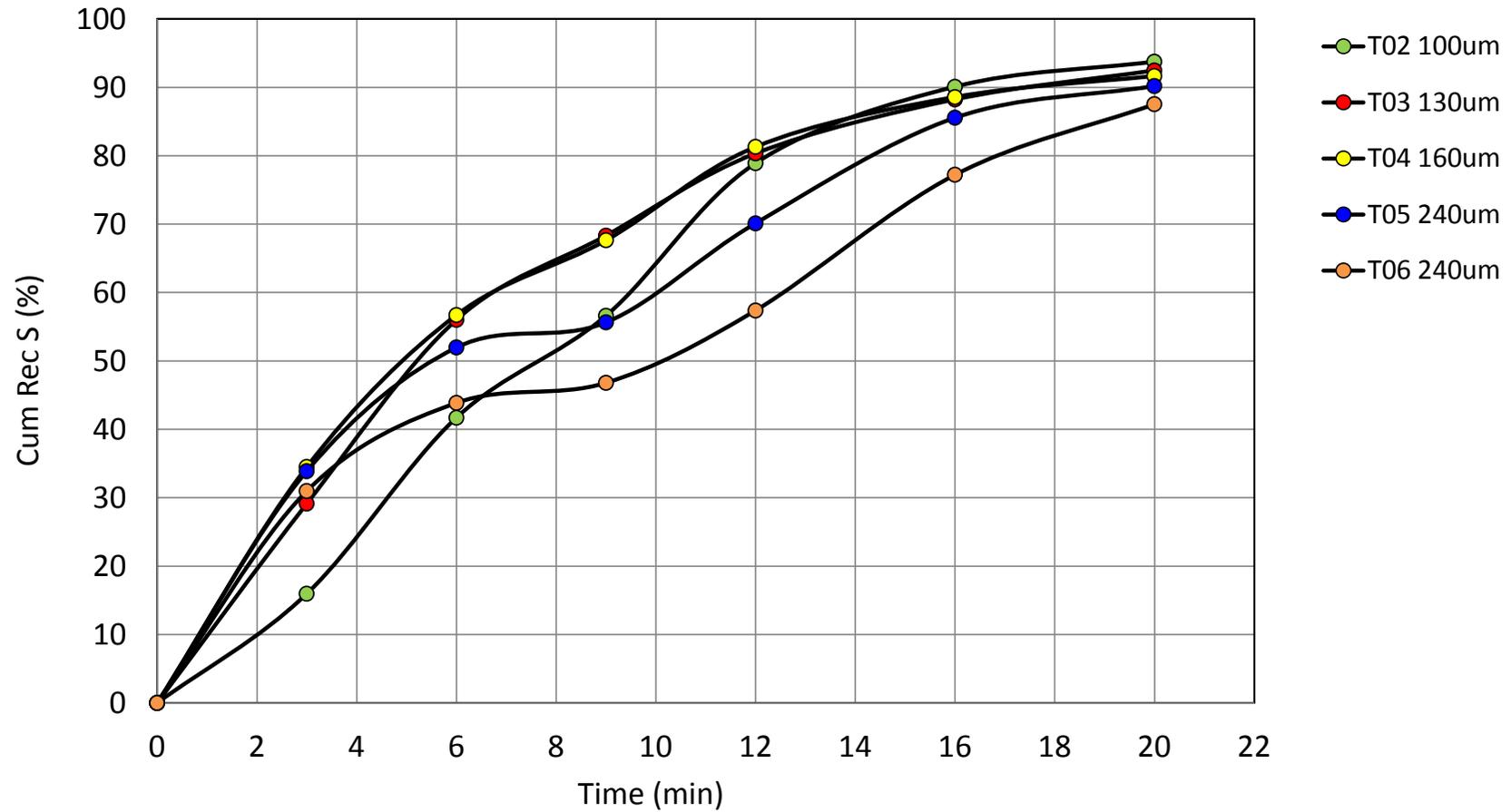
TEST	Product	WT %	Sn %	Dist %	Fe %	Dist %	As %	Dist %	S %	Dist %	SiO2 %	Dist %	CaO %	Dist %	MgO %	Dist %	Al2O3 %	Dist %	Mn %	Dist %	Cu %	Dist %	Pb %	Dist %	Zn %	Dist %	Sn Acid Sol ppm	Dist %
T02	RoTail	62.9	1.41	88.1	18.35	43.9	0.10	23.1	1.50	6.2	42.70	91.1	0.96	89.7	3.87	90.1	8.73	90.0	0.48	89.5								
T03	RoTail	63.6	1.39	87.5	18.40	44.6	0.08	18.5	1.77	7.5	42.70	91.3	0.95	89.8	3.82	90.6	8.82	90.1	0.47	89.5								
T04	RoTail	63.6	1.38	87.1	18.80	45.1	0.07	16.1	1.98	8.3	42.70	91.4	1.00	90.0	3.93	90.6	9.02	90.4	0.48	89.1								
T05	RoTail	65.8	1.40	88.9	19.00	47.6	0.09	21.2	2.19	9.8	42.10	92.8	0.99	91.7	3.92	92.4	8.93	92.2	0.49	91.2								
T06	RoTail	66.0	1.35	88.4	19.40	48.5	0.08	19.2	2.88	12.5	41.30	92.8	0.96	92.1	3.81	92.6	8.46	92.6	0.47	91.2								
T07	RoT/Cl1tail	77.1	1.22	96.5	21.06	63.0	0.24	69.9	5.64	30.9	38.69	97.7	0.90	97.5	3.52	97.3	8.26	97.1	0.56	97.1								
T08	RoT/Cl1tail	74.7	1.29	96.2	20.52	59.2	0.21	59.2	5.22	26.3	38.95	96.9	0.88	96.5	3.54	96.1	8.13	95.5	0.56	96.7								
T09	RoT/Cl1tail	69.1	1.35	92.5	19.19	50.8	0.09	23.4	2.45	11.4	41.69	96.0	0.94	94.6	3.83	96.1	8.64	96.0	0.60	94.4								
T10	RoT/Cl1tail	71.5	1.27	93.9	20.35	55.1	0.14	36.0	3.77	18.7	40.57	96.9	0.92	95.1	3.66	96.5	8.29	96.7	0.58	95.3								
T11	RoT/Cl1tail	82.0	1.20	97.2	22.74	72.0	0.21	64.8	7.86	45.4	35.99	98.0	0.87	96.8	3.34	97.5	7.61	97.5	0.53	97.6								
T12	RoT/Cl1tail	69.1	1.38	94.0	19.10	50.5	0.11	26.8	2.15	10.0	42.16	96.5	1.00	95.6	3.85	95.8	8.75	95.9	0.60	96.0	0.03	23.7	0.11	12.1	0.04	3.6	96	40.0
T13	RoT/Cl1tail	69.7	1.41	95.6	19.23	51.2	0.15	37.0	2.25	10.7	42.05	96.8	0.97	95.0	3.77	96.5	8.76	96.2	0.59	96.4	0.03	22.9	0.12	12.6	0.07	5.7	106	42.6
T14/T15	RoT/Cl1tail	68.7	1.35	91.5	18.83	49.9	0.09	22.7	1.91	9.2	42.67	95.4	1.05	94.3	3.79	95.8	8.70	95.7	0.59	95.1	0.03	23.8	0.12	13.0	0.03	2.6		
T16/T17	RoT/Cl1tail	70.6	1.33	94.5	18.96	52.1	0.10	25.3	2.12	11.2	42.50	97.2	0.99	95.2	3.77	96.9	8.70	97.2	0.59	97.2	0.03	22.6	0.12	14.1	0.04	3.9		
T18/T19	RoT/Cl1tail	69.2	1.30	94.0	18.80	50.1	0.11	26.6	2.06	9.8	42.55	97.1	0.98	95.9	3.77	96.7	8.85	96.9	0.59	96.2	0.02	17.4	0.13	13.2	0.05	4.0		
T20/T21	RoT/Cl1tail	69.9	1.30	94.2	18.82	51.0	0.10	24.5	1.94	9.6	42.03	97.2	0.99	96.4	3.78	96.7	8.78	97.0	0.59	96.9	0.03	21.0	0.11	12.7	0.03	3.1		

Blend For Gravity Circuit

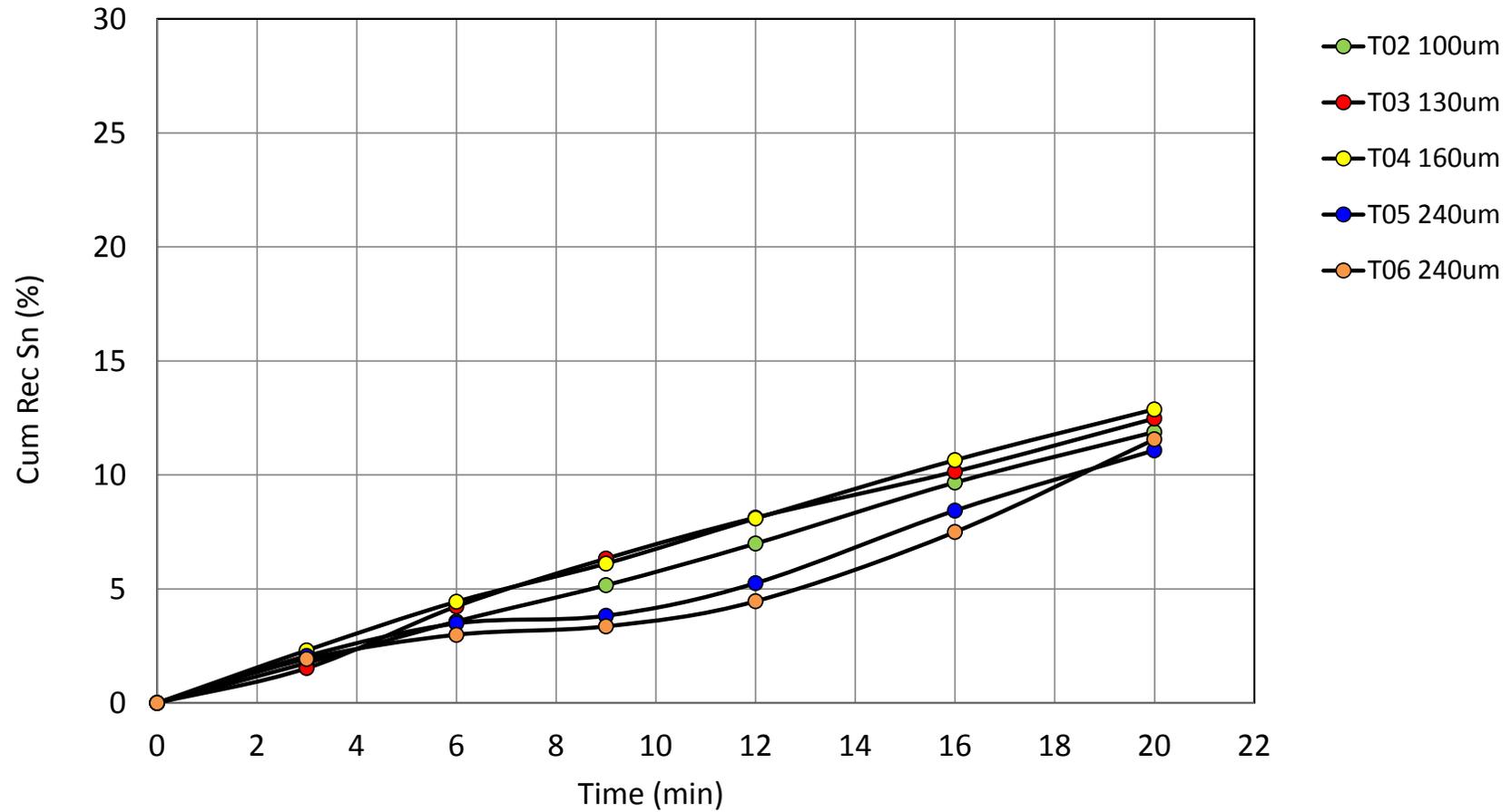
TEST	Product	WT %	WT gm	Sn %	Dist %	Fe %	Dist %	As %	Dist %	S %	Dist %	SiO2 %	Dist %	CaO %	Dist %
T07	RoT/Cl1tail	1.9	1515.4	1.22	96.5	21.06	63.0	0.24	69.9	5.64	30.9	38.69	97.7	0.90	97.5
T08	RoT/Cl1tail	1.8	1475.2	1.29	96.2	20.52	59.2	0.21	59.2	5.22	26.3	38.95	96.9	0.88	96.5
T09	RoT, Con4	1.8	1422.5	1.33	94.1	19.54	53.3	0.11	29.1	2.92	14.0	41.11	97.6	0.93	96.2
T10	RoT/Cl1tail	1.8	1429.8	1.27	93.9	20.35	55.1	0.14	36.0	3.77	18.7	40.57	96.9	0.92	95.1
T11	RoT/Cl1tail	2.0	1630.3	1.20	97.2	22.74	72.0	0.21	64.8	7.86	45.4	35.99	98.0	0.87	96.8
T12	RoT, Con4	1.8	1429.0	1.36	96.2	19.54	53.7	0.15	38.7	2.76	13.4	41.37	98.4	0.99	97.5
T13	RoT, Con4	1.8	1451.2	1.38	97.4	19.75	54.8	0.23	58.6	3.09	15.4	41.05	98.4	0.95	96.6
T14/T15	RoT, Con4	21.5	17215.0	1.34	94.2	19.30	53.3	0.13	34.1	2.56	12.8	41.85	97.4	1.02	96.1
T16/T17	RoT, Con4	22.1	17683.2	1.30	97.0	19.68	56.5	0.17	46.8	3.04	16.8	41.33	98.8	0.96	96.7
T18/T19	RoT, Con4	21.6	17305.6	1.28	96.6	19.36	53.7	0.19	48.0	2.78	13.8	41.59	98.7	0.96	97.5
T20/T21	RoT, Con4	21.7	17376.9	1.29	96.3	19.28	54.0	0.15	38.6	2.52	12.9	41.27	98.6	0.97	97.8
Total		100.0	79934.1	1.30	96.0	19.55	55.0	0.16	43.1	2.96	15.4	41.26	98.3	0.97	97.0

Target 3% Sulphur

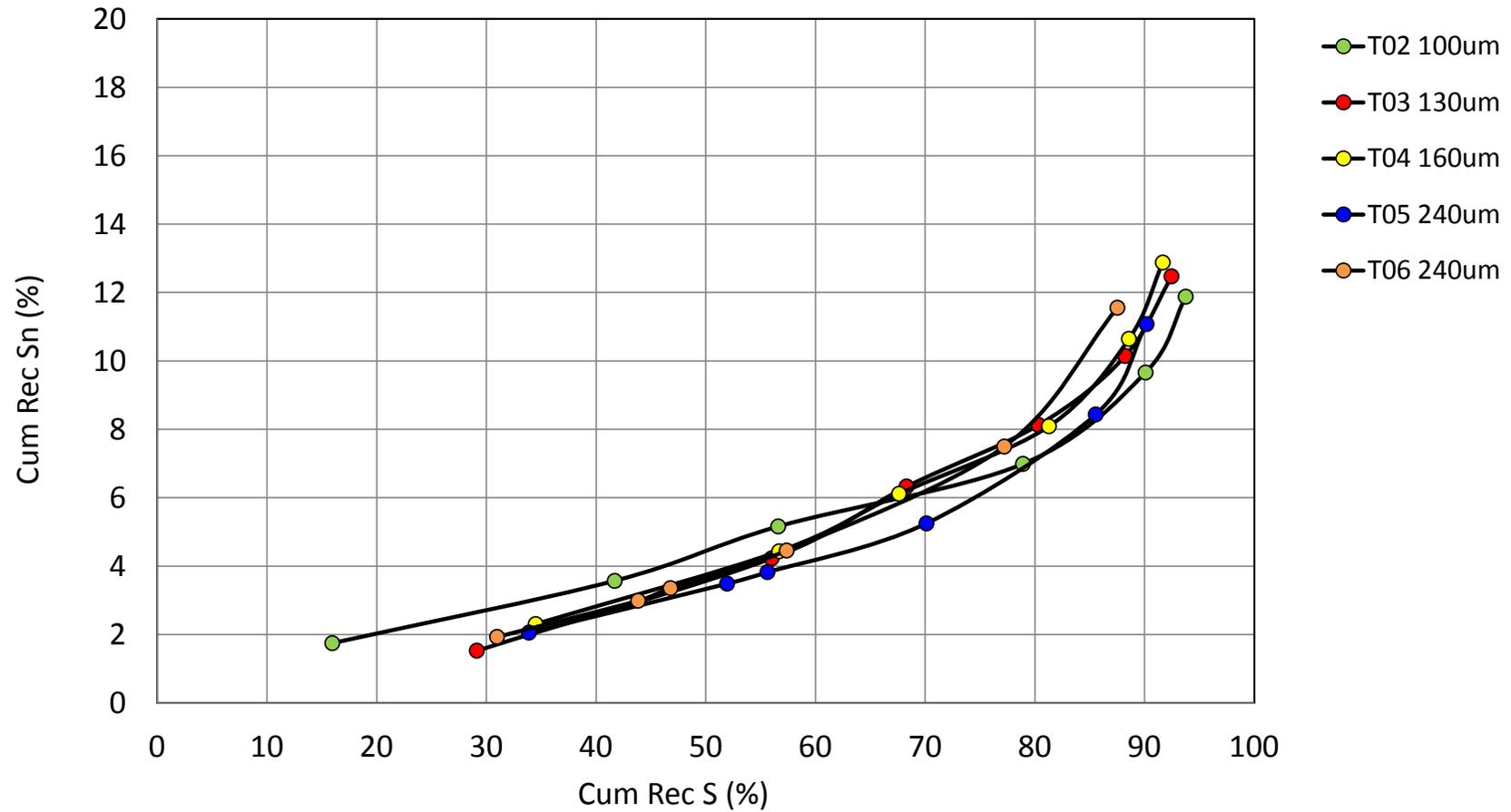
Severn SBC Composite
Sulphur Recovery vs Time



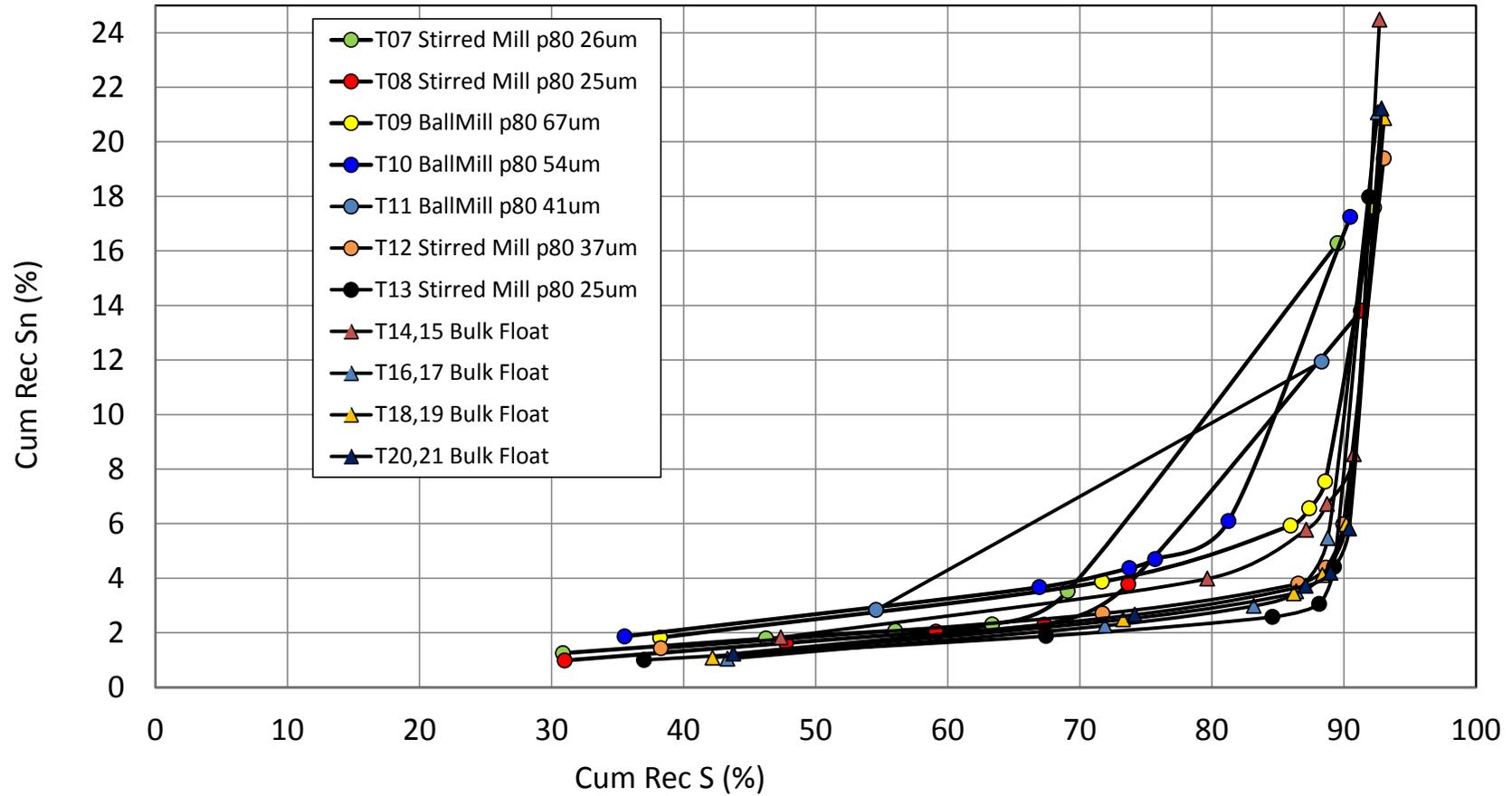
Severn SBC Composite
Tin Recovery vs Time



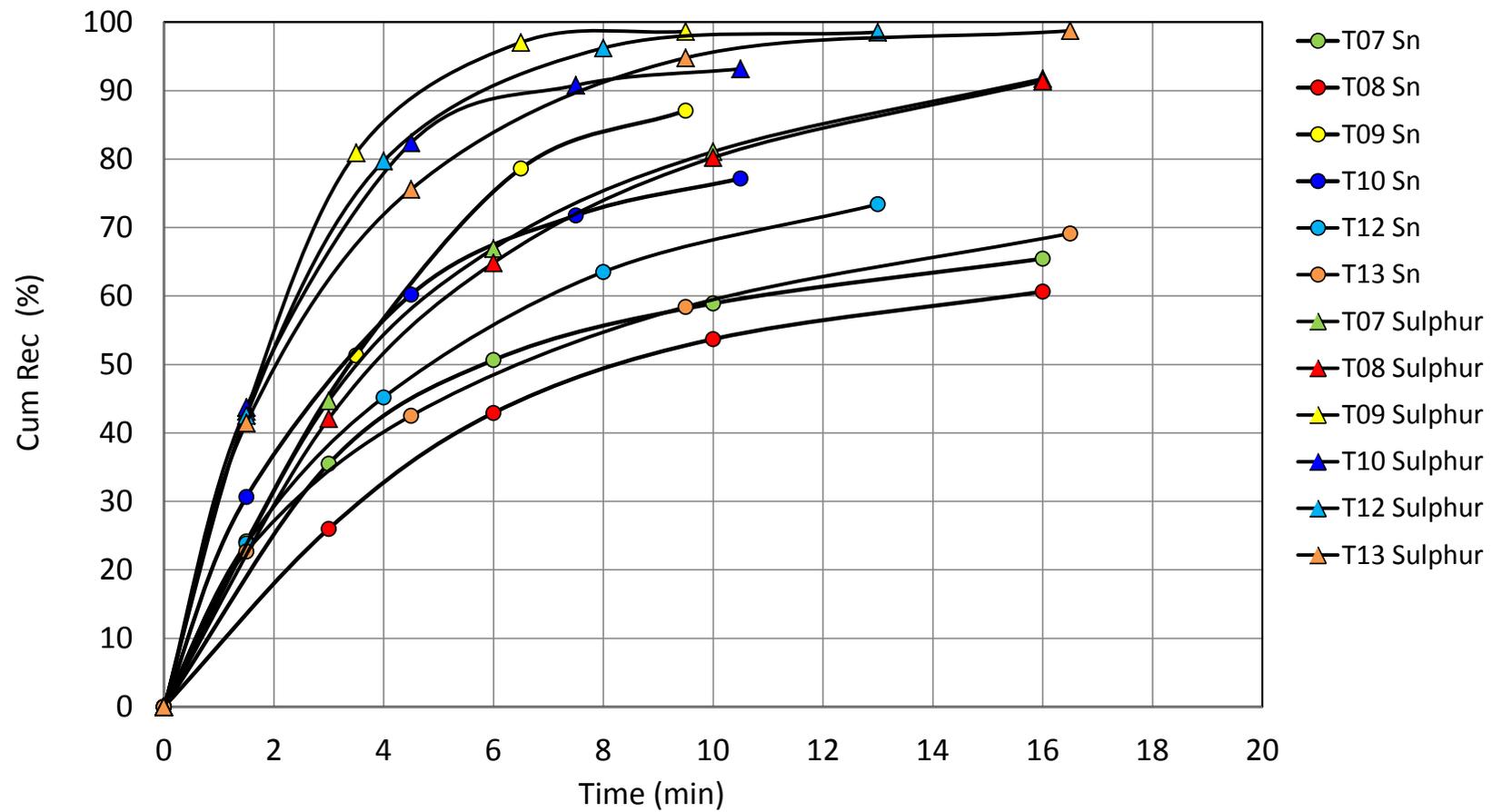
Severn SBC Composite
Sulphur Recovery vs Tin Recovery



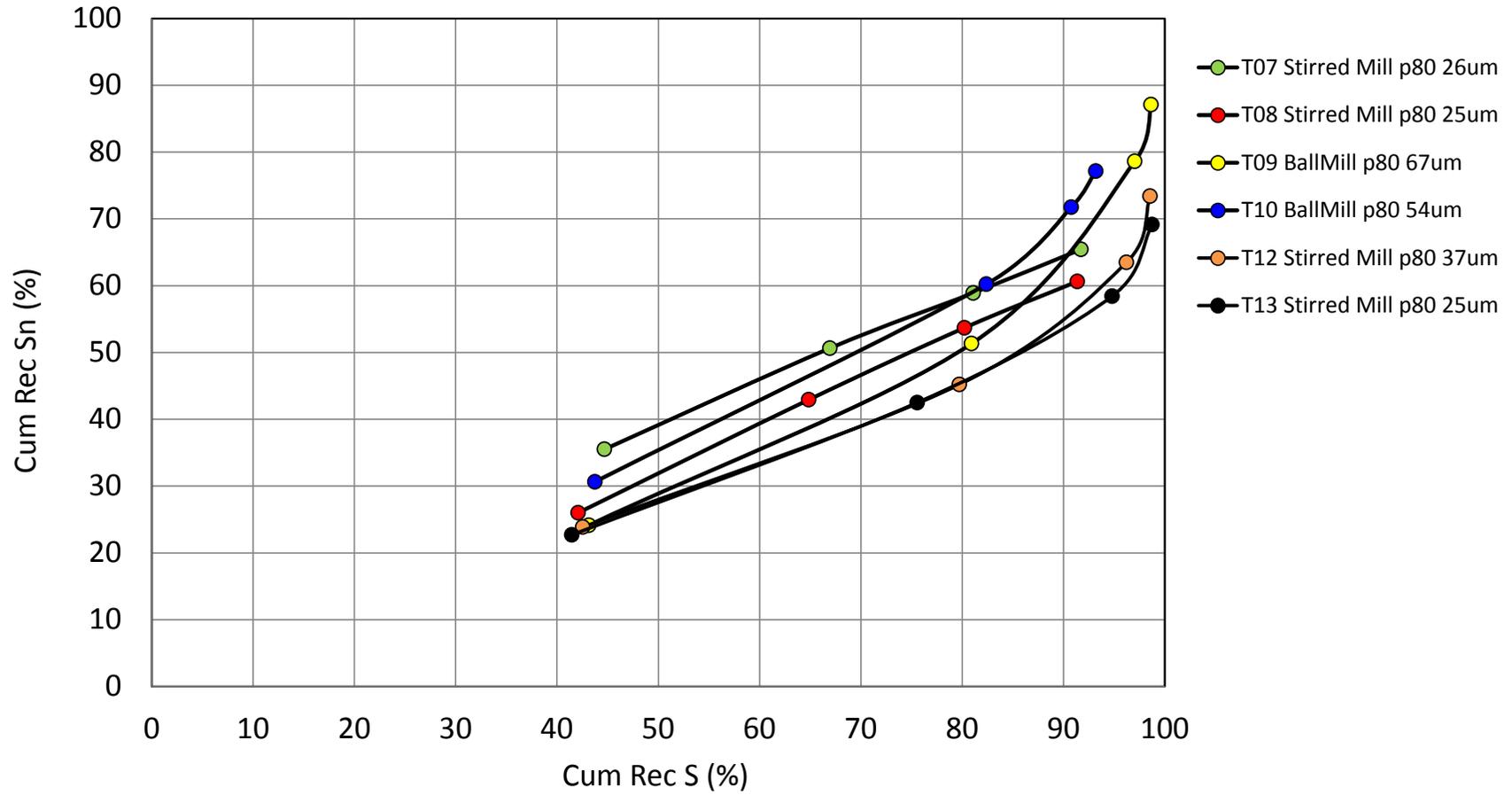
Severn SBC Composite
Cleaner Sulphur Recovery vs Tin Recovery



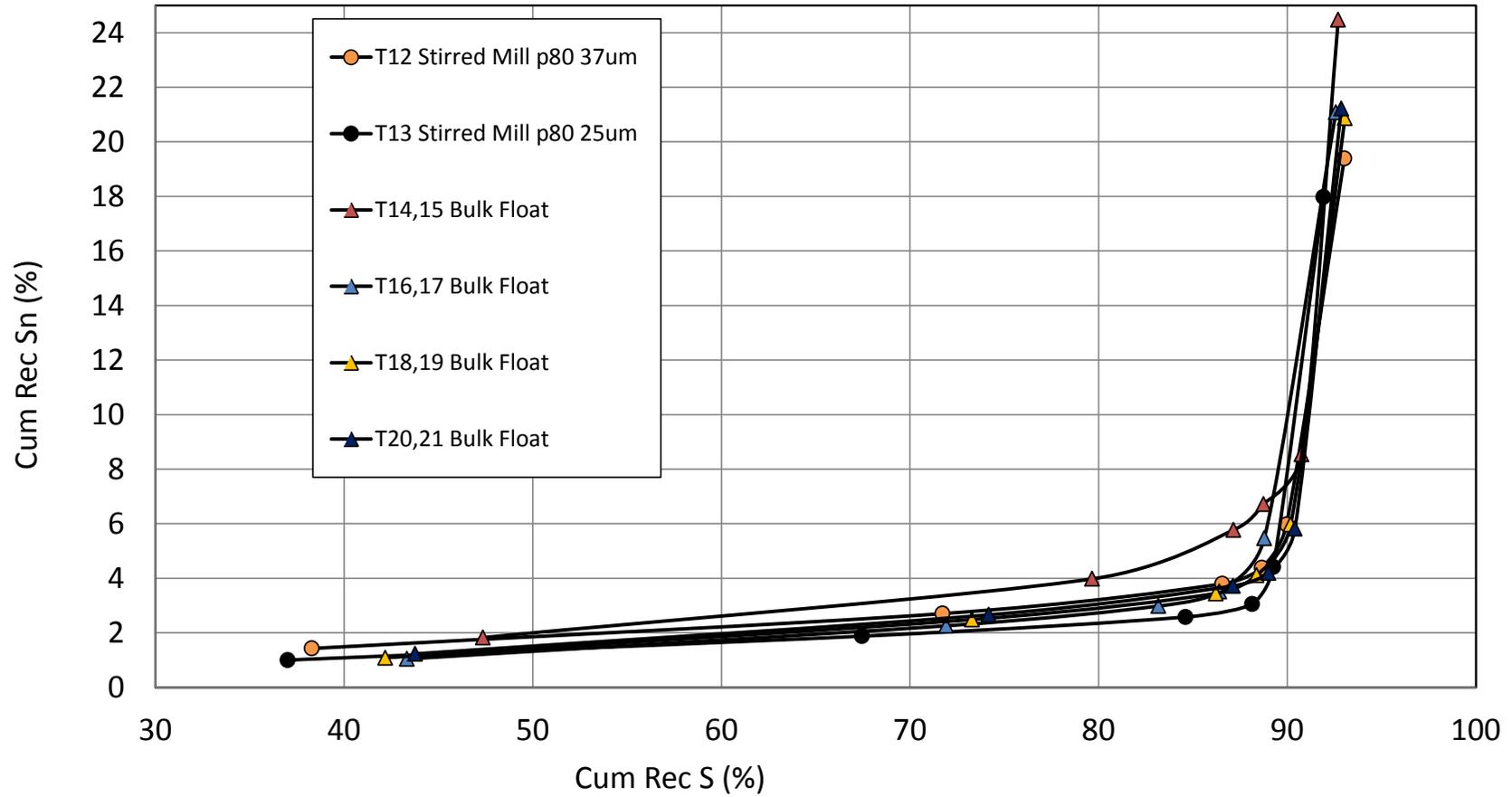
Severn SBC Composite
Cleaner 2 Recovery vs Time



Severn SBC Composite
Cleaner 2 Sulphur Recovery vs Tin Recovery



Severn SBC Composite
Cleaner Sulphur Recovery vs Tin Recovery

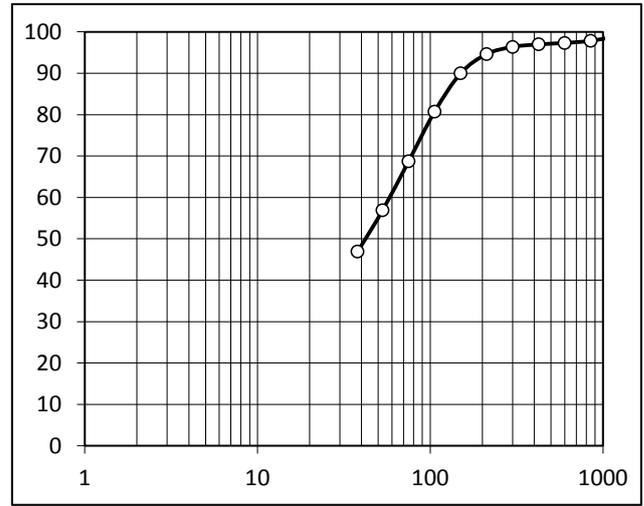




BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoTail
FROM TEST	T02
DATE	260514
TECHNICIAN	MS

RoTail T02	SIZE um	WEIGHTS		
		gm	(%)	%PASS
p80	1700	0.00	0.00	100.0
	1180	2.55	1.11	98.9
	850	2.44	1.06	97.8
	600	1.18	0.51	97.3
	425	0.78	0.34	97.0
	300	1.40	0.61	96.4
	212	4.02	1.74	94.6
	150	10.67	4.63	90.0
	106	21.42	9.29	80.7
	104	75	27.62	11.97
53		27.30	11.84	56.9
38		23.04	9.99	46.9
SUB		108.24	46.93	0.0
TOTAL	230.66	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	ppm	dist	%	dist
600	2.67	1.25	2.4	18.75	2.8	0.17	4.2	8.25	13.2	43.30	2.7	0.21	1.2
212	2.69	0.44	0.9	12.50	1.8	0.08	2.0	2.34	3.8	55.70	3.5	0.17	1.0
150	4.63	0.44	1.5	14.55	3.7	0.07	3.0	2.06	5.7	53.30	5.8	0.30	3.1
106	9.29	0.70	4.7	16.40	8.4	0.11	9.5	2.08	11.5	48.80	10.6	0.40	8.2
75	11.97	1.22	10.6	17.45	11.5	0.16	17.7	1.90	13.6	47.10	13.2	0.47	12.4
<75	68.75	1.61	80.0	19.00	71.8	0.10	63.6	1.27	52.2	40.10	64.3	0.49	74.1
CALC	100.00	1.38	100.0	18.19	100.0	0.11	100.0	1.67	100.0	42.86	100.0	0.45	100.0
ASSAY		1.38		18.20		0.11		1.69		43.00		0.47	

ANALYSES

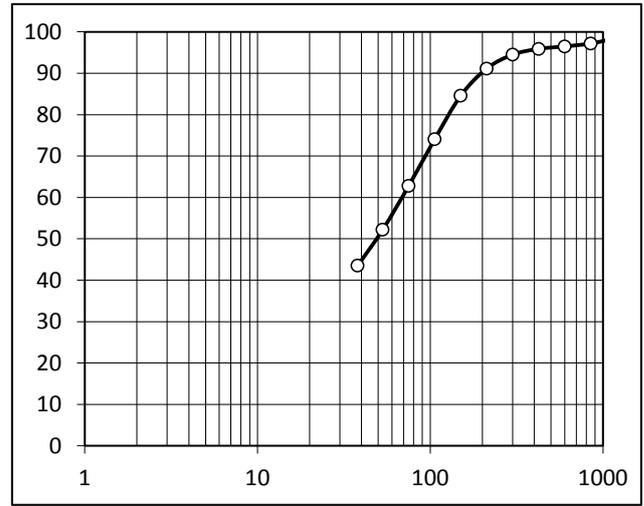
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
600	2.67	0.57	1.6	2.59	1.8	9.46	2.9
212	2.69	0.65	1.8	3.53	2.5	9.75	3.0
150	4.63	0.66	3.2	3.74	4.6	9.18	4.8
106	9.29	0.78	7.6	3.62	8.9	8.15	8.6
75	11.97	0.89	11.2	3.54	11.2	7.65	10.4
<75	68.75	1.03	74.5	3.92	71.1	9.07	70.5
CALC	100.00	0.95	100.0	3.79	100.0	8.85	100.0
ASSAY		0.96		3.82		8.89	



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoTail
FROM TEST	T03
DATE	260514
TECHNICIAN	MS

RoTail T03	SIZE um	WEIGHTS		
		gm	(%)	%PASS
p80	1700	0.00	0.00	100.0
	1180	3.19	1.52	98.5
	850	2.71	1.29	97.2
	600	1.49	0.71	96.5
	425	1.23	0.58	95.9
	300	2.96	1.41	94.5
	212	7.10	3.37	91.1
	150	13.80	6.56	84.6
131	106	22.16	10.53	74.0
	75	23.70	11.26	62.8
	53	22.32	10.60	52.2
	38	18.25	8.67	43.5
	SUB	91.59	43.51	0.0
	TOTAL	210.50	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	ppm	dist	%	dist
600	3.51	0.91	2.4	18.00	3.4	0.16	6.4	7.75	14.2	46.00	3.8	0.16	1.2
212	5.36	0.43	1.7	14.25	4.1	0.06	3.7	2.60	7.3	53.50	6.7	0.22	2.6
150	6.56	0.62	3.0	16.15	5.7	0.10	7.5	2.57	8.8	49.60	7.6	0.36	5.1
106	10.53	0.97	7.6	17.30	9.8	0.10	12.0	2.31	12.7	47.60	11.7	0.43	9.8
75	11.26	1.47	12.3	17.80	10.8	0.10	12.9	1.85	10.9	45.90	12.0	0.49	12.0
<75	62.78	1.57	73.1	19.50	66.1	0.08	57.5	1.40	46.0	39.90	58.3	0.51	69.4
CALC	100.00	1.35	100.0	18.52	100.0	0.09	100.0	1.91	100.0	42.97	100.0	0.46	100.0
ASSAY		1.35		18.25		0.09		1.92		43.00		0.46	

ANALYSES

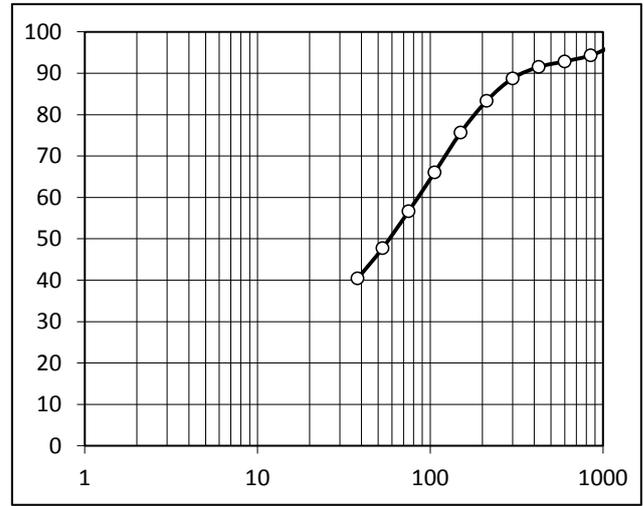
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
600	3.51	0.52	1.9	2.78	2.5	9.40	3.7
212	5.36	0.62	3.5	3.55	5.0	9.32	5.7
150	6.56	0.71	4.9	3.63	6.2	8.54	6.3
106	10.53	0.80	8.9	3.55	9.7	7.86	9.4
75	11.26	0.94	11.2	3.48	10.2	7.40	9.4
<75	62.78	1.04	69.4	4.05	66.3	9.19	65.4
CALC	100.00	0.94	100.0	3.83	100.0	8.82	100.0
ASSAY		0.95		3.85		8.82	



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoTail
FROM TEST	T04
DATE	260514
TECHNICIAN	MS

RoTail T04	SIZE um	WEIGHTS			
		gm	(%)	%PASS	
p80	1700	0.00	0.00	100.0	
	1180	8.03	3.07	96.9	
	850	6.82	2.61	94.3	
	600	3.81	1.46	92.9	
	425	3.52	1.35	91.5	
	300	7.19	2.75	88.8	
	185	212	14.23	5.44	83.3
		150	20.08	7.67	75.7
		106	25.16	9.61	66.1
		75	24.55	9.38	56.7
53		23.28	8.90	47.8	
	38	19.25	7.36	40.4	
	SUB	105.76	40.42	0.0	
	TOTAL	261.68	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	ppm	dist	%	dist
600	7.13	1.02	5.4	20.00	7.6	0.24	19.4	9.81	28.5	42.30	7.1	0.20	3.2
212	9.53	0.57	4.0	15.25	7.8	0.06	6.5	3.45	13.4	51.10	11.5	0.26	5.5
150	7.67	0.84	4.7	16.90	6.9	0.09	7.8	2.80	8.8	48.30	8.7	0.39	6.6
106	9.61	1.15	8.1	17.35	8.9	0.08	8.7	2.16	8.5	47.80	10.8	0.46	9.8
75	9.38	1.59	11.0	17.95	9.0	0.06	6.4	1.64	6.3	46.40	10.2	0.52	10.8
<75	56.67	1.60	66.8	19.75	59.8	0.08	51.3	1.50	34.6	38.80	51.7	0.51	64.1
CALC	100.00	1.36	100.0	18.72	100.0	0.09	100.0	2.45	100.0	42.53	100.0	0.45	100.0
ASSAY		1.31		18.30		0.07		2.37		42.80		0.45	

ANALYSES

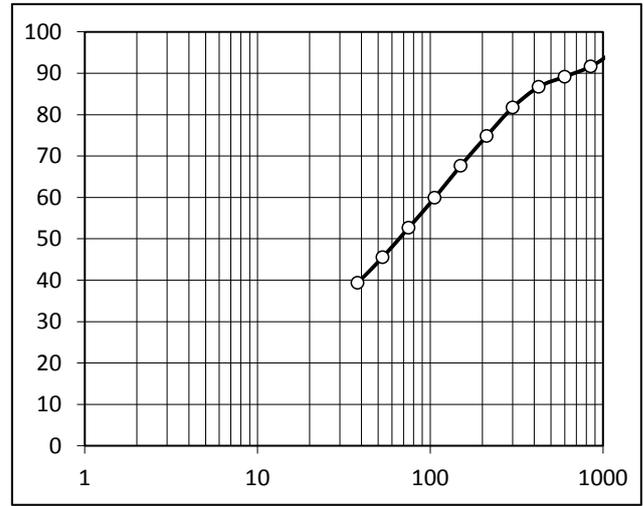
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
600	7.13	0.59	4.5	2.60	4.9	8.46	6.9
212	9.53	0.63	6.4	3.48	8.8	8.70	9.5
150	7.67	0.74	6.0	3.50	7.1	8.03	7.1
106	9.61	0.86	8.8	3.51	9.0	7.76	8.6
75	9.38	0.99	9.9	3.52	8.8	7.34	7.9
<75	56.67	1.07	64.4	4.08	61.4	9.22	60.0
CALC	100.00	0.94	100.0	3.77	100.0	8.71	100.0
ASSAY		0.94		3.73		8.78	



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoTail
FROM TEST	T05
DATE	260514
TECHNICIAN	MS

RoTail T05	SIZE um	WEIGHTS			
		gm	(%)	%PASS	
p80	1700	0.00	0.00	100.0	
	1180	10.66	4.50	95.5	
	850	9.13	3.86	91.6	
	600	5.84	2.47	89.2	
	425	5.82	2.46	86.7	
	300	11.79	4.98	81.7	
	278	212	16.31	6.89	74.8
		150	17.02	7.19	67.7
		106	18.37	7.76	59.9
		75	17.11	7.23	52.7
		53	16.89	7.13	45.5
	38	14.62	6.18	39.4	
	SUB	93.20	39.36	0.0	
	TOTAL	236.76	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO ₂		MnO	
		%	dist	%	dist	%	dist	%	dist	ppm	dist	%	dist
600	10.83	0.98	7.9	20.80	11.7	0.17	19.0	10.40	36.6	40.70	10.5	0.20	4.9
212	14.33	0.71	7.6	17.00	12.7	0.11	16.2	4.20	19.6	48.90	16.7	0.31	10.0
150	7.19	1.00	5.4	17.30	6.5	0.09	6.7	2.77	6.5	48.40	8.3	0.42	6.8
106	7.76	1.31	7.6	17.70	7.1	0.07	5.6	2.25	5.7	47.00	8.7	0.48	8.4
75	7.23	1.75	9.4	18.25	6.9	0.05	3.7	1.86	4.4	45.60	7.8	0.52	8.4
<75	52.67	1.58	62.1	20.10	55.1	0.09	48.8	1.59	27.3	38.30	48.0	0.52	61.6
CALC	100.00	1.34	100.0	19.21	100.0	0.10	100.0	3.07	100.0	42.01	100.0	0.44	100.0
ASSAY		1.32		19.10		0.08		3.21		41.70		0.44	

ANALYSES

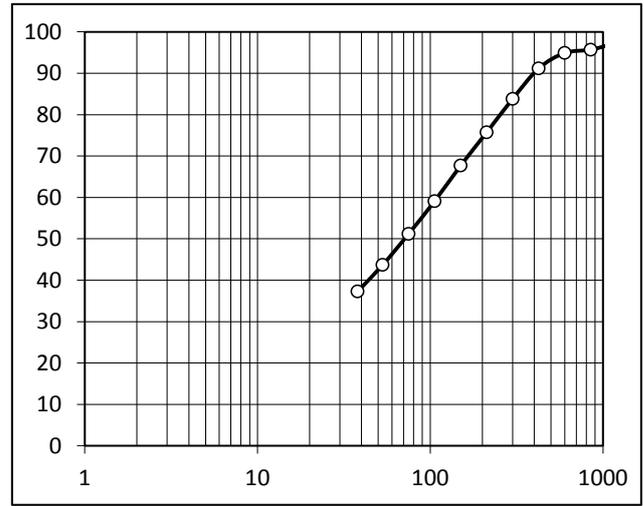
SIZE um	WT %	CaO		MgO		Al ₂ O ₃	
		%	dist	%	dist	%	dist
600	10.83	0.59	6.9	2.67	7.7	7.78	9.8
212	14.33	0.66	10.2	3.47	13.3	8.28	13.9
150	7.19	0.79	6.1	3.55	6.8	7.64	6.4
106	7.76	0.89	7.5	3.45	7.2	7.37	6.7
75	7.23	0.99	7.7	3.39	6.6	6.79	5.7
<75	52.67	1.08	61.5	4.14	58.4	9.34	57.5
CALC	100.00	0.92	100.0	3.73	100.0	8.56	100.0
ASSAY		0.94		3.81		8.53	



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoTail
FROM TEST	T06
DATE	270514
TECHNICIAN	MS

RoTail T06	SIZE um	WEIGHTS			
		gm	(%)	%PASS	
p80	1700	0.00	0.00	100.0	
	1180	7.25	2.64	97.4	
	850	4.54	1.65	95.7	
	600	2.21	0.80	94.9	
	425	10.17	3.70	91.2	
	300	20.20	7.36	83.8	
	258	212	22.31	8.13	75.7
		150	21.98	8.00	67.7
		106	23.60	8.59	59.1
		75	21.71	7.91	51.2
		53	20.68	7.53	43.7
	38	17.47	6.36	37.3	
	SUB	102.46	37.32	0.0	
	TOTAL	274.58	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	ppm	dist	%	dist
600	5.10	0.93	3.6	17.60	4.7	0.19	10.2	7.95	12.9	46.90	5.8	0.18	2.0
212	19.19	0.87	12.8	18.95	18.9	0.17	34.5	6.10	37.3	43.90	20.3	0.35	14.9
150	8.00	1.07	6.6	17.75	7.4	0.08	6.8	3.09	7.9	46.30	8.9	0.44	7.8
106	8.59	1.31	8.7	18.10	8.1	0.07	6.4	2.54	7.0	45.70	9.5	0.48	9.2
75	7.91	1.57	9.6	18.25	7.5	0.05	4.2	2.16	5.4	45.30	8.6	0.52	9.1
<75	51.21	1.49	58.7	20.10	53.5	0.07	37.9	1.80	29.4	38.10	47.0	0.50	56.9
CALC	100.00	1.30	100.0	19.25	100.0	0.09	100.0	3.13	100.0	41.54	100.0	0.45	100.0
ASSAY		1.30		1.00		0.05		3.30		41.40		0.45	

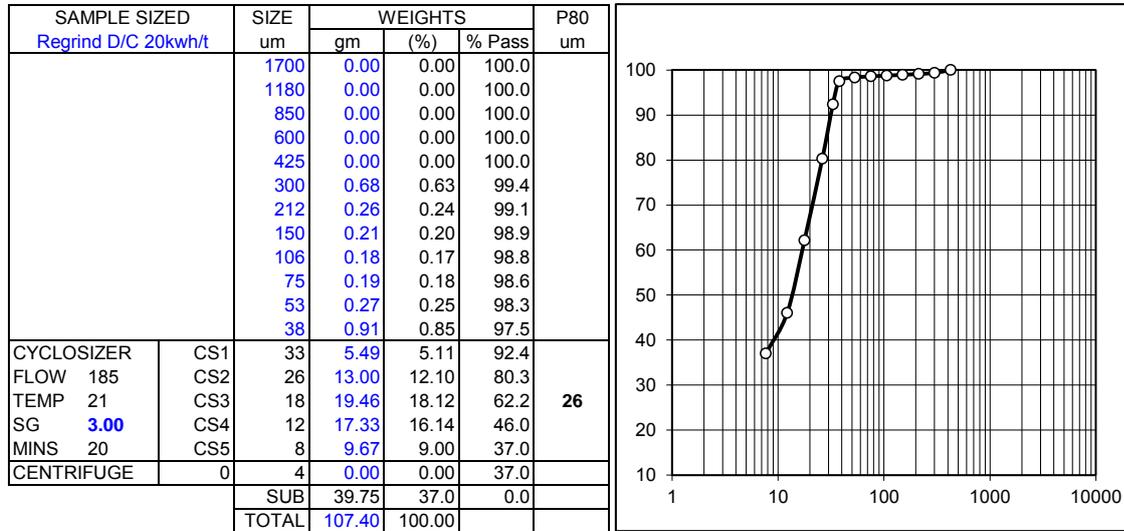
ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
600	5.10	0.66	3.6	2.44	3.4	8.65	5.2
212	19.19	0.70	14.5	3.27	17.1	7.64	17.3
150	8.00	0.87	7.5	3.47	7.6	7.66	7.2
106	8.59	0.94	8.7	3.49	8.2	7.54	7.7
75	7.91	1.02	8.7	3.44	7.4	7.29	6.8
<75	51.21	1.03	56.9	4.05	56.4	9.23	55.8
CALC	100.00	0.93	100.0	3.68	100.0	8.47	100.0
ASSAY		0.93		3.69		8.53	



BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

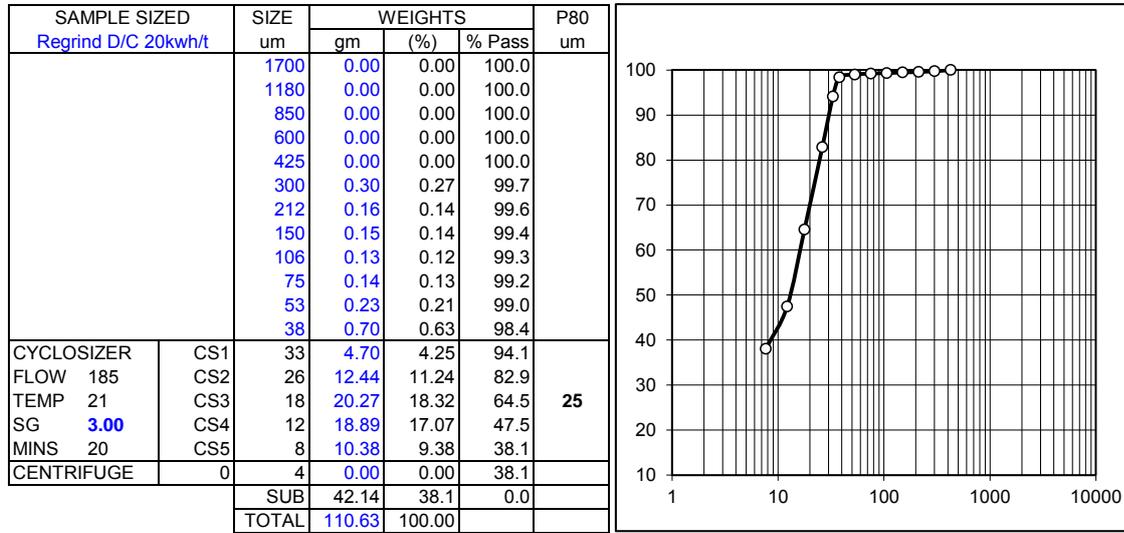
PROJECT	T0879
SAMPLE	Regrind D/C 20kwh/t
TEST NO	T07
DATE	30614
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

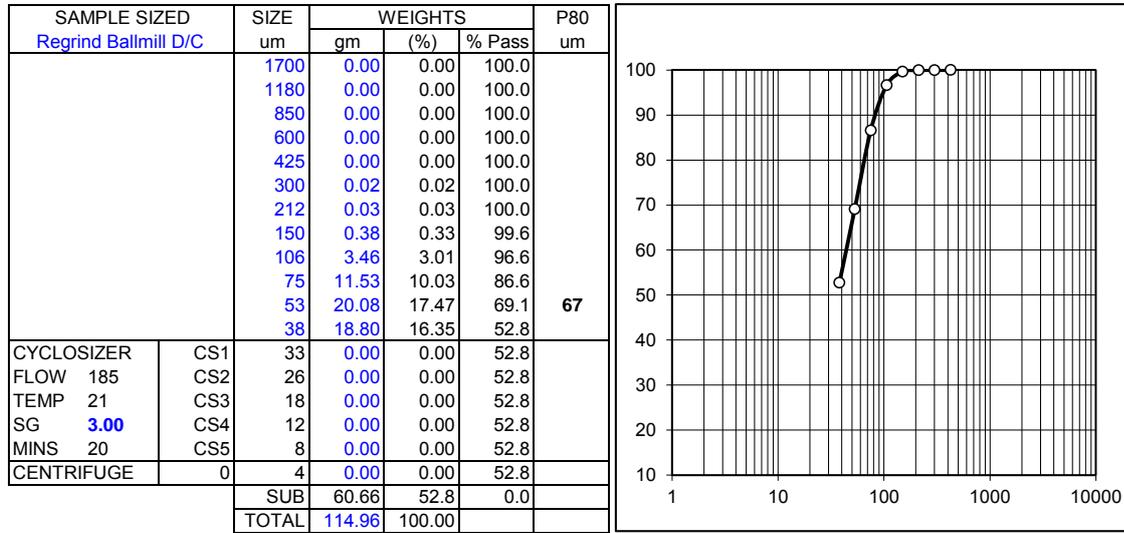
PROJECT	T0879
SAMPLE	Regrind D/C 20kwh/t
TEST NO	T08
DATE	50614
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

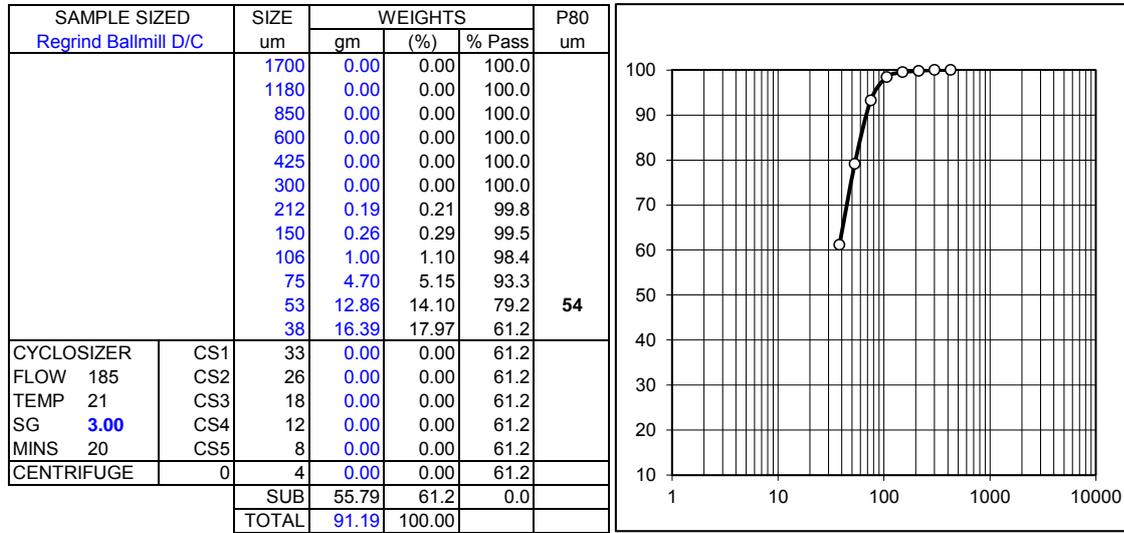
PROJECT	T0879
SAMPLE	Regrind Ballmill D/C
TEST NO	T09
DATE	50614
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

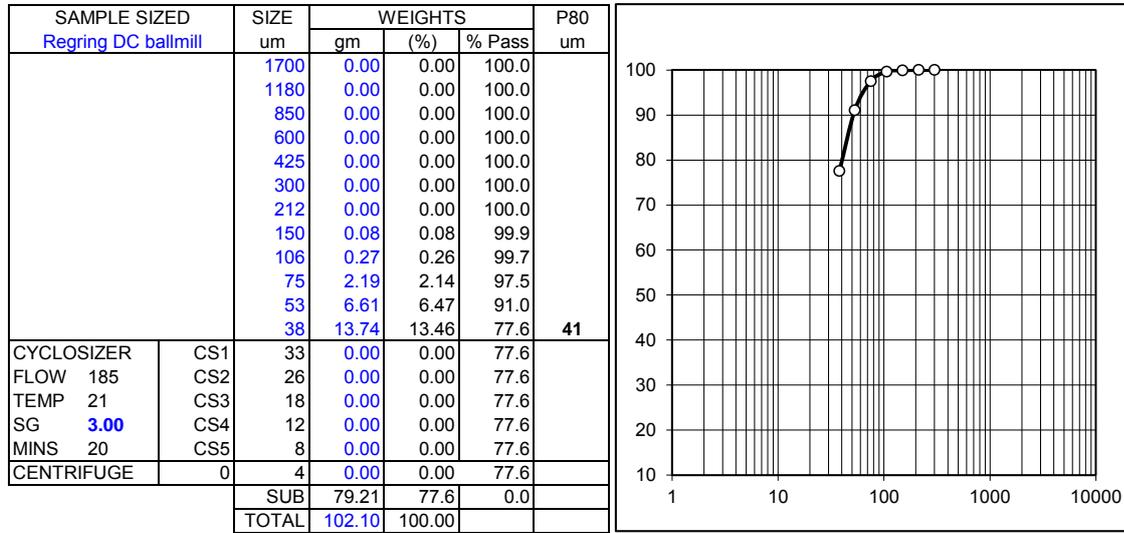
PROJECT	T0879
SAMPLE	Regrind Ballmill D/C
TEST NO	T10
DATE	60614
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

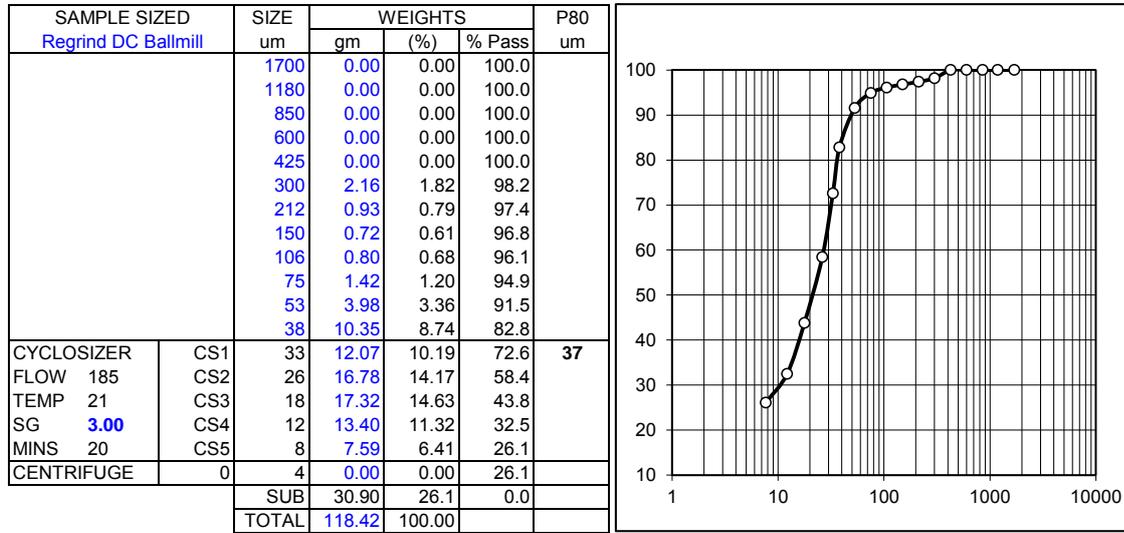
PROJECT	T0879
SAMPLE	Regring DC ballmill
TEST NO	Comb T11
DATE	110614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

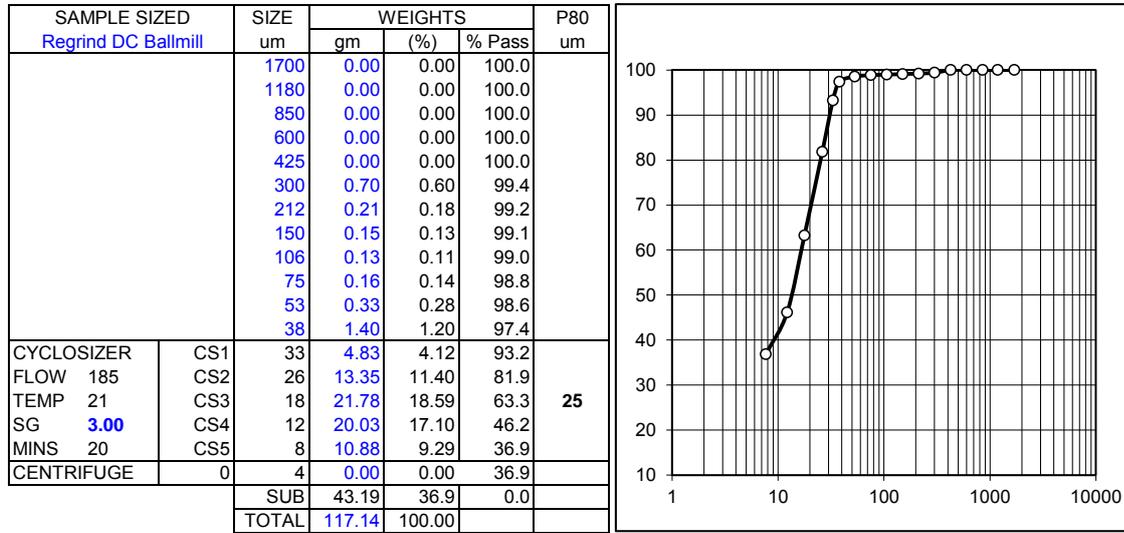
PROJECT	T0879
SAMPLE	Regrind DC Ballmill
TEST NO	T12
DATE	170614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

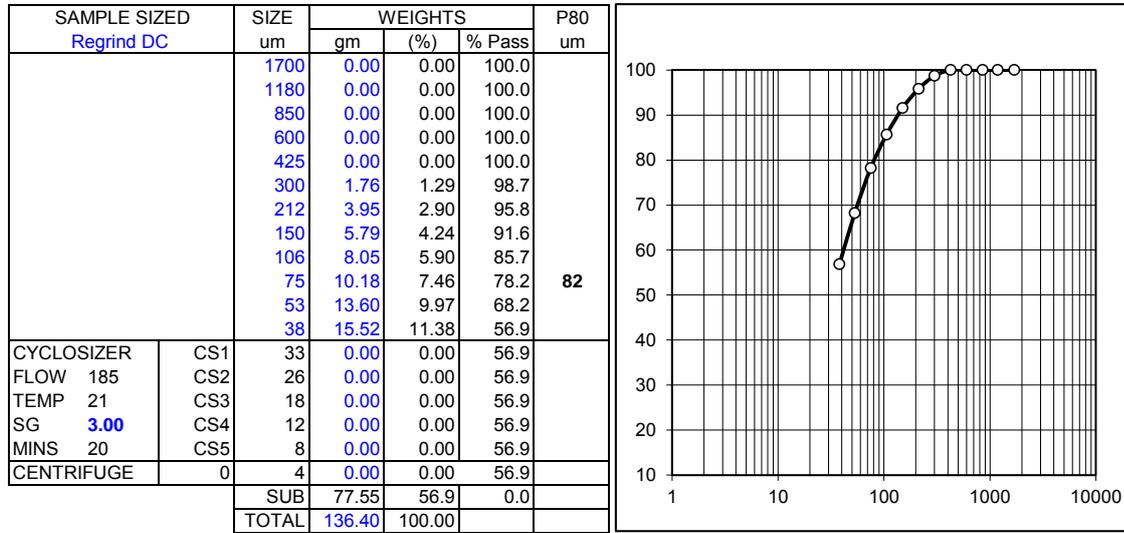
PROJECT	T0879
SAMPLE	Regrind DC Ballmill
TEST NO	T13
DATE	170614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

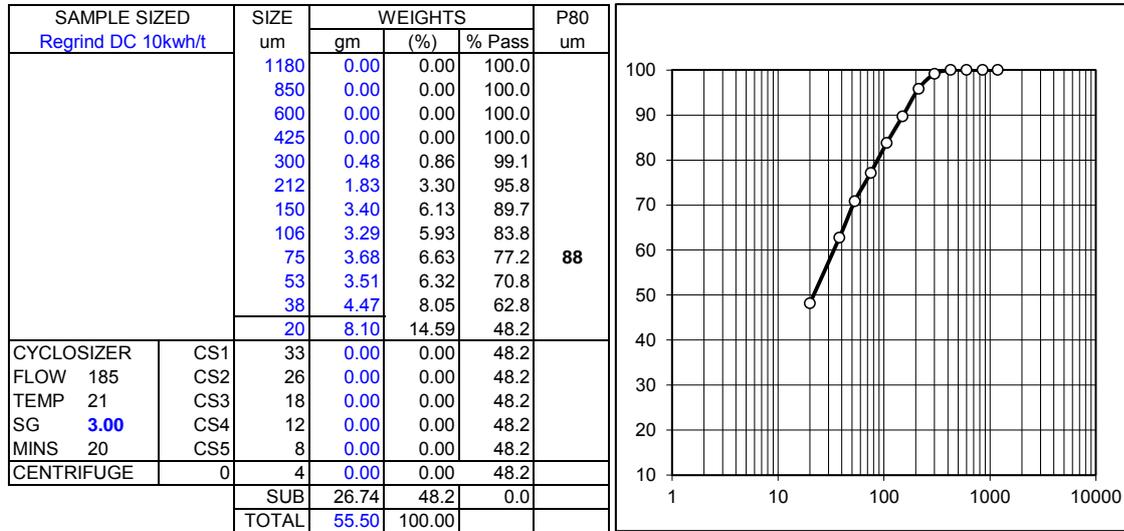
PROJECT	T0879
SAMPLE	Regrind DC
TEST NO	T14-T15
DATE	220614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

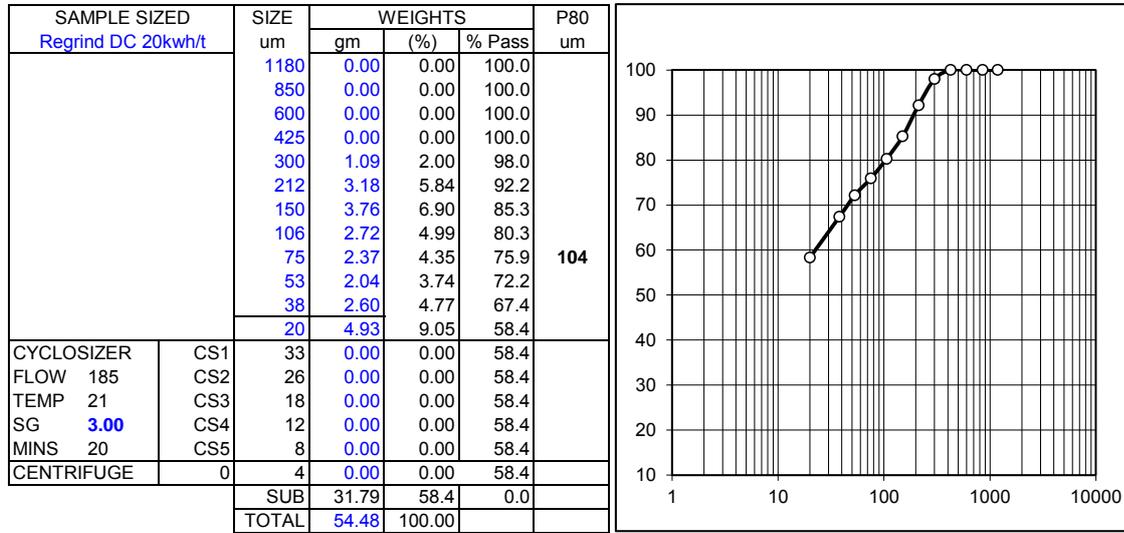
PROJECT	T0879
SAMPLE	Regrind DC 10kwh/t
TEST NO	T16
DATE	220614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

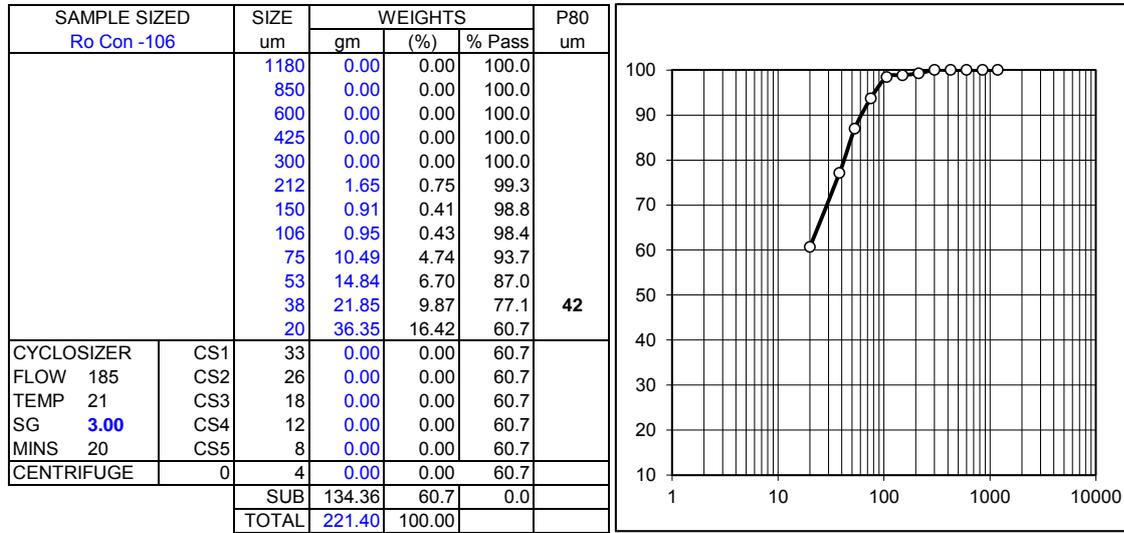
PROJECT	T0879
SAMPLE	Regrind DC 20kwh/t
TEST NO	T16
DATE	250614
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

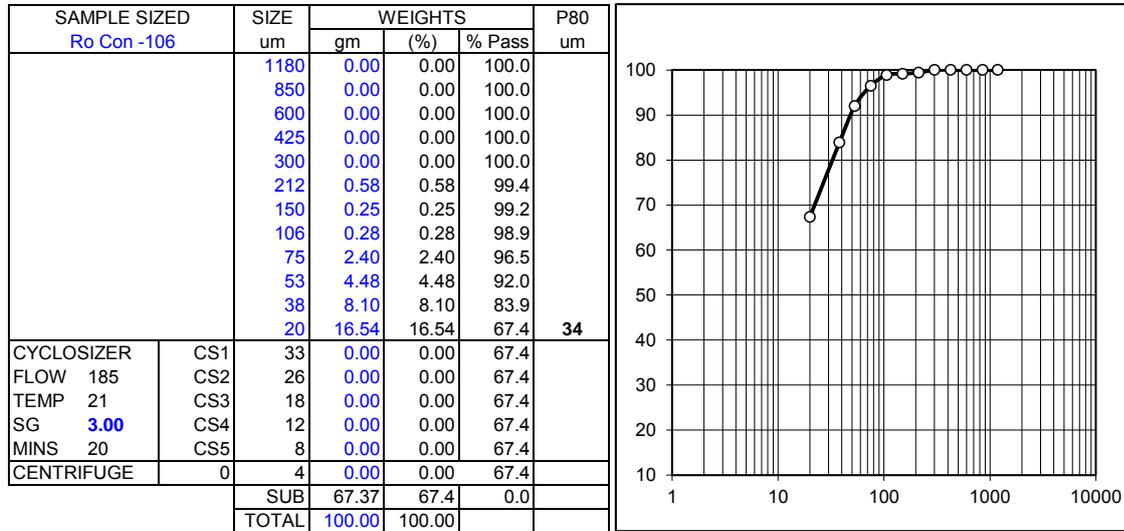
PROJECT	T0879
SAMPLE	Ro Con -106
TEST NO	T16
DATE	260614
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Ro Con -106
TEST NO	T18
DATE	260614
TECHNICIAN	DK





WorleyParsons

resources & energy

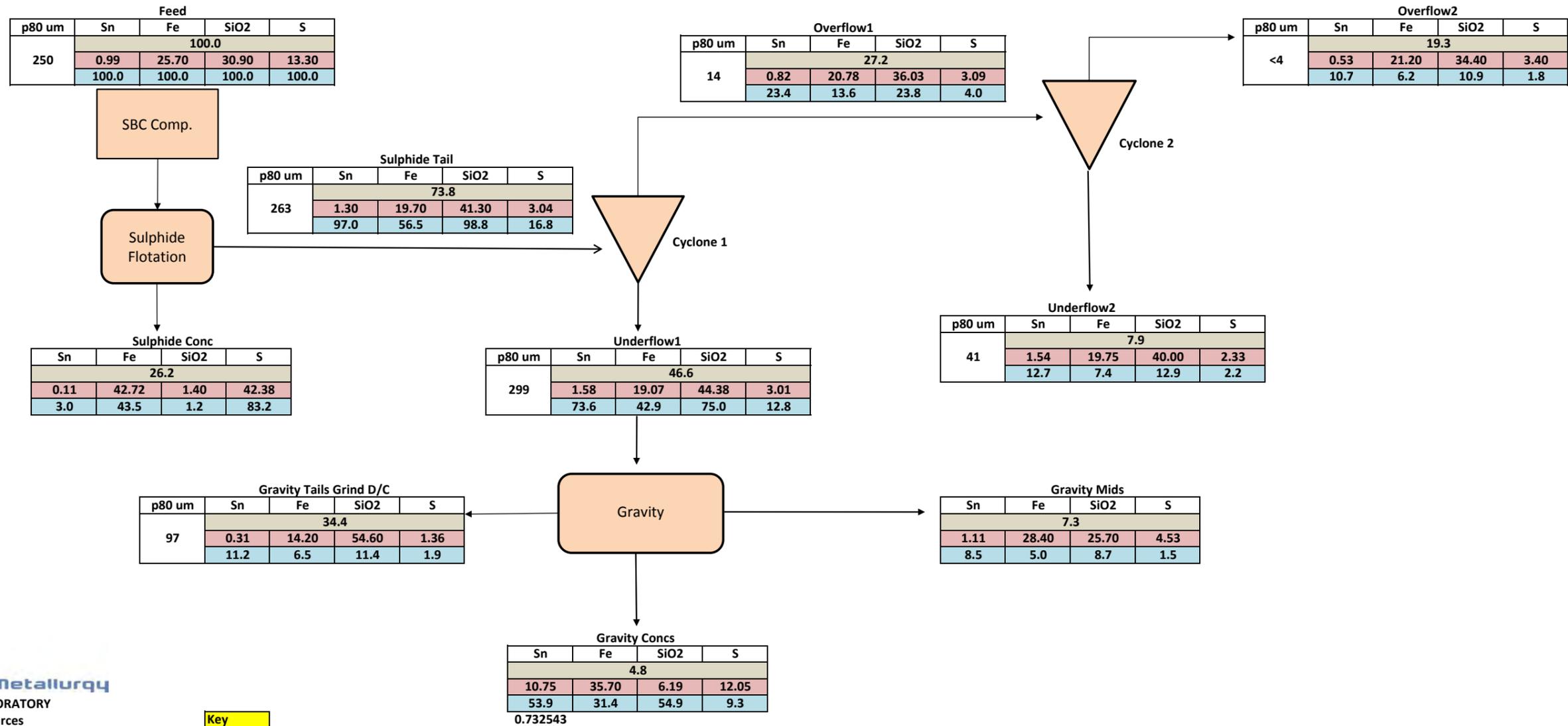
EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 7 – Gravity Separation Results



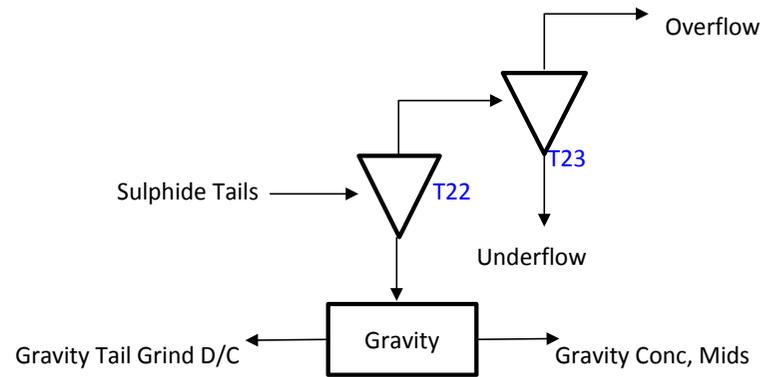
BURNIE LABORATORY
 Stellar Resources
 T0879 SBC ORE MASS BALANCE
 ALS Metallurgy Burnie 0714
 Sulphide Flotation: T16,17
 Cyclone and Gravity:T22,23,24

Key
% Mass
%Sn
Sn Dist



BURNIE LABORATORY: SEPARATION REPORT SHEET

TEST TYPE	Cyclone & Gravity Separation
Stage 1	Cyclone T22
Stage 2	Cyclone T23
Stage 3	Mozley Separation T24



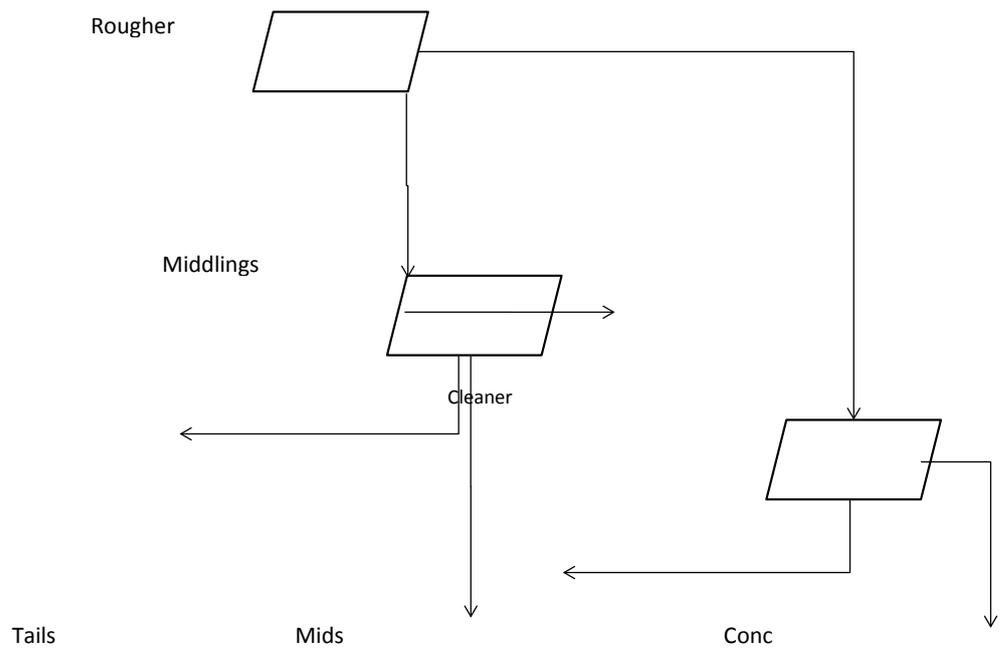
PROJECT	T0879
TEST NO	T22, T23, T24
DATE	21/07/14
TECH	MS

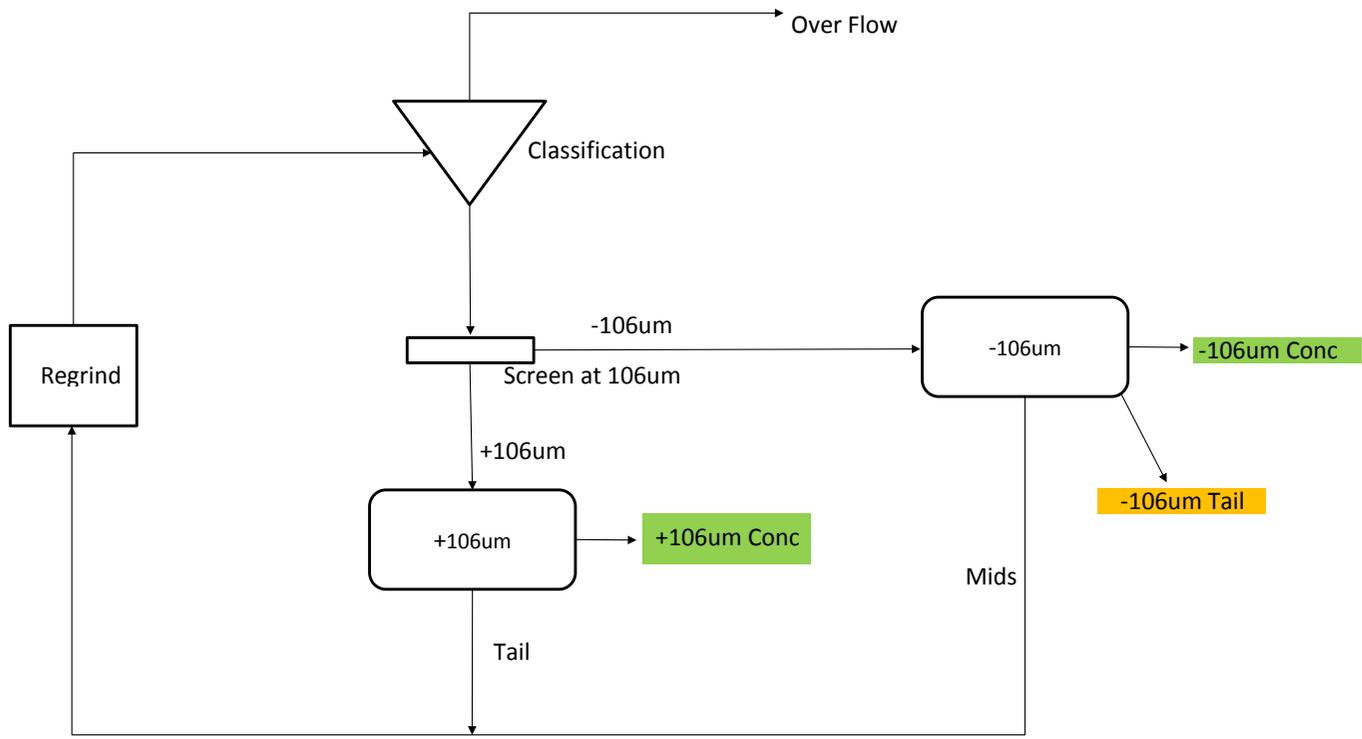
START MATERIAL	
SBC - SRT (T22 cyclone) Feed	
FROM TEST NO	
START WEIGHT (gm)	1852.45

SEPARATION RESULTS

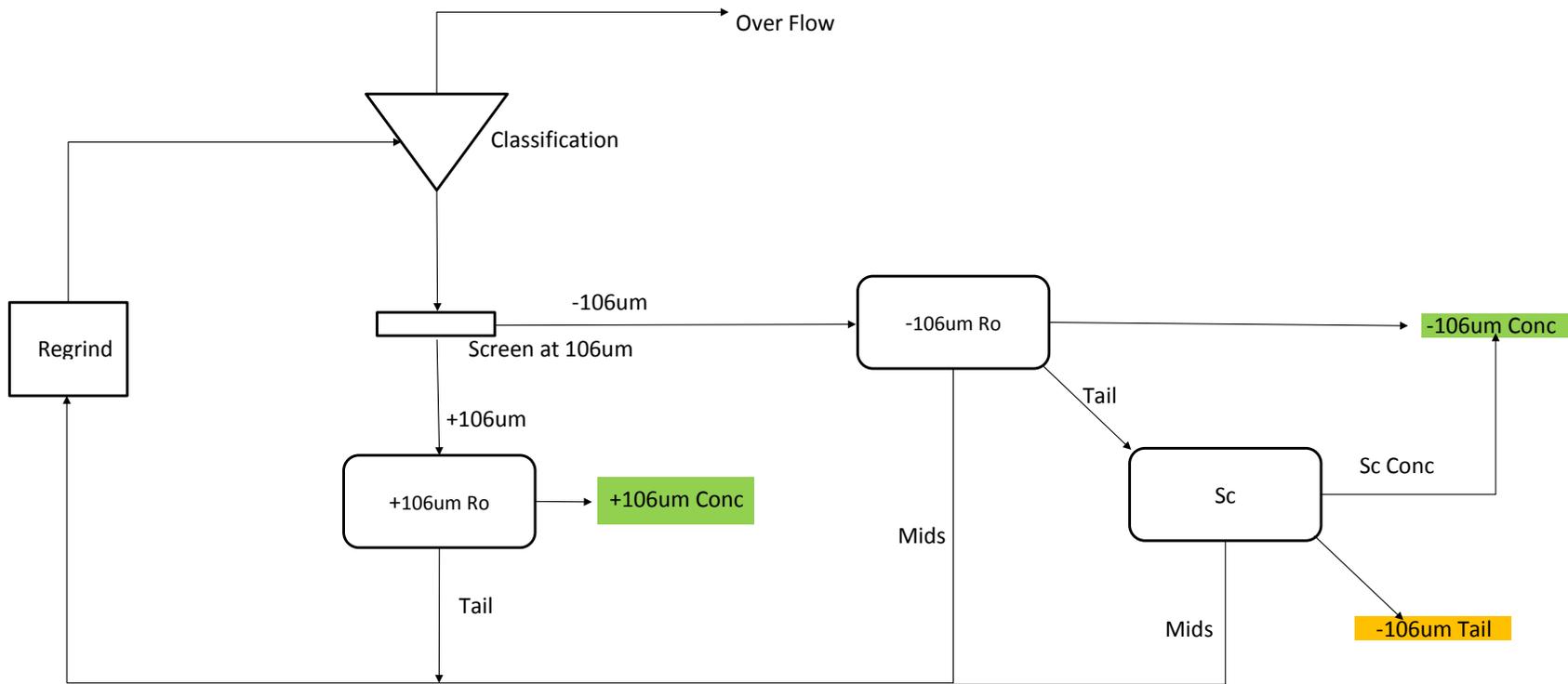
Product	Weight (gm)	P80 (Sizing)	Weight (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	As (%)	Dist (%)	S (%)	Dist (%)	SiO2 (%)	Dist (%)	MnO (%)	Dist (%)
T23 Overflow	484.30	<8	26.14	0.53	11.0	21.20	28.5	0.21	38.8	3.40	29.6	34.40	21.6	0.44	20.8
Underflow	198.80	41	10.73	1.54	13.1	19.75	10.9	0.20	15.2	2.33	8.3	40.00	10.3	0.65	12.6
T24 Gravity Conc	120.39		6.50	10.75	55.6	35.70	11.9	0.52	23.9	12.05	26.0	6.19	1.0	1.07	12.6
Gravity Mids	184.36		9.95	1.11	8.8	28.40	14.5	0.08	5.6	4.53	15.0	25.70	6.1	1.12	20.2
Gravity Tail Grind D/C	864.60	97	46.67	0.31	11.5	14.20	34.1	0.05	16.5	1.36	21.1	54.60	61.1	0.40	33.8
Total	1852.45		100.00	1.26	100.0	19.44	100.0	0.14	100.0	3.01	100.0	41.73	100.0	0.55	100.0

Product	Weight (gm)	P80 (Sizing)	Weight (%)	CaO (%)	Dist (%)	MgO (%)	Dist (%)	Al2O3 (%)	Dist (%)	Sample No
T23 Overflow	484.30	>8	26.14	0.52	15.8	4.35	31.4	11.90	36.4	879201
Underflow	198.80	41	10.73	1.13	14.0	3.33	9.9	6.64	8.3	879202
T24 Gravity Conc	120.39		6.50	0.69	5.2	2.02	3.6	2.17	1.6	879203
Gravity Mids	184.36		9.95	1.37	15.8	3.60	9.9	6.33	7.4	879204
Gravity Tail Grind D/C	864.60	97	46.67	0.91	49.2	3.52	45.3	8.49	46.3	879205
Total	1852.45		100.00	0.86	100.0	3.63	100.0	8.56	100.0	

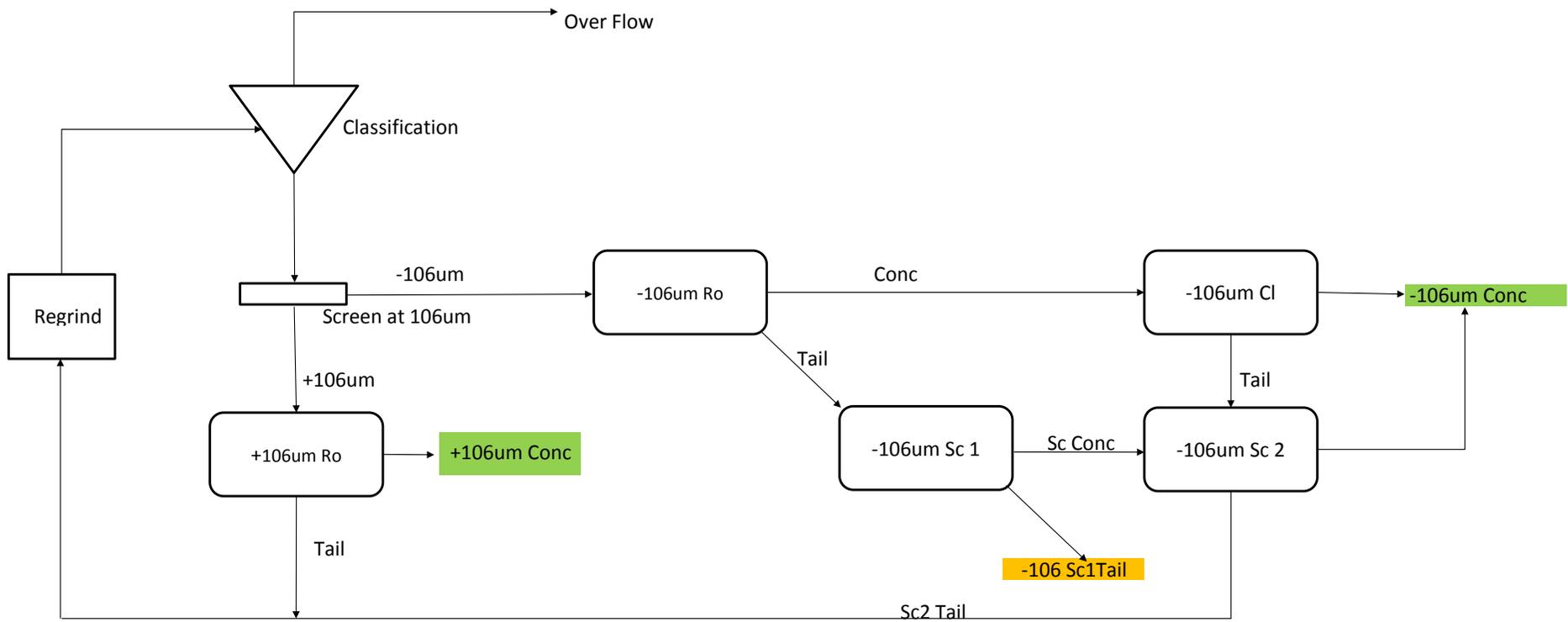




T0879 LC01 C1-4



T0879 LC01 C05



T0879 LC01 C06

PROJECT	T0879
TEST NO	LC01
FEED	SULPHIDE TAILS
FROM TEST	
DATE	50814
TECH	ID

EXIT STREAMS		1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	AVERAGE		
CYCLE NO																																			
Gravity final conc 1 (+106 Conc)	gm	35.54	40.57	43.98	45.58	44.50	46.95	49.10	53.20	48.70	58.10	52.10	54.90	54.40	54.70	52.70	53.60	58.40	53.10	56.70	55.90	54.30	55.20	51.50	53.90	54.40	54.10	56.70	51.40	51.70	52.40	56.70	57.00		
dry wt and assays	%Sn	9.49	9.19	8.14	9.01	8.92	9.90	9.16	8.80	8.31	8.00	9.04	9.68	9.68	9.68	9.68	9.10	9.10	9.10	9.06	9.21	9.21	9.21	19.80	19.80	19.80	9.15	9.15	10.45	10.45	10.45	10.45	11.34		
	%Fe	37.50	38.10	38.60	37.60	37.80	39.50	34.30	38.10	37.90	38.40	38.00	36.60	36.60	36.60	37.40	37.40	37.40	36.60	37.10	37.10	37.10	37.10	35.20	35.20	35.20	36.60	36.60	43.70	43.70	43.70	43.70	37.91		
	%S	11.10	11.75	11.40	11.55	13.15	9.61	11.75	10.80	9.33	9.97	9.61	11.40	11.40	11.40	11.40	11.10	11.10	11.10	9.62	10.80	10.80	10.80	18.25	18.25	18.25	11.45	11.45	12.90	12.90	12.90	12.90	12.70		
	%SiO2	6.23	6.10	6.10	6.21	6.23	5.27	6.86	5.26	6.57	6.31	5.83	6.21	6.21	6.21	6.21	6.21	6.38	6.38	6.38	7.78	6.61	6.61	6.61	2.24	2.24	2.24	7.05	7.05	7.05	7.47	7.47	6.06		
Gravity final conc 2 (-106 Conc)	gm	24.79	26.80	35.20	44.30	41.26	43.37	58.80	46.40	70.80	65.80	46.50	52.90	62.10	66.70	64.90	61.90	61.50	63.80	63.00	64.30	59.10	58.40	55.50	54.90	60.40	60.10	59.40	59.80	57.10	65.70	63.30	968.20		
dry wt and assays	%Sn	26.50	30.30	30.40	26.50	30.00	28.6	18.65	24.10	19.20	19.20	22.20	25.60	25.60	25.60	20.70	20.70	20.70	22.90	22.90	21.20	22.90	19.80	19.80	19.80	20.90	20.90	23.50	23.50	23.50	23.50	21.57			
	%Fe	31.70	29.20	29.00	31.70	29.10	29.0	37.7	34.40	35.20	36.50	27.60	29.20	29.20	29.20	33.00	33.00	33.00	31.70	31.70	34.50	35.20	35.20	35.20	35.70	35.70	44.90	44.90	44.90	44.90	36.02				
	%S	14.70	15.95	17.30	20.20	19.35	18.5	19.2	10.80	16.30	12.55	11.75	17.60	17.60	17.60	17.60	17.60	17.60	16.30	16.30	19.85	18.25	18.25	18.25	18.60	18.60	17.60	17.60	17.60	17.60	17.79				
	%SiO2	2.50	2.12	1.85	1.83	1.86	1.86	1.87	1.97	2.30	2.26	3.18	2.15	2.15	2.15	2.99	2.99	2.99	2.99	2.99	2.59	2.59	2.59	2.04	2.24	2.24	7.05	7.05	7.05	7.47	7.47	2.51			
Gravity Final Tail (-106 Tails)	gm	364.80	522.30	953.69	1018.90	1021.80	1231.30	877.60	956.50	1120.10	967.70	863.50	1086.80	1022.70	1013.50	1029.30	1039.20	883.30	1068.10	1081.30	1058.10	1067.20	1028.40	1070.30	984.70	1023.40	955.00	1039.10	1064.40	1053.40	1096.00	998.30	16510.20		
dry wt and assays	%Sn	0.30	0.42	0.44	0.47	0.38	0.41	0.42	0.44	0.32	0.34	0.38	0.36	0.33	0.38	0.38	0.41	0.41	0.41	0.39	0.39	0.39	0.39	0.40	0.40	0.37	0.37	0.37	0.37	0.39	0.39	0.39	0.39		
	%Fe	13.60	16.75	18.15	18.25	16.95	16.3	18.75	16.90	15.30	16.25	16.60	16.75	17.20	17.00	16.80	17.45	17.45	17.45	17.20	17.20	17.20	17.20	17.15	17.15	17.15	17.10	17.10	16.55	16.55	16.55	17.12			
	%S	1.08	1.41	1.78	1.28	1.79	1.76	1.64	1.72	1.14	1.50	1.10	1.63	1.56	1.65	1.58	1.69	1.69	1.69	1.52	1.52	1.52	1.69	1.62	1.62	1.64	1.64	1.56	1.56	1.56	1.56	1.61			
	%SiO2	55.40	50.20	46.00	47.30	48.50	48.3	45.7	49.00	52.80	48.30	50.50	48.70	48.30	47.50	48.60	48.20	48.20	48.20	48.30	48.30	48.30	48.30	47.10	47.90	47.90	47.70	47.70	47.70	47.70	48.90	48.90	48.14		
Over Flow	gm	739.1	1109.8	885.4	802.0	874.0	707.7	1283.6	846.2	912.0	904.8	989.9	871.8	920.9	943.6	929.1	791.7	1045.9	711.1	793.2	827.0	818.0	848.6	843.4	929.7	925.0	954.4	894.5	935.6	871.3	812.0	753.8	13755.24		
dry wt and assays	%Sn	0.65	0.65	0.65	0.65	0.65	0.65	0.53	0.53	0.53	0.53	0.53	0.53	0.53	0.53	0.53	0.53	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47			
	%Fe	19.35	19.35	19.35	19.35	19.35	20.34	20.34	20.34	20.34	20.34	20.34	20.34	20.34	20.34	20.34	20.34	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.70	20.68		
	%S	2.96	2.96	2.96	2.96	2.96	3.16	3.16	3.16	3.16	3.16	3.16	3.16	3.16	3.16	3.16	3.16	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14	3.14			
	%SiO2	39.70	39.70	39.70	39.70	39.70	37.44	37.44	37.44	37.44	37.44	37.44	37.44	37.44	37.44	37.44	37.44	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40	37.40			
Combined Concentrate	gm	60.33	67.37	79.18	89.78	85.76	90.32	107.90	99.60	119.50	123.90	98.60	107.80	116.50	121.40	117.60	115.50	119.90	116.90	119.70	120.20	113.40	113.60	107.00	108.80	114.80	114.20	116.10	111.20	108.80	118.10	120.00	1838.20		
dry wt and assays	%Sn	16.48	17.59	18.04	17.63	19.06	18.88	14.33	15.93	14.76	13.95	15.25	17.49	18.17	18.43	18.47	15.32	15.05	15.43	16.34	16.53	16.34	15.37	19.80	19.80	19.80	15.33	15.16	15.47	17.30	17.71	17.33			
	%Fe	35.12	34.56	34.33	34.69	33.61	34.46	36.15	36.38	36.30	37.39	33.10	32.97	32.66	32.53	32.52	35.04	35.14	35.00	34.02	34.21	34.29	35.76	35.20	35.20	36.13	36.14	36.12	44.33	44.37	44.33	36.91			
	%S	12.58	13.42	14.02	15.81	16.13	13.88	15.81	10.80	13.46	11.34	10.62	14.44	14.70	14.81	14.82	14.58	14.43	14.65	13.14	13.74	13.67	15.45	18.25	18.25	18.25	15.21	15.11	15.30	15.37	15.51	15.38			
	%SiO2	4.70	4.52	4.21	4.05	4.13	3.63	4.14	3.73	4.04	4.16	4.58	4.22	4.05	3.98	3.97	4.56	4.64	4.53	5.05	4.46	4.51	4.26	2.24	2.24	2.24	4.68	4.74	4.62	4.77	4.61	4.75			

REGIND DATA		2003	2005	2005	2007	2010	2010	2010	2010	2010	2010	2001	2001	2007	2003	2006	2001	2003	2006	2008	2008	2003	2015	2006	2008	2008	2001	2008	2007	2008	2003	2007
New Feed (gm) (dry)		2003	2005	2005	2007	2010	2010	2010	2010	2010	2010	2001	2001	2007	2003	2006	2001	2003	2006	2008	2008	2003	2015	2006	2008	2008	2001	2008	2007	2008	2003	2007
Regrind feed Damp Wt (gm)		0.0	736.2	927	1099	1249	1314	1475	1178	1344	1237	1346	1371	1298	1268	1246	1290	1310	1172	1334	1294	1281	1251	1280	1277	1302	1225	1258	1301	1278	1284	1296
Regrind Time (min per 100gm)		3.0	3.0	2.8	3.0	3.0	3.0	3.0	3.3	3.5	3.5	3.5	4.0	4.0	4.0	4.0	4.0	4.0	4.0	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	
Regrind Time (min.sec)		0.0	22.1	26.0	33.0	37.5	39.4	44.3	38.9	46.4	42.7	47.3	51.9	50.7	49.8	51.6	52.4	46.9	53.4	53.7	53.2	51.9	53.1	53.0	54.0	50.8	52.2	54.0	53.0	53.3	53.8	
Regrind D/C underflow (%Wt)																																

DISTRIBUTIONS	AV 16-31	FROM NEW FEED (%)																															
		Cyc 1	Cyc 2	Cyc 3	Cyc 4	Cyc 5	Cyc 6	Cyc 7	Cyc 8	Cyc 9	Cyc 10	Cyc 11	Cyc 12	Cyc 13	Cyc 14	Cyc 15	Cyc 16	Cyc 17	Cyc 18	Cyc 19	Cyc 20	Cyc 21	Cyc 22	Cyc 23	Cyc 24	Cyc 25	Cyc 26	Cyc 27	Cyc 28	Cyc 29	Cyc 30	Cyc 31	
MASS	+106 Conc	2.70	1.76	2.01	2.18	2.26	2.21	2.33	2.44	2.64	2.42	2.88	2.59	2.72	2.70	2.71	2.61	2.66	2.90	2.63	2.81	2.77	2.69	2.74	2.56	2.67	2.70	2.68	2.81	2.55	2.57	2.60	2.81
	-106 Conc	3.00	1.23	1.33	1.75	2.20	2.05	2.15	2.92	2.30	3.51	3.26	2.31	2.62	3.08	3.31	3.22	3.07	3.05	3.17	3.13	3.19	2.93	2.90	2.75	2.72	3.00	2.98	2.95	2.97	2.83	3.26	
	-106 Tail	51.20	18.10	25.92	47.32	50.56	50.70	61.10	43.55	47.46	55.58	48.02	42.85	53.93	50.75	51.07	51.56	43.83	53.00	53.65	52.50	52.95	51.03	53.11	48.86	50.78	47.39	51.56	52.81	52.27	54.38	49.53	
	Over Flow	42.66	36.67	55.07	43.93	39.79	43.37	35.12	63.69	41.99	45.25	44.90	49.12	43.26	45.69	46.82	46.10	39.28	51.90	35.28	39.36	41.03	40.59	42.11	41.85	46.13	45.90	47.36	44.38	46.42	43.23	40.29	
	Calc Recycle	0.44	42.23	15.68	4.82	5.19	1.68	-0.69	-12.59	5.61	-6.76	0.94	3.14	-2																			

SBC LC01	Coarse Gravity Conc		Fine Gravity Conc		Gravity Fine Tail		Over Flow		Feed		Combined Conc	
%Wt		2.79		3.11		52.05		42.04		100.0		5.90
%Sn	9.14	19.0	21.72	50.5	0.40	15.5	0.48	15.0	1.34	100.0	15.77	69.5
%Fe	37.16	5.2	32.64	5.1	17.37	45.7	20.65	43.9	19.78	100.0	34.78	10.4
%S	10.76	10.0	17.34	18.0	1.61	28.0	3.14	44.0	3.00	100.0	14.23	28.0
%SiO2	6.68	0.5	2.69	0.2	48.09	61.0	37.41	38.3	41.03	100.0	4.57	0.7

C16-22

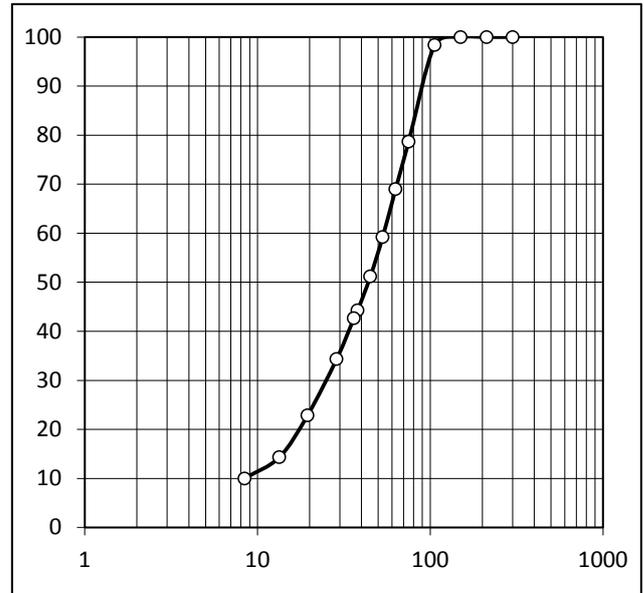
MASS	+106 Conc	2.81	2.79	Gravity final conc 1	gm	387.2
	-106 Conc	3.13	3.11	(+106 Conc)	%Sn	9.14
	-106 Tail	52.36	52.05	dry wt and assays	%Fe	37.16
	Over Flow	42.29	42.04		%S	10.76
	Calc Recycle	-0.59			%SiO2	6.68
TIN	+106 Conc	19.29		Gravity final conc 2	gm	432.00
	-106 Conc	51.14		(-106 Conc)	%Sn	21.72
	-106 Tail	15.69		dry wt and assays	%Fe	32.64
	Over Flow	15.21			%S	17.34
	Calc Recycle	-1.33			%SiO2	2.69
TIN REC OA (%)		70.43		Gravity Final Tail	gm	7225.60
TIN REC GRAVITY (%)		81.77		(-106 Tails)	%Sn	0.40
IRON	+106 Conc	5.26		dry wt and assays	%Fe	17.37
	-106 Conc	5.16			%S	1.61
	-106 Tail	45.90			%SiO2	48.09
	Over Flow	44.06		Over Flow	gm	5835.50
	Calc Recycle	-0.39			%Sn	0.48
SULPHUR	+106 Conc	10.12		dry wt and assays	%Fe	20.65
	-106 Conc	18.20			%S	3.14
	-106 Tail	28.34			%SiO2	37.41
	Over Flow	44.55				
	Calc Recycle	-1.21				
SILICA	+106 Conc	0.44				
	-106 Conc	0.20				
	-106 Tail	59.69				
	Over Flow	37.50				
	Calc Recycle	2.16				
	Calc Recycle	0.61				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc6 -106
	Mozley Tail
DATE	110814
TECHNICIAN	MS

LC01 Cyc6 -106 Mozley Tail		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	77	850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	0.02	0.02	100.0
		106	1.91	1.62	98.4
		75	23.19	19.68	78.7
		63	11.41	9.68	69.0
		53	11.55	9.80	59.2
		45	9.45	8.02	51.2
		38	8.16	6.92	44.3
CYCLOSIZER	CS1	36	1.88	1.60	42.7
FLOW 185	CS2	29	9.79	8.31	34.4
TEMP 21	CS3	19	13.56	11.51	22.9
SG 2.60	CS4	13	10.06	8.54	14.3
MINS 20	CS5	8	5.09	4.32	10.0
	SUB		11.78	10.00	0.0
	TOTAL		117.85	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	21.32	0.23	11.1	12.05	15.7	0.06	13.5	0.77	9.8	57.40	24.8	0.26	13.6
63	9.68	0.22	4.8	12.55	7.4	0.05	5.1	0.90	5.2	57.20	11.2	0.29	6.9
53	9.80	0.22	4.9	12.70	7.6	0.06	6.2	0.91	5.3	57.50	11.4	0.31	7.5
45	8.02	0.22	4.0	13.75	6.7	0.06	5.1	1.06	5.1	55.90	9.1	0.35	6.9
38	6.92	0.20	3.1	14.45	6.1	0.05	3.6	1.04	4.3	53.80	7.5	0.40	6.8
26	9.90	0.49	10.9	23.90	14.5	0.08	8.3	2.48	14.7	35.90	7.2	0.71	17.3
12	20.04	0.77	34.8	19.50	23.9	0.14	29.5	2.42	29.1	42.60	17.3	0.50	24.6
<12	14.31	0.82	26.5	20.70	18.1	0.19	28.6	3.08	26.4	39.70	11.5	0.47	16.5
CALC	100.00	0.44	100.0	16.37	100.0	0.09	100.0	1.67	100.0	49.39	100.0	0.41	100.0
ASSAY		0.41		16.45		0.10		1.68		49.70		0.40	

ANALYSES

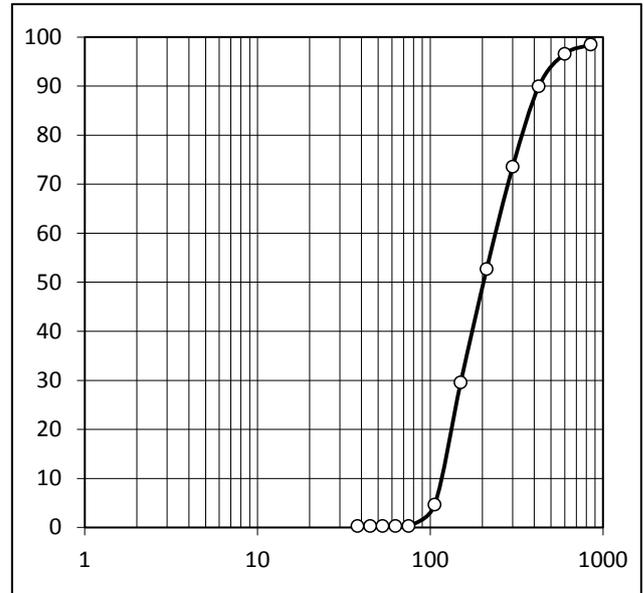
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
75	21.32	0.92	19.3	3.62	22.0	8.82	23.8				
63	9.68	0.93	8.9	3.47	9.6	8.46	10.4				
53	9.80	0.92	8.9	3.38	9.5	8.29	10.3				
45	8.02	1.01	8.0	3.47	7.9	8.13	8.3				
38	6.92	1.07	7.3	3.48	6.9	7.98	7.0				
26	9.90	1.25	12.2	3.28	9.3	6.85	8.6				
12	20.04	1.06	20.9	3.42	19.6	7.05	17.9				
<12	14.31	1.04	14.6	3.75	15.3	7.59	13.8				
CALC	100.00	1.02	100.0	3.51	100.0	7.89	100.0				
ASSAY		0.99		3.65		8.21					



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc6 +106
	Mozley Tail
DATE	190814
TECHNICIAN	MS

LC01 Cyc6 +106 Mozley Tail		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	349	850	1.90	1.53	98.5
		600	2.37	1.90	96.6
		425	8.26	6.63	89.9
		300	20.42	16.39	73.5
		212	26.00	20.87	52.7
		150	28.79	23.11	29.6
		106	31.04	24.92	4.6
		75	5.40	4.34	0.3
		63	0.00	0.00	0.3
	53	0.00	0.00	0.3	
	45	0.00	0.00	0.3	
	38	0.00	0.00	0.3	
CYCLOSIZER	CS1	36	0.00	0.00	0.3
FLOW	185	CS2	29	0.00	0.3
TEMP	21	CS3	19	0.00	0.3
SG	2.60	CS4	13	0.00	0.3
MINS	20	CS5	8	0.00	0.3
		SUB	0.38	0.31	0.0
		TOTAL	124.56	98.47	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist										
425	10.06	1.00	10.1	2.00	10.1	3.00	10.1	4.00	10.1	5.00	10.1	6.00	10.1
300	16.39	1.00	16.4	2.00	16.4	3.00	16.4	4.00	16.4	5.00	16.4	6.00	16.4
212	20.87	1.00	20.9	2.00	20.9	3.00	20.9	4.00	20.9	5.00	20.9	6.00	20.9
150	23.11	1.00	23.1	2.00	23.1	3.00	23.1	4.00	23.1	5.00	23.1	6.00	23.1
106	24.92	1.00	24.9	2.00	24.9	3.00	24.9	4.00	24.9	5.00	24.9	6.00	24.9
<106	4.64	1.00	4.6	2.00	4.6	3.00	4.6	4.00	4.6	5.00	4.6	6.00	4.6
CALC	100.00	1.00	100.0	2.00	100.0	3.00	100.0	4.00	100.0	5.00	100.0	6.00	100.0
ASSAY		1.00		2.00		3.00		4.00		5.00		6.00	

ANALYSES

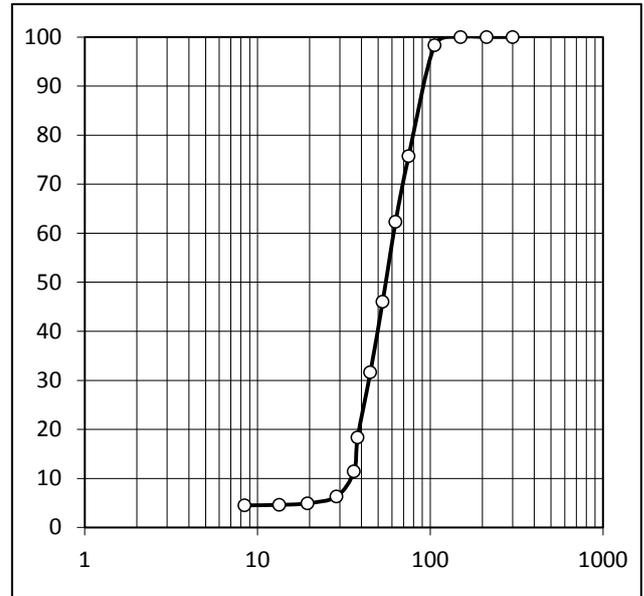
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
425	10.06	1.00	10.1	2.00	10.1	3.00	10.1				
300	16.39	1.00	16.4	2.00	16.4	3.00	16.4				
212	20.87	1.00	20.9	2.00	20.9	3.00	20.9				
150	23.11	1.00	23.1	2.00	23.1	3.00	23.1				
106	24.92	1.00	24.9	2.00	24.9	3.00	24.9				
<106	4.64	1.00	4.6	2.00	4.6	3.00	4.6				
CALC	100.00	1.00	100.0	2.00	100.0	3.00	100.0				
ASSAY		1.00		2.00		3.00					



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc6 -106
	Mozley Mids
DATE	110814
TECHNICIAN	MS

LC01 Cyc6 -106 Mozley Mids		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	81	850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	0.03	0.03	100.0
		106	1.70	1.67	98.3
		75	23.04	22.59	75.7
		63	13.65	13.38	62.3
		53	16.63	16.30	46.0
45	14.68	14.39	31.6		
38	13.54	13.27	18.4		
CYCLOSIZER	CS1	36	7.09	6.95	11.4
FLOW 185	CS2	29	5.19	5.09	6.3
TEMP 21	CS3	19	1.42	1.39	4.9
SG 2.60	CS4	13	0.33	0.32	4.6
MINS 20	CS5	8	0.10	0.10	4.5
	SUB		4.60	4.51	0.0
	TOTAL		102.00	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	24.28	1.73	24.6	36.90	22.2	0.1	14.6	8.33	21.8	11.65	35.9	1.09	25.8
63	13.38	1.81	14.2	39.50	13.1	0.1	11.0	10.70	15.4	8.61	14.6	1.06	13.8
53	16.30	1.83	17.5	41.30	16.7	0.2	23.2	7.57	13.3	8.76	18.1	1.08	17.1
45	14.39	1.58	13.3	41.30	14.7	0.1	13.0	11.70	18.1	6.27	11.5	1.07	15.0
38	12.04	1.35	9.5	41.60	12.4	0.1	8.1	10.55	13.7	6.00	9.2	1.10	12.9
26	12.04	1.36	9.6	44.40	13.3	0.2	14.4	9.73	12.6	4.17	6.4	1.01	11.8
<26	6.32	3.03	11.2	48.10	7.5	0.3	15.6	7.59	5.2	5.28	4.2	0.58	3.6
CALC	98.76	1.71	100.0	40.32	100.0	0.1	100.0	9.29	100.0	7.87	100.0	1.03	100.0
ASSAY		1.63		40.70		0.1		10.20		7.61		1.06	

ANALYSES

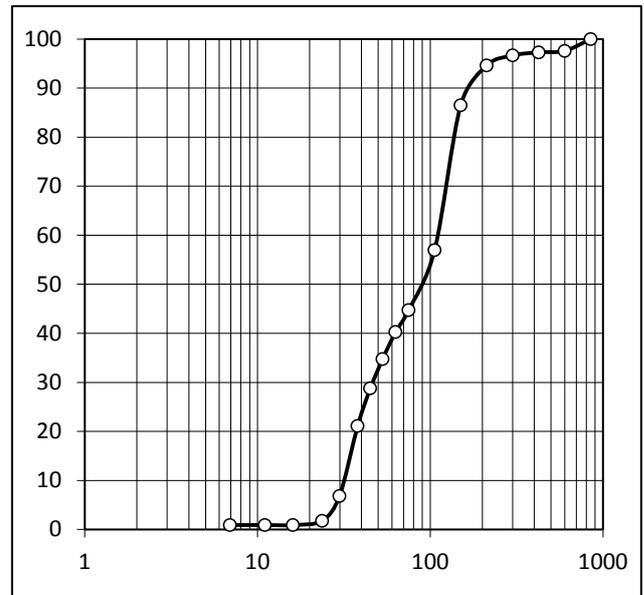
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
75	24.28	1.02	30.0	3.10	29.4	3.92	30.5				
63	13.38	0.92	14.9	2.74	14.3	3.02	13.0				
53	16.30	0.90	17.8	2.63	16.7	4.87	25.4				
45	14.39	0.80	14.0	2.46	13.8	2.39	11.0				
38	12.04	0.74	10.8	2.43	11.4	2.31	8.9				
26	12.04	0.57	8.3	2.14	10.1	1.98	7.6				
<26	6.32	0.54	4.1	1.74	4.3	1.73	3.5				
CALC	98.76	0.82	100.0	2.6	100.0	3.12	100.0				
ASSAY		0.83		2.58		2.81					



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Combined Conc
DATE	210814
TECHNICIAN	MS

LC01 Combined Conc 0		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	140	850	0.00	0.00	100.0
		600	2.83	2.41	97.6
		425	0.36	0.31	97.3
		300	0.73	0.62	96.7
		212	2.39	2.04	94.6
		150	9.50	8.10	86.5
		106	34.62	29.53	57.0
		75	14.39	12.28	44.7
		63	5.20	4.44	40.3
	53	6.47	5.52	34.8	
	45	7.00	5.97	28.8	
	38	8.97	7.65	21.1	
CYCLOSIZER	CS1	30	16.79	14.32	6.8
FLOW 185	CS2	24	5.90	5.03	1.8
TEMP 21	CS3	16	1.02	0.87	0.9
SG 3.50	CS4	11	0.00	0.00	0.9
MINS 20	CS5	7	0.00	0.00	0.9
	SUB		1.06	0.90	0.0
	TOTAL		117.23	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	13.49	17.80	13.0	37.00	14.5	1.15	17.0	21.80	18.7	2.90	9.8	0.16	4.1
106	29.53	7.61	12.1	38.70	33.2	0.22	7.1	10.45	19.7	5.31	39.1	1.06	59.1
75	12.28	16.25	10.8	31.50	11.2	0.65	8.8	7.61	5.9	7.60	23.3	0.87	20.1
63	4.44	28.30	6.8	27.80	3.6	1.32	6.4	18.25	5.2	4.75	5.3	0.24	2.0
53	5.52	26.50	7.9	31.00	5.0	1.23	7.5	21.10	7.4	2.88	4.0	0.16	1.7
45	5.97	23.00	7.4	33.80	5.9	1.11	7.3	22.50	8.6	2.21	3.3	0.16	1.8
38	7.65	21.80	9.0	35.40	7.9	1.11	9.3	20.30	9.9	2.15	4.1	0.21	3.0
24	19.36	29.60	31.0	29.70	16.7	1.48	31.5	18.40	22.7	2.09	10.1	0.18	6.6
Cal <24	1.77	20.80	2.0	39.18	2.0	2.60	5.1	17.34	2.0	2.66	1.2	0.49	1.6
ASSAY	100.00	18.50	100.0	34.40	100.0	0.91	100.0	15.70	100.0	4.01	100.0	0.53	100.0

ANALYSES

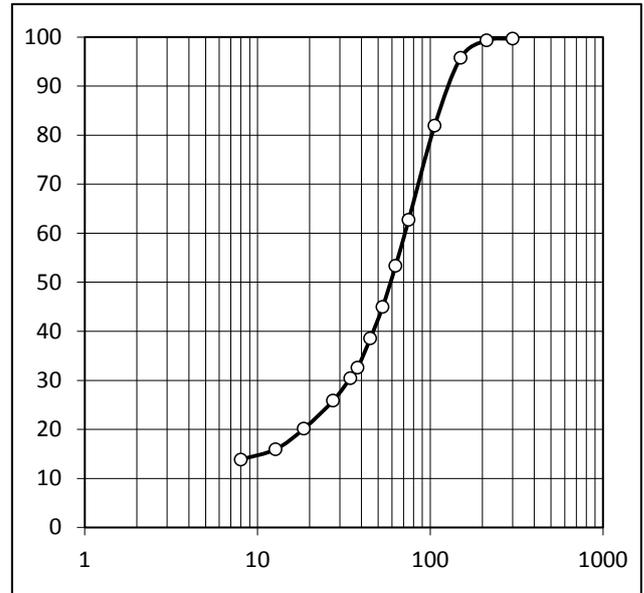
SIZE um	WT %	CaO		MgO		Al2O3		C		C inorganic	
		%	dist	%	dist	%	dist	%	dist	%	dist
150	13.49	0.25	7.6	0.85	8.2	0.98	9.7	0.93	5.4	0.71	4.5
106	29.53	0.75	49.8	2.53	53.4	2.00	43.4	4.21	53.1	4.03	55.4
75	12.28	0.92	25.4	2.42	21.2	2.88	26.0	3.56	18.7	3.41	19.5
63	4.44	0.33	3.3	0.88	2.8	1.36	4.4	1.18	2.2	1.09	2.2
53	5.52	0.20	2.5	0.60	2.4	0.78	3.2	0.88	2.1	0.80	2.1
45	5.97	0.16	2.1	0.55	2.3	0.56	2.5	0.95	2.4	0.82	2.3
38	7.65	0.14	2.4	0.56	3.1	0.58	3.3	1.24	4.1	1.06	3.8
24	19.36	0.14	6.1	0.44	6.1	0.49	7.0	1.08	8.9	1.01	9.1
Cal <24	1.77	0.22	0.9	0.46	0.6	0.43	0.6	4.10	3.1	1.55	1.3
ASSAY	100.00	0.45	100.0	1.40	100.0	1.36	100.0	2.34	100.0	2.15	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc6
	Regrind Discharge
DATE	210814
TECHNICIAN	MS

LC01 Cyc6 Regrind Discharge		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	103	850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.40	0.30	99.7
		212	0.51	0.39	99.3
		150	4.71	3.57	95.7
		106	18.26	13.83	81.9
		75	25.34	19.20	62.7
		63	12.34	9.35	53.4
		53	11.07	8.39	45.0
		45	8.46	6.41	38.6
		38	7.92	6.00	32.6
CYCLOSIZER	CS1	34	2.79	2.11	30.4
FLOW 185	CS2	27	6.07	4.60	25.9
TEMP 21	CS3	19	7.54	5.71	20.1
SG 2.80	CS4	13	5.53	4.19	15.9
MINS 20	CS5	8	2.76	2.09	13.9
	SUB		18.29	13.86	0.0
	TOTAL		131.99	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	4.26	0.25	1.7	12.75	2.8	0.06	3.6	1.26	1.4	55.70	5.5	0.21	1.9
106	13.83	0.31	7.0	14.35	10.2	0.06	11.9	1.17	4.4	54.50	17.3	0.31	9.3
75	19.20	0.47	14.8	16.30	16.1	0.06	16.5	2.67	13.9	49.90	22.0	0.39	16.3
63	9.35	0.67	10.3	19.35	9.3	0.08	10.7	4.12	10.4	44.50	9.6	0.48	9.8
53	8.39	0.80	11.0	21.10	9.1	0.08	9.6	4.97	11.3	41.40	8.0	0.54	9.8
45	6.41	0.92	9.7	23.50	7.7	0.10	9.2	5.43	9.4	38.20	5.6	0.60	8.4
38	6.00	0.94	9.2	24.20	7.5	0.09	7.7	5.71	9.3	35.90	5.0	0.63	8.2
27	6.71	1.79	19.7	33.10	11.4	0.13	12.5	6.65	12.1	20.60	3.2	0.85	12.4
13	9.90	0.67	10.9	20.10	10.2	0.08	11.3	3.80	10.2	43.00	9.8	0.49	10.5
8	2.09	0.43	1.5	20.10	2.2	0.08	2.4	3.22	1.8	42.60	2.0	0.44	2.0
CALC<8	13.86	0.18	4.2	18.93	13.5	0.02	4.7	4.25	15.9	37.83	12.1	0.38	11.3
ASSAY	100.00	0.61	100.0	19.45	100.0	0.07	100.0	3.70	100.0	43.50	100.0	0.46	100.0

ANALYSES

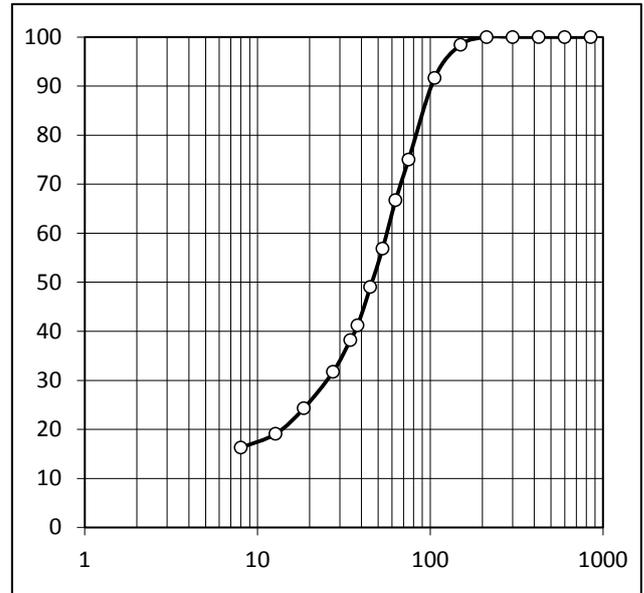
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
150	4.26	0.59	3.0	4.03	4.8	10.20	5.5				
106	13.83	0.72	11.9	4.11	16.0	9.51	16.6				
75	19.20	0.78	17.8	3.57	19.3	8.22	20.0				
63	9.35	0.83	9.2	3.34	8.8	7.38	8.7				
53	8.39	0.87	8.7	3.14	7.4	6.74	7.1				
45	6.41	0.92	7.0	3.07	5.5	6.20	5.0				
38	6.00	0.90	6.4	3.09	5.2	6.05	4.6				
27	6.71	0.93	7.4	2.70	5.1	4.61	3.9				
13	9.90	1.00	11.8	3.40	9.5	7.19	9.0				
8.0239	2.09	0.98	2.4	3.84	2.3	7.82	2.1				
CALC	13.86	0.87	14.3	4.17	16.2	9.97	17.5				
ASSAY	100.00	0.84	100.0	3.56	100.0	7.91	100.0				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc10
	Regrind Discharge
DATE	210814
TECHNICIAN	MS

LC01 Cyc10 Regrind Discharge		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	84	850	0.00	0.00	100.0
		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	2.30	1.58	98.4
		106	9.85	6.75	91.7
		75	24.31	16.66	75.0
		63	12.10	8.29	66.7
		53	14.35	9.84	56.9
45	11.45	7.85	49.0		
38	11.44	7.84	41.2		
CYCLOSIZER	CS1	34	4.35	2.98	38.2
FLOW 185	CS2	27	9.44	6.47	31.7
TEMP 21	CS3	19	10.82	7.42	24.3
SG 2.80	CS4	13	7.63	5.23	19.1
MINS 20	CS5	8	4.11	2.82	16.3
		SUB	23.74	16.27	0.0
		TOTAL	145.89	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	1.58	0.24	0.6	12.50	0.9	0.07	1.4	1.10	0.5	55.90	2.1	0.21	0.6
106	6.75	0.28	3.1	14.05	4.6	0.07	5.9	1.12	2.2	53.60	8.6	0.29	3.7
75	16.66	0.38	10.4	16.05	12.9	0.07	14.6	1.83	8.8	50.60	20.0	0.38	11.9
63	8.29	0.58	7.9	19.35	7.7	0.07	7.3	1.82	4.4	46.90	9.2	0.50	7.8
53	9.84	0.64	10.3	20.10	9.5	0.06	7.4	3.72	10.6	42.80	10.0	0.56	10.4
45	7.85	0.74	9.5	22.80	8.6	0.08	7.8	4.28	9.7	39.10	7.3	0.64	9.5
38	7.84	0.78	10.0	24.20	9.1	0.08	7.8	4.40	10.0	36.70	6.8	0.71	10.5
27	9.45	1.44	22.3	33.30	15.1	0.13	15.4	6.23	17.1	20.40	4.6	0.90	16.1
13	12.65	0.65	13.5	21.20	12.9	0.10	15.8	3.20	11.7	41.40	12.4	0.56	13.4
8	2.82	0.45	2.1	20.50	2.8	0.08	2.8	2.32	1.9	42.60	2.8	0.51	2.7
CALC<8	16.27	0.39	10.3	20.31	15.9	0.07	13.8	4.89	23.1	42.14	16.3	0.44	13.4
ASSAY	100.00	0.61	100.0	20.80	100.0	0.08	100.0	3.45	100.0	42.20	100.0	0.53	100.0

ANALYSES

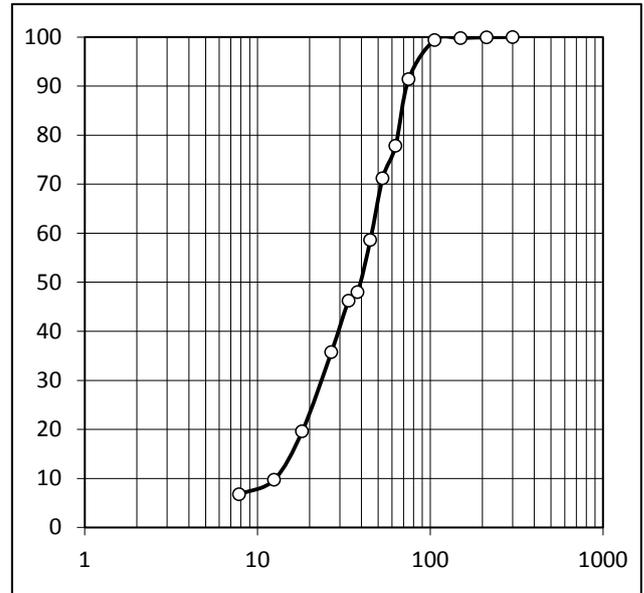
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
150	1.58	0.62	1.2	4.40	1.9	10.25	2.1				
106	6.75	0.66	5.4	4.29	8.1	9.48	8.2				
75	16.66	0.74	14.9	3.81	17.8	8.61	18.4				
63	8.29	0.83	8.3	3.51	8.2	7.62	8.1				
53	9.84	0.84	10.0	3.22	8.9	6.89	8.7				
45	7.85	0.87	8.2	3.19	7.0	6.41	6.5				
38	7.84	0.90	8.5	3.13	6.9	5.97	6.0				
27	9.45	0.88	10.0	2.69	7.1	4.33	5.3				
13	12.65	1.00	15.2	3.31	11.7	6.63	10.8				
8.0239	2.82	1.00	3.4	3.82	3.0	7.56	2.7				
CALC	16.27	0.76	15.0	4.25	19.4	11.14	23.3				
ASSAY	100.00	0.83	100.0	3.57	100.0	7.79	100.0				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc16 -106
	Mozley Tail
DATE	81014
TECHNICIAN	MS

LC01 Cyc16 -106 Mozley Tail		SIZE um	WEIGHTS			
			gm	(%)	%PASS	
p80		850	0.00	0.00	100.0	
		600	0.00	0.00	100.0	
		425	0.00	0.00	100.0	
		300	0.00	0.00	100.0	
		212	0.06	0.07	99.9	
		150	0.14	0.16	99.8	
		106	0.33	0.37	99.4	
		75	7.07	7.99	91.4	
		65	63	12.01	13.58	77.8
			53	5.87	6.64	71.2
45	11.13		12.58	58.6		
38	9.39		10.61	48.0		
CYCLOSIZER	CS1	34	1.58	1.79	46.2	
FLOW 185	CS2	27	9.27	10.48	35.7	
TEMP 21	CS3	18	14.28	16.14	19.6	
SG 2.90	CS4	12	8.75	9.89	9.7	
MINS 20	CS5	8	2.60	2.94	6.8	
	SUB		5.99	6.77	0.0	
	TOTAL		88.47	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	8.59	0.25	5.1	12.85	6.3	0.05	4.6	0.83	4.3	55.60	10.0	0.37	5.4
63	13.58	0.22	7.1	13.05	10.1	0.06	8.8	0.87	7.2	56.20	16.0	0.40	9.2
53	6.64	0.22	3.5	13.90	5.3	0.07	5.0	0.97	3.9	54.90	7.7	0.44	5.0
45	12.58	0.22	6.6	14.15	10.2	0.05	6.8	0.98	7.5	55.40	14.6	0.47	10.0
38	10.61	0.23	5.8	15.10	9.2	0.05	5.7	1.16	7.5	51.60	11.5	0.54	9.7
26	12.26	0.48	14.0	26.10	18.3	0.08	10.6	2.47	18.4	32.50	8.4	1.00	20.8
12	26.03	0.65	40.3	19.45	28.9	0.13	36.5	2.20	34.8	43.40	23.7	0.66	29.2
<12	9.71	0.76	17.6	21.10	11.7	0.21	22.0	2.79	16.5	39.20	8.0	0.65	10.7
CALC	100.00	0.42	100.0	17.49	100.0	0.09	100.0	1.65	100.0	47.58	100.0	0.59	100.0
ASSAY		0.40		17.35		0.09		1.69		47.80		0.59	

ANALYSES

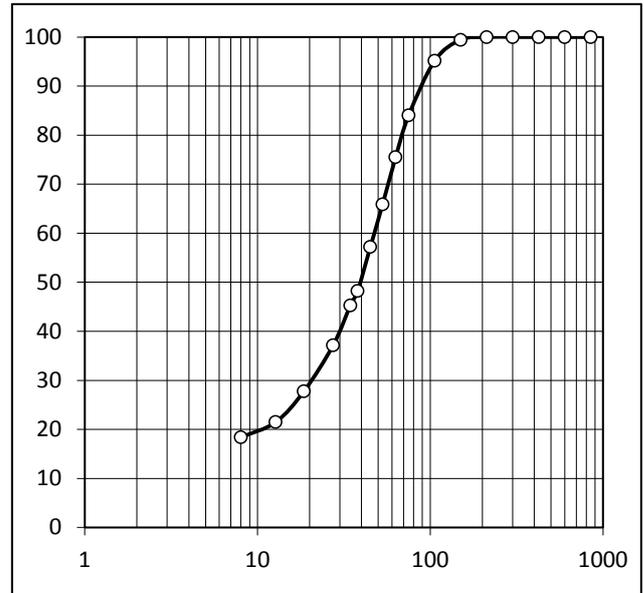
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
75	8.59	0.88	7.3	3.84	9.3	8.97	10.0				
63	13.58	0.90	11.7	3.76	14.4	8.70	15.3				
53	6.64	0.95	6.1	3.59	6.7	8.52	7.3				
45	12.58	0.98	11.9	3.66	13.0	8.26	13.5				
38	10.61	1.06	10.8	3.53	10.6	7.97	11.0				
26	12.26	1.28	15.1	3.26	11.3	6.58	10.5				
12	26.03	1.07	26.8	3.35	24.6	6.90	23.3				
<12	9.71	1.11	10.4	3.65	10.0	7.35	9.2				
CALC	100.00	1.04	100.0	3.54	100.0	7.72	100.0				
ASSAY		1.04		3.59		7.87					



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc 16
	Regrind Discharge
DATE	81014
TECHNICIAN	MS

LC01 Cyc 16 Regrind Discharge		SIZE um	WEIGHTS				
			gm	(%)	%PASS		
p80		850	0.00	0.00	100.0		
		600	0.00	0.00	100.0		
		425	0.00	0.00	100.0		
		300	0.00	0.00	100.0		
		212	0.00	0.00	100.0		
		150	0.63	0.56	99.4		
		106	4.83	4.29	95.2		
		75	12.51	11.11	84.0		
		69		63	9.63	8.55	75.5
				53	10.79	9.58	65.9
45	9.77			8.68	57.2		
38	10.12			8.99	48.2		
CYCLOSIZER	CS1			34	3.34	2.97	45.3
FLOW	185	CS2	27	9.16	8.14	37.1	
TEMP	21	CS3	19	10.54	9.36	27.8	
SG	2.80	CS4	13	7.08	6.29	21.5	
MINS	20	CS5	8	3.50	3.11	18.4	
		SUB	20.69	18.38	0.0		
		TOTAL	112.59	100.00			



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	0.56	0.20	0.2	12.80	0.3	0.05	0.3	1.28	0.2	55.40	0.8	0.31	0.3
106	4.29	0.24	1.7	13.35	2.8	0.05	2.7	1.01	1.4	53.50	5.6	0.36	2.3
75	11.11	0.31	5.6	15.00	8.0	0.06	8.3	1.57	5.7	51.60	13.9	0.44	7.2
63	8.55	0.47	6.6	17.75	7.3	0.05	5.3	2.36	6.6	47.80	9.9	0.57	7.2
53	9.58	0.61	9.6	19.35	8.9	0.06	7.2	3.11	9.7	44.50	10.3	0.68	9.6
45	8.68	0.74	10.5	21.80	9.1	0.07	7.6	2.60	7.3	41.60	8.7	0.77	9.8
38	8.99	0.82	12.1	22.70	9.8	0.07	7.9	4.06	11.8	37.10	8.1	0.85	11.2
27	11.10	1.47	26.8	32.80	17.5	0.12	16.7	6.60	23.8	19.75	5.3	1.15	18.8
13	15.65	0.63	16.2	21.20	16.0	0.09	17.6	3.05	15.5	41.50	15.7	0.71	16.3
8	3.11	0.42	2.1	20.00	3.0	0.08	3.1	2.44	2.5	43.40	3.3	0.63	2.9
CALC<8	18.38	0.29	8.6	19.61	17.3	0.10	23.3	2.61	15.5	41.51	18.5	0.54	14.5
ASSAY	100.00	0.61	100.0	20.80	100.0	0.08	100.0	3.08	100.0	41.30	100.0	0.68	100.0

ANALYSES

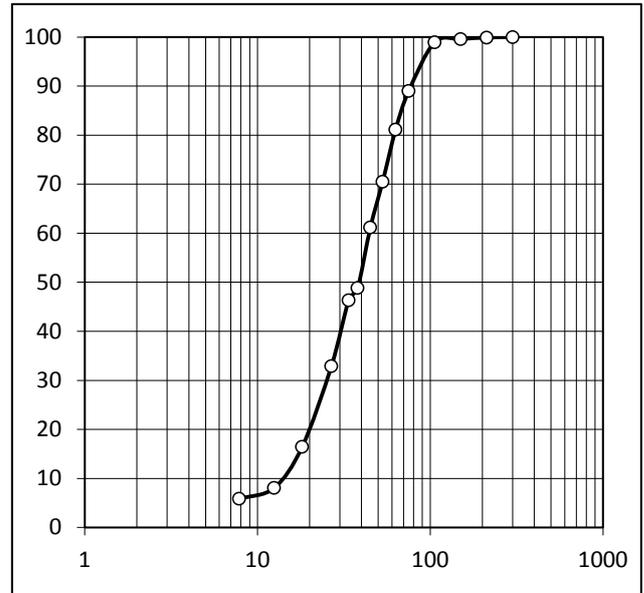
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
150	0.56	0.59	0.4	4.57	0.7	10.00	0.7				
106	4.29	0.64	3.1	4.45	5.3	9.96	5.5				
75	11.11	0.73	9.2	4.00	12.3	9.09	13.1				
63	8.55	0.82	8.0	3.73	8.9	8.06	8.9				
53	9.58	0.87	9.5	3.45	9.2	7.42	9.2				
45	8.68	0.96	9.5	3.34	8.1	6.89	7.7				
38	8.99	0.94	9.6	3.15	7.9	6.11	7.1				
27	11.10	0.95	12.0	2.68	8.3	4.30	6.2				
13	15.65	1.03	18.3	3.25	14.1	6.67	13.5				
8.0239	3.11	1.03	3.6	3.73	3.2	7.55	3.0				
CALC	18.38	0.81	16.8	4.32	22.1	10.52	25.0				
ASSAY	100.00	0.88	100.0	3.60	100.0	7.73	100.0				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc25 -106
	Mozley Tail
DATE	221014
TECHNICIAN	DK

LC01 Cyc25 -106 Mozley Tail		SIZE um	WEIGHTS			
			gm	(%)	%PASS	
p80	850	0.00	0.00	100.0		
	600	0.00	0.00	100.0		
	425	0.00	0.00	100.0		
	300	0.00	0.00	100.0		
	212	0.13	0.11	99.9		
	150	0.37	0.31	99.6		
	106	0.76	0.64	98.9		
	75	11.85	9.96	89.0		
	63	9.35	7.86	81.1		
	53	12.61	10.60	70.5		
62	45	11.13	9.36	61.2		
	38	14.67	12.33	48.8		
	CYCLOSIZER	CS1	34	2.99	2.51	46.3
	FLOW 185	CS2	27	15.97	13.43	32.9
	TEMP 21	CS3	18	19.52	16.41	16.5
SG 2.90	CS4	12	10.01	8.42	8.0	
MINS 20	CS5	8	2.62	2.20	5.8	
	SUB		6.95	5.84	0.0	
	TOTAL		118.93	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
106	1.06	0.18	0.5	9.0	0.6	0.06	0.7	0.55	0.4	66.5	1.5	0.16	0.3
75	9.96	0.19	4.7	11.7	6.8	0.05	5.5	0.52	3.2	60	12.5	0.28	4.6
63	7.86	0.19	3.7	12.4	5.7	0.06	5.2	0.6	2.9	58.4	9.6	0.34	4.5
53	10.60	0.19	5.0	13.0	8.0	0.06	7.1	0.73	4.8	57.7	12.8	0.4	7.1
45	9.36	0.21	4.9	14.2	7.7	0.06	6.2	0.68	3.9	56.8	11.1	0.47	7.3
38	12.33	0.22	6.8	15.2	10.9	0.06	8.2	1.1	8.4	51.6	13.3	0.57	11.7
27	15.94	0.47	18.7	24.8	23.1	0.08	14.2	2.89	28.4	33.4	11.1	1.01	26.8
12	24.83	0.69	42.8	20.0	29.0	0.15	41.4	2.22	34.0	42.6	22.1	0.71	29.4
8	2.20	0.75	4.1	21.0	2.7	0.19	4.7	2.51	3.4	39.2	1.8	0.65	2.4
CALC-8	5.84	0.59	8.6	16.34	5.6	0.10	6.8	2.93	10.6	35.28	4.3	0.60	5.9
ASSAY	100.00	0.40	100.00	17.15	100.00	0.09	100.00	1.62	100.00	47.90	100.00	0.60	100.00

ANALYSES

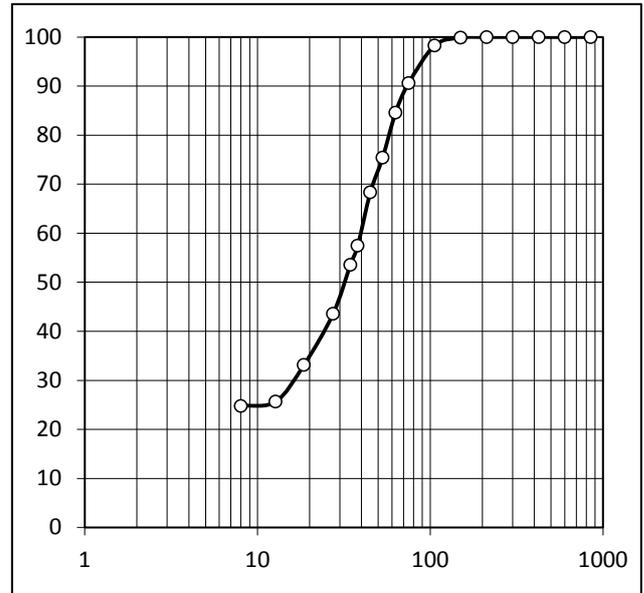
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
106	1.06	0.62	0.7	3.51	1.0	8.52	1.1				
75	9.96	0.81	8.0	3.78	10.6	8.97	11.3				
63	7.86	0.86	6.7	3.63	8.0	8.65	8.6				
53	10.60	0.91	9.6	3.65	10.9	8.36	11.2				
45	9.36	1.00	9.3	3.56	9.4	8.39	9.9				
38	12.33	1.07	13.1	3.52	12.2	7.84	12.2				
27	15.94	1.24	19.6	3.31	14.8	6.45	13.0				
12	24.83	1.11	27.3	3.38	23.6	6.87	21.6				
8	2.20	1.15	2.5	3.81	2.4	7.57	2.1				
CALC-8	5.84	0.59	3.4	4.37	7.2	11.92	8.8				
ASSAY	100.00	1.01	100.00	3.56	100.00	7.90	100.00				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc 25
	Regrind Discharge
DATE	221014
TECHNICIAN	DK

LC01 Cyc 25 Regrind Discharge		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	850	0.00	0.00	100.0	
	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	0.00	0.00	100.0	
	212	0.00	0.00	100.0	
	150	0.14	0.13	99.9	
	106	1.76	1.59	98.3	
	75	8.49	7.67	90.6	
	63	6.65	6.01	84.6	
	58	53	10.15	9.18	75.4
	45	7.84	7.09	68.3	
	38	12.05	10.89	57.4	
CYCLOSIZER	CS1	34	4.33	3.91	53.5
FLOW 185	CS2	27	11.02	9.96	43.6
TEMP 21	CS3	19	11.54	10.43	33.1
SG 2.80	CS4	13	8.26	7.47	25.7
MINS 20	CS5	8	1.00	0.90	24.8
	SUB		27.39	24.76	0.0
	TOTAL		110.62	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
106	1.72	0.24	0.7	14.00	1.1	0.07	1.5	0.91	0.5	54.40	2.3	0.36	0.9
75	7.67	0.33	4.0	15.70	5.7	0.07	6.7	1.58	3.9	51.40	9.7	0.47	5.2
63	6.01	0.43	4.1	18.00	5.2	0.06	4.5	2.22	4.3	47.40	7.0	0.59	5.1
53	9.18	0.55	8.0	19.25	8.4	0.07	8.0	2.71	8.0	45.40	10.2	0.69	9.2
45	7.09	0.56	6.3	20.50	6.9	0.06	5.3	2.88	6.6	43.00	7.5	0.72	7.4
38	10.89	0.74	12.8	22.20	11.5	0.08	10.9	3.53	12.4	39.60	10.6	0.84	13.3
27	13.88	1.49	32.8	32.20	21.3	0.13	22.5	5.00	22.5	24.40	8.3	1.10	22.1
13	17.90	0.71	20.2	20.60	17.6	0.08	17.9	3.30	19.1	42.40	18.6	0.68	17.6
8	0.90	0.45	0.6	20.60	0.9	0.07	0.8	2.82	0.8	43.70	1.0	0.63	0.8
CALC<8	24.76	0.27	10.5	18.15	21.4	0.07	21.8	2.72	21.8	41.09	24.9	0.51	18.3
ASSAY	100.00	0.63	100.0	21.00	100.0	0.08	100.0	3.09	100.0	40.80	100.0	0.69	100.0

ANALYSES

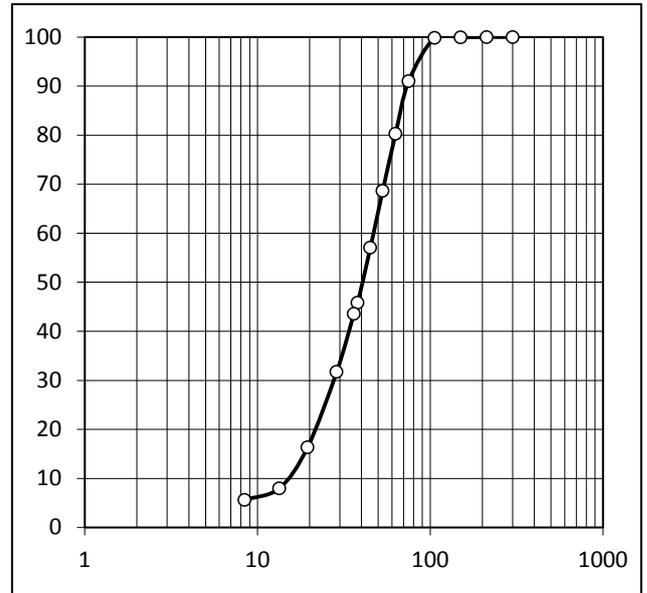
SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
106	1.72	0.72	1.4	4.84	2.4	9.90	2.2				
75	7.67	0.72	6.4	4.17	9.1	8.95	9.1				
63	6.01	0.77	5.3	3.71	6.3	7.96	6.3				
53	9.18	0.85	9.0	3.54	9.2	7.36	8.9				
45	7.09	0.87	7.1	3.33	6.7	6.87	6.4				
38	10.89	0.93	11.6	3.19	9.9	6.31	9.1				
27	13.88	0.95	15.2	2.80	11.0	4.76	8.7				
13	17.90	0.99	20.4	3.17	16.1	6.50	15.4				
8	0.90	0.99	1.0	3.50	0.9	7.13	0.9				
CALC	24.76	0.80	22.7	4.03	28.3	10.08	33.0				
ASSAY	100.00	0.87	100.0	3.52	100.0	7.57	100.0				



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc31 -106
	Mozley Tail
DATE	041114
TECHNICIAN	MS

LC01 Cyc31 -106 Mozley Tail		SIZE um	WEIGHTS			
			gm	(%)	%PASS	
p80	850	0.00	0.00	100.0		
	600	0.00	0.00	100.0		
	425	0.00	0.00	100.0		
	300	0.00	0.00	100.0		
	212	0.00	0.00	100.0		
	150	0.07	0.06	99.9		
	106	0.10	0.09	99.8		
	75	9.72	8.85	91.0		
	63	11.75	10.70	80.3		
	63	53	12.82	11.68	68.6	
63	45	12.71	11.58	57.0		
	38	12.31	11.21	45.8		
	CYCLOSIZER	CS1	36	2.47	2.25	43.6
	FLOW 185	CS2	29	13.01	11.85	31.7
	TEMP 21	CS3	19	16.91	15.40	16.3
SG 2.60	CS4	13	9.16	8.34	8.0	
MINS 20	CS5	8	2.60	2.37	5.6	
	SUB		6.17	5.62	0.0	
	TOTAL		109.80	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
75	9.01	0.21	4.9	12.35	6.7	0.05	5.0	0.50	2.9	59.60	11.0	0.33	5.2
63	10.70	0.22	6.0	13.00	8.4	0.06	7.1	0.75	5.1	57.40	12.6	0.38	7.1
53	11.68	0.21	6.3	13.05	9.2	0.05	6.5	0.83	6.2	56.60	13.5	0.41	8.4
45	11.58	0.22	6.5	14.15	9.9	0.07	9.0	0.99	7.3	55.60	13.2	0.49	10.0
38	11.21	0.22	6.3	14.90	10.1	0.05	6.2	0.98	7.0	53.00	12.2	0.55	10.8
29	14.10	0.49	17.7	23.40	19.9	0.07	11.0	2.60	23.5	35.10	10.1	0.94	23.2
13	23.74	0.64	39.0	19.20	27.5	0.14	36.9	1.65	25.1	45.50	22.1	0.67	27.9
8	2.37	0.67	4.1	21.10	3.0	0.19	5.0	2.43	3.7	41.10	2.0	0.64	2.7
CALC-8	5.62	0.64	9.2	16.14	5.5	0.21	13.2	5.29	19.1	29.86	3.4	0.47	4.7
ASSAY	100.00	0.39	100.00	16.60	100.00	0.09	100.00	1.56	100.00	48.90	100.00	0.57	100.00

ANALYSES

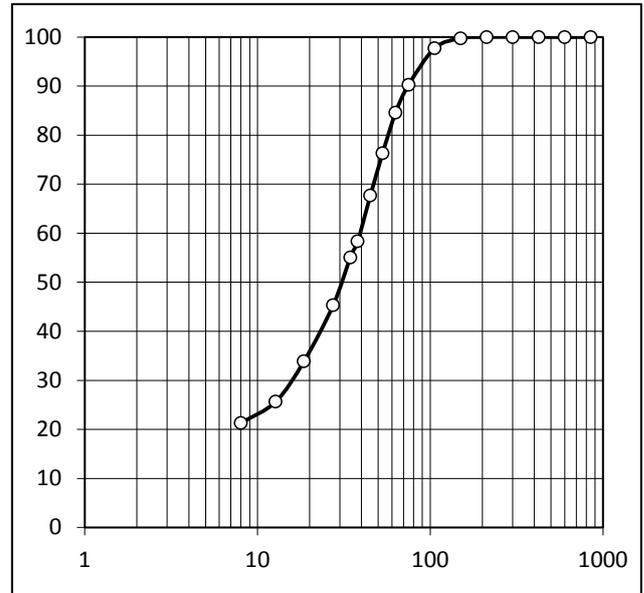
SIZE um	WT %	CaO		MgO		Al2O3				
		%	dist	%	dist	%	dist			
75	9.01	0.85	7.7	3.84	9.8	8.95	10.2			
63	10.70	0.82	8.8	3.72	11.2	8.62	11.6			
53	11.68	0.87	10.2	3.56	11.7	8.20	12.1			
45	11.58	0.98	11.3	3.58	11.7	8.01	11.7			
38	11.21	1.02	11.4	3.57	11.3	7.71	10.9			
29	14.10	1.24	17.5	3.19	12.7	6.49	11.5			
13	23.74	1.10	26.1	3.48	23.3	7.16	21.4			
8	2.37	1.12	2.7	3.63	2.4	7.25	2.2			
CALC-8	5.62	0.78	4.4	3.63	5.8	11.85	8.4			
ASSAY	100.00	1.00	100.00	3.54	100.00	7.93	100.00			



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	LC01 Cyc 231
	Regrind Discharge
DATE	71114
TECHNICIAN	MS

LC01 Cyc 231 Regrind Discharge		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	850	0.00	0.00	100.0	
	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	0.00	0.00	100.0	
	212	0.00	0.00	100.0	
	150	0.26	0.25	99.7	
	106	2.09	2.04	97.7	
	75	7.63	7.44	90.3	
	63	5.83	5.68	84.6	
	57	53	8.47	8.26	76.3
	45	8.88	8.66	67.7	
	38	9.53	9.29	58.4	
CYCLOSIZER	CS1	34	3.39	3.31	55.1
FLOW 185	CS2	27	10.02	9.77	45.3
TEMP 21	CS3	19	11.72	11.43	33.9
SG 2.80	CS4	13	8.43	8.22	25.7
MINS 20	CS5	8	4.48	4.37	21.3
	SUB		21.83	21.29	0.0
	TOTAL		102.56	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
106	2.29	0.26	1.0	15.50	1.7	0.06	1.5	1.34	1.1	51.50	2.9	0.37	1.2
75	7.44	0.28	3.6	15.90	5.8	0.07	5.8	1.47	3.9	50.50	9.1	0.45	4.9
63	5.68	0.36	3.5	17.85	5.0	0.06	3.8	1.94	4.0	47.40	6.5	0.59	4.9
53	8.26	0.47	6.7	19.10	7.7	0.09	8.3	2.16	6.4	46.00	9.2	0.67	8.1
45	8.66	0.56	8.4	20.80	8.8	0.08	7.7	2.68	8.3	42.90	9.0	0.76	9.7
38	9.29	0.63	10.1	20.90	9.5	0.09	9.3	3.08	10.3	41.30	9.3	0.80	10.9
34	3.31	2.99	17.0	40.60	6.6	0.19	7.0	9.93	11.8	7.97	0.6	1.29	6.3
27	9.77	0.92	15.5	26.40	12.6	0.10	10.9	4.25	14.9	30.10	7.1	1.02	14.7
19	11.43	0.73	14.4	20.60	11.5	0.12	15.2	2.68	11.0	42.90	11.9	0.73	12.3
13	8.22	0.59	8.4	20.10	8.1	0.11	10.0	2.64	7.8	45.00	9.0	0.65	7.9
8	4.37	0.43	3.2	19.65	4.2	0.09	4.4	2.49	3.9	45.40	4.8	0.62	4.0
CALC<8	21.29	0.22	8.2	17.58	18.3	0.07	16.2	2.20	16.8	40.07	20.7	0.48	15.1
ASSAY	100.00	0.58	100.0	20.40	100.0	0.09	100.0	2.79	100.0	41.30	100.0	0.68	100.0

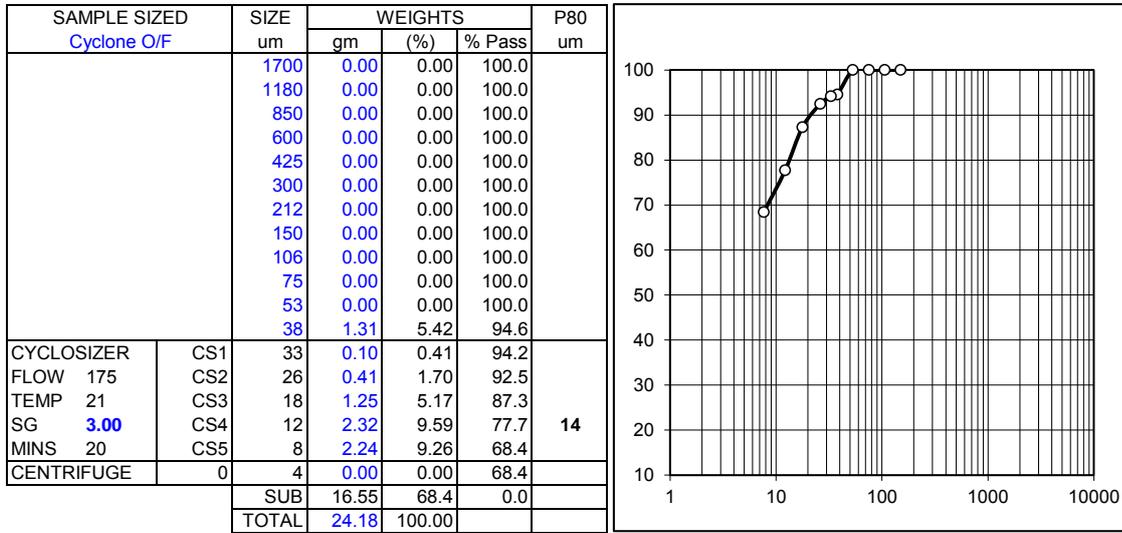
ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
106	2.29	0.64	1.6	4.51	2.9	9.39	2.8				
75	7.44	0.72	5.8	4.12	8.5	8.98	8.6				
63	5.68	0.82	5.1	3.82	6.0	8.31	6.1				
53	8.26	0.89	8.0	3.59	8.2	7.83	8.3				
45	8.66	0.97	9.1	3.44	8.3	7.21	8.0				
38	9.29	0.98	9.9	3.36	8.6	6.92	8.3				
34	3.31	0.69	2.5	2.39	2.2	2.48	1.1				
27	9.77	1.13	12.0	3.07	8.3	5.99	7.5				
19	11.43	1.02	12.7	3.24	10.3	6.80	10.0				
13	8.22	1.01	9.0	3.34	7.6	6.90	7.3				
8	4.37	0.99	4.7	3.45	4.2	7.32	4.1				
CALC	21.29	0.85	19.6	4.24	25.0	10.14	27.8				
ASSAY	100.00	0.92	100.0	3.61	100.0	7.76	100.0				



BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Cyclone O/F
TEST NO	T22
DATE	150714
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

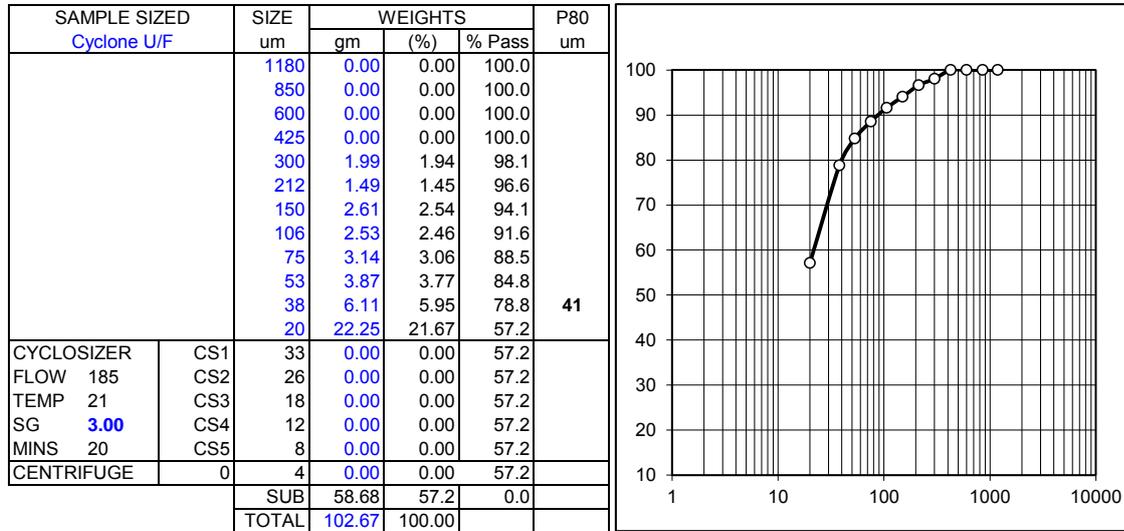
PROJECT	T0879
SAMPLE	Cyclone U/F
TEST NO	T22
DATE	150714
TECHNICIAN	MS

SAMPLE SIZED CYCLONE FEED				SAMPLE SIZED CYCLONE UF				SAMPLE SIZED CYCLONE OF				P80	P80	P80
SIZE um	WEIGHTS 100			SIZE um	WEIGHTS 60			SIZE um	WEIGHTS 40					
	gm	(%)	%PASS		gm	(%)	% Pass		gm	(%)	%PASS			
1700	0.00	0.00	100.0	1700	0.00	0.00	100.0				100.0			
1180	0.00	0.00	100.0	1180	0.00	0.00	100.0				100.0			
850	0.00	0.00	100.0	850	1.48	1.12	98.9				100.0			
600	4.32	2.44	97.6	600	2.14	1.63	97.2	600		3.7	96.3	39.9		
425	7.34	4.15	93.4	425	6.58	5.00	92.2	425		2.9	93.4	72.3		
300	15.89	8.99	84.4	300	15.79	12.00	80.2	300		4.5	89.0	80.1	263	299
212	18.62	10.54	73.9	212	19.33	14.69	65.6	212		4.3	84.7	83.7		
150	17.83	10.09	63.8	150	19.61	14.90	50.6	150		2.9	81.8	88.6		
106	12.92	7.31	56.5	106	14.57	11.07	39.6	106		1.7	80.1	90.9		103
75	12.33	6.98	49.5	75	13.98	10.63	29.0	75		1.5	78.6	91.4		
53	10.21	5.78	43.7	53	11.32	8.60	20.3	53		1.5	77.1	89.4		
38	10.02	5.67	38.1	38	11.15	8.47	11.9	38		1.5	75.6	89.7		
SUB	67.26	38.06		SUB	15.62	11.9		SUB		77.3		18.7		
TOTAL	176.7	100.0		TOTAL	131.57	100.00		TOTAL		101.7				



BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

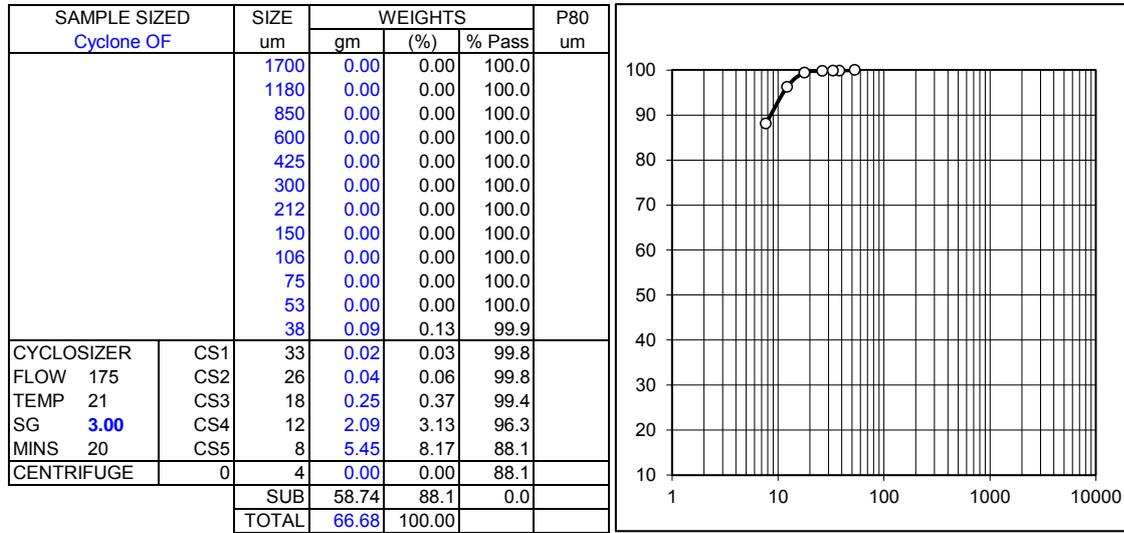
PROJECT	T0879
SAMPLE	Cyclone U/F
TEST NO	T23
DATE	170714
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

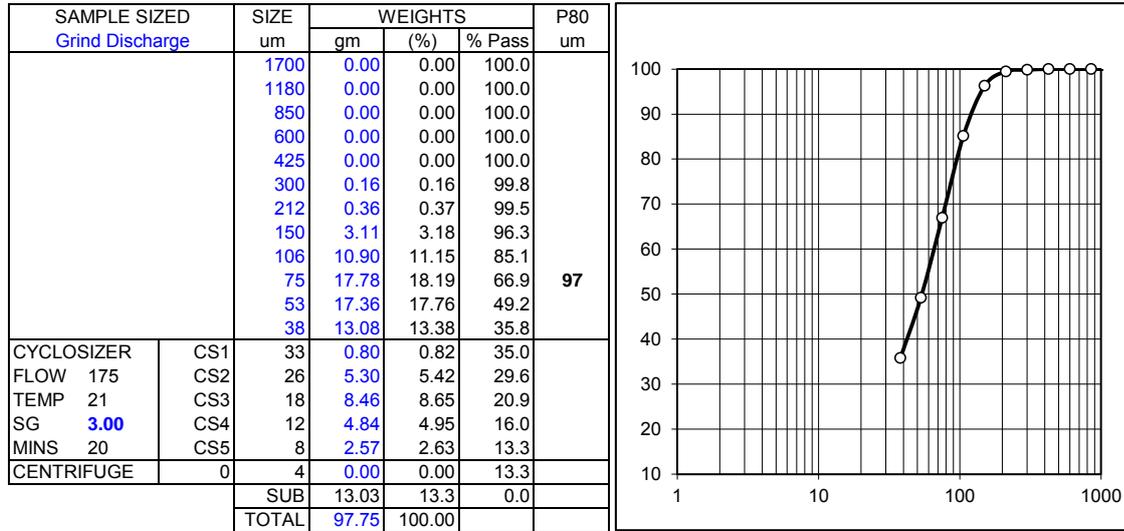
PROJECT	T0879
SAMPLE	Cyclone OF
TEST NO	T23
DATE	180714
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Grind Discharge
TEST NO	T24
DATE	180714
TECHNICIAN	MS

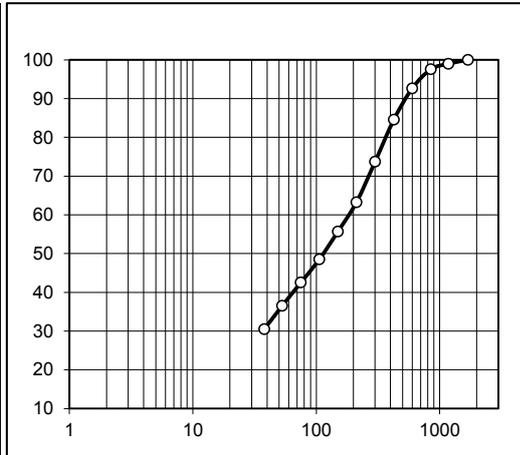




BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Bulk Sulphide Tail
TEST NO	
DATE	100914
TECHNICIAN	MS

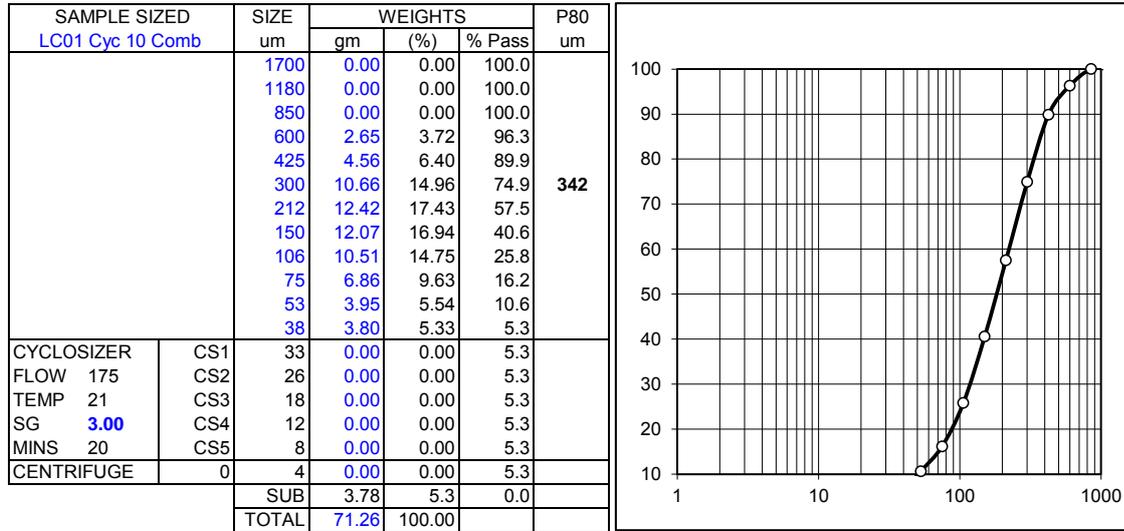
SAMPLE SIZED Bulk Sulphide Tail		SIZE um	WEIGHTS		P80 um	
			gm	(%)		% Pass
		1700	0.00	0.00	100.0	
		1180	5.06	0.99	99.0	
		850	7.32	1.43	97.6	
		600	25.08	4.91	92.7	
		425	41.38	8.11	84.6	
		300	55.15	10.81	73.7	
		212	53.42	10.47	63.3	
		150	38.61	7.57	55.7	
		106	36.70	7.19	48.5	
		75	30.59	5.99	42.5	
		53	30.62	6.00	36.5	
		38	30.62	6.00	30.5	
CYCLOSIZER		20	35.72	7.00	23.5	
FLOW	175	CS2	16	0.00	0.00	23.5
TEMP	21	CS3	11	0.00	0.00	23.5
SG	6.50	CS4	7	0.00	0.00	23.5
MINS	20	CS5	5	0.00	0.00	23.5
CENTRIFUGE	0		2	0.00	0.00	23.5
		SUB	120.03	23.52	0.0	
		TOTAL	510.30	100.00		





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

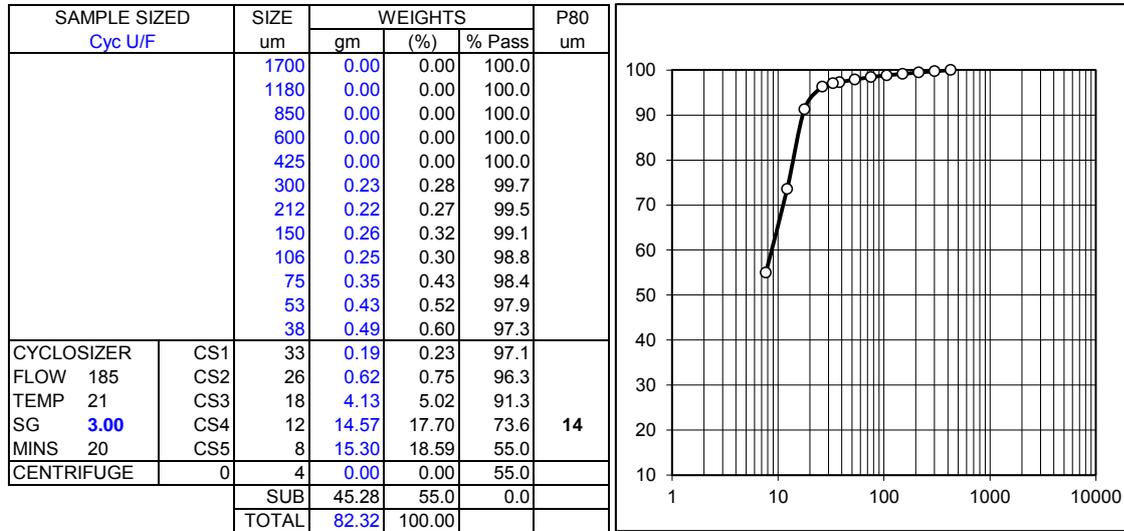
PROJECT	T0879
SAMPLE	LC01 Cyc 10 Comb
	Mids + Tail
DATE	110914
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

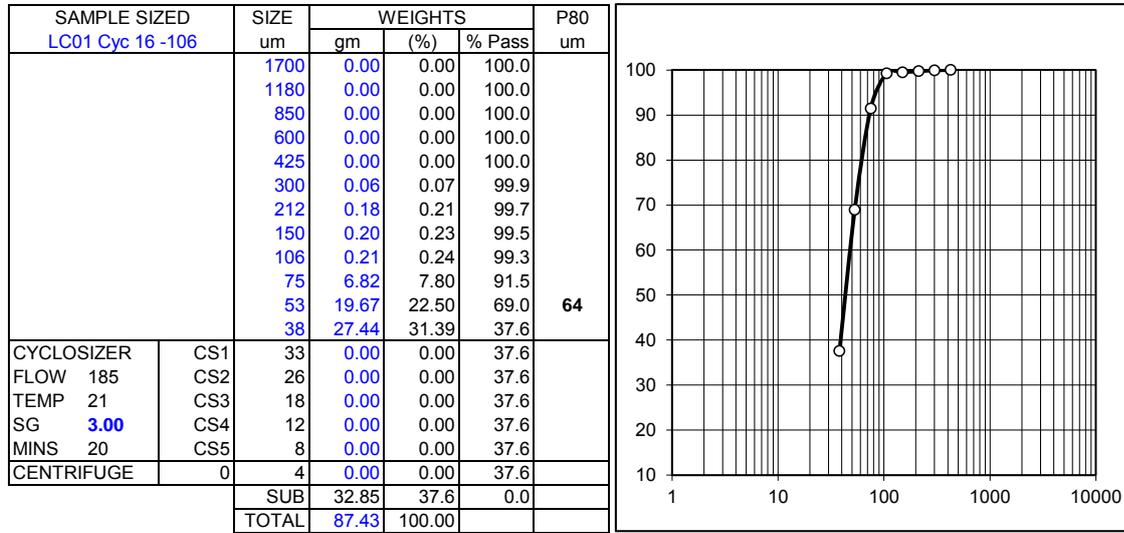
PROJECT	T0879
SAMPLE	Cyc U/F
TEST NO	T43
DATE	260914
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

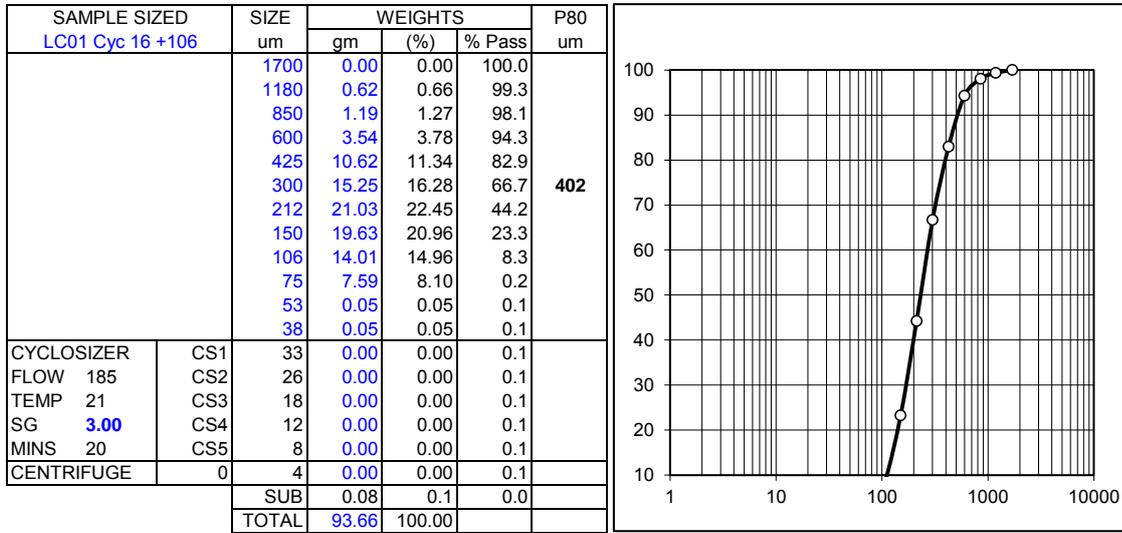
PROJECT	T0879
SAMPLE	LC01 Cyc 16 -106
	Mozley Mids
DATE	61014
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

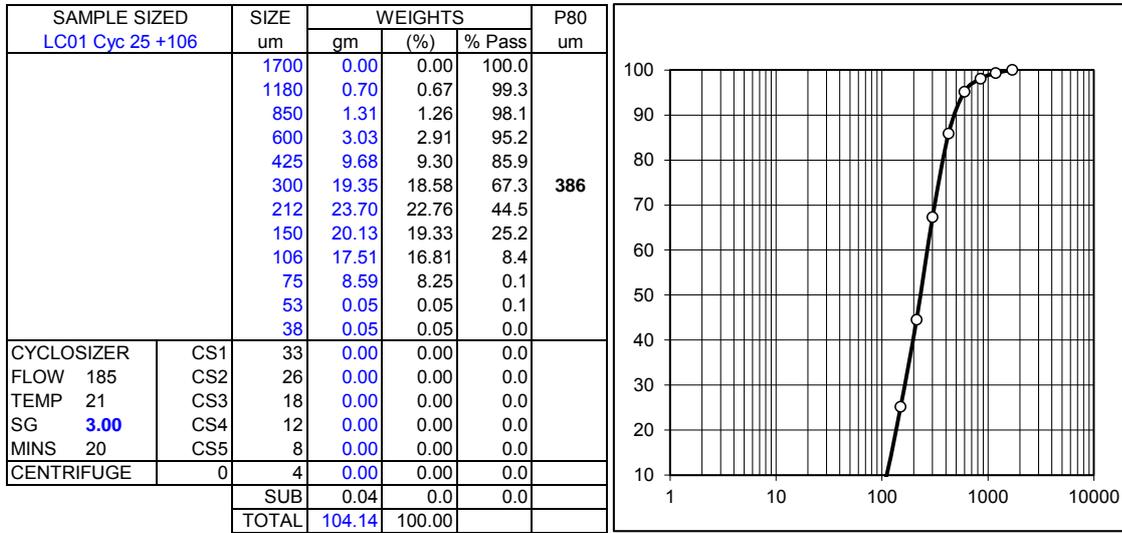
PROJECT	T0879
SAMPLE	LC01 Cyc 16 +106
	Mozley Tails
DATE	61014
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

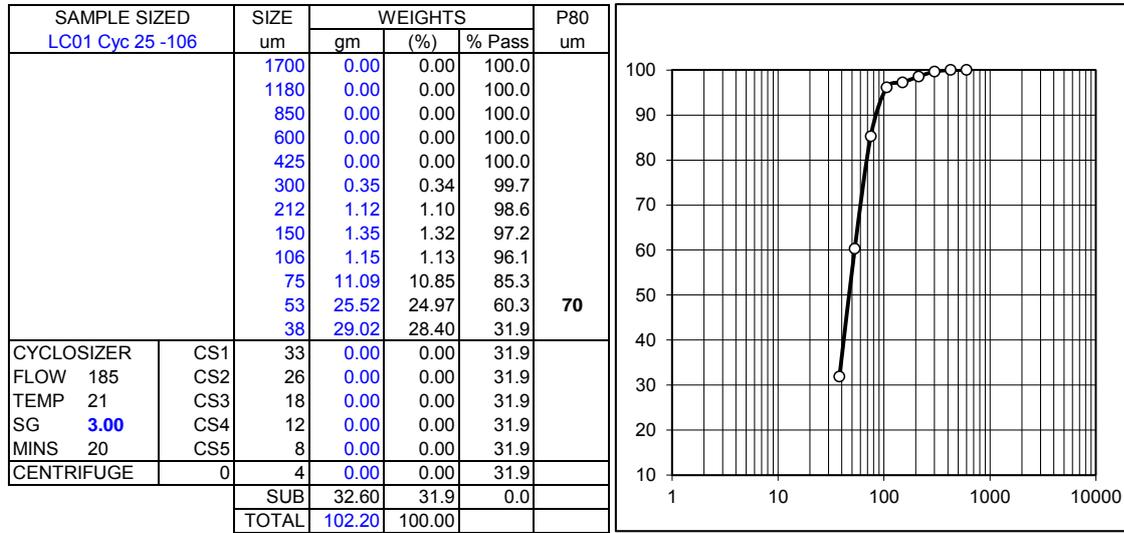
PROJECT	T0879
SAMPLE	LC01 Cyc 25 +106
	Mozley Tails
DATE	211014
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

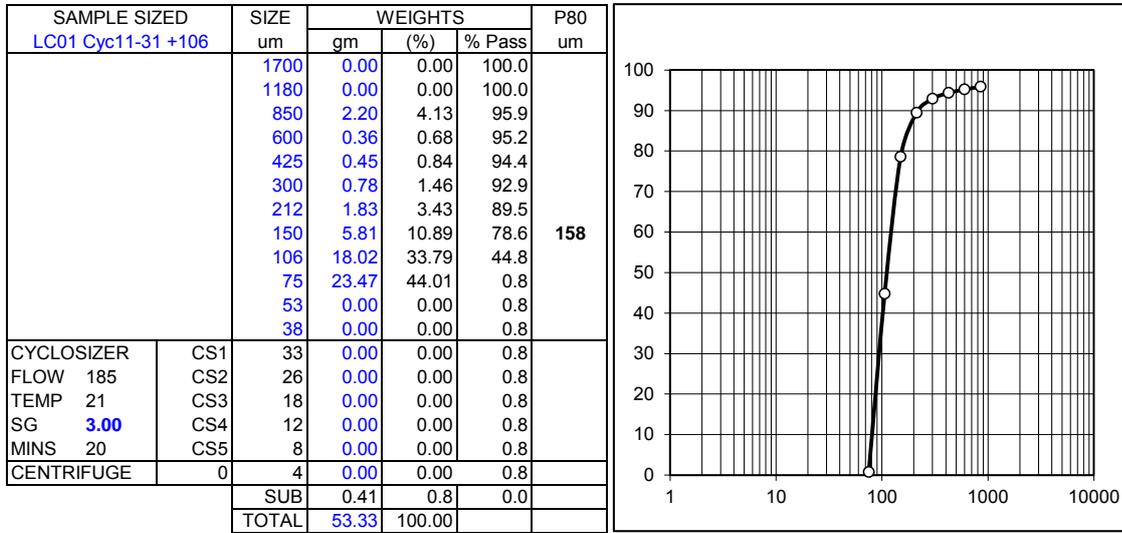
PROJECT	T0879
SAMPLE	LC01 Cyc 25 -106
	Mozley Mids
DATE	211014
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

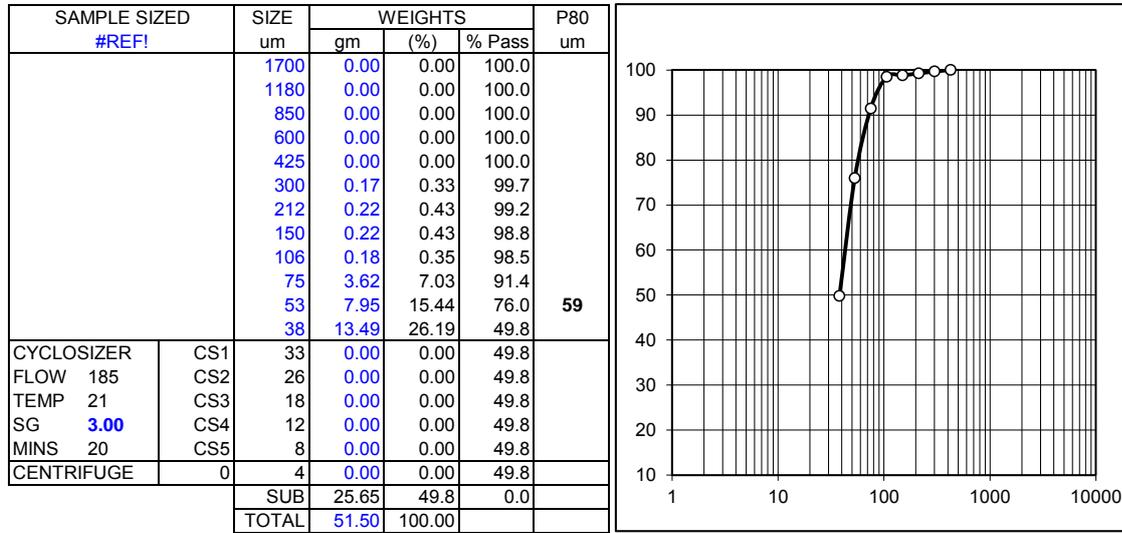
PROJECT	T0879
SAMPLE	LC01 Cyc11-31 +106
	CONC
DATE	311014
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

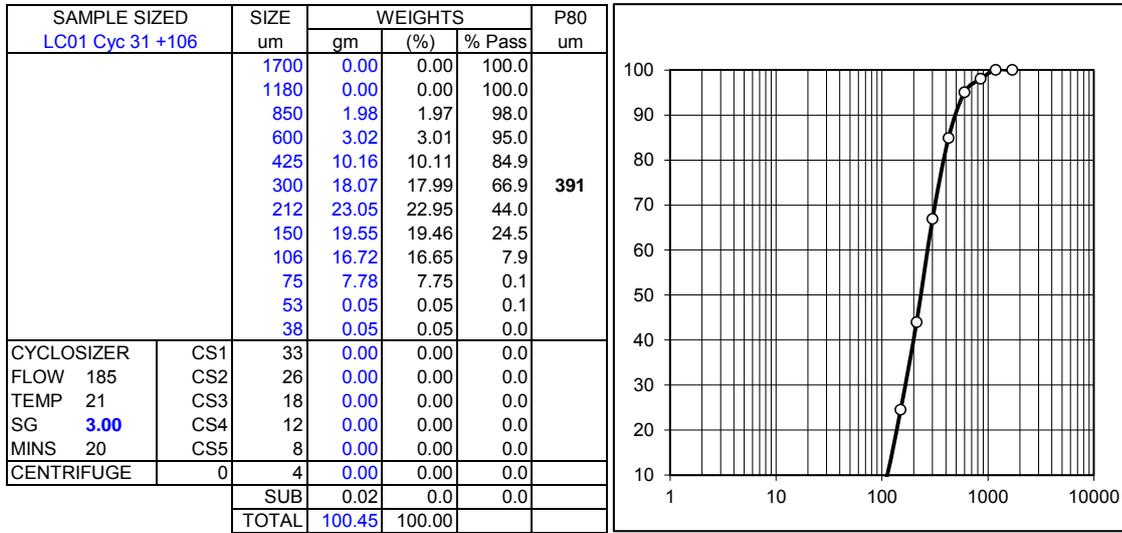
PROJECT	T0879
SAMPLE	LC01 Cyc11-31 -106 Moz Conc
DATE	311014
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

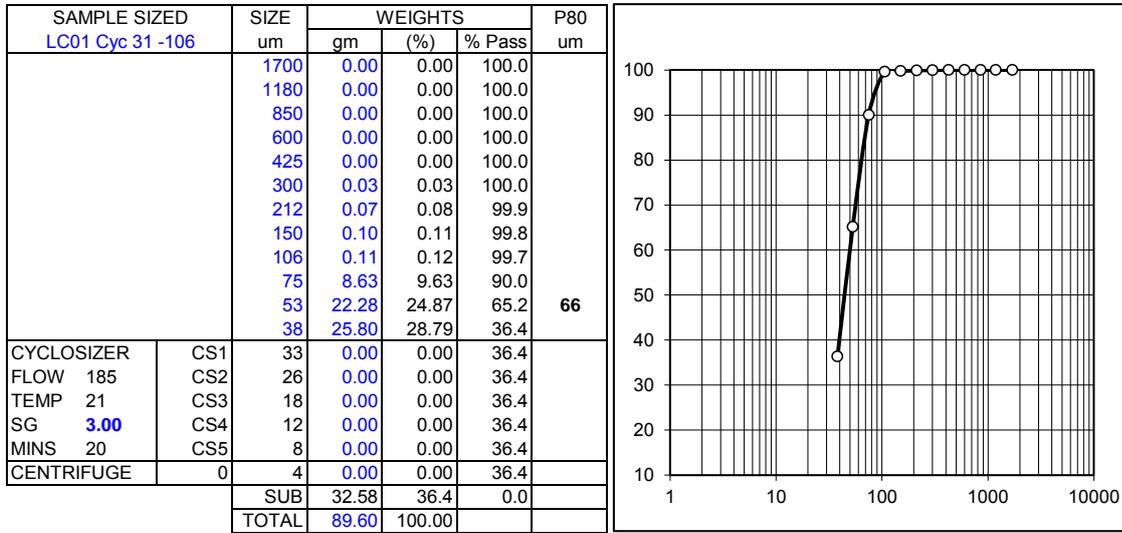
PROJECT	T0879
SAMPLE	LC01 Cyc 31 +106
	Mozley Tails
DATE	311014
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

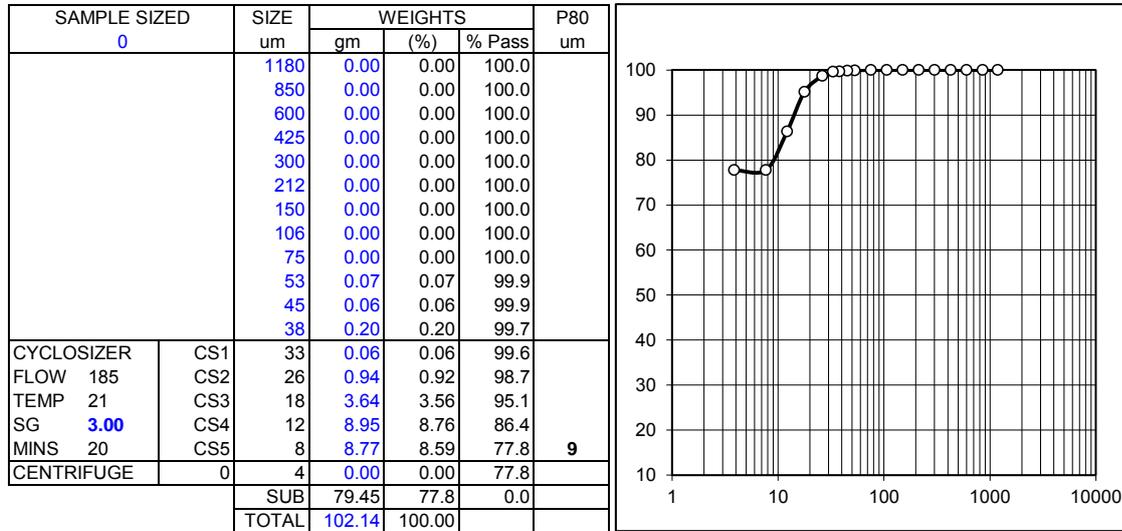
PROJECT	T0879
SAMPLE	LC01 Cyc 31 -106
	Mozley Mids
DATE	41114
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

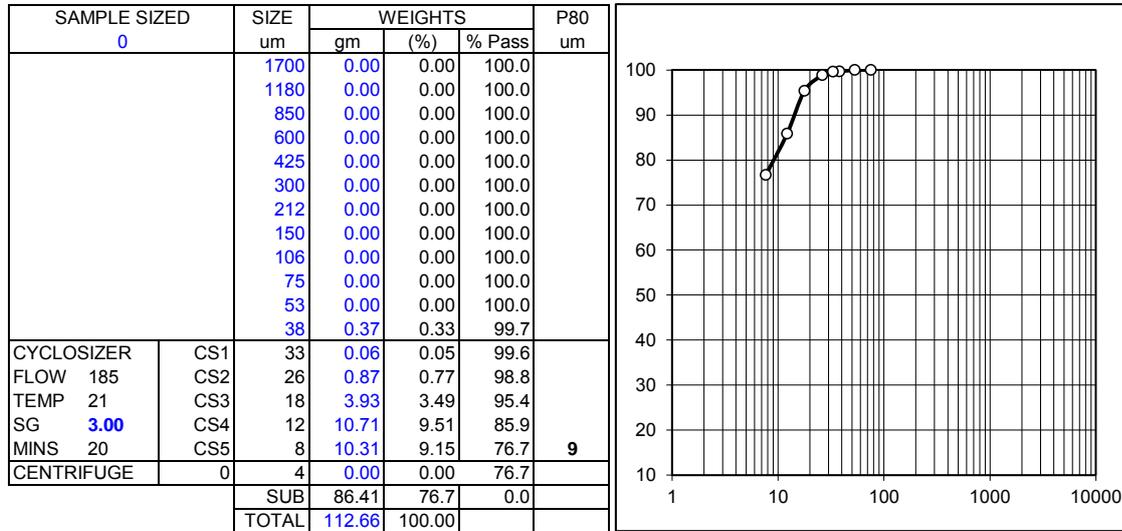
PROJECT	T0879
SAMPLE	LC01 Cyc11-31 Cyclone O/F
TEST NO	
DATE	61114
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

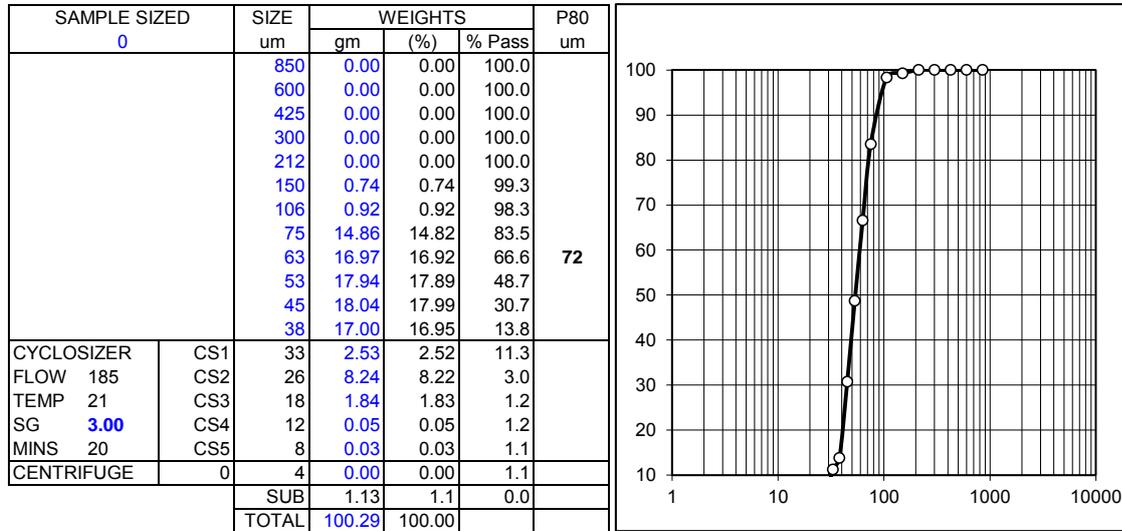
PROJECT	T0879
SAMPLE	LC01 CYC 11-31 Cyclone OF
TEST NO	
DATE	131114
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

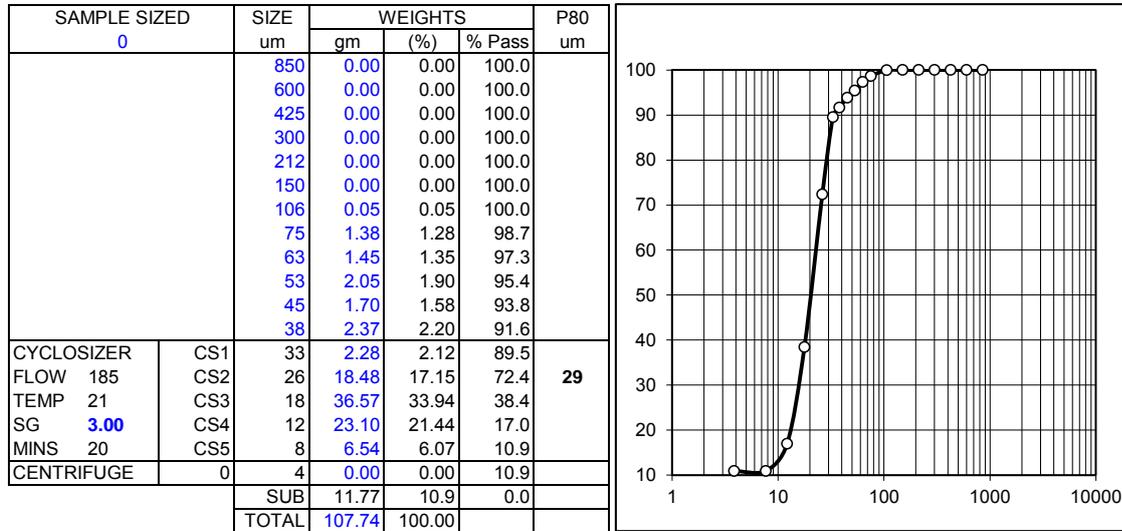
PROJECT	T0879
SAMPLE	LC01 Cyc11-31 Fine Tail +40
TEST NO	
DATE	61114
TECHNICIAN	MS





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	LC01 Cyc11-31 Fine Tail -40
TEST NO	
DATE	61114
TECHNICIAN	MS





BURNIE LABORATORY: BATCH UF FALCON SEPARATION

PROJECT	T0879
TEST NO	T25
DATE	120814
TECHNICIAN	ID

CONDITIONS

Separation of	Sn
Feed Pulp Density (%)	12
Feed In Time (min)	16
UF-100 Speed (g's)	218
Total Feed Weight (gm)	3987.7
Calc Feed Rate (gm/min)	249.2

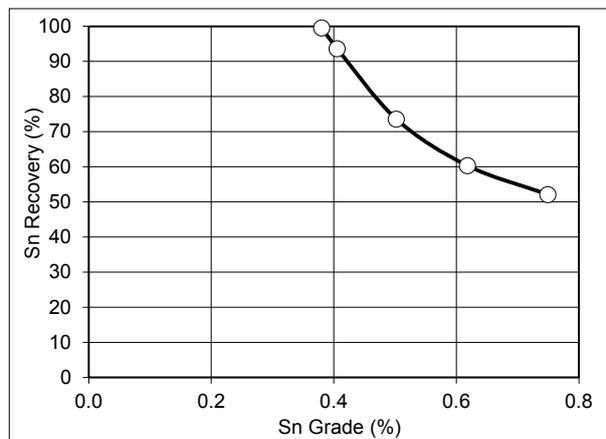
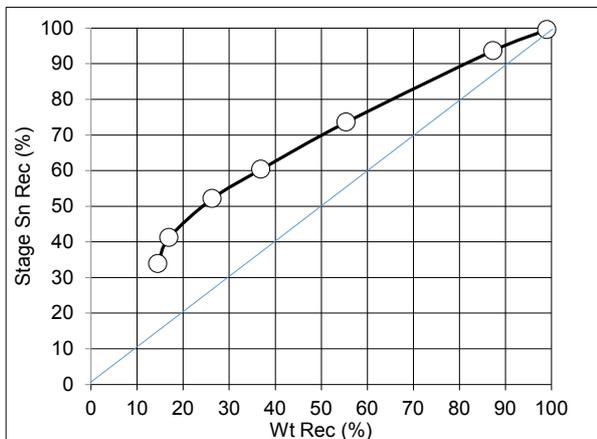
34.3 Ltr H2O

FEED MATERIAL
LC01 cyc 1-6
Mozley tail -106

Product	Feed on Time (min)	Product Mass (gm)	Product Mass (%)	Calc Feed Mass (gm)	Calc Mass to Conc (gm)	Calc Mass to Conc (%)	Sn Tail (%)	Sn Dist (%)	Sn Stage Rec (%)	Sn Calc Conc (%)
Tail	1.00	2.3	0.1	249.2	246.9	99.1	0.19	0.0	99.5	0.38
Tail	2.00	60.8	1.5	498.5	435.4	87.3	0.19	0.8	93.6	0.41
Tail	4.00	381.1	9.6	996.9	552.7	55.4	0.23	5.8	73.6	0.50
Tail	6.00	499.3	12.5	1495.4	551.9	36.9	0.25	8.3	60.3	0.62
Tail	8.00	525.8	13.2	1993.9	524.6	26.3	0.26	9.1	52.1	0.75
Tail	12.00	1015.1	25.5	2990.8	508.7	16.9	0.30	20.2	41.2	0.92
Tail	16.00	923.6	23.2	3987.7	579.7	14.5	0.36	22.0	33.8	0.88
Conc		579.7	14.5				0.88	33.8		
Total		3987.7	100.0				0.38	100.0		
Head							0.52			

	Fe %	Dist %	S %	Dist %	SiO2 %	Dist %	Al2O3 %	Dist %	As %	Dist %
Tail	12.25	0.0	1.11	0.0	57.20	0.1	10.30	0.1	0.08	0.1
Tail	11.00	1.0	0.64	0.7	60.50	1.9	8.66	1.7	0.05	1.0
Tail	13.95	7.9	0.97	6.4	53.40	10.4	8.36	10.0	0.05	6.1
Tail	16.00	11.9	1.20	10.4	51.20	13.1	8.23	13.0	0.07	11.1
Tail	16.45	12.9	1.40	12.8	48.90	13.2	8.08	13.4	0.06	10.0
Tail	17.25	26.1	1.10	19.3	49.00	25.5	7.98	25.5	0.07	22.6
Tail	17.15	23.6	1.72	27.5	48.00	22.7	7.75	22.6	0.08	23.5
SRT Con	19.20	16.6	2.28	22.9	43.80	13.0	7.52	13.7	0.14	25.8
Calc Head	16.83	100.0	1.45	100.0	48.88	100.0	7.95	100.0	0.08	100.0
Assay Head	17.45		1.79		46.60		7.66		0.1	

*Number in red means less





BURNIE LABORATORY: BATCH UF FALCON SEPARATION

PROJECT	T0879
TEST NO	T26
DATE	180814
TECHNICIAN	ID

CONDITIONS

Separation of	Sn
Feed Pulp Density (%)	12
Feed In Time (min)	8
UF-100 Speed (g's)	218
Total Feed Weight (gm)	1206.6
Calc Feed Rate (gm/min)	150.8

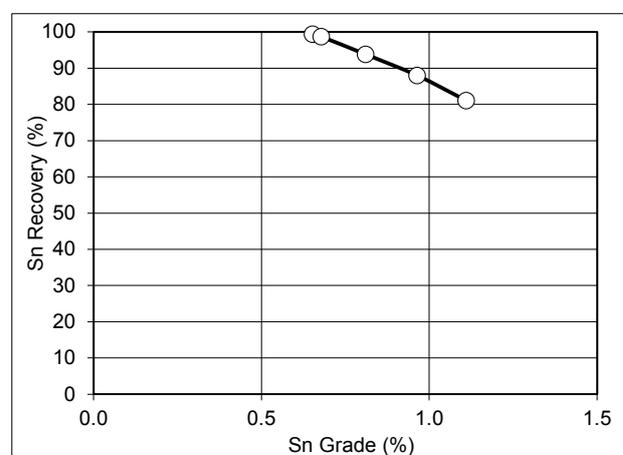
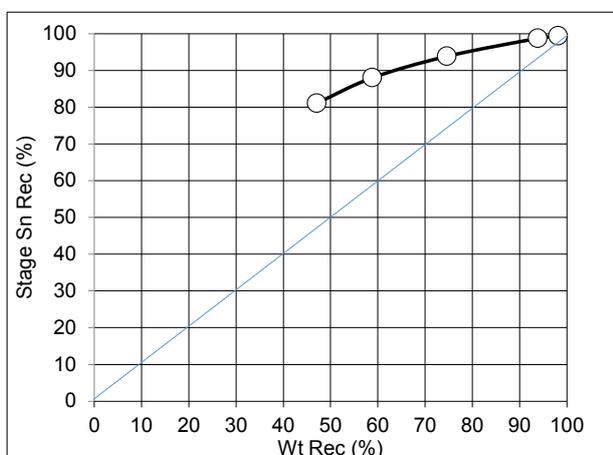
32.2 Ltr H2O

FEED MATERIAL
LC01 cyc 1-6
-106 Mozley tail
-38um

Product	Feed on Time (min)	Product Mass (gm)	Product Mass (%)	Calc Feed Mass (gm)	Calc Mass to Conc (gm)	Calc Mass to Conc (%)	Sn Tail (%)	Sn Dist (%)	Sn Stage Rec (%)	Sn Calc Conc (%)
Tail	1.00	2.8	0.2	150.8	148.0	98.1	0.23	0.1	99.3	0.65
Tail	2.00	15.8	1.3	301.7	283.1	93.8	0.12	0.2	98.7	0.68
Tail	4.00	134.7	11.2	603.3	450.0	74.6	0.16	2.8	93.8	0.81
Tail	6.00	219.2	18.2	905.0	532.5	58.8	0.21	5.9	88.0	0.96
Tail	8.00	266.1	22.1	1206.6	568.0	47.1	0.29	9.9	81.1	1.11
Conc		568.0	47.1				1.11	81.1		
Total		1206.6	100.0				0.64	100.0		
Head							0.58			

	Fe %	Dist %	S %	Dist %	SiO2 %	Dist %	Al2O3 %	Dist %	As %	Dist %
Tail	17.45	0.2	1.93	0.2	40.20	0.2	14.00	0.4	0.11	0.2
Tail	10.35	0.6	0.61	0.3	61.90	2.1	9.49	1.7	0.05	0.5
Tail	14.95	7.6	0.85	3.7	52.80	15.5	8.75	13.3	0.07	5.7
Tail	18.80	15.5	1.34	9.5	44.20	21.1	8.10	20.0	0.06	8.0
Tail	21.00	21.0	1.89	16.3	40.80	23.7	7.73	23.2	0.08	13.0
SRT Con	25.90	55.2	3.79	69.9	30.10	37.3	6.44	41.3	0.21	72.6
Calc Head	22.08	100.0	2.55	100.0	38.00	100.0	7.34	100.0	0.14	100.0
Assay Head	21.70		2.45		38.30		7.36		0.12	

*Number in red means less





WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

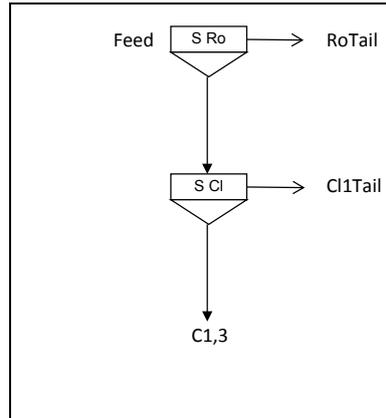
HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 8 – Gravity Concentrate Dressing

PROJECT	T0879
TEST NO	T30
DATE	270814
TECHNICIAN	MJR

Milling			
Mill	type		
Media	type		
Media	kg		
Solids	g		
Water	g		
Time	min		
Speed	rpm		
Lime	g		
End pH	pH		
End p80	µm		



PRODUCT FLOATED
LC01 Comb Conc Cyc 1-6

NOTES
Sulphide Rougher/Cleaner

Float Cell	Volume	Regrind Power
Rougher	0.5	Start
Cleaner	0.5	Finish
Speed	850	W/h kWh/t

	pH	100 H2SO4 g/t	1 ASS g/t	1 CuSO4 g/t	0.1 PAX g/t		0.495 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	4.3								2					
Condition	3.6		248						2					
Condition				62					2					
Condition					31		61		1					
S Ro Conc 1	4.1									2-5	2.0	2.0	100	
Condition					47		46		1					
S Ro Conc 2	4.4									2-5	3.0	5.0	200	
Condition		16			47		77		1					
S Ro Conc 3	4.7									2-5	5.0	10.0	400	
Condition			93						1					
Condition							46		1					
S Cl1 C1	4.0									1-3	2.0	2.0	150	56
Condition					9		46		1					
S Cl1 C2	4.3									2-4	3.0	5.0	100	13
Condition					16		31		1					
S Cl1 C3	4.6									2-5	3.0	8.0	150	4
REAGENT TOTALS (g/t)		16	341	62	149		307							

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
S Cl1C1	83.6	25.9	0.62	0.87	42.8	33.0	2.60	79.6	47.1	78.9	1.81	11.7	0.04	1.9
S Cl1C2	13.2	4.1	2.28	0.50	40.7	5.0	1.89	9.1	30.3	8.0	4.15	4.2	0.13	1.0
S Cl1C3	5.6	1.7	6.39	0.60	37.3	1.9	0.62	1.3	23.1	2.6	6.15	2.7	0.30	1.0
S Cl1 Tail	9.0	2.8	20.0	3.01	31.7	2.6	0.45	1.5	7.39	1.3	5.64	3.9	0.51	2.6
Ro Tail	210.8	65.43	27.0	95.0	29.6	57.5	0.11	8.5	2.16	9.1	4.77	77.5	0.78	93.6
CALC	322.2	100.0	18.6	100.0	33.7	100.0	0.85	100.0	15.5	100.0	4.02	100.0	0.55	100.0
ASSAY HEAD			19.2		34.4		0.91		12.3		3.84		0.53	

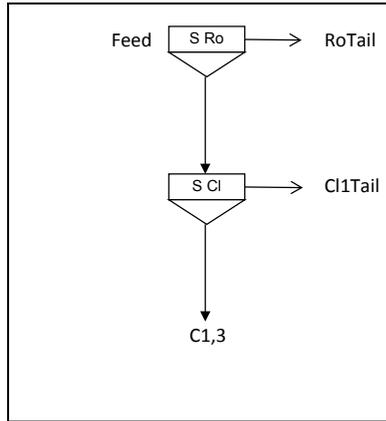
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
S Cl1C1	83.6	25.9	0.62	0.9	42.8	33.0	2.60	79.6	47.1	78.9	1.81	11.7	0.04	1.9
S Cl1C2	96.8	30.0	0.85	1.4	42.5	37.9	2.50	88.8	44.8	86.9	2.13	15.9	0.05	2.9
S Cl1C3	102.4	31.8	1.15	2.0	42.2	39.9	2.40	90.0	43.6	89.5	2.35	18.5	0.07	3.8
S Cl1 Tail	111.4	34.6	2.67	5.0	41.4	42.5	2.24	91.5	40.7	90.9	2.61	22.5	0.10	6.4
FEED	322.2	100.0	18.6	100.0	33.7	100.0	0.85	100.0	15.5	100.0	4.02	100.0	0.55	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	C %	DIST	C organic %	DIST	C inorg %	DIST
S Cl1C1	83.6	25.9	0.12	6.8	0.24	4.4	0.58	10.9	0.59	6.5	0.04	5.4	0.54	6.4
S Cl1C2	13.2	4.1	0.30	2.7	0.71	2.1	1.41	4.2	1.65	2.8	0.16	3.4	1.50	2.8
S Cl1C3	5.6	1.7	0.47	1.8	1.38	1.7	2.13	2.7	2.81	2.1	0.25	2.2	2.55	2.0
S Cl1 Tail	9.0	2.8	0.52	3.2	1.72	3.4	1.98	4.0	3.36	4.0	0.31	4.5	3.06	3.9
Ro Tail	210.8	65.4	0.60	85.6	1.89	88.3	1.65	78.2	3.07	84.7	0.25	84.5	2.83	84.8
CALC	322.2	100.0	0.46	100.0	1.40	100.0	1.38	100.0	2.37	100.0	0.19	100.0	2.18	100.0
ASSAY HEAD			0.43		1.40		1.33		2.34		0.48		1.86	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorg %	CUM
S Cl1C1	83.6	25.9	0.12	6.8	0.24	4.4	0.58	10.9	0.59	6.5	0.04	5.4	0.54	6.4
S Cl1C2	96.8	30.0	0.14	9.5	0.30	6.5	0.69	15.1	0.73	9.3	0.06	8.8	0.67	9.2
S Cl1C3	102.4	31.8	0.16	11.2	0.36	8.2	0.77	17.8	0.85	11.4	0.07	11.0	0.77	11.3
S Cl1 Tail	111.4	34.6	0.19	14.4	0.47	11.7	0.87	21.8	1.05	15.3	0.09	15.5	0.96	15.2
FEED	322.2	100.0	0.46	100.0	1.40	100.0	1.38	100.0	2.37	100.0	0.19	100.0	2.18	100.0

PROJECT	T0879
TEST NO	T49
DATE	311014
TECHNICIAN	MJR

Milling			
Mill	type		
Media	type		
Media	kg		
Solids	g		
Water	g		
Time	min		
Speed	rpm		
Lime	g		
End pH	pH		
End p80	µm		



PRODUCT FLOATED
LC01 Comb Conc Cyc 11-31

NOTES
Sulphide Rougher/Cleaner Feed +106 1021g, -106 915g

Float Cell	Volume	Regrind Power
Rougher	3.8	Start
Cleaner	1.5	Finish
Speed	850	W/h kWh/t

	pH	100 H2SO4 g/t	1 ASS g/t	1 CuSO4 g/t	0.2 PAX g/t		0.495 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	4.2								2					
Condition	3.9		254						2					
Condition				62					2					
Condition					31		18		1					
S Ro Conc 1	4.1									2-5	2.5	2.5	500	
Condition					31		13		1					
S Ro Conc 2	4.2									2-5	3.5	6.0	300	
Condition					42		13		1					
S Ro Conc 3	4.4									2-5	5.0	11.0	400	
Condition			104						1					
Condition							8		1					
S Cl1 C1	4.0									1-3	1.5	1.5	500	70
Condition					9		8		1					
S Cl1 C2	4.2									2-4	3.0	4.5	300	55
Condition					16		5		1					
S Cl1 C3	4.4									2-5	3.0	7.5	150	22
REAGENT TOTALS (g/t)			358	62	129		64							

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T49 S Cl1C1	348.4	18.1	0.74	0.89	44.2	22.6	2.14	53.9	40.2	55.2	1.62	6.0	0.04	0.9
S Cl1C2	165.6	8.6	1.06	0.61	42.7	10.4	2.47	29.6	40.2	26.3	2.39	4.2	0.08	0.9
S Cl1C3	32.3	1.7	5.24	0.59	41.3	2.0	1.73	4.0	21.8	2.8	5.57	1.9	0.29	0.6
S Cl1 Tail	20.1	1.0	18.2	1.26	32.9	1.0	0.49	0.7	8.73	0.7	5.66	1.2	0.72	1.0
Ro Tail	1360.4	70.60	20.5	96.6	32.2	64.2	0.12	11.8	2.80	15.0	6.03	86.7	1.06	96.6
CALC	1926.8	100.0	15.0	100.0	35.4	100.0	0.72	100.0	13.2	100.0	4.91	100.0	0.77	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T49 S Cl1C1	348.4	18.1	0.74	0.9	44.2	22.6	2.14	53.9	40.2	55.2	1.62	6.0	0.04	0.9
S Cl1C2	514.0	26.7	0.84	1.5	43.7	32.9	2.25	83.5	40.2	81.5	1.87	10.2	0.05	1.8
S Cl1C3	546.3	28.4	1.10	2.1	43.6	34.9	2.22	87.5	39.1	84.3	2.09	12.1	0.07	2.4
S Cl1 Tail	566.4	29.4	1.71	3.4	43.2	35.8	2.15	88.2	38.0	85.0	2.21	13.3	0.09	3.4
FEED	1926.8	100.0	15.0	100.0	35.4	100.0	0.72	100.0	13.2	100.0	4.91	100.0	0.77	100.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	C %	DIST	C organic %	DIST	C inorg %	DIST
T49 S Cl1C1	348.4	18.1	0.09	2.6	0.20	2.2	0.45	4.8	0.46	3.1	0.08	16.0	0.38	2.6
S Cl1C2	165.6	8.6	0.15	2.0	0.34	1.8	0.69	3.5	0.87	2.8	0.10	9.5	0.77	2.5
S Cl1C3	32.3	1.7	0.37	1.0	1.08	1.1	1.85	1.8	2.29	1.4	0.15	2.8	2.14	1.4
S Cl1 Tail	20.1	1.0	0.49	0.8	1.69	1.1	1.91	1.2	3.42	1.3	0.14	1.6	3.29	1.3
Ro Tail	1360.4	70.6	0.84	93.6	2.16	93.8	2.11	88.6	3.49	91.4	0.09	70.2	3.40	92.1
CALC	1926.8	100.0	0.63	100.0	1.63	100.0	1.68	100.0	2.70	100.0	0.09	100.0	2.61	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00		0.00	

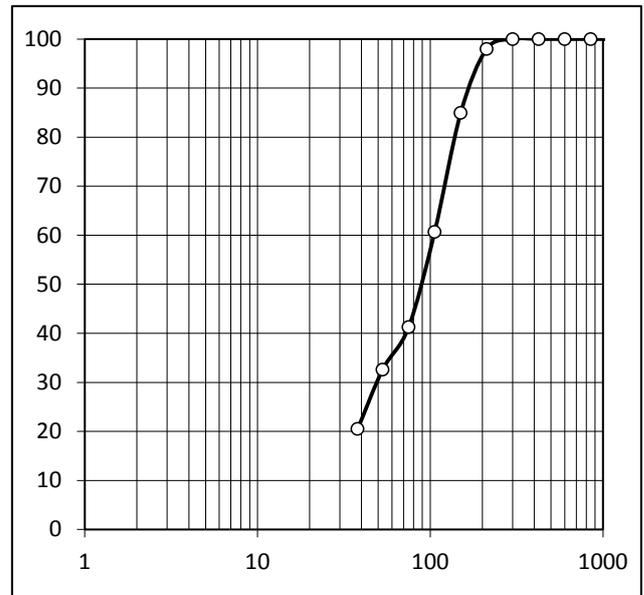
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorg %	CUM
T49 S Cl1C1	348.4	18.1	0.09	2.6	0.20	2.2	0.45	4.8	0.46	3.1	0.08	16.0	0.38	2.6
S Cl1C2	514.0	26.7	0.11	4.6	0.25	4.0	0.53	8.4	0.59	5.9	0.09	25.5	0.51	5.2
S Cl1C3	546.3	28.4	0.12	5.6	0.29	5.1	0.61	10.2	0.69	7.3	0.09	28.2	0.60	6.6
S Cl1 Tail	566.4	29.4	0.14	6.4	0.34	6.2	0.65	11.4	0.79	8.6	0.09	29.8	0.70	7.9
FEED	1926.8	100.0	0.63	100.0	1.63	100.0	1.68	100.0	2.70	100.0	0.09	100.0	2.61	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	RoT+CL1T 1000G Mags
TEST NO	T49
DATE	7/11/2014
TECHNICIAN	MS

RoT+CL1T 1000G Mags T49		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	1700	0.00	0.00	100.0	
	1180	0.00	0.00	100.0	
	850	0.00	0.00	100.0	
	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	0.00	0.00	100.0	
	212	0.95	2.01	98.0	
	150	6.17	13.07	84.9	
141	106	11.45	24.25	60.7	
	75	9.15	19.38	41.3	
	53	4.10	8.68	32.6	
	38	5.71	12.09	20.5	
CYCLOSIZER	CS1	37	0.00	0.00	20.5
FLOW 185	CS2	29	0.00	0.00	20.5
TEMP 21	CS3	20	0.00	0.00	20.5
SG 2.50	CS4	14	0.00	0.00	20.5
MINS 20	CS5	9	0.00	0.00	20.5
		SUB	9.68	20.50	0.0
		TOTAL	47.21	100.00	



ANALYSES

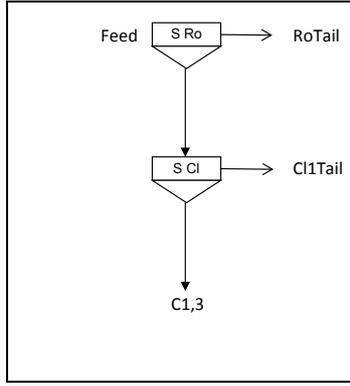
SIZE um	WT %	Sn		Fe		As		S		SiO2		Mn	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	15.08	2.58	16.2	62.70	15.6	0.09	19.3	2.12	27.3	2.72	9.9	0.30	7.1
106	24.25	1.20	12.2	59.50	23.8	0.07	24.1	1.90	39.3	3.71	21.7	0.75	28.5
75	19.38	1.20	9.7	54.70	17.5	0.05	13.8	1.48	24.5	5.42	25.3	1.27	38.6
53	8.68	1.31	4.8	65.90	9.4	0.06	7.4	0.28	2.1	3.41	7.1	0.37	5.0
38	12.09	0.94	4.7	66.70	13.3	0.07	12.0	0.25	2.6	4.00	11.7	0.31	5.9
-38	20.50	6.12	52.4	60.00	20.3	0.08	23.3	0.24	4.2	4.93	24.4	0.46	14.8
CALC	100.00	2.40	100.0	60.58	100.0	0.07	100.0	1.17	100.0	4.15	100.0	0.64	100.0
ASSAY	200.00	2.89		59.10		0.06		1.22		4.20		0.66	

ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
150	15.08	0.13	9.0	2.01	12.7	0.44	10.0				
106	24.25	0.23	25.6	2.84	28.8	0.66	24.1				
75	19.38	0.36	32.1	3.43	27.8	1.21	35.3				
53	8.68	0.11	4.4	1.58	5.7	0.29	3.8				
38	12.09	0.13	7.2	1.27	6.4	0.27	4.9				
-38	20.50	0.23	21.7	2.18	18.7	0.71	21.9				
CALC HEAD	100.00	0.22	100.0	2.39	100.0	0.66	100.0				
ASSAY	200.00	0.22		2.18		0.71					

PROJECT	T0879
TEST NO	T57
DATE	241114
TECHNICIAN	MJR

Milling			
Mill	type		
Media	type		
Media	kg		
Solids	g		
Water	g		
Time	min		
Speed	rpm		
Lime	g		
End pH	pH		
End p80	µm		



PRODUCT FLOATED
LC01 Comb Conc Cyc 11-31

NOTES
Sulphide Rougher/Cleaner Feed
T50 Non Mags 435.8
T55 Non Mags 39.4

Float Cell	Volume	Regrind Power
Rougher	3.8	Start
Cleaner	1.5	Finish
Speed	850	W/h kWh/t

	pH	100 H2SO4 g/t	1 ASS g/t	1 CuSO4 g/t	0.2 PAX g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Condition	4.2						2					
Condition	3.9		254	64			2					
Condition					30	42	2					
Condition					30	21	1	2-5	2.0	2.0	100	
S Ro Conc 1	4.1				30	21	1	2-5	3.0	5.0	200	
Condition					64	31	1	2-5	5.0	10.0	350	
S Ro Conc 2	4.2											
Condition			127				1					
S Ro Conc 3	4.4						1					
Condition						31	1	1-3	1.5	1.5	80	21
S Cl1 C1	4.0				8	21	1	2-4	1.5	3.0	80	#REF!
Condition					17	21	1	2-5	3.0	6.0	200	9
S Cl1 C2	4.2											
Condition												
S Cl1 C3	4.4											
REAGENT TOTALS (g/t)			381	64	148	168						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T57 S Cl1C1+2	17.1	3.6	2.85	0.40	38.4	6.2	0.52	16.6	28.9	41.4	6.55	3.4	0.36	1.0
S Cl1C3	18.1	3.8	4.90	0.72	36.9	6.3	0.28	9.4	19.0	28.7	7.55	4.1	0.50	1.5
S Cl1 Tail	20.1	4.3	12.6	2.06	29.3	5.5	0.11	4.1	3.60	6.1	9.66	5.9	1.34	4.3
Ro Tail	417.1	88.29	28.4	96.8	20.9	82.0	0.09	69.9	0.68	23.8	6.87	86.6	1.39	93.2
CALC	472.4	100.0	25.9	100.0	22.5	100.0	0.11	100.0	2.53	100.0	7.00	100.0	1.32	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T57 S Cl1C1+2	17.1	3.6	2.85	0.4	38.4	6.2	0.52	16.6	28.9	41.4	6.55	3.4	0.36	1.0
S Cl1C3	35.2	7.5	3.90	1.1	37.6	12.5	0.40	26.0	23.8	70.2	7.06	7.5	0.43	2.4
S Cl1 Tail	55.3	11.7	7.05	3.2	34.6	18.0	0.29	30.1	16.4	76.2	8.01	13.4	0.76	6.8
FEED	472.4	100.0	25.9	100.0	22.5	100.0	0.11	100.0	2.53	100.0	7.00	100.0	1.32	100.0

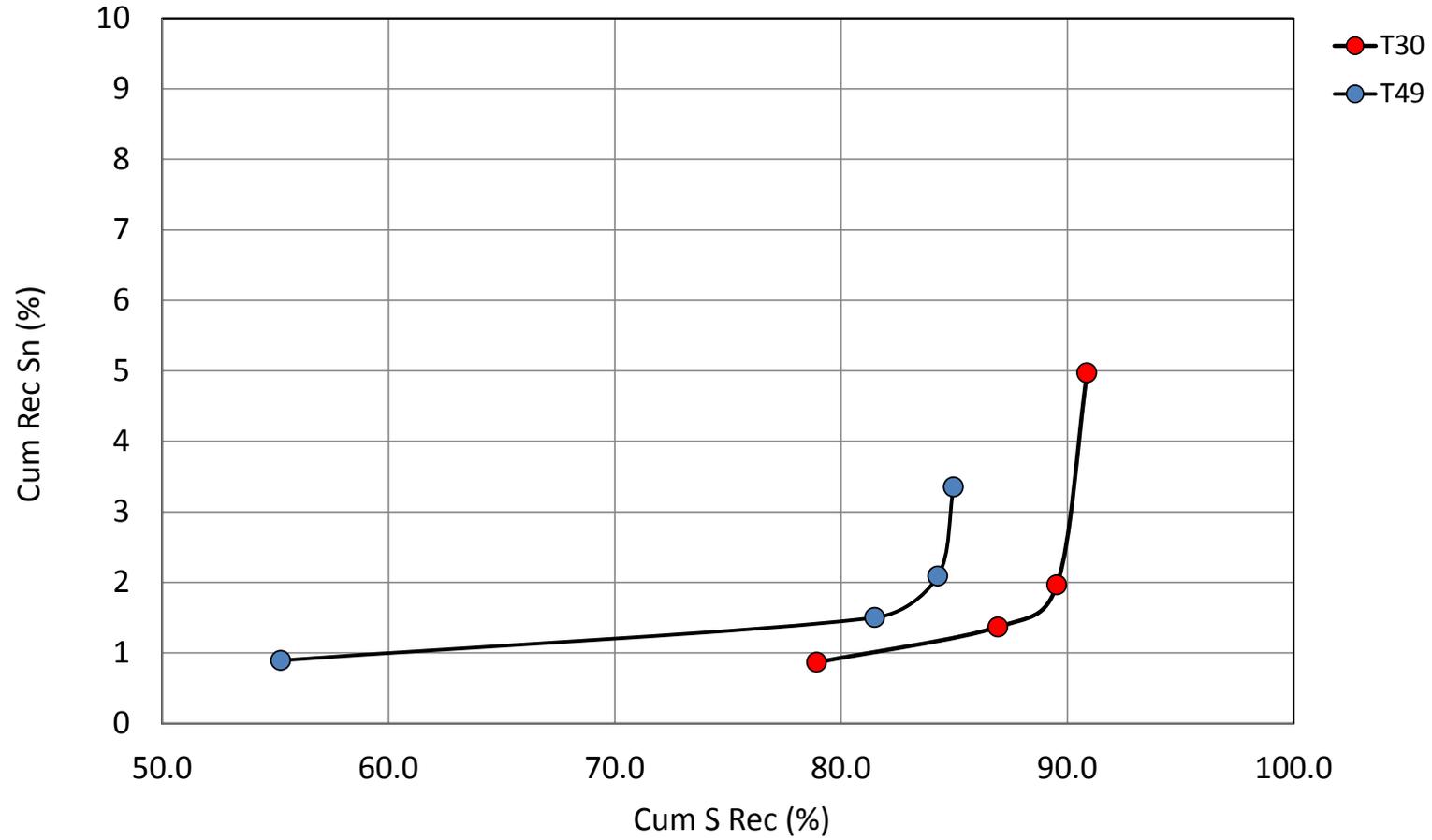
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	C %	DIST	C organic %	DIST	C inorg %	DIST
T57 S Cl1C1+2	17.1	3.6	0.40	1.3	2.01	2.9	1.82	2.4	2.37	1.9	0.22	9.3	2.15	1.8
S Cl1C3	18.1	3.8	0.58	2.0	1.81	2.8	2.61	3.6	3.32	2.9	0.20	9.0	3.12	2.7
S Cl1 Tail	20.1	4.3	0.76	3.0	3.93	6.7	3.18	4.9	4.91	4.7	0.19	9.5	4.72	4.6
Ro Tail	417.1	88.3	1.15	93.6	2.48	87.6	2.79	89.1	4.57	90.5	0.07	72.3	4.50	90.9
CALC	472.4	100.0	1.08	100.0	2.50	100.0	2.76	100.0	4.46	100.0	0.09	100.0	4.37	100.0
ASSAY HEAD			0.00		0.00		0.00		0.00		0.00		0.00	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorg %	CUM
T57 S Cl1C1+2	17.1	3.6	0.40	1.3	2.01	2.9	1.82	2.4	2.37	1.9	0.22	9.3	2.15	1.8
S Cl1C3	35.2	7.5	0.49	3.4	1.91	5.7	2.23	6.0	2.86	4.8	0.21	18.3	2.65	4.5
S Cl1 Tail	55.3	11.7	0.59	6.4	2.64	12.4	2.57	10.9	3.60	9.5	0.20	27.7	3.40	9.1
FEED	472.4	100.0	1.08	100.0	2.50	100.0	2.76	100.0	4.46	100.0	0.09	100.0	4.37	100.0

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
Ro Tail+Cl1 Tail+Cl1 C3	455.3	96.4	26.8	99.6	21.9	93.8	0.10	83.4	1.54	58.6	7.02	96.6	1.35	99.0
Ro Tail+Cl1 Tail	437.2	92.5	27.7	98.9	21.3	87.5	0.09	74.0	0.81	29.8	7.00	92.5	1.39	97.6
Ro Tail	417.1	88.3	28.4	96.8	20.9	82.0	0.09	69.9	0.68	23.8	6.87	86.6	1.39	93.2

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorg %	CUM
Ro Tail+Cl1 Tail+Cl1 C3	455.3	96.4	1.11	98.7	2.52	97.1	2.80	97.6	4.54	98.1	0.08	90.7	4.45	98.2
Ro Tail+Cl1 Tail	437.2	92.5	1.13	96.6	2.55	94.3	2.81	94.0	4.59	95.2	0.08	81.7	4.51	95.5
Ro Tail	417.1	88.3	1.15	93.6	2.48	87.6	2.79	89.1	4.57	90.5	0.07	72.3	4.50	90.9

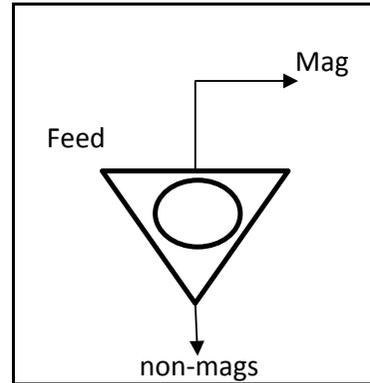
Cleaner Sulphur Recovery vs Tin Recovery



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T34
DATE	
TECH	MW

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	T30 Sulphide Tails
Current (A)	
Magnetic intense1 (G)	1000.0
Magnetic intense2 (G)	
Comments	Pre mag sep.



FEED MATERIAL T 30 sulphide tail	
FROM TEST NO	T30
START WT (gm)	100.60

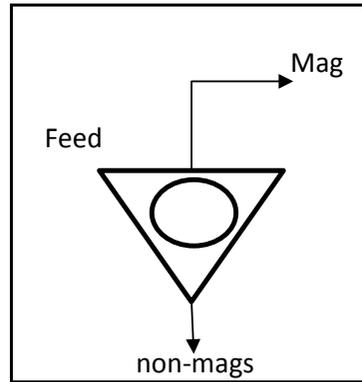
MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	25.5	25.5	25.35	1.37	1.5	63.20	50.7	4.23	20.2	0.99	14.5	0.15	5.4
Non Magnetics	75.1	75.1	74.65	31.50	98.5	20.90	49.3	5.69	79.8	1.98	85.5	0.90	94.6
TOTAL	100.60		100.00	23.86	100.0	31.62	100.0	5.32	100.0	1.73	100.0	0.71	100.0

BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T50
DATE	06/11/14
TECH	MW

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	T49 Ro Tail+Cl1 Tail
Current (A)	
Magnetic intense1 (G)	1000.0
Magnetic intense2 (G)	
Comments	



FEED MATERIAL	
T49 Ro Tail+Cl1 Tail	
FROM TEST NO	T49
START WT (gm)	1299.28

Await for CO3

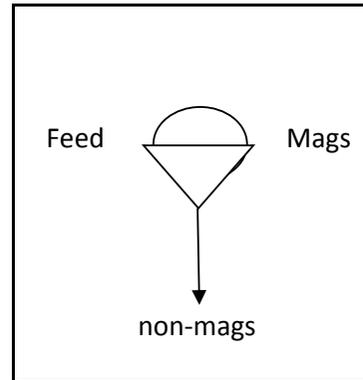
MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	342.8	342.8	26.38	2.89	3.8	59.10	48.3	4.20	17.2	1.22	10.3	0.22	6.4
Non Magnetics	894.3	894.3	68.83	27.60	94.6	21.80	46.5	7.03	75.3	2.43	53.6	1.19	90.9
>300um	62.2	62.18	4.79	6.72	1.6	35.40	5.2	10.05	7.5	23.50	36.1	0.51	2.7
TOTAL	1299.28		100.00	20.08	100.0	32.29	100.0	6.43	100.0	3.12	100.0	0.90	100.0

BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T55
DATE	191114
TECH	ID

TEST TYPE	SALA Wet Drum
Feed Solids (g)	286.0
Feed Water (L)	
Pump Flow Rate (lpm)	1.2
Density (%)	
Time (min)	6.3
Pump 01 Output (%)	
Pump 02 Output (%)	
Comments	No pumps, water hose, sample washed in



FEED MATERIAL	
1000 Gauss Mags ground to P80=34	
FROM TEST NO	T50
START WT (gm)	286

MAGNETIC SEPARATION RESULTS

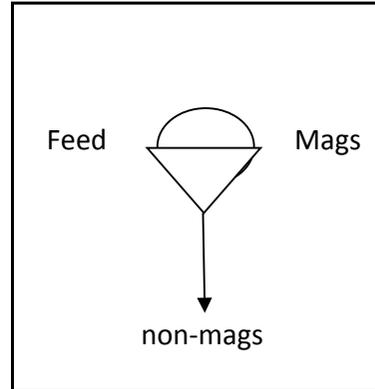
PRODUCT				Tin		Iron		Silica		Sulphur			
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)		
Magnetics	227.3	227.3	80.04	0.48	15.6	67.90	90.1	2.80	51.5	0.62	43.5		
Non Magnetics(calc)	56.7	56.7	19.96	10.45	84.4	30.00	9.9	10.55	48.5	3.23	56.5		
TOTAL	284.00		100.00	2.47	100.0	60.33	100.0	4.35	100.0	1.14	100.0		



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T35
DATE	010914
TECH	ID

TEST TYPE	SALA Wet Drum
Feed Solids (g)	1897.0
Feed Water (L)	20.0
Pump Flow Rate (lpm)	1.5
Density (%)	8.0
Time (min)	18.0
Pump 01 Output (%)	60
Pump 02 Output (%)	60
Comments	



FEED MATERIAL	
Sulphide float tails	
FROM TEST NO	
START WT (gm)	1897

MAGNETIC SEPARATION RESULTS

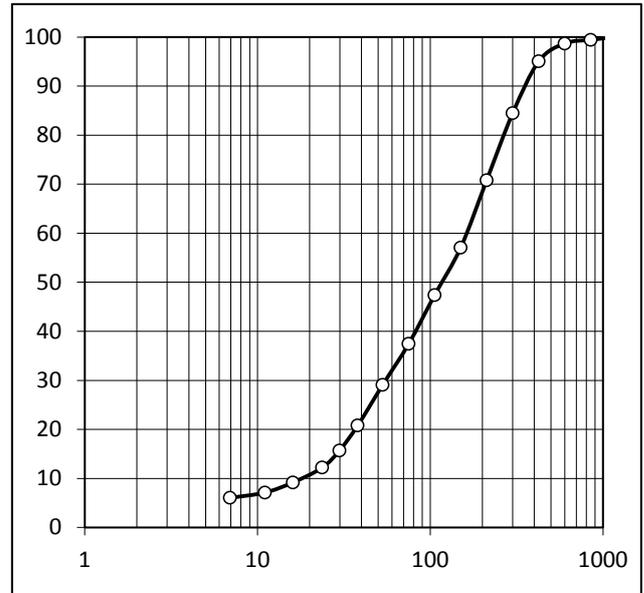
PRODUCT			Tin		Iron		Silica		Sulphur		Calcium Oxide		
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	84.3	84.3	4.44	0.83	2.8	49.70	11.2	12.95	1.4	4.76	7.0	0.32	1.5
Non Magnetics	1812.7	1812.7	95.56	1.32	97.2	18.25	88.8	42.20	98.6	2.96	93.0	0.96	98.5
TOTAL	1897.00		100.00	1.30	100.0	19.65	100.0	40.90	100.0	3.04	100.0	0.93	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	T35 Mags
DATE	100914
TECHNICIAN	MS

T35 Mags		SIZE um	WEIGHTS			
			gm	(%)	%PASS	
p80		1700	0.00	0.00	100.0	
		1180	0.00	0.00	100.0	
		850	0.35	0.56	99.4	
		600	0.46	0.74	98.7	
		425	2.25	3.62	95.1	
	271		300	6.57	10.58	84.5
			212	8.51	13.70	70.8
			150	8.52	13.72	57.1
			106	6.01	9.68	47.4
			75	6.18	9.95	37.4
	53	5.20	8.37	29.1		
	38	5.14	8.28	20.8		
CYCLOSIZER	CS1	30	3.16	5.09	15.7	
FLOW 185	CS2	24	2.17	3.49	12.2	
TEMP 21	CS3	16	1.87	3.01	9.2	
SG 3.50	CS4	11	1.29	2.08	7.1	
MINS 20	CS5	7	0.67	1.08	6.0	
	SUB		3.75	6.04	0.0	
	TOTAL		62.10	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	42.93	0.96	49.7	46.90	40.5	0.07	33.4	3.34	30.1	13.90	46.1	0.41	44.0
75	19.63	0.63	14.9	54.80	21.6	0.09	19.6	7.52	31.0	10.40	15.8	0.36	17.7
38	16.65	1.08	21.7	59.60	20.0	0.13	24.1	5.41	18.9	6.68	8.6	0.37	15.4
24	8.58	0.72	7.4	44.50	7.7	0.14	13.4	3.76	6.8	18.75	12.4	0.46	9.9
7	6.17	0.71	5.3	53.40	6.6	0.08	5.5	5.19	6.7	10.20	4.9	0.39	6.0
CALC<7	6.04	0.15	1.1	29.34	3.6	0.06	4.1	5.07	6.4	26.34	12.3	0.47	7.0
ASSAY	100.00	0.83	100.0	49.70	100.0	0.09	100.0	4.76	100.0	12.95	100.0	0.40	100.0

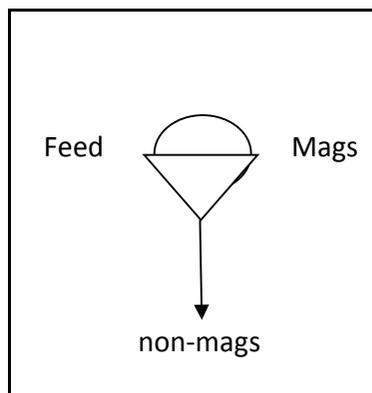
ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3					
		%	dist	%	dist	%	dist				
150	42.93	0.32	42.9	7.47	64.4	1.80	37.5				
75	19.63	0.32	19.6	2.78	11.0	1.56	14.9				
38	16.65	0.29	15.1	1.66	5.6	0.98	7.9				
24	8.58	0.61	16.4	2.86	4.9	3.18	13.2				
7	6.17	0.28	5.4	4.47	5.5	1.44	4.3				
CALC<7	6.04	0.03	0.6	7.12	8.6	7.55	22.1				
ASSAY	100.00	0.32	100.0	4.98	100.0	2.06	100.0				

BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T47
DATE	101014
TECH	ID

TEST TYPE	SALA Wet Drum
Feed Solids (g)	1000.0
Feed Water (L)	10.0
Pump Flow Rate (lpm)	1.4
Density (%)	10.0
Time (min)	7.3
Pump 01 Output (%)	52
Pump 02 Output (%)	52
Comments	



FEED MATERIAL	
-38 from LC01 cyc 1-10	
-106 Mozley tail	
FROM TEST NO	LC01
START WT (gm)	1000

MAGNETIC SEPARATION RESULTS

PRODUCT			Tin		Iron		Silica		Sulphur				
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)		
Magnetics	98.8	98.8	9.88	0.61	15.5	37.90	22.4	23.10	11.9	4.93	32.3		
Non Magnetics(calc)	901.2	901.2	90.12	0.37	84.5	14.40	77.6	18.72	88.1	1.14	67.7		
TOTAL	1000.00		100.00	0.39	100.0	16.72	100.0	19.15	100.0	1.51	100.0		



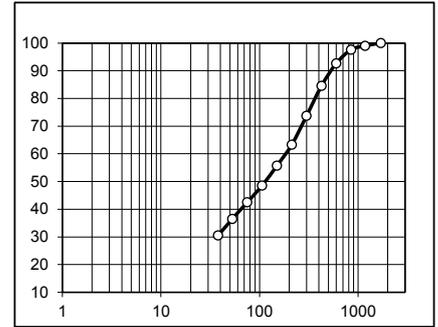
BURNIE LABORATORY: SIZE AND MAGNETIC SEPARATION ANALYSIS

PROJECT	T0879
SAMPLE	Bulk Sulphide Tail
FROM TEST NO	
DATE	110914
TECHNICIAN	DG

RAPID MAGNETIC SEPERATION RECOVERY ON FRACTIONS (3000 Gauss)

SIZING

SIZE um	WEIGHTS	
	(%)	%PASS
150	44.29	100
75	13.19	86.8
38	12.00	74.8
20	7.00	67.8
<20	23.52	44.3
TOTAL	100.00	



SEPARATIONS

Products	WT %	WT %	Fraction									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150	29.77	13.19	0.72	23.7	31.80	52.2	23.50	15.2	1.63	16.9	0.73	25.6
Non Mags+150	70.23	31.10	0.98	76.3	12.35	47.8	55.50	84.8	3.39	83.1	0.90	74.4
Calc +150 Total	100.00	44.29	0.90	100.0	18.14	100.0	45.97	100.0	2.87	100.0	0.85	100.0
Mags+75	23.60	3.11	0.75	9.7	36.40	44.8	17.00	9.1	2.44	21.0	0.57	12.9
Non Mags+75	76.40	10.08	2.15	90.3	13.85	55.2	52.20	90.9	2.84	79.0	1.19	87.1
Calc +75 Total	100.00	13.19	1.82	100.0	19.17	100.0	43.89	100.0	2.75	100.0	1.04	100.0
Mags+38	14.02	1.68	0.70	4.5	40.30	28.2	15.65	5.2	3.63	18.0	0.48	6.3
Non Mags+38	85.98	10.32	2.42	95.5	16.75	71.8	46.10	94.8	2.69	82.0	1.16	93.7
Calc +38 Total	100.00	12.00	2.18	100.0	20.05	100.0	41.83	100.0	2.82	100.0	1.06	100.0
Mags+20	7.12	0.50	0.56	1.7	53.20	17.6	9.70	1.8	4.32	13.5	0.36	2.3
Non Mags+20	92.88	6.50	2.47	98.3	19.05	82.4	39.90	98.2	2.13	86.5	1.17	97.7
Calc +20 Total	100.00	7.00	2.33	100.0	21.48	100.0	37.75	100.0	2.29	100.0	1.11	100.0
-20		23.52	1.21		22.90		33.40		2.52		0.92	
CALC FEED		100.00	1.35		19.86		41.67		2.72		0.94	
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	

SUMMARY

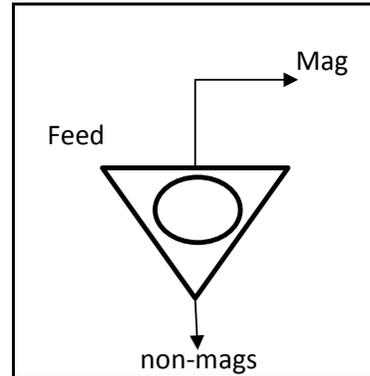
FRACTIONS um	Picno SG	WT %	Overall									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150		13.19	0.72	7.04	31.80	21.11	23.50	7.44	1.63	7.89	0.73	10.28
Mags+75		3.11	0.75	1.73	36.40	5.71	17.00	1.27	2.44	2.79	0.57	1.90
Mags+38		1.68	0.70	0.87	40.30	3.41	15.65	0.63	3.63	2.24	0.48	0.86
Mags+20		0.50	0.56	0.21	53.20	1.34	9.70	0.12	4.32	0.79	0.36	0.19
Non Mags+150		31.10	0.98	22.59	12.35	19.34	55.50	41.43	3.39	38.73	0.90	29.91
Non Mags+75		10.08	2.15	16.06	13.85	7.03	52.20	12.62	2.84	10.51	1.19	12.81
Non Mags+38		10.32	2.42	18.51	16.75	8.70	46.10	11.42	2.69	10.19	1.16	12.79
Non Mags+20		6.50	2.47	11.90	19.05	6.24	39.90	6.23	2.13	5.09	1.17	8.13
Total Mags		18.48	0.72	9.85	33.93	31.57	21.32	9.45	2.02	13.72	0.67	13.24
Total Non Mags		58.00	1.61	69.06	14.14	41.31	51.51	71.69	3.03	64.52	1.03	63.64
-20		23.52	1.21	21.09	22.90	27.12	33.40	18.85	2.52	21.77	0.92	23.12
CALC FEED		100.00	1.35	100.00	19.86	100.00	41.67	100.00	2.72	100.00	0.94	100.00
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T39-1
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	3000.0
Magnetic intense2 (G)	
Comments	+150 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

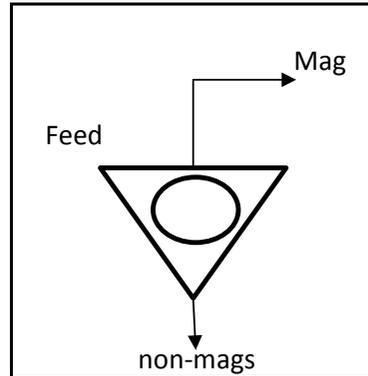
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	18.6	18.55	29.77	0.72	23.7	31.80	52.2	23.50	15.2	1.63	16.9	0.73	25.6
Non Magnetics	43.8	43.76	70.23	0.98	76.3	12.35	47.8	55.50	84.8	3.39	83.1	0.90	74.4
TOTAL	62.31		100.00	0.90	100.0	18.14	100.0	45.97	100.0	2.87	100.0	0.85	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T39-2
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	3000.0
Magnetic intense2 (G)	
Comments	+75 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

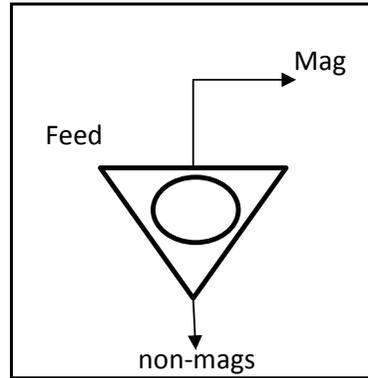
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	5.9	5.91	23.60	0.75	9.7	36.40	44.8	17.00	9.1	2.44	21.0	0.57	12.9
Non Magnetics	19.1	19.13	76.40	2.15	90.3	13.85	55.2	52.20	90.9	2.84	79.0	1.19	87.1
TOTAL	25.04		100.00	1.82	100.0	19.17	100.0	43.89	100.0	2.75	100.0	1.04	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T39-3
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	3000.0
Magnetic intense2 (G)	
Comments	+38 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

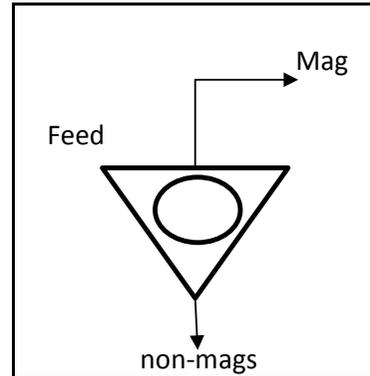
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	2.8	2.82	14.02	0.70	4.5	40.30	28.2	15.65	5.2	3.63	18.0	0.48	6.3
Non Magnetics	17.3	17.3	85.98	2.42	95.5	16.75	71.8	46.10	94.8	2.69	82.0	1.16	93.7
TOTAL	20.12		100.00	2.18	100.0	20.05	100.0	41.83	100.0	2.82	100.0	1.06	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T39-4
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	3000.0
Magnetic intense2 (G)	
Comments	+20 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	0.8	0.8	7.12	0.56	1.7	53.20	17.6	9.70	1.8	4.32	13.5	0.36	2.3
Non Magnetics	10.4	10.43	92.88	2.47	98.3	19.05	82.4	39.90	98.2	2.13	86.5	1.17	97.7
TOTAL	11.23		100.00	2.33	100.0	21.48	100.0	37.75	100.0	2.29	100.0	1.11	100.0



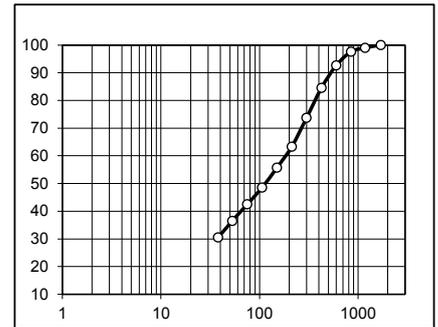
BURNIE LABORATORY: SIZE AND MAGNETIC SEPARATION ANALYSIS

PROJECT	T0879
SAMPLE	Bulk Sulphide Tail
FROM TEST NO	
DATE	110914
TECHNICIAN	DG

RAPID MAGNETIC SEPERATION RECOVERY ON FRACTIONS (6000 Gauss)

SIZING

SIZE um	WEIGHTS	
	(%)	%PASS
150	44.29	100
75	13.19	86.8
38	12.00	74.8
20	7.00	67.8
<20	23.52	44.3
TOTAL	100.00	



SEPARATIONS

Products	WT %	WT %	Fraction									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150	72.26	32.00	0.72	62.2	21.20	89.6	38.20	58.7	2.48	60.0	0.73	63.1
Non Mags+150	27.74	12.29	1.14	37.8	6.44	10.4	70.10	41.3	4.31	40.0	1.11	36.9
Calc +150 Total	100.00	44.29	0.84	100.0	17.11	100.0	47.05	100.0	2.99	100.0	0.84	100.0
Mags+75	65.79	8.68	0.87	35.5	25.50	89.5	30.20	45.2	1.84	45.8	0.72	45.6
Non Mags+75	34.21	4.51	3.04	64.5	5.74	10.5	70.30	54.8	4.18	54.2	1.65	54.4
Calc +75 Total	100.00	13.19	1.61	100.0	18.74	100.0	43.92	100.0	2.64	100.0	1.04	100.0
Mags+38	61.50	7.38	0.85	24.2	28.60	86.6	26.30	39.2	1.58	34.2	0.71	40.6
Non Mags+38	38.50	4.62	4.26	75.8	7.06	13.4	65.10	60.8	4.85	65.8	1.66	59.4
Calc +38 Total	100.00	12.00	2.16	100.0	20.31	100.0	41.24	100.0	2.84	100.0	1.08	100.0
Mags+20	68.17	4.77	1.06	31.6	26.90	84.4	29.20	52.8	1.75	51.3	0.87	54.0
Non Mags+20	31.83	2.23	4.92	68.4	10.65	15.6	55.90	47.2	3.56	48.7	1.59	46.0
Calc +20 Total	100.00	7.00	2.29	100.0	21.73	100.0	37.70	100.0	2.33	100.0	1.10	100.0
-20		23.52	1.21		22.90		33.40		2.52		0.92	
CALC FEED		100.00	1.29		19.39		42.07		2.77		0.93	
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	

SUMMARY

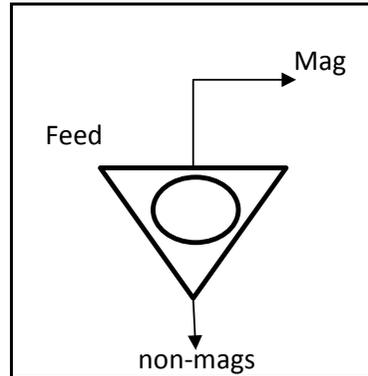
FRACTIONS um	Picno SG	WT %	Overall									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150		32.00	0.72	17.90	21.20	34.99	38.20	29.06	2.48	28.68	0.73	25.14
Mags+75		8.68	0.87	5.86	25.50	11.41	30.20	6.23	1.84	5.77	0.72	6.72
Mags+38		7.38	0.85	4.87	28.60	10.89	26.30	4.61	1.58	4.21	0.71	5.64
Mags+20		4.77	1.06	3.93	26.90	6.62	29.20	3.31	1.75	3.02	0.87	4.47
Non Mags+150		12.29	1.14	10.88	6.44	4.08	70.10	20.47	4.31	19.13	1.11	14.67
Non Mags+75		4.51	3.04	10.65	5.74	1.34	70.30	7.54	4.18	6.82	1.65	8.01
Non Mags+38		4.62	4.26	15.28	7.06	1.68	65.10	7.15	4.85	8.10	1.66	8.25
Non Mags+20		2.23	4.92	8.52	10.65	1.22	55.90	2.96	3.56	2.87	1.59	3.81
Total Mags		52.83	0.79	32.56	23.45	63.90	34.41	43.21	2.18	41.68	0.74	41.97
Total Non Mags		23.65	2.47	45.33	6.82	8.32	67.82	38.12	4.32	36.91	1.37	34.75
-20		23.52	1.21	22.10	22.90	27.77	33.40	18.67	2.52	21.42	0.92	23.28
CALC FEED		100.00	1.29	100.00	19.39	100.00	42.07	100.00	2.77	100.00	0.93	100.00
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T40-1
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	6000.0
Magnetic intense2 (G)	
Comments	+150 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

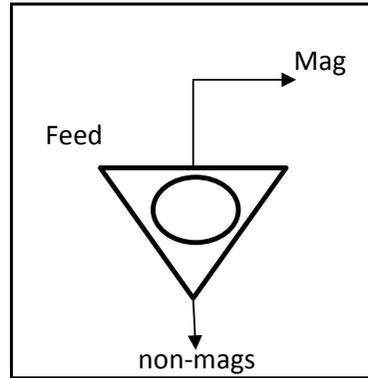
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	44.9	44.86	72.26	0.72	62.2	21.20	89.6	38.20	58.7	2.48	60.0	0.73	63.1
Non Magnetics	17.2	17.22	27.74	1.14	37.8	6.44	10.4	70.10	41.3	4.31	40.0	1.11	36.9
TOTAL	62.08		100.00	0.84	100.0	17.11	100.0	47.05	100.0	2.99	100.0	0.84	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T40-2
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	6000.0
Magnetic intense2 (G)	
Comments	+75 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

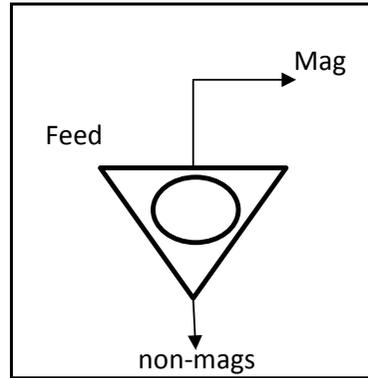
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	16.5	16.48	65.79	0.87	35.5	25.50	89.5	30.20	45.2	1.84	45.8	0.72	45.6
Non Magnetics	8.6	8.57	34.21	3.04	64.5	5.74	10.5	70.30	54.8	4.18	54.2	1.65	54.4
TOTAL	25.05		100.00	1.61	100.0	18.74	100.0	43.92	100.0	2.64	100.0	1.04	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T40-3
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	6000.0
Magnetic intense2 (G)	
Comments	+38 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

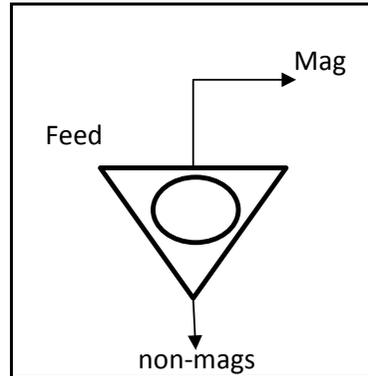
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	12.4	12.43	61.50	0.85	24.2	28.60	86.6	26.30	39.2	1.58	34.2	0.71	40.6
Non Magnetics	7.8	7.78	38.50	4.26	75.8	7.06	13.4	65.10	60.8	4.85	65.8	1.66	59.4
TOTAL	20.21		100.00	2.16	100.0	20.31	100.0	41.24	100.0	2.84	100.0	1.08	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T40-4
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	6000.0
Magnetic intense2 (G)	
Comments	+20 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	7.9	7.88	68.17	1.06	31.6	26.90	84.4	29.20	52.8	1.75	51.3	0.87	54.0
Non Magnetics	3.7	3.68	31.83	4.92	68.4	10.65	15.6	55.90	47.2	3.56	48.7	1.59	46.0
TOTAL	11.56		100.00	2.29	100.0	21.73	100.0	37.70	100.0	2.33	100.0	1.10	100.0



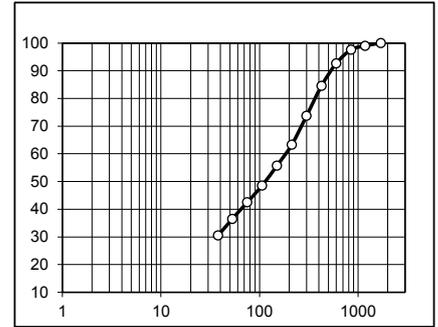
BURNIE LABORATORY: SIZE AND MAGNETIC SEPARATION ANALYSIS

PROJECT	T0879
SAMPLE	Bulk Sulphide Tail
FROM TEST NO	
DATE	110914
TECHNICIAN	DG

RAPID MAGNETIC SEPERATION RECOVERY ON FRACTIONS (10000 Gauss)

SIZING

SIZE um	WEIGHTS	
	(%)	%PASS
150	44.29	100
75	13.19	86.8
38	12.00	74.8
20	7.00	67.8
<20	23.52	44.3
TOTAL	100.00	



SEPARATIONS

Products	WT %	WT %	Fraction									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150	92.18	40.83	0.81	86.7	18.30	97.9	44.50	87.3	2.77	88.1	0.80	88.4
Non Mags+150	7.82	3.46	1.46	13.3	4.71	2.1	76.20	12.7	4.40	11.9	1.24	11.6
Calc +150 Total	100.00	44.29	0.86	100.0	17.24	100.0	46.98	100.0	2.90	100.0	0.83	100.0
Mags+75	92.18	12.16	0.81	86.7	18.30	97.9	44.50	87.3	2.77	88.1	0.80	88.4
Non Mags+75	7.82	1.03	1.46	13.3	4.71	2.1	76.20	12.7	4.40	11.9	1.24	11.6
Calc +75 Total	100.00	13.19	0.86	100.0	17.24	100.0	46.98	100.0	2.90	100.0	0.83	100.0
Mags+38	73.43	8.81	1.16	39.3	25.40	92.2	30.80	54.9	2.13	51.9	0.78	54.1
Non Mags+38	26.57	3.19	4.95	60.7	5.90	7.8	70.00	45.1	5.46	48.1	1.83	45.9
Calc +38 Total	100.00	12.00	2.17	100.0	20.22	100.0	41.21	100.0	3.01	100.0	1.06	100.0
Mags+20	76.32	5.34	1.23	39.7	26.40	93.0	28.70	58.6	1.56	54.1	0.84	58.4
Non Mags+20	23.68	1.66	6.02	60.3	6.42	7.0	65.40	41.4	4.26	45.9	1.93	41.6
Calc +20 Total	100.00	7.00	2.36	100.0	21.67	100.0	37.39	100.0	2.20	100.0	1.10	100.0
-20		23.52	1.21		22.90		33.40		2.52		0.92	
CALC FEED		100.00	1.20		19.24		42.42		2.77		0.90	
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	

SUMMARY

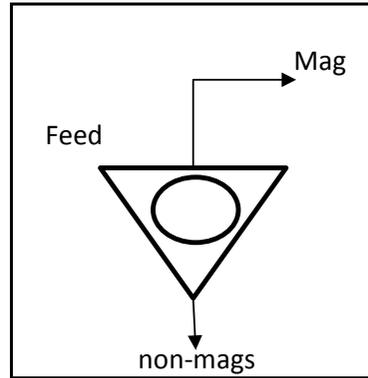
FRACTIONS um	Picno SG	WT %	Overall									
			%Sn	dist	%Fe	dist	%SiO2	dist	%S	dist	%CaO	dist
Mags+150		40.83	0.81	27.45	18.30	38.84	44.50	42.83	2.77	40.77	0.80	36.29
Mags+75		12.16	0.81	8.17	18.30	11.57	44.50	12.75	2.77	12.14	0.80	10.81
Mags+38		8.81	1.16	8.48	25.40	11.63	30.80	6.40	2.13	6.77	0.78	7.64
Mags+20		5.34	1.23	5.45	26.40	7.33	28.70	3.61	1.56	3.00	0.84	4.99
Non Mags+150		3.46	1.46	4.20	4.71	0.85	76.20	6.22	4.40	5.49	1.24	4.77
Non Mags+75		1.03	1.46	1.25	4.71	0.25	76.20	1.85	4.40	1.64	1.24	1.42
Non Mags+38		3.19	4.95	13.10	5.90	0.98	70.00	5.26	5.46	6.28	1.83	6.48
Non Mags+20		1.66	6.02	8.28	6.42	0.55	65.40	2.56	4.26	2.55	1.93	3.55
Total Mags		67.14	0.89	49.56	19.88	69.37	41.44	65.59	2.59	62.68	0.80	59.73
Total Non Mags		9.34	3.46	26.82	5.42	2.63	72.17	15.89	4.74	15.95	1.56	16.23
-20		23.52	1.21	23.62	22.90	28.00	33.40	18.52	2.52	21.37	0.92	24.04
CALC FEED		100.00	1.20	100.00	19.24	100.00	42.42	100.00	2.77	100.00	0.90	100.00
ASSAY HEAD			1.34		19.55		40.90		3.08		0.95	



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T41-1
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	10000.0
Magnetic intense2 (G)	
Comments	+150 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

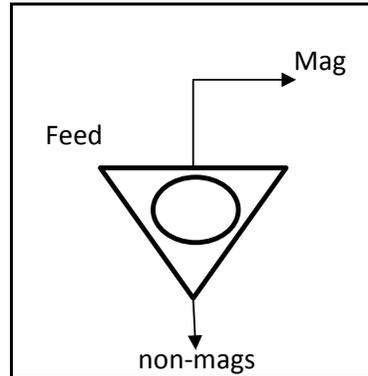
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	56.6	56.6	92.18	0.81	86.7	18.30	97.9	44.50	87.3	2.77	88.1	0.80	88.4
Non Magnetics	4.8	4.8	7.82	1.46	13.3	4.71	2.1	76.20	12.7	4.40	11.9	1.24	11.6
TOTAL	61.40		100.00	0.86	100.0	17.24	100.0	46.98	100.0	2.90	100.0	0.83	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T41-2
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	10000.0
Magnetic intense2 (G)	
Comments	+75 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

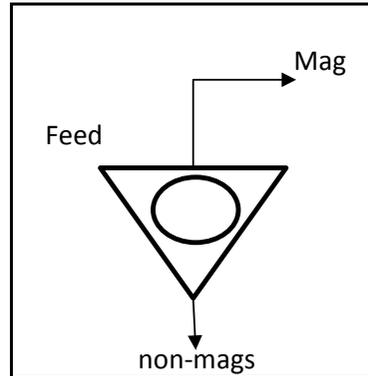
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	56.6	56.6	92.18	0.81	86.7	18.30	97.9	44.50	87.3	2.77	88.1	0.80	88.4
Non Magnetics	4.8	4.8	7.82	1.46	13.3	4.71	2.1	76.20	12.7	4.40	11.9	1.24	11.6
TOTAL	61.40		100.00	0.86	100.0	17.24	100.0	46.98	100.0	2.90	100.0	0.83	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T41-3
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	10000.0
Magnetic intense2 (G)	
Comments	+38 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

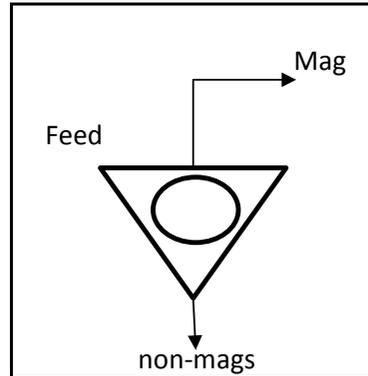
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	14.9	14.87	73.43	1.16	39.3	25.40	92.2	30.80	54.9	2.13	51.9	0.78	54.1
Non Magnetics	5.4	5.38	26.57	4.95	60.7	5.90	7.8	70.00	45.1	5.46	48.1	1.83	45.9
TOTAL	20.25		100.00	2.17	100.0	20.22	100.0	41.21	100.0	3.01	100.0	1.06	100.0



BURNIE LABORATORY: MAGNETIC SEPARATION REPORT SHEET

PROJECT	T0887
TEST NO	T41-4
DATE	110914
TECH	DG

TEST TYPE	Rapid Mag Sep
Feed Solids (g)	Sulphide Bulk Tail
Current (A)	
Magnetic intense1 (G)	10000.0
Magnetic intense2 (G)	
Comments	+20 um fraction



FEED MATERIAL	
Sulphide Bulk Tail	
FROM TEST NO	
START WT (gm)	

MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
Magnetics	8.8	8.8	76.32	1.23	39.7	26.40	93.0	28.70	58.6	1.56	54.1	0.84	58.4
Non Magnetics	2.7	2.73	23.68	6.02	60.3	6.42	7.0	65.40	41.4	4.26	45.9	1.93	41.6
TOTAL	11.53		100.00	2.36	100.0	21.67	100.0	37.39	100.0	2.20	100.0	1.10	100.0



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 9 – Final Gravity Concentrate Analysis

Element	Sn	Fe	As	S	SiO ₂	Mn	CaO	MgO	Al ₂ O ₃	C _{total}	C _{organic}
Units	%	%	%	%	%	%	%	%	%	%	%
Sample Description											
T66 End Leach Res A	54.4	3.80	0.13	1.13	13.5	0.11	0.7	0.56	2.84	0.61	0.16
T66 End Leach Res B	56.1	3.83	0.13	1.16	12.8	0.11	0.71	0.56	2.73	0.57	0.14
Final Gravity Concentrate	55.3	3.82	0.13	1.15	13.1	0.11	0.71	0.56	2.785	0.59	0.15
T66 Leach Feed	28.8	21	0.08	0.66	7	1.09	1.17	2.57	2.65	4.45	0.09

C _{inorganic} %	Ag ppm	Al %	As ppm	Au ppm	B ppm	Ba ppm	Be ppm	Bi ppm	Ca %	Cd ppm	Ce ppm	Co ppm	Cr ppm	Cs ppm	Cu ppm	Fe %
0.44	3.28	0.2	100	0.2	20	190	2.7	18.7	0.4	<0.01	59	5	240	1.6	154	3.10
0.43	3.12	0.2	93.9	<0.2	20	180	2.9	18.1	0.4	<0.01	60	4.7	273	1.5	146	3.02
0.435	3.2	0.2	97	0.2	20	185	2.8	18.4	0.4	<0.01	59	4.9	257	1.6	150	3.06
4.36	1.67	0.9	125	<0.2	20	120	4.4	52.2	0.7	<0.01	39	3.4	122	3.8	127	19.3

Ga	Ge	Hf	Hg	In	K	La	Li	Mg	Mn	Mo	Na	Nb	Ni	P	Pb	Rb	Re
ppm	ppm	ppm	ppm	ppm	%	ppm	ppm	%	ppm	ppm	%	ppm	ppm	ppm	ppm	ppm	ppm
1.8	0.1	0.2	0.3	1.11	0.1	28	6.8	0.2	978	137	0	<0.05	30	90	685	15	0
1.8	0.1	0.2	0.3	1.12	0.1	28	6.8	0.2	917	129	0	<0.05	28	90	630	15	0
1.8	0.1	0.2	0.3	1.11	0.1	28	6.8	0.2	948	133	0	<0.05	29	90	658	15	0
6.3	0.3	0.2	0.2	7.28	0.1	17	18	1.3	9860	78.9	0	0.14	15	440	377	23	0

S	Sb	Sc	Se	Sn	Sr	Ta	Te	Th	Ti	Tl	U	V	W	Y	Zn	Zr
%	ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	%	ppm						
1.3	5.8	1.2	0.2	490	36	<0.01	0.01	2.1	0.01	0.3	0.6	6	145	5.7	57	5.1
1.3	5.6	1.1	0.3	500	34	<0.01	0.01	2.0	0.01	0.3	0.5	6	145	5.7	54	5.0
1.3	5.7	1.2	0.3	495	35	<0.01	0.01	2.1	0.01	0.3	0.5	6	145	5.7	56	5.1
0.7	6	7	0.3	166	35	<0.01	0	1.8	0.01	0.4	0.8	39	560	8.3	98	5.7



McKnight
Mineralogy

ABN 65962932907

PO Box 451 Buninyong
VIC 3357

Ph 03 53279262

M 0407860394

s.mcknight@ballarat.edu.au

mineralogy@hotmail.net.au

**QXRD Analysis of Leach
Sample Supplied by ALS
Metallurgy Burnie
(amended)**

Attn: John Glen

S W McKnight
16/12/2014

Samples Supplied

Leach Con: 879733 T66 END LEACH RESIDUE

Phases Identified in the Sample

Cassiterite
Siderite
Quartz
Dravite
Rutile

Pyrrhotite
Gypsum
Scheelite
Pyrite
Topaz

Arsenopyrite?
Zircon
Phlogopite
Rhodocrosite?

Results – semiquantitative – amended to 55.0 wt% Sn as per assay:

Phase	Weight%
Arsenopyrite	0.2
Cassiterite	70.1
Chlorite	0
Diopside	0
Dolomite	0
Dravite	4.2
Gypsum	0.9
Marcasite	0
Microcline	0
Phlogopite	0
Pyrite	0.7
Pyrrhotite-4C	1
Quartz	7.4
Rhodocrosite?	0.4
Rutile	1.6
Scheelite	0.7
Siderite	12
Topaz	0.6
Zircon	0.1



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 10 – De-sliming Results

Test 27
Cyclone u/f
Mass split: 41.49

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
300	150	18.05	0.62	10.3	15.80	14.9	0.08	10.3	2.51	19.7	50.90	19.5	0.42	12.4	0.79	14.0	3.64	17.8	9.00	20.4
126	106	5.78	0.84	4.5	15.50	4.7	0.05	2.1	1.66	4.2	51.40	6.3	0.52	4.9	0.89	5.0	3.62	5.7	8.05	5.8
89	75	7.22	0.78	5.2	15.35	5.8	0.09	4.6	1.77	5.6	52.90	8.1	0.50	5.9	0.91	6.4	3.49	6.8	7.76	7.0
63	53	8.54	0.83	6.5	16.30	7.2	0.10	6.1	1.75	6.5	54.10	9.8	0.55	7.7	0.97	8.1	3.42	7.9	7.58	8.1
49	45	4.38	0.89	3.6	16.70	3.8	0.09	2.8	2.02	3.8	50.80	4.7	0.56	4.0	0.99	4.2	3.30	3.9	7.14	3.9
41	38	4.31	0.93	3.7	17.65	4.0	0.11	3.4	1.51	2.8	51.60	4.7	0.61	4.3	1.08	4.6	3.54	4.1	7.35	4.0
33	29	7.41	2.75	18.7	25.00	9.6	0.22	11.6	3.76	12.1	31.30	4.9	0.90	10.9	1.19	8.6	3.05	6.1	6.02	5.6
19	13	29.49	1.13	30.6	19.85	30.5	0.19	40.0	2.13	27.3	42.80	26.8	0.66	31.9	1.13	32.7	3.51	28.0	6.99	25.9
10	8	7.81	1.05	7.5	22.00	8.9	0.26	14.5	3.00	10.2	37.60	6.2	0.65	8.3	1.12	8.6	3.76	8.0	7.43	7.3
3	Cal <8	7.03	1.49	9.6	29.00	10.6	0.09	4.5	2.55	7.8	59.52	8.9	0.83	9.6	1.12	7.7	6.09	11.6	13.47	11.9
	ASSAY	100.00	1.09	100.0	19.20	100.0	0.14	100.0	2.30	100.0	47.10	100.0	0.61	100.0	1.02	100.0	3.69	100.0	7.96	100.0

Cyclone o/f
Mass split: 58.51

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
300	150																			
126	106																			
89	75																			
63	53																			
49	45																			
41	38																			
33	29																			
19	13																			
10	8	8.89	0.69	15.0	19.40	8.5	0.18	8.4	2.60	6.6	42.20	10.1	0.55	11.9	1.04	11.9	3.70	7.9	7.78	5.9
3	CALC<8	91.11	0.38	85.0	20.28	91.5	0.19	91.6	3.58	93.4	36.71	89.9	0.40	88.1	0.75	88.1	4.24	92.1	12.03	94.1
	ASSAY	100.00	0.41	100.0	20.20	100.0	0.19	100.0	3.49	100.0	37.20	100.0	0.41	100.0	0.78	100.0	4.19	100.0	11.65	100.0

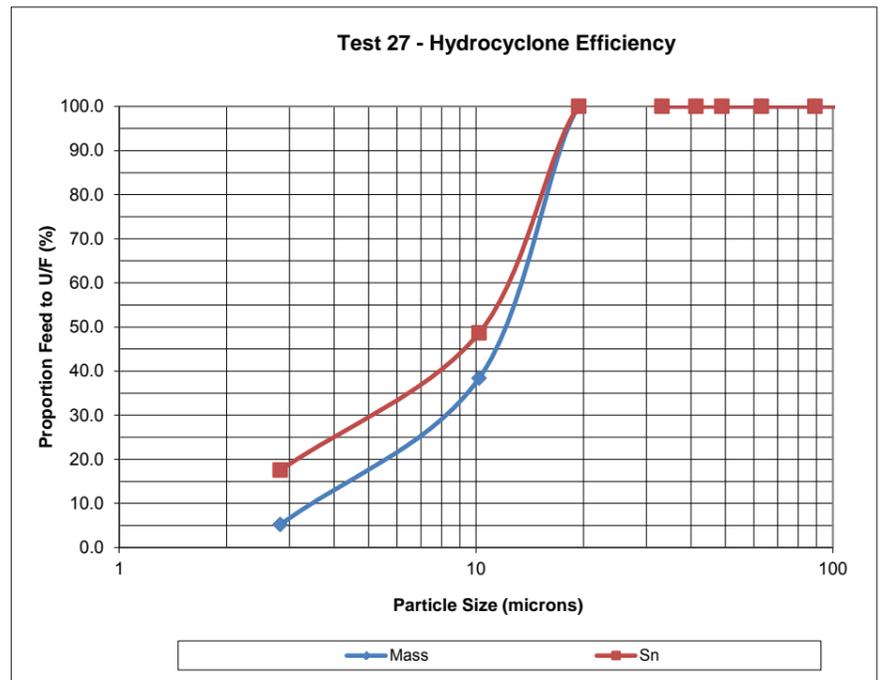
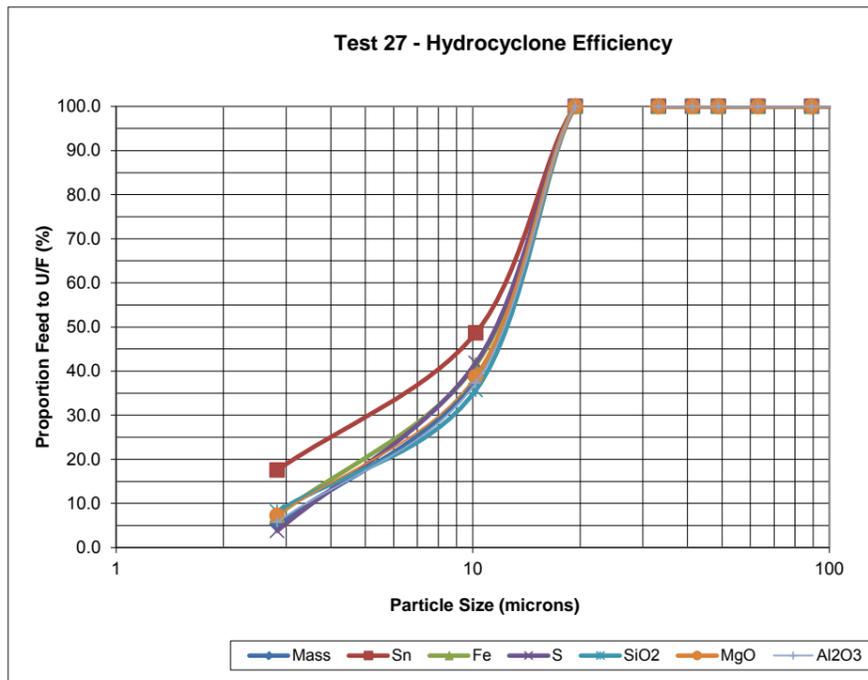
Cyclone feed
Mass split: 100.00

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist														
300	150	7.49	0.62	6.7	15.8	6.0	0.08	3.5	2.51	6.3	50.9	9.2	0.42	6.4	0.79	6.7	3.64	6.8	9.0	6.7
126	106	2.40	0.84	2.9	15.5	1.9	0.05	0.7	1.66	1.3	51.4	3.0	0.52	2.5	0.89	2.4	3.62	2.2	8.1	1.9
89	75	2.99	0.78	3.4	15.4	2.3	0.09	1.6	1.77	1.8	52.9	3.8	0.50	3.0	0.91	3.1	3.49	2.6	7.8	2.3
63	53	3.54	0.83	4.2	16.3	2.9	0.10	2.1	1.75	2.1	54.1	4.6	0.55	4.0	0.97	3.9	3.42	3.0	7.6	2.7
49	45	1.82	0.89	2.3	16.7	1.5	0.09	1.0	2.02	1.2	50.8	2.2	0.56	2.1	0.99	2.0	3.30	1.5	7.1	1.3
41	38	1.79	0.93	2.4	17.7	1.6	0.11	1.2	1.51	0.9	51.6	2.2	0.61	2.2	1.08	2.2	3.54	1.6	7.4	1.3
33	29	3.07	2.75	12.2	25.0	3.9	0.22	4.0	3.76	3.9	31.3	2.3	0.90	5.6	1.19	4.2	3.05	2.4	6.0	1.8
19	13	12.24	1.13	20.0	19.9	12.3	0.19	13.7	2.13	8.7	42.8	12.7	0.66	16.4	1.13	15.7	3.51	10.8	7.0	8.5
10	8	8.44	0.83	10.1	20.4	8.7	0.21	10.5	2.75	7.8	40.4	8.3	0.59	10.1	1.07	10.3	3.72	7.9	7.6	6.4
3	<8	56.22	0.44	35.7	20.7	58.9	0.19	61.7	3.52	66.1	37.9	51.6	0.42	47.8	0.77	49.5	4.33	61.2	12.1	67.2
	ASSAY	100.00	0.69	100.0	19.8	100.0	0.17	100.0	3.00	100.0	41.3	100.0	0.49	100.0	0.88	100.0	3.98	100.0	10.1	100.0

Recoveries to u/f

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist																
300	150	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
126	106	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
89	75	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
63	53	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
49	45	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
41	38	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
33	29	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
19	13	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
10	8	38.4	48.7		41.4		47.4		41.8		35.7		42.4		40.1		38.8		37.3	
3	<8	5.2	17.5		7.3		2.5		3.8		8.2		10.3		7.5		7.3		5.8	
	ASSAY	41.5	65.3		40.3		34.3		31.9		47.3		51.3		48.1		38.4		32.6	

D50 11.9 10.4 11.6 10.7 11.5 12.2 11.4 11.7 11.9 12.1



Test 28
Cyclone u/f
Mass split: 51.71

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
300	150	13.41	0.56	8.1	15.60	11.2	0.07	5.9	2.33	12.8	51.90	15.8	0.40	9.6	0.78	10.7	3.61	13.4	9.01	15.3
126	106	4.48	0.74	3.6	15.70	3.8	0.07	2.0	1.37	2.5	52.70	5.4	0.50	4.0	0.89	4.1	3.59	4.5	8.05	4.6
89	75	5.55	0.68	4.1	15.10	4.5	0.07	2.4	1.73	3.9	53.40	6.7	0.47	4.7	0.86	4.9	3.34	5.2	7.53	5.3
63	53	6.77	0.75	5.5	15.55	5.6	0.07	3.0	1.94	5.4	53.10	8.2	0.50	6.0	0.92	6.4	3.24	6.1	7.10	6.1
49	45	3.46	0.80	3.0	16.10	3.0	0.08	1.7	1.89	2.7	51.90	4.1	0.54	3.3	1.00	3.5	3.26	3.1	7.09	3.1
41	38	3.44	0.94	3.5	17.45	3.2	0.10	2.2	1.82	2.6	51.40	4.0	0.60	3.7	1.09	3.8	3.45	3.3	7.17	3.1
33	29	6.74	2.47	17.9	24.50	8.9	0.20	8.4	3.29	9.1	32.70	5.0	0.89	10.7	1.19	8.2	3.07	5.7	6.08	5.2
19	13	26.56	1.10	31.4	19.95	28.4	0.19	31.5	1.77	19.2	42.90	25.8	0.66	31.3	1.09	29.5	3.53	26.0	7.03	23.7
10	8	10.83	0.91	10.6	22.30	12.9	0.26	17.6	3.13	13.8	41.60	10.2	0.64	12.4	1.13	12.5	3.94	11.9	8.03	11.0
3	Cal <8	18.76	0.62	12.5	18.34	18.4	0.22	25.3	3.68	28.2	34.93	14.9	0.43	14.3	0.86	16.5	3.99	20.8	9.40	22.4
	ASSAY	100.00	0.93	100.0	18.65	100.0	0.16	100.0	2.45	100.0	44.10	100.0	0.56	100.0	0.98	100.0	3.60	100.0	7.87	100.0

Cyclone o/f
Mass split: 48.29

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
300	150																			
126	106																			
89	75																			
63	53																			
49	45																			
41	38																			
33	29																			
19	13																			
10	8	5.02	0.71	8.9	19.75	4.8	0.18	5.0	2.73	4.8	41.00	5.6	0.53	6.6	1.11	7.4	3.66	4.3	7.64	3.2
3	CALC<8	94.98	0.38	91.1	20.54	95.2	0.18	95.0	2.85	95.2	36.26	94.4	0.39	93.4	0.73	92.6	4.33	95.7	12.18	96.8
	ASSAY	100.00	0.40	100.0	20.50	100.0	0.18	100.0	2.84	100.0	36.50	100.0	0.40	100.0	0.75	100.0	4.30	100.0	11.95	100.0

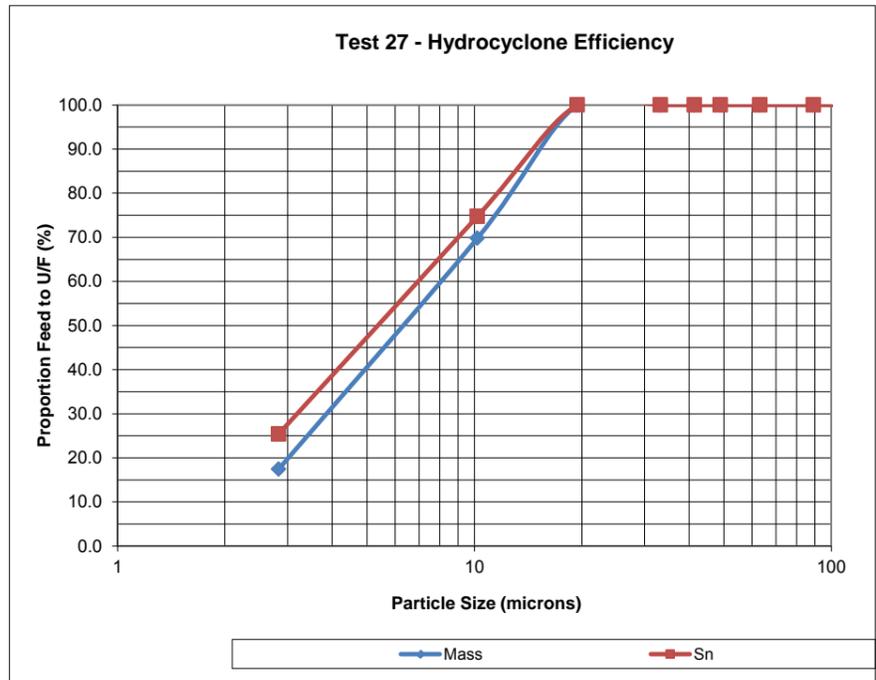
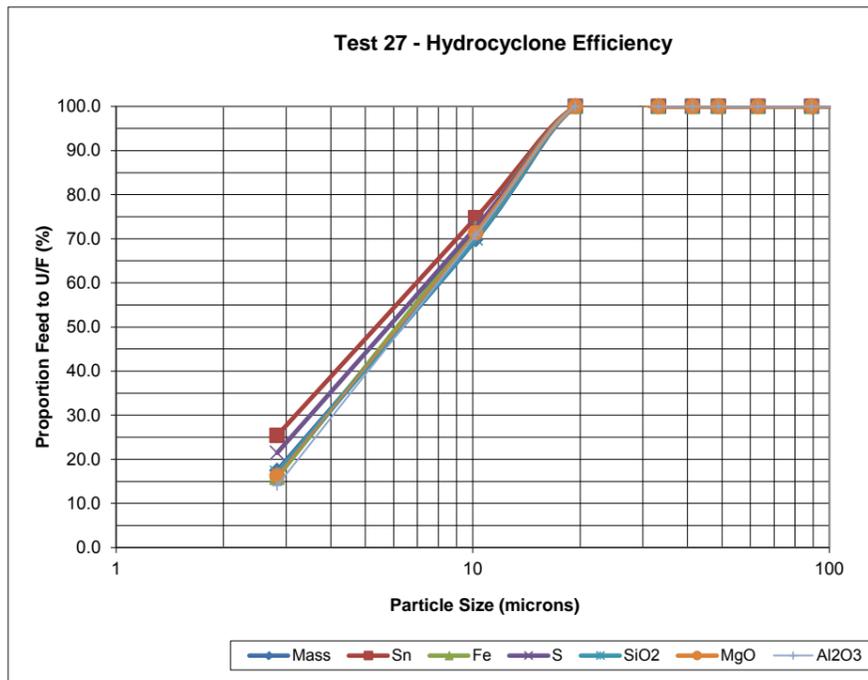
Cyclone feed
Mass split: 100.00

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist	%	dist														
300	150	6.93	0.56	5.8	15.6	5.5	0.07	2.9	2.33	6.1	51.9	8.9	0.40	5.7	0.78	6.2	3.61	6.4	9.0	6.3
126	106	2.31	0.74	2.5	15.7	1.9	0.07	1.0	1.37	1.2	52.7	3.0	0.50	2.4	0.89	2.4	3.59	2.1	8.1	1.9
89	75	2.87	0.68	2.9	15.1	2.2	0.07	1.2	1.73	1.9	53.4	3.8	0.47	2.8	0.86	2.8	3.34	2.4	7.5	2.2
63	53	3.50	0.75	3.9	15.6	2.8	0.07	1.4	1.94	2.6	53.1	4.6	0.50	3.6	0.92	3.7	3.24	2.9	7.1	2.5
49	45	1.79	0.80	2.1	16.1	1.5	0.08	0.8	1.89	1.3	51.9	2.3	0.54	2.0	1.00	2.1	3.26	1.5	7.1	1.3
41	38	1.78	0.94	2.5	17.5	1.6	0.10	1.0	1.82	1.2	51.4	2.3	0.60	2.2	1.09	2.2	3.45	1.6	7.2	1.3
33	29	3.48	2.47	12.8	24.5	4.4	0.20	4.1	3.29	4.3	32.7	2.8	0.89	6.4	1.19	4.8	3.07	2.7	6.1	2.2
19	13	13.74	1.10	22.4	20.0	14.0	0.19	15.4	1.77	9.2	42.9	14.6	0.66	18.8	1.09	17.2	3.53	12.3	7.0	9.8
10	8	8.02	0.85	10.1	21.5	8.8	0.24	11.2	3.01	9.2	41.4	8.2	0.61	10.1	1.12	10.4	3.86	7.9	7.9	6.5
3	<8	55.57	0.42	35.0	20.2	57.3	0.19	61.0	2.99	63.0	36.0	49.5	0.40	45.9	0.75	48.2	4.27	60.3	11.7	66.0
	ASSAY	100.00	0.67	100.0	19.5	100.0	0.17	100.0	2.64	100.0	40.4	100.0	0.48	100.0	0.87	100.0	3.94	100.0	9.8	100.0

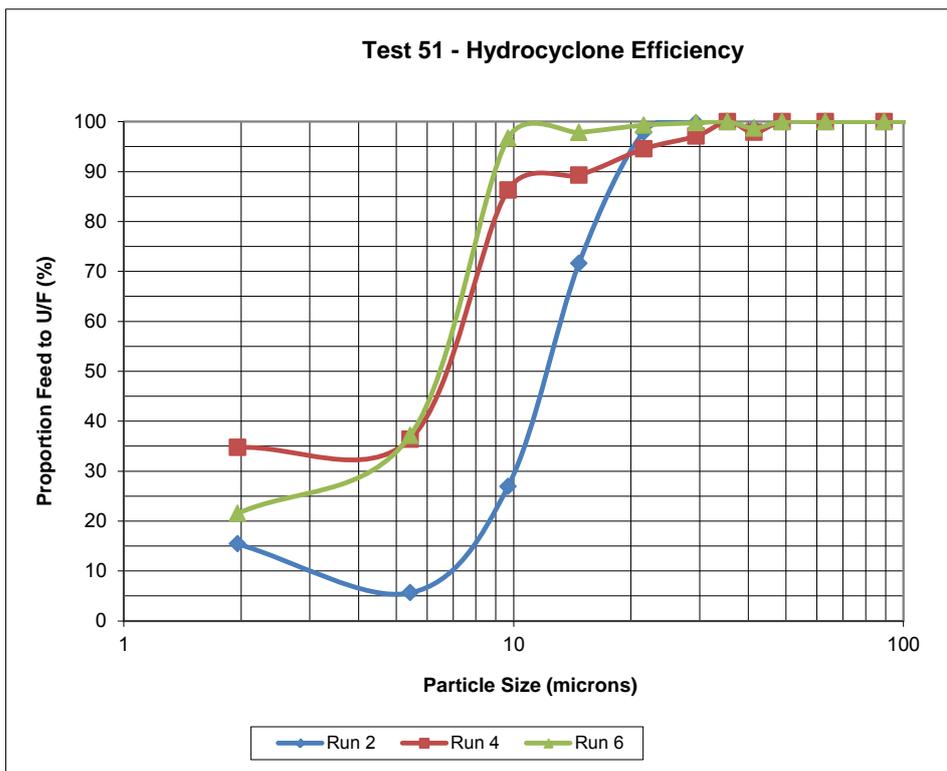
Recoveries to u/f

Mean size	SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO		CaO		MgO		Al2O3	
			%	dist																
300	150	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
126	106	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
89	75	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
63	53	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
49	45	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
41	38	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
33	29	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
19	13	100.0	100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0		100.0	
10	8	69.8	74.8		72.3		76.9		72.6		70.1		73.6		70.2		71.3		70.8	
3	<8	17.5	25.4		15.9		20.2		21.5		16.9		18.7		19.9		16.3		14.0	
	ASSAY	51.7	71.3		49.3		48.8		48.0		56.4		60.0		58.3		47.3		41.4	

D50 7.4 6.5 7.3 6.7 6.9 7.4 7.0 7.2 7.3 7.5



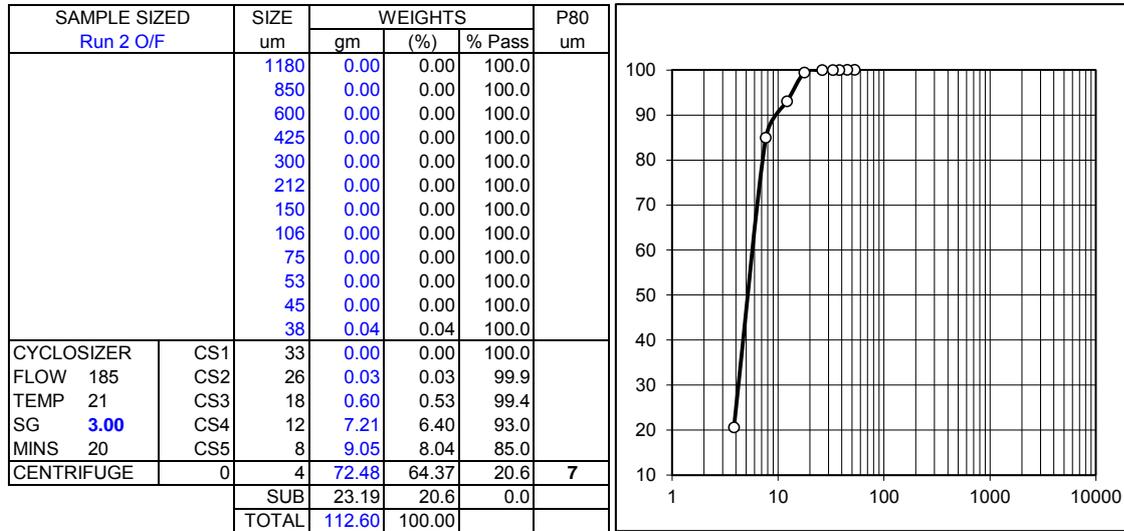
		Run 2				Run 4				Run 6			
Mass split		O/F	U/F	Feed	Rec to u/f	O/F	U/F	Feed	Rec to u/f	O/F	U/F	Feed	Rec to u/f
		59.7	40.3	100.0		37.5	62.5	100.0		36.6	63.4	100.0	
Mean size	Size (um)												
252	212	0.0	0.1	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	
178	150	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.1	0.0	100.0
126	106	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0
89	75	0.0	0.1	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0
63	53	0.0	1.3	0.5	100.0	0.0	0.9	0.5	100.0	0.0	0.9	0.5	100.0
49	45	0.0	2.8	1.1	100.0	0.0	1.9	1.2	100.0	0.0	1.9	1.2	100.0
41	38	0.0	3.8	1.5	98.6	0.1	2.5	1.6	97.8	0.1	2.4	1.5	98.7
35	33	0.0	1.6	0.6	100.0	0.0	1.2	0.7	100.0	0.0	1.3	0.8	100.0
29	26	0.0	14.7	5.9	99.7	0.5	10.3	6.6	97.1	0.0	11.3	7.2	99.8
22	18	0.5	36.2	14.9	97.9	2.2	23.0	15.2	94.5	0.3	23.5	15.0	99.3
15	12	6.4	23.9	13.4	71.6	3.9	19.6	13.7	89.3	0.8	21.5	14.0	97.8
10	8	8.0	4.4	6.6	26.9	2.7	10.1	7.3	86.3	0.6	10.8	7.1	96.7
5	4	64.4	5.7	40.7	5.6	65.5	22.5	38.6	36.4	58.7	20.0	34.2	37.1
2	SUB	20.6	5.6	14.5	15.4	25.2	8.0	14.5	34.8	39.4	6.2	18.4	21.5
TOTAL		100.0	100.0	100.0	40.3	100.0	100.0	100.0	62.5	100.0	100.0	100.0	63.4
D50					12.3				6.6				6.3





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Run 2 O/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK

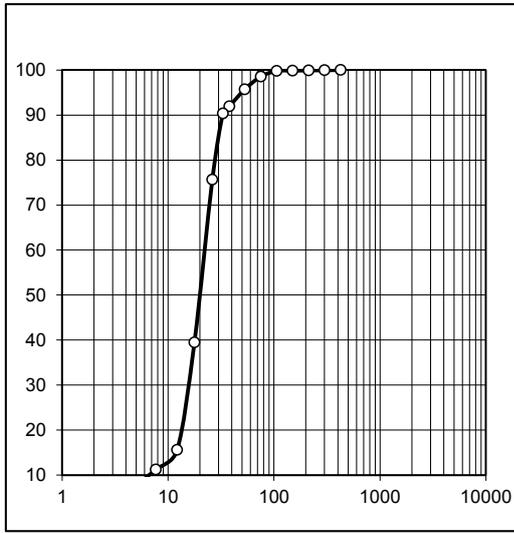




BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Run 2 U/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK

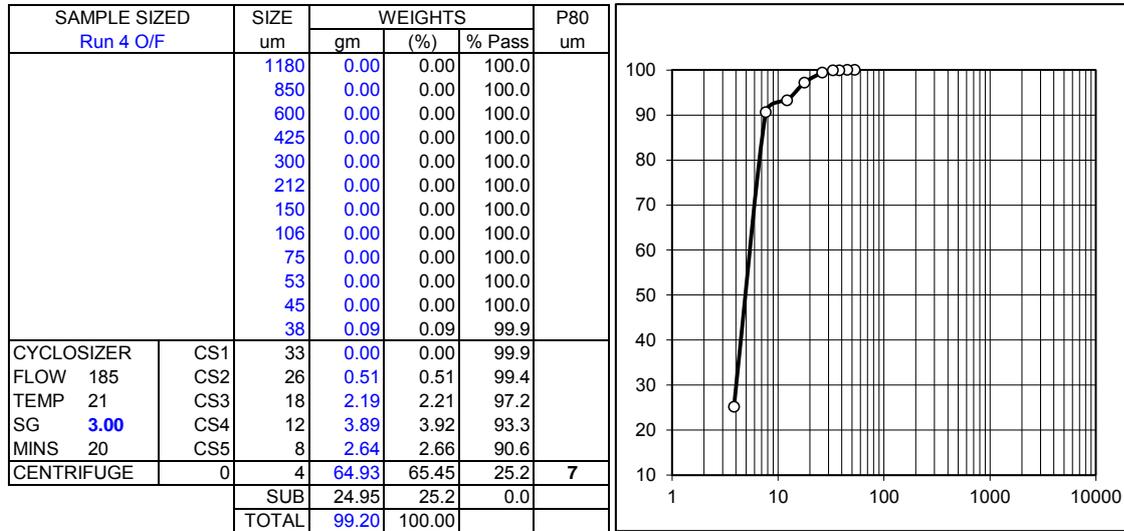
SAMPLE SIZED Run 2 U/F		SIZE um	WEIGHTS			P80 um	
			gm	(%)	% Pass		
		2360	0.00	0.00	100.0		
		1180	0.00	0.00	100.0		
		850	0.00	0.00	100.0		
		600	0.00	0.00	100.0		
		425	0.00	0.00	100.0		
		300	0.07	0.06	99.9		
		212	0.05	0.04	99.9		
		150	0.06	0.05	99.9		
		106	0.08	0.07	99.8		
		75	1.52	1.26	98.5		
		53	3.40	2.82	95.7		
		38	4.53	3.75	92.0		
CYCLOSIZER	CS1	33	1.94	1.61	90.4		28
FLOW	185	CS2	26	17.76	14.71	75.6	
TEMP	21	CS3	18	43.66	36.15	39.5	
SG	3.00	CS4	12	28.84	23.88	15.6	
MINS	20	CS5	8	5.29	4.38	11.2	
CENTRIFUGE	0	4	6.86	5.68	5.6		
		SUB	6.71	5.6	0.0		
		TOTAL	120.77	100.00			





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

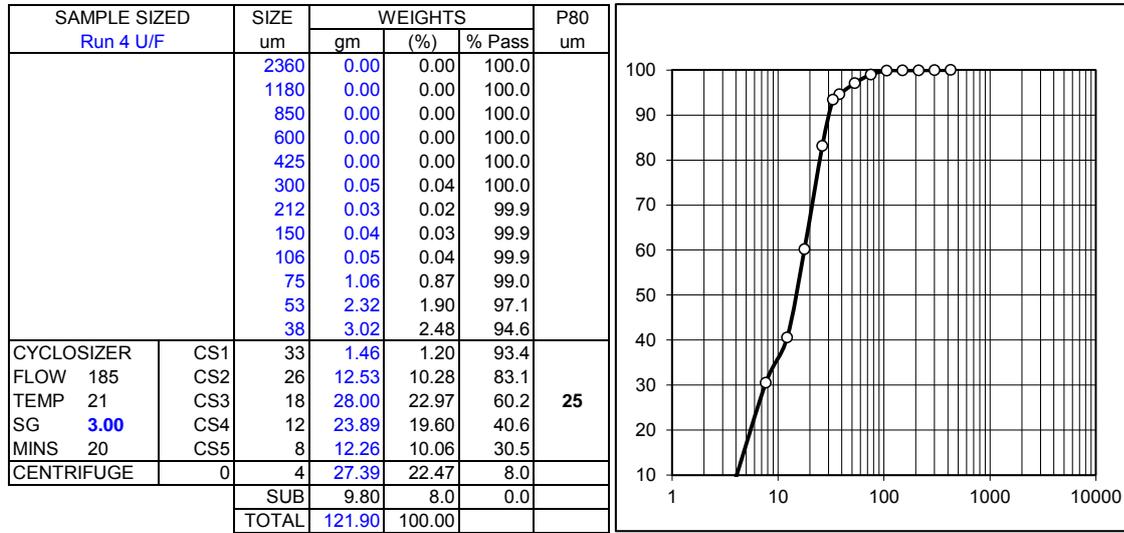
PROJECT	T0879
SAMPLE	Run 4 O/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Run 4 U/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK

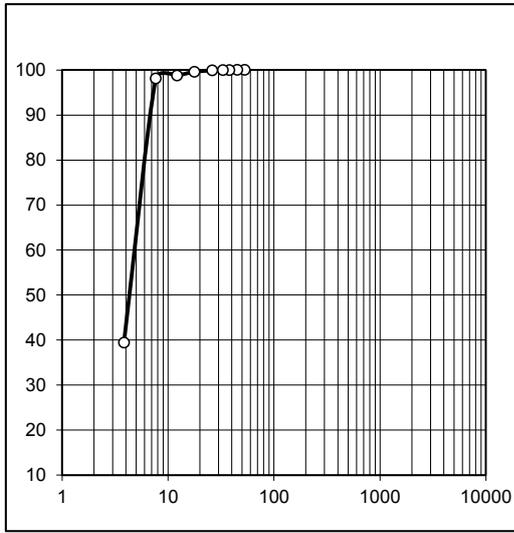




BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Run 6 O/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK

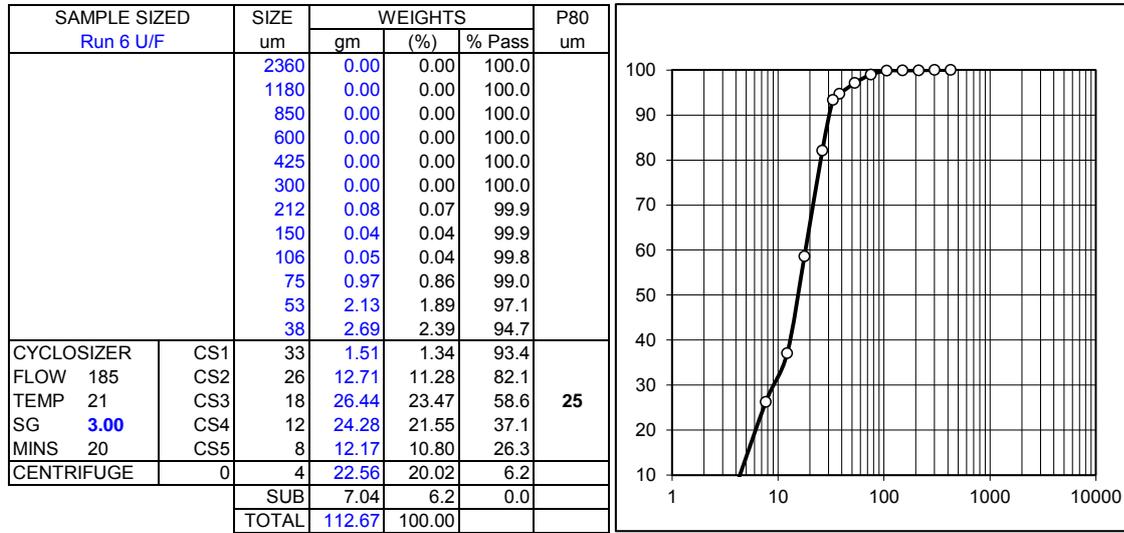
SAMPLE SIZED Run 6 O/F		SIZE um	WEIGHTS			P80 um
			gm	(%)	% Pass	
		1180	0.00	0.00	100.0	
		850	0.00	0.00	100.0	
		600	0.00	0.00	100.0	
		425	0.00	0.00	100.0	
		300	0.00	0.00	100.0	
		212	0.00	0.00	100.0	
		150	0.00	0.00	100.0	
		106	0.00	0.00	100.0	
		75	0.00	0.00	100.0	
		53	0.00	0.00	100.0	
		45	0.00	0.00	100.0	
		38	0.06	0.05	99.9	
CYCLOSIZER	CS1	33	0.00	0.00	99.9	
FLOW 185	CS2	26	0.05	0.05	99.9	
TEMP 21	CS3	18	0.32	0.29	99.6	
SG 3.00	CS4	12	0.91	0.83	98.8	
MINS 20	CS5	8	0.71	0.65	98.1	
CENTRIFUGE	0	4	64.39	58.69	39.4	6
		SUB	43.27	39.4	0.0	
		TOTAL	109.71	100.00		





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Run 6 U/F
TEST NO	T51
DATE	191114
TECHNICIAN	DK



CYCLONE TEST DATA

SAMPLE	Feed from LC01 C11-31 cyclone over flow+-40um from GLC -106 tails	
TEST TYPE	Cyclone test (red cyclone foot)	

PROJECT	T0879
TEST NO	T51
DATE	181114
PERFORMED BY	ID

Run #	Spigot, mm	Vortex finder, mm	Under flow (DAMP)	Over flow (DAMP)	Over flow/Total %	Cutpoint	KPA
1	4.5	18	189	593.7	75.9		200
2	4.5	14	269	517	65.8	12.3	200
3	9.5	11	550	205	27.2		200
4	6	11	607	468	43.5	6.6	200
5	6	8	371	128	25.7		200
6	4.5	8	433	322	42.6	6.3	200
Run #	Under flow (Dry, gm)	Over flow (Dry, gm)	Over flow/Total %	Underflow flow/Total %	Cutpoint		
2	435.8	645.5	59.70	40.30	~12um		
4	540	324	37.50	62.50	~5um		
6	383.9	221.9	36.63	63.37	~5um		
Run #	Cyclone O/f		26.1	Cyclone U/f		48.4	#DIV/0!
Run #	Tare (gm)	Tare + Pulp (gm)		Tare (gm)	Tare + Pulp (gm)		
1	355	2945		79	324		
2	355	2825		79	438		
3	355	1675		280	1700		
4	355	3205		280	1395		
5	355	1360		280	1200		
6				#DIV/0!			

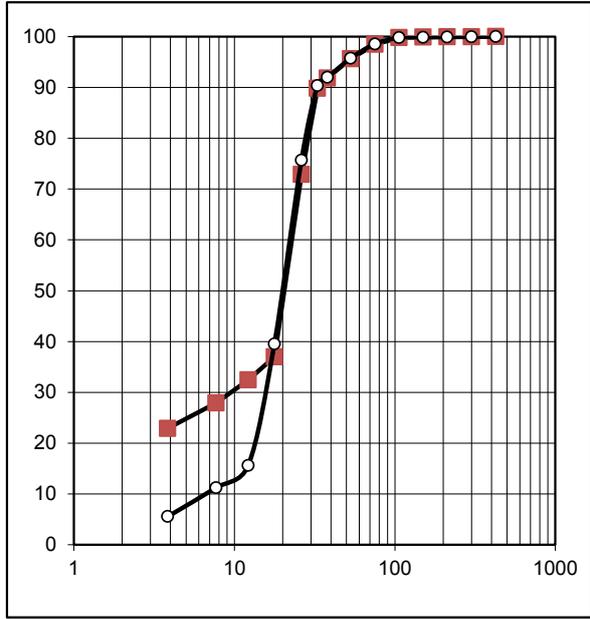


BURNIE LABORATORY
 SIZE ANALYSIS REPORT SHEET WITH CS6

PROJECT	T0879
SAMPLE	Cyc U/F
	T56
DATE	251114
TECHNICIAN	MS

SIZING

Product Sized Cyc U/F		SIZE um	WEIGHTS		
			gm	(%)	%PASS
P80		425	0.00	0.00	100.0
		300	0.03	0.04	100.0
		212	0.03	0.04	99.9
		150	0.04	0.05	99.9
		106	0.07	0.08	99.8
		75	1.10	1.32	98.5
		53	2.37	2.85	95.6
		38	3.15	3.79	91.8
CYCLOSIZER	29	33	1.68	2.02	89.8
FLOW 185		26	14.08	16.93	72.9
TEMP 21		18	29.84	35.88	37.0
SG 3.00		12	3.80	4.57	32.4
MINS 20		8	3.77	4.53	27.9
CENTRIFUGE	CS6	4	4.16	5.00	22.9
SUB			19.04	22.90	0.0
TOTAL			83.16	100.0	



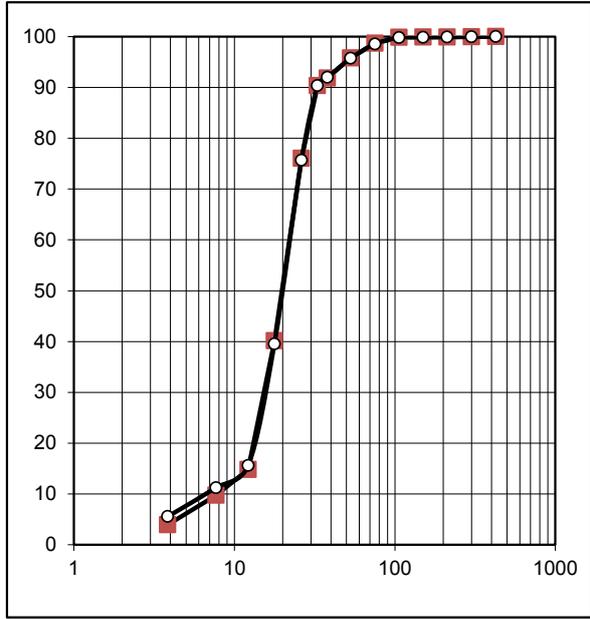


BURNIE LABORATORY
 SIZE ANALYSIS REPORT SHEET WITH CS6

PROJECT	T0879
SAMPLE	Cyc U/F
	T56.B
DATE	261114
TECHNICIAN	MS

SIZING

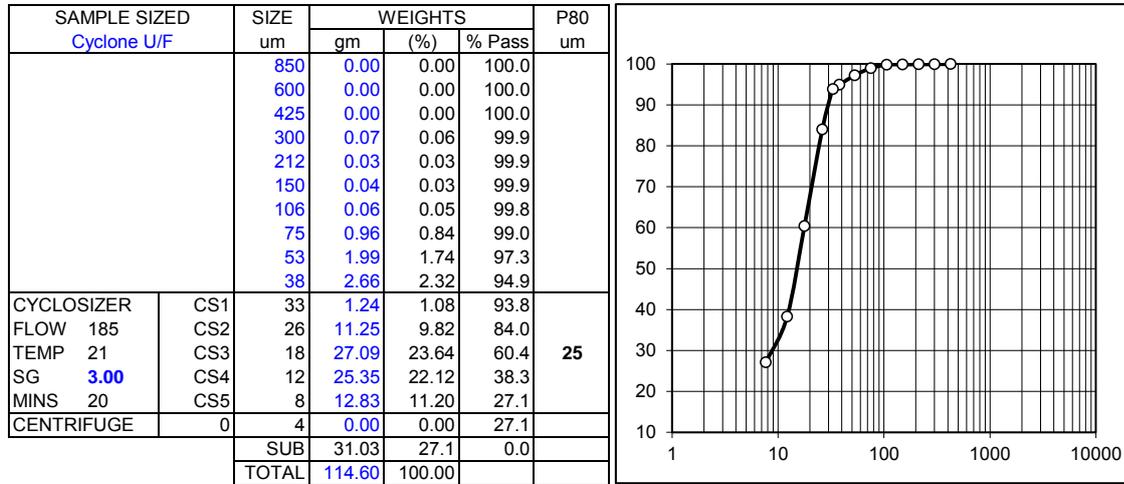
Product Sized Cyc U/F		SIZE um	WEIGHTS		
			gm	(%)	%PASS
	P80	425	0.00	0.00	100.0
		300	0.06	0.06	99.9
		212	0.03	0.03	99.9
		150	0.04	0.04	99.9
		106	0.06	0.06	99.8
		75	1.18	1.15	98.7
		53	2.95	2.88	95.8
		38	4.05	3.95	91.8
CYCLOSIZER	28	33	1.55	1.51	90.3
FLOW 185		26	14.65	14.29	76.0
TEMP 21		18	36.81	35.89	40.1
SG 3.00		12	25.99	25.34	14.8
MINS 20		8	5.19	5.06	9.7
CENTRIFUGE	CS6	4	5.95	5.80	3.9
SUB			4.04	3.94	0.0
TOTAL			102.55	100.0	





BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

PROJECT	T0879
SAMPLE	Cyclone U/F
TEST NO	T63
DATE	51214
TECHNICIAN	MS

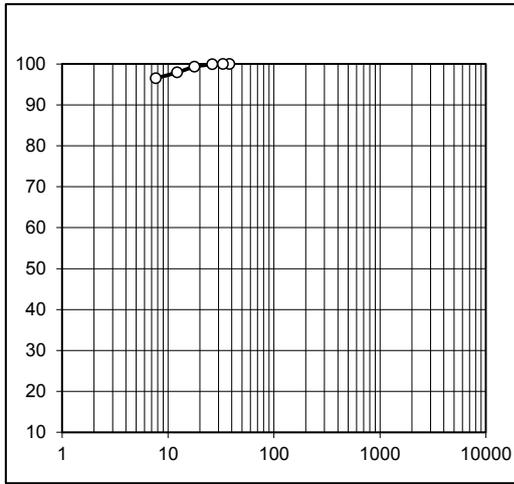




BURNIE LABORATORY
GENERAL SIZING REPORT SHEET

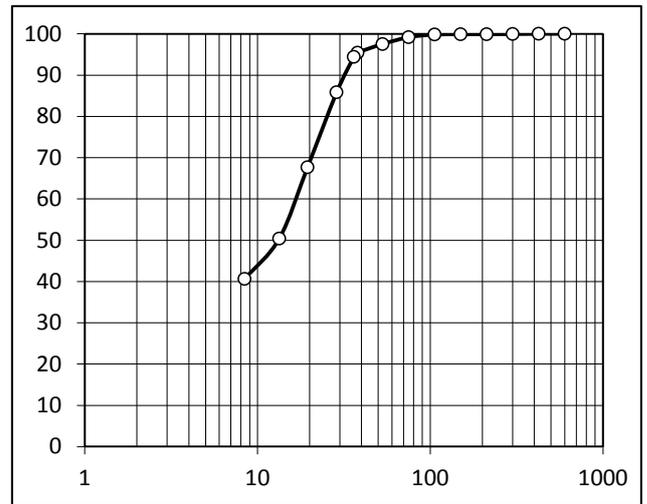
PROJECT	T0879
SAMPLE	Cyclone O/F
TEST NO	T63
DATE	51214
TECHNICIAN	MS

SAMPLE SIZED Cyclone O/F		SIZE um	WEIGHTS			P80 um
			gm	(%)	% Pass	
		850	0.00	0.00	100.0	
		600	0.00	0.00	100.0	
		425	0.00	0.00	100.0	
		300	0.00	0.00	100.0	
		212	0.00	0.00	100.0	
		150	0.00	0.00	100.0	
		106	0.00	0.00	100.0	
		75	0.00	0.00	100.0	
		53	0.00	0.00	100.0	
		38	0.00	0.00	100.0	
CYCLOSIZER	CS1	33	0.00	0.00	100.0	
FLOW 185	CS2	26	0.09	0.09	99.9	
TEMP 21	CS3	18	0.60	0.57	99.3	
SG 3.00	CS4	12	1.50	1.42	97.9	
MINS 20	CS5	8	1.47	1.39	96.5	
CENTRIFUGE	0	4	0.00	0.00	96.5	
		SUB	102.20	96.5	0.0	
		TOTAL	105.86	100.00		



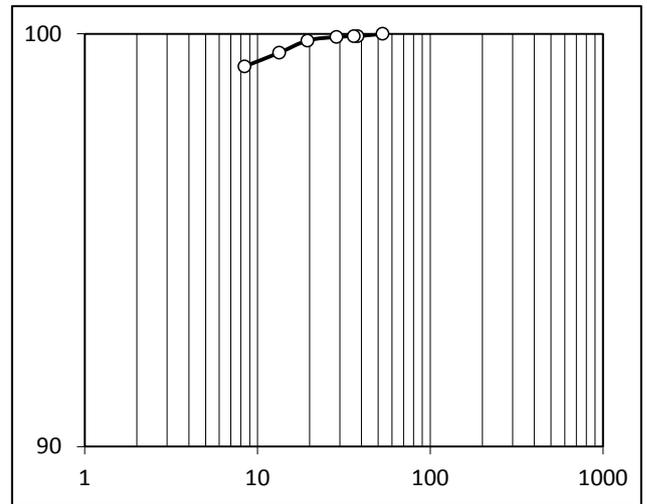
PROJECT	T0879
SAMPLE NAME	Cyclone Underflow
TEST NO	T70
DATE	230115
TECHNICIAN	MS

Cyclone Underflow T70		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.07	0.06	99.9
		212	0.03	0.03	99.9
		150	0.04	0.04	99.9
		106	0.06	0.05	99.8
		75	0.71	0.64	99.2
		53	1.83	1.65	97.5
	38	2.30	2.08	95.4	
CYCLOSIZER		36	1.14	1.03	94.4
FLOW 185		29	9.49	8.57	85.8
TEMP 21	26	19	20.11	18.17	67.7
SG 2.60		13	19.10	17.25	50.4
MINS 20		8	10.85	9.80	40.6
		SUB	44.97	40.62	0.0
		TOTAL	110.70	100.00	



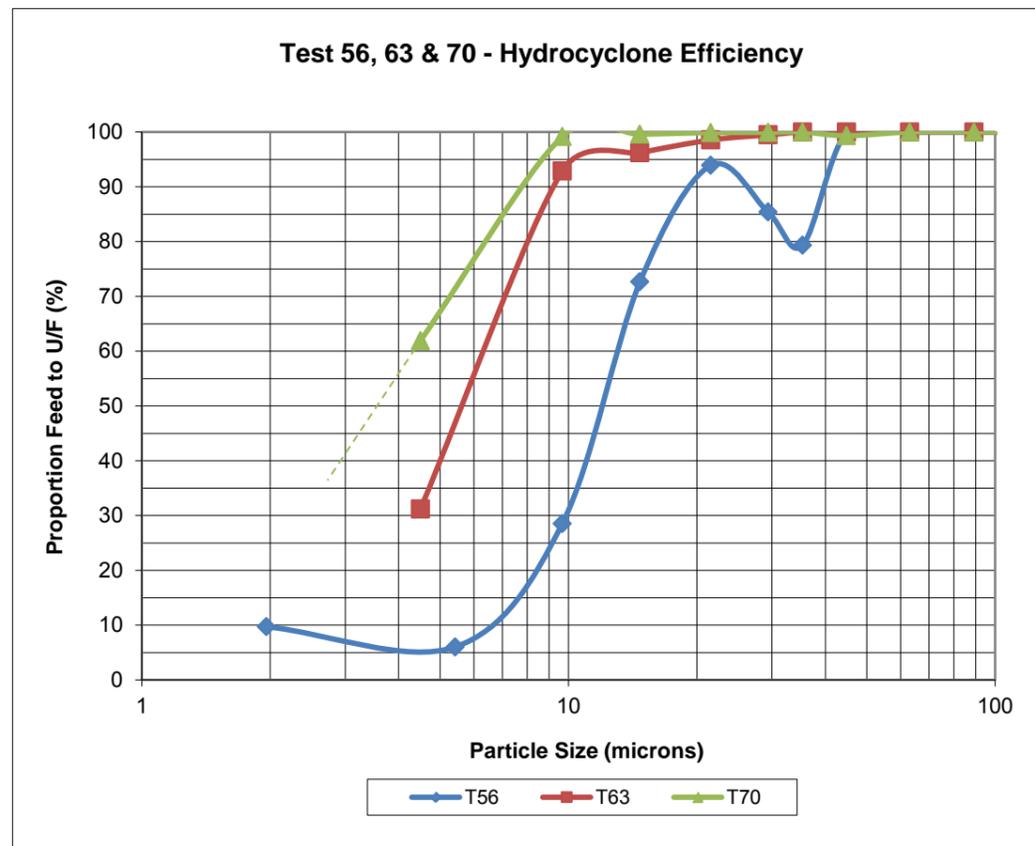
PROJECT	T0879
SAMPLE NAME	Cyclone Overflow
TEST NO	T70
DATE	270115
TECHNICIAN	MS

Cyclone Overflow T70		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80		600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	0.00	0.00	100.0
		212	0.00	0.00	100.0
		150	0.00	0.00	100.0
		106	0.00	0.00	100.0
		75	0.00	0.00	100.0
		53	0.00	0.00	100.0
	38	0.06	0.06	99.9	
CYCLOSIZER		36	0.00	0.00	99.9
FLOW 185		29	0.02	0.02	99.9
TEMP 21		19	0.09	0.09	99.8
SG 2.60		13	0.31	0.30	99.5
MINS 20		8	0.35	0.33	99.2
		SUB	104.20	99.21	0.0
		TOTAL	105.03	100.00	

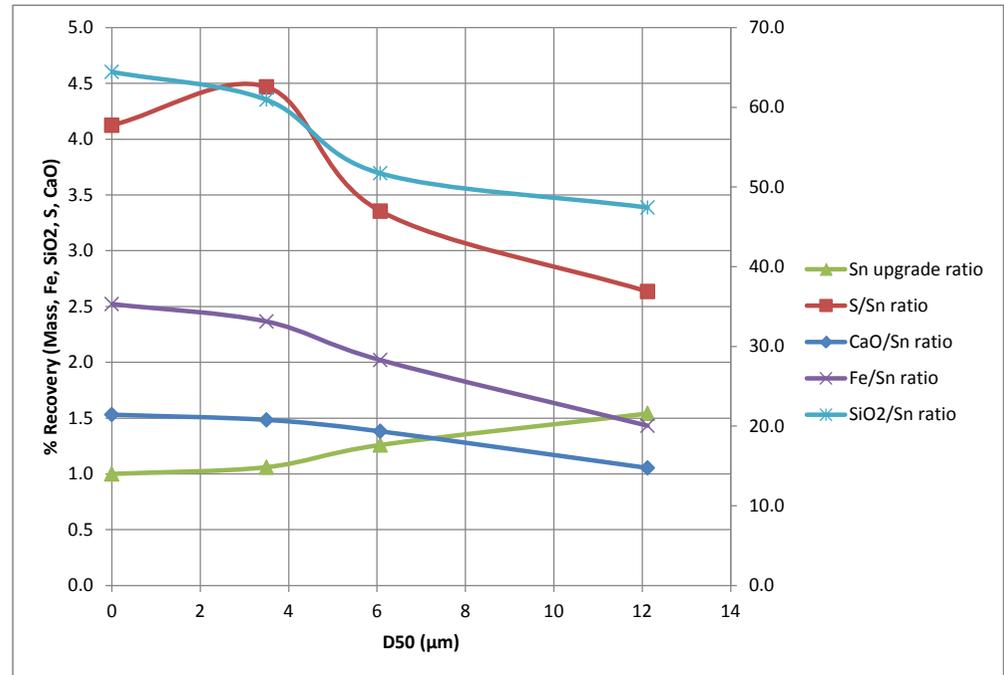
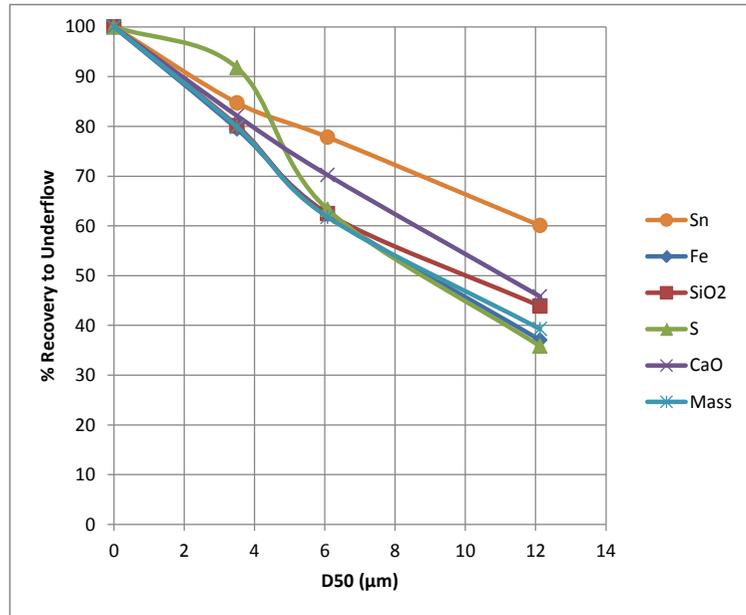


Test no.		T56				T63				T70					
Product		O/F	U/F	Feed	Rec to u/f	O/F	U/F	Feed	Rec to u/f	O/F	U/F	Feed	Rec to u/f		
Mass split		60.7	39.3	100.0		38.2	61.8	100.0		20.1	79.9	100.0			
Mean size	Size (um)					Mean size	Size (um)								
252	212	0.0	0.1	0.1	100.0	252	212	0.0	0.1	0.1	100.0	0.0	0.1	0.1	100.0
178	150	0.0	0.0	0.0	100.0	178	150	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0
126	106	0.0	0.1	0.0	100.0	126	106	0.0	0.1	0.0	100.0	0.0	0.1	0.0	100.0
89	75	0.0	1.2	0.5	100.0	89	75	0.0	0.8	0.5	100.0	0.0	0.6	0.5	100.0
63	53	0.0	2.9	1.1	100.0	63	53	0.0	1.7	1.1	100.0	0.0	1.7	1.3	100.0
45	38	0.0	3.9	1.6	99.9	45	38	0.0	2.3	1.4	100.0	0.1	2.1	1.7	99.3
35	33	0.3	1.5	0.7	79.3	35	33	0.0	1.1	0.7	100.0	0.0	1.0	0.8	100.0
29	26	1.6	14.3	6.6	85.4	29	26	0.1	9.8	6.1	99.5	0.0	8.6	6.9	99.9
22	18	1.5	35.9	15.0	93.9	22	18	0.6	23.6	14.8	98.5	0.1	18.2	14.5	99.9
15	12	6.2	25.3	13.7	72.6	15	12	1.4	22.1	14.2	96.2	0.3	17.3	13.8	99.6
10	8	8.2	5.1	7.0	28.5	10	8	1.4	11.2	7.4	92.9	0.3	9.8	7.9	99.2
5	4	58.6	5.8	37.8	6.0	5	SUB	96.5	27.1	53.6	31.2	99.2	40.6	52.4	61.9
2	SUB	23.6	3.9	15.9	9.7										
TOTAL		100.0	100.0	100.0	39.3	TOTAL		100.0	100.0	100.0	61.8	100.0	100.0	100.0	79.9
D50					12.1	D50					6.1				4
Sn distribution		39.9	60.1	100.0	60.1			22.2	77.8	100.0	77.8	15.3	84.7	100.0	84.7

0.1 0.1
0.0 0.0
0.0 0.0
0.5 0.5
1.2 1.3
1.6 1.8
0.7 0.9
6.5 7.8
14.7 17.9
14.0 16.3
7.7 8.3
53.0 45.0
100.0 100.0



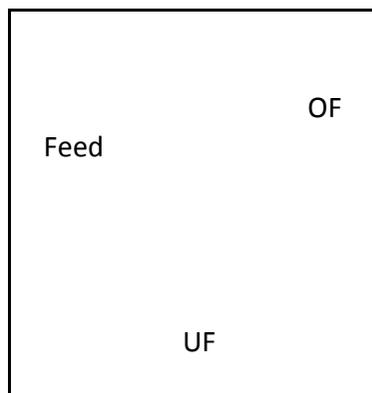
Test no.	D50 (μm)	% Mass Recovery to U/F	U/F % <CS5 (<8 μm)	% Sn Recovery to U/F	% Fe Recovery to U/F	% SiO ₂ Recovery to U/F	% S Recovery to U/F	% CaO Recovery to U/F	Sn upgrade ratio	Fe/Sn ratio	SiO ₂ /Sn ratio	S/Sn ratio	CaO/Sn ratio
T56	12.1	39.3	9.7	0.93	18.7	44.1	2.45	0.98	1.54	20.1	47.4	2.6	1.05
T63	6.1	61.8	27.1	0.76	21.5	39.3	2.55	1.05	1.26	28.3	51.7	3.4	1.38
T70	4	79.9	40.6	0.64	21.2	39.0	2.86	0.95	1.06	33.1	60.9	4.5	1.48
Feed	0	100.0	53.0	0.60	21.3	38.9	2.49	0.92	1.00	35.3	64.4	4.1	1.53



BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T27
DATE	010914
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	1950.5
Spigot (mm)	4.5
Vortex finder (mm)	18.0
KPA	200.0
Comments	Mimic 12um Cutpoint



FEED MATERIAL	
From LC01 cyclone overflow	
FROM TEST NO	
START WT (gm)	1950.5

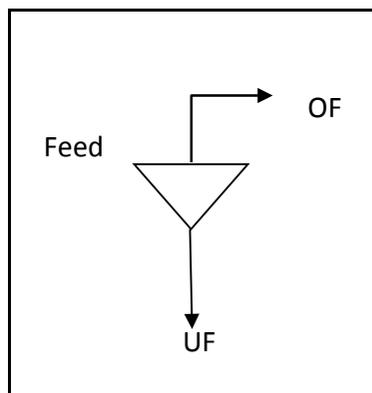
MAGNETIC SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	1141.2	1141.2	58.51	0.41	34.7	20.20	59.7	37.20	52.7	3.49	68.1	0.78	51.9
UF	809.3	809.3	41.49	1.09	65.3	19.20	40.3	47.10	47.3	2.30	31.9	1.02	48.1
TOTAL	1950.50		100.00	0.69	100.0	19.79	100.0	41.31	100.0	3.00	100.0	0.88	100.0

BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T28
DATE	010914
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	3341.0
Spigot (mm)	4.5
Vortex finder (mm)	14.0
KPA	200.0
Comments	Mimic 8um Cutpoint



FEED MATERIAL	
From LC01 cyclone over flow	
FROM TEST NO	
START WT (gm)	3341.0

MAGNETIC SEPARATION RESULTS

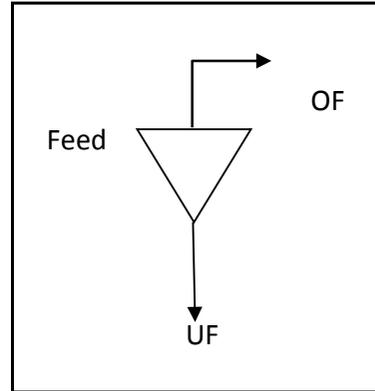
PRODUCT				Tin		Iron		Silica		Sulphur		Calcium Oxide	
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	1613.5	1613.5	48.29	0.40	28.7	20.50	50.7	36.50	43.6	2.84	52.0	0.75	41.7
UF	1727.5	1727.5	51.71	0.93	71.3	18.65	49.3	44.10	56.4	2.45	48.0	0.98	58.3
TOTAL	3341.00		100.00	0.67	100.0	19.54	100.0	40.43	100.0	2.64	100.0	0.87	100.0



BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T37
DATE	110914
TECH	DG

TEST TYPE	Mini Cyclone Sep
Feed Solids (g)	2524.9
Spigot (mm)	6.0
Vortex finder (mm)	5.5
KPA	
Comments	Lazer Sizings Part of diagnostic tin float



FEED MATERIAL	
From LC01 cyc7-10 Overflow	
FROM TEST NO	
START WT (gm)	2524.9

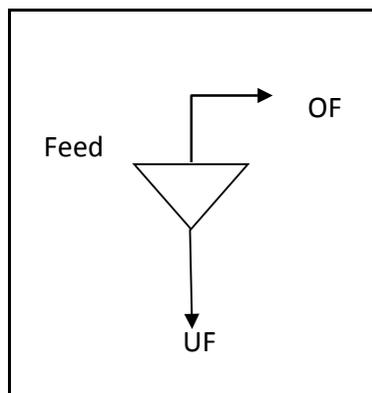
SEPARATION RESULTS

NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	350.2	350.2	13.87	0.33	8.7	20.60	14.0	35.80	13.3	3.32	14.6	0.65	11.1
UF	2174.7	2174.7	86.13	0.56	91.3	20.30	86.0	37.70	86.7	3.13	85.4	0.84	88.9
TOTAL	2524.90		100.00	0.53	100.0	20.34	100.0	37.44	100.0	3.16	100.0	0.81	100.0

BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T43
DATE	250914
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	2211.5
Spigot (mm)	4.5
Vortex finder (mm)	11.0
KPA	200.0
Comments	Red foot



FEED MATERIAL	
From LC01 cyclone over flow	
FROM TEST NO	LC01
START WT (gm)	2211.5

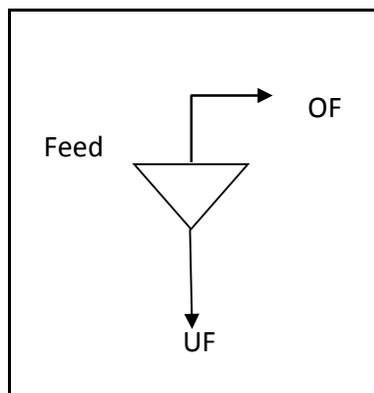
MAGNETIC SEPARATION RESULTS

PRODUCT			Tin		Iron		Silica		Sulphur		Calcium Oxide		
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	1613.5	1613.5	72.96	0.40	53.7	20.50	74.8	36.50	69.1	2.84	75.8	0.75	67.4
calc UF	598	598	27.04	0.93	46.3	18.65	25.2	44.10	30.9	2.45	24.2	0.98	32.6
TOTAL	2211.50		100.00	0.54	100.0	20.00	100.0	38.56	100.0	2.73	100.0	0.81	100.0

BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T56
DATE	241114
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	
Spigot (mm)	4.5
Vortex finder (mm)	14.0
KPA	200.0
Comments	Red foot



FEED MATERIAL cyclone over flow, -40 fine tail combined	
FROM TEST NO	LC01
START WT (gm)	0.0

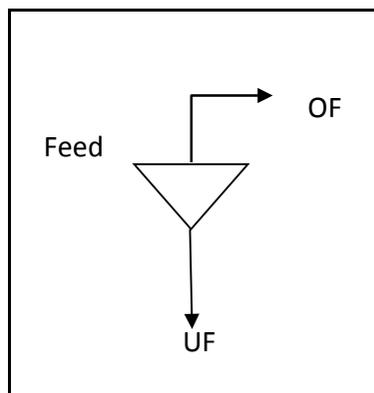
MAGNETIC SEPARATION RESULTS

PRODUCT			Tin		Iron		Silica		Sulphur		Calcium Oxide		
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	6015.2	6015.2	60.71	0.40	39.9	20.50	62.9	36.50	56.1	2.84	64.2	0.75	54.2
calc UF	3892.9	3892.9	39.29	0.93	60.1	18.65	37.1	44.10	43.9	2.45	35.8	0.98	45.8
TOTAL	9908.10		100.00	0.61	100.0	19.77	100.0	39.49	100.0	2.69	100.0	0.84	100.0

BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T63
DATE	031214
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	
Spigot (mm)	4.5
Vortex finder (mm)	8.0
KPA	200.0
Comments	Red foot 22% solids



FEED MATERIAL cyclone over flow, -40 fine tail combined	
FROM TEST NO	LC01
START WT (gm)	0.0

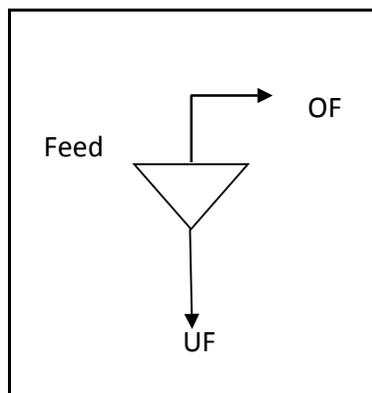
MAGNETIC SEPARATION RESULTS

PRODUCT			Tin		Iron		Silica		Sulphur		Calcium Oxide		
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	1392.1	1392.1	38.20	0.35	22.2	21.00	37.6	38.20	37.5	2.39	36.7	0.72	29.8
calc UF	2252.4	2252.4	61.80	0.76	77.8	21.50	62.4	39.30	62.5	2.55	63.3	1.05	70.2
TOTAL	3644.50		100.00	0.60	100.0	21.31	100.0	38.88	100.0	2.49	100.0	0.92	100.0

BURNIE LABORATORY: CYCLONE SEPARATION REPORT SHEET

PROJECT	T0879
TEST NO	T70
DATE	220115
TECH	ID

TEST TYPE	Cyclone Separation
Feed Solids (g)	
Spigot (mm)	4.5
Vortex finder (mm)	8.0
KPA	200.0
Comments	Red foot 22% solids



FEED MATERIAL cyclone over flow, -40 fine tail combined	
FROM TEST NO	LC01
START WT (gm)	4223.8

MAGNETIC SEPARATION RESULTS

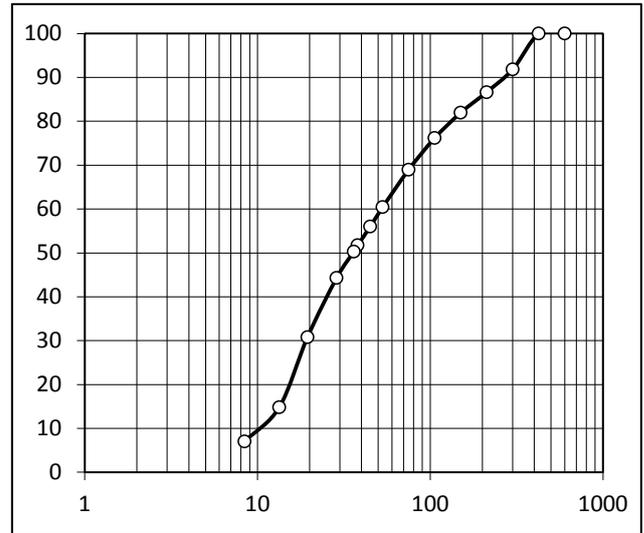
PRODUCT			Tin		Iron		Silica		Sulphur		Calcium Oxide		
NAME	Wt (gm)	Calc(gm)	Wt (%)	Sn (%)	Dist (%)	Fe (%)	Dist (%)	SiO2 (%)	Dist (%)	S (%)	Dist (%)	CaO (%)	Dist (%)
OF	849.6	849.6	20.11	0.46	15.3	21.74	20.5	38.40	19.9	1.01	8.2	0.82	17.9
calc UF	3374.2	3374.2	79.89	0.64	84.7	21.20	79.5	39.00	80.1	2.86	91.8	0.95	82.1
TOTAL	4223.80		100.00	0.60	100.0	21.31	100.0	38.88	100.0	2.49	100.0	0.92	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	T27 Cyclone underflow
DATE	260814
TECHNICIAN	MS

T27 Cyclone underflow 0		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	135	600	0.00	0.00	100.0
		425	0.00	0.00	100.0
		300	10.32	8.17	91.8
		212	6.55	5.18	86.7
		150	5.94	4.70	82.0
		106	7.30	5.78	76.2
		75	9.12	7.22	69.0
		53	10.79	8.54	60.4
		45	5.53	4.38	56.0
		38	5.45	4.31	51.7
CYCLOSIZER	CS1	36	1.78	1.41	50.3
FLOW 185	CS2	29	7.58	6.00	44.3
TEMP 21	CS3	19	17.08	13.51	30.8
SG 2.60	CS4	13	20.19	15.97	14.8
MINS 20	CS5	8	9.87	7.81	7.0
	SUB		8.89	7.03	0.0
	TOTAL		126.39	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	18.05	0.62	10.3	15.80	14.9	0.08	10.3	2.51	19.7	50.90	19.5	0.42	12.4
106	5.78	0.84	4.5	15.50	4.7	0.05	2.1	1.66	4.2	51.40	6.3	0.52	4.9
75	7.22	0.78	5.2	15.35	5.8	0.09	4.6	1.77	5.6	52.90	8.1	0.50	5.9
53	8.54	0.83	6.5	16.30	7.2	0.10	6.1	1.75	6.5	54.10	9.8	0.55	7.7
45	4.38	0.89	3.6	16.70	3.8	0.09	2.8	2.02	3.8	50.80	4.7	0.56	4.0
38	4.31	0.93	3.7	17.65	4.0	0.11	3.4	1.51	2.8	51.60	4.7	0.61	4.3
29	7.41	2.75	18.7	25.00	9.6	0.22	11.6	3.76	12.1	31.30	4.9	0.90	10.9
13	29.49	1.13	30.6	19.85	30.5	0.19	40.0	2.13	27.3	42.80	26.8	0.66	31.9
8	7.81	1.05	7.5	22.00	8.9	0.26	14.5	3.00	10.2	37.60	6.2	0.65	8.3
Cal <8	7.03	1.49	9.6	29.00	10.6	0.09	4.5	2.55	7.8	59.52	8.9	0.83	9.6
ASSAY	100.00	1.09	100.0	19.20	100.0	0.14	100.0	2.30	100.0	47.10	100.0	0.61	100.0

ANALYSES

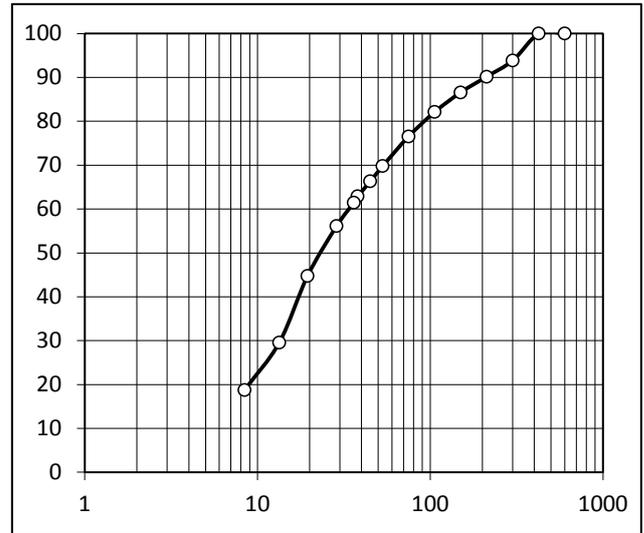
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
150	18.05	0.79	14.0	3.64	17.8	9.00	20.4
106	5.78	0.89	5.0	3.62	5.7	8.05	5.8
75	7.22	0.91	6.4	3.49	6.8	7.76	7.0
53	8.54	0.97	8.1	3.42	7.9	7.58	8.1
45	4.38	0.99	4.2	3.30	3.9	7.14	3.9
38	4.31	1.08	4.6	3.54	4.1	7.35	4.0
29	7.41	1.19	8.6	3.05	6.1	6.02	5.6
13	29.49	1.13	32.7	3.51	28.0	6.99	25.9
8	7.81	1.12	8.6	3.76	8.0	7.43	7.3
Cal <8	7.03	1.12	7.7	6.09	11.6	13.47	11.9
ASSAY	100.00	1.02	100.0	3.69	100.0	7.96	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	T28 Cyclone underflow
DATE	260814
TECHNICIAN	MS

T28 Cyclone underflow 0		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	7.62	6.16	93.8	
	212	4.53	3.66	90.2	
	150	4.44	3.59	86.6	
	106	5.54	4.48	82.1	
	94	75	6.87	5.55	76.6
		53	8.38	6.77	69.8
45		4.28	3.46	66.3	
38		4.26	3.44	62.9	
CYCLOSIZER	CS1	36	1.74	1.41	61.5
FLOW 185	CS2	29	6.60	5.33	56.1
TEMP 21	CS3	19	14.10	11.39	44.8
SG 2.60	CS4	13	18.77	15.17	29.6
MINS 20	CS5	8	13.40	10.83	18.8
		SUB	23.21	18.76	0.0
		TOTAL	123.74	100.00	



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
150	13.41	0.56	8.1	15.60	11.2	0.07	5.9	2.33	12.8	51.90	15.8	0.40	9.6
106	4.48	0.74	3.6	15.70	3.8	0.07	2.0	1.37	2.5	52.70	5.4	0.50	4.0
75	5.55	0.68	4.1	15.10	4.5	0.07	2.4	1.73	3.9	53.40	6.7	0.47	4.7
53	6.77	0.75	5.5	15.55	5.6	0.07	3.0	1.94	5.4	53.10	8.2	0.50	6.0
45	3.46	0.80	3.0	16.10	3.0	0.08	1.7	1.89	2.7	51.90	4.1	0.54	3.3
38	3.44	0.94	3.5	17.45	3.2	0.10	2.2	1.82	2.6	51.40	4.0	0.60	3.7
29	6.74	2.47	17.9	24.50	8.9	0.20	8.4	3.29	9.1	32.70	5.0	0.89	10.7
13	26.56	1.10	31.4	19.95	28.4	0.19	31.5	1.77	19.2	42.90	25.8	0.66	31.3
8	10.83	0.91	10.6	22.30	12.9	0.26	17.6	3.13	13.8	41.60	10.2	0.64	12.4
Cal <8	18.76	0.62	12.5	18.34	18.4	0.22	25.3	3.68	28.2	34.93	14.9	0.43	14.3
ASSAY	100.00	0.93	100.0	18.65	100.0	0.16	100.0	2.45	100.0	44.10	100.0	0.56	100.0

ANALYSES

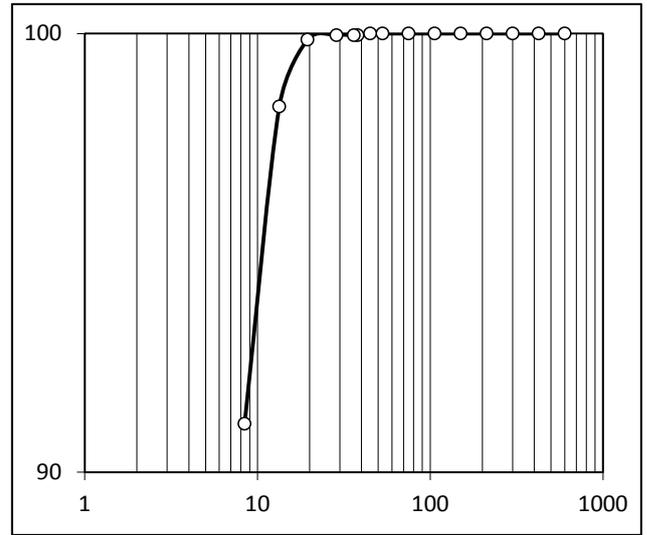
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
150	13.41	0.78	10.7	3.61	13.4	9.01	15.3
106	4.48	0.89	4.1	3.59	4.5	8.05	4.6
75	5.55	0.86	4.9	3.34	5.2	7.53	5.3
53	6.77	0.92	6.4	3.24	6.1	7.10	6.1
45	3.46	1.00	3.5	3.26	3.1	7.09	3.1
38	3.44	1.09	3.8	3.45	3.3	7.17	3.1
29	6.74	1.19	8.2	3.07	5.7	6.08	5.2
13	26.56	1.09	29.5	3.53	26.0	7.03	23.7
8	10.83	1.13	12.5	3.94	11.9	8.03	11.0
Cal <8	18.76	0.86	16.5	3.99	20.8	9.40	22.4
ASSAY	100.00	0.98	100.0	3.60	100.0	7.87	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	T27 Cyclone Overflow
DATE	260814
TECHNICIAN	MS

T27 Cyclone Overflow 0		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	0.00	0.00	100.0	
	212	0.00	0.00	100.0	
	150	0.00	0.00	100.0	
	106	0.00	0.00	100.0	
	75	0.00	0.00	100.0	
	53	0.00	0.00	100.0	
	45	0.00	0.00	100.0	
	38	0.04	0.04	100.0	
CYCLOSIZER		36	0.00	0.00	100.0
FLOW 185		29	0.00	0.00	100.0
TEMP 21		19	0.12	0.11	99.9
SG 2.60		13	1.74	1.52	98.3
MINS 20		8	8.26	7.23	91.1
SUB		104.11	91.11	0.0	
TOTAL		114.27	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
8	8.89	0.69	15.0	19.40	8.5	0.18	8.4	2.60	6.6	42.20	10.1	0.55	11.9
CALC<8	91.11	0.38	85.0	20.28	91.5	0.19	91.6	3.58	93.4	36.71	89.9	0.40	88.1
ASSAY	100.00	0.41	100.0	20.20	100.0	0.19	100.0	3.49	100.0	37.20	100.0	0.41	100.0

ANALYSES

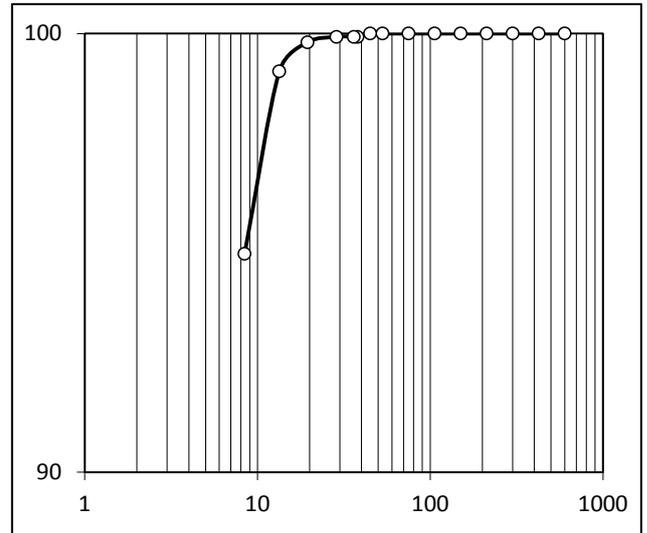
SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
8	8.89	1.04	11.9	3.70	7.9	7.78	5.9
CALC<8	91.11	0.75	88.1	4.24	92.1	12.03	94.1
ASSAY	100.0	0.78	100.0	4.19	100.0	11.65	100.0



BURNIE LABORATORY
[04] SIZING WITH FRACTION ASSAYS

PROJECT	T0879
SAMPLE NAME	T27 Cyclone Overflow
DATE	260814
TECHNICIAN	MS

T27 Cyclone Overflow 0		SIZE um	WEIGHTS		
			gm	(%)	%PASS
p80	600	0.00	0.00	100.0	
	425	0.00	0.00	100.0	
	300	0.00	0.00	100.0	
	212	0.00	0.00	100.0	
	150	0.00	0.00	100.0	
	106	0.00	0.00	100.0	
	75	0.00	0.00	100.0	
	53	0.00	0.00	100.0	
	45	0.00	0.00	100.0	
	38	0.09	0.07	99.9	
CYCLOSIZER		36	0.00	0.00	99.9
FLOW 185		29	0.00	0.00	99.9
TEMP 21		19	0.15	0.12	99.8
SG 2.60		13	0.80	0.66	99.1
MINS 20		8	5.03	4.16	95.0
SUB		114.90	94.98	0.0	
TOTAL		120.97	100.00		



ANALYSES

SIZE um	WT %	Sn		Fe		As		S		SiO2		MnO	
		%	dist	%	dist	%	dist	%	dist	%	dist	%	dist
8	5.02	0.71	8.9	19.75	4.8	0.18	5.0	2.73	4.8	41.00	5.6	0.53	6.6
CALC<8	94.98	0.38	91.1	20.54	95.2	0.18	95.0	2.85	95.2	36.26	94.4	0.39	93.4
ASSAY	100.00	0.40	100.0	20.50	100.0	0.18	100.0	2.84	100.0	36.50	100.0	0.40	100.0

ANALYSES

SIZE um	WT %	CaO		MgO		Al2O3	
		%	dist	%	dist	%	dist
8	5.02	1.11	7.4	3.66	4.3	7.64	3.2
CALC<8	94.98	0.73	92.6	4.33	95.7	12.18	96.8
ASSAY	100.0	0.75	100.0	4.30	100.0	11.95	100.0



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

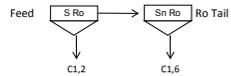
Appendix 11 – Tin Flotation Results



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T29
DATE	270814
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC(2)	
Media type		
Solids kg	500	
Water g	200	
Time min	5	
Speed rpm	60HZ	
Lime g		
End pH	pH	
End p80	um	



PRODUCT FLOATED
T28 Cyc Underflow

NOTES
500gm Feed

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	700	W/h	kWh/t

	pH	1.0 PAX g/t	0.5 H2SO4 g/t	10.0 SSF g/t	100.0 SPA7080 g/t	1.0 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Conditioning	4.5												
Conditioning S Ro C1	4.5		25			40			7-10	4.0	4.0	200	15
Conditioning S Ro C2			10						9-11	2.0	6.0	70	9
HIC Conditioning	4.0			41	203			5					
Condition	5.7			20	203			1					
Condition SSF						305		3					
Condition SPA	4.7					305	80	3	4-9	6.5	6.5	200	9
Sn Ro Con1						305		3					
Condition	5.3					305	40	3	5-7	4.0	10.5	200	28
Sn Ro Con2						305		3					
Condition	5.5					305	20	3	5-7	3.5	14.0	200	30
Sn Ro Con3						305		3					
Condition	5.9		41			203	20	3	5-7	4.0	18.0	200	19
Sn Ro Con4						203		3					
Condition	5.5					203	20	3	5-7	4.0	22.0	200	15
Sn Ro Con5						203		3					
Condition	5.8						20	3	5-7	4.0	26.0	200	5
Sn Ro Con6													
REAGENT TOTALS (g/t)			36	102	406	1626	241						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T29 S RoC1	30.9	6.3	0.62	4.0	30.1	9.9	1.17	44.9	15.1	42.1	23.5	3.3	0.22	3.1
S RoC2	6.6	1.3	0.93	1.3	25.4	1.8	0.56	4.6	10.9	6.5	31.4	1.0	0.35	1.0
SnRoC1	17.1	3.5	6.10	21.8	23.5	4.3	0.25	5.3	4.00	6.2	30.0	2.4	0.41	3.2
SnRoC2	55.7	11.3	2.93	34.1	30.4	18.1	0.12	8.3	1.68	8.4	26.1	6.7	0.80	20.1
SnRoC3	60.9	12.4	1.08	13.8	25.9	16.8	0.10	7.6	0.95	5.2	30.9	8.6	0.93	25.6
SnRoC4	38.9	7.9	0.66	5.4	19.9	8.3	0.09	4.3	1.06	3.7	43.3	7.7	0.77	13.5
SnRoC5	29.4	6.0	0.46	2.8	14.5	4.5	0.08	2.9	0.62	1.6	56.7	7.6	0.37	4.9
SnRoC6	10.2	2.1	0.49	1.0	16.4	1.8	0.08	1.0	1.01	0.9	46.1	2.2	0.49	2.3
Sn Ro T	242.4	49.3	0.31	15.7	13.4	34.5	0.07	21.1	1.16	25.4	54.5	60.6	0.24	26.3
CALC	492.1	100.0	0.97	100.0	19.0	100.0	0.16	100.0	2.25	100.0	44.3	100.0	0.45	100.0
ASSAY HEAD			0.93		18.7		0.16		2.45		44.1		0.56	

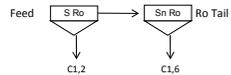
CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T29 S RoC1	30.9	6.3	0.62	4.0	30.1	9.9	1.17	44.9	15.1	42.1	23.5	3.3	0.22	3.1
S RoC2	37.5	7.6	0.67	5.3	29.3	11.7	1.06	49.5	14.4	48.5	24.9	4.3	0.24	4.1
SnRoC1	17.1	3.5	6.10	21.8	23.5	4.3	0.25	5.3	4.00	6.2	30.0	2.4	0.41	3.2
SnRoC2	72.8	14.8	3.67	56.0	28.8	22.4	0.15	13.6	2.22	14.6	27.0	9.0	0.71	23.3
SnRoC3	133.7	27.2	2.49	69.7	27.5	39.2	0.13	21.2	1.64	19.8	28.8	17.6	0.81	48.9
SnRoC4	172.6	35.1	2.08	75.1	25.8	47.4	0.12	25.5	1.51	23.5	32.1	25.4	0.80	62.4
SnRoC5	202.0	41.0	1.84	77.9	24.1	52.0	0.11	28.4	1.38	25.2	35.6	33.0	0.74	67.3
SnRoC6	212.2	43.1	1.78	79.0	23.7	53.8	0.11	29.5	1.36	26.1	36.1	35.2	0.73	69.6

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	C %	DIST	C organic %	DIST	C inorganic %	DIST
T29 S RoC1	30.9	6.3	0.50	3.3	2.33	4.2	4.38	3.5	2.58	6.4	0.44	18.0	2.14	5.8
S RoC2	6.6	1.3	0.69	1.0	2.58	1.0	5.94	1.0	2.87	1.5	0.35	3.1	0.35	0.2
SnRoC1	17.1	3.5	0.59	2.2	2.23	2.2	5.27	2.4	3.36	4.6	0.20	4.5	3.16	4.7
SnRoC2	55.7	11.3	0.72	8.6	2.56	8.2	4.08	6.0	5.54	24.9	0.10	7.4	5.44	26.4
SnRoC3	60.9	12.4	0.72	9.4	2.80	9.8	5.04	8.0	4.96	24.4	0.09	7.2	4.87	25.8
SnRoC4	38.9	7.9	0.91	7.6	2.94	6.6	6.78	6.9	3.36	10.6	0.11	5.7	3.26	11.0
SnRoC5	29.4	6.0	0.80	5.0	3.24	5.5	7.76	6.0	1.72	4.1	0.11	4.3	1.60	4.1
SnRoC6	10.2	2.1	1.67	3.6	4.16	2.4	9.66	2.6	2.04	1.7	0.14	1.9	1.90	1.7
Sn Ro T	242.4	49.3	1.15	59.5	4.30	60.1	10.0	63.6	1.11	21.7	0.15	48.0	0.96	20.3
CALC	492.1	100.0	0.95	100.0	3.52	100.0	7.75	100.0	2.52	100.0	0.15	100.0	2.33	100.0
ASSAY HEAD			0.98		3.60		7.87							

CUM PRODUCTS	CUM WT	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorganic %	CUM
T29 S RoC1	30.9	6.3	0.50	3.3	2.33	4.2	4.38	3.5	2.58	6.4	0.44	18.0	2.14	5.8
S RoC2	37.5	7.6	0.53	4.3	2.37	5.1	4.65	4.6	2.63	8.0	0.42	21.0	1.82	6.0
SnRoC1	17.1	3.5	0.59	2.2	2.23	2.2	5.27	2.4	3.36	4.6	0.20	4.5	3.16	4.7
SnRoC2	72.8	14.8	0.69	10.7	2.48	10.4	4.36	8.3	5.03	29.6	0.12	11.9	4.90	31.1
SnRoC3	133.7	27.2	0.70	20.1	2.63	20.2	4.67	16.4	5.00	54.0	0.11	19.1	4.89	56.9
SnRoC4	172.6	35.1	0.75	27.6	2.70	26.8	5.15	23.3	4.63	64.5	0.11	24.8	4.52	68.0
SnRoC5	202.0	41.0	0.76	32.6	2.78	32.3	5.53	29.3	4.20	68.6	0.11	29.0	4.10	72.1
SnRoC6	212.2	43.1	0.80	36.3	2.84	34.8	5.72	31.9	4.10	70.3	0.11	30.9	3.99	73.8

PROJECT	T0879
TEST NO	T31
DATE	270814
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC(2)	
Media type		
Solids kg	500	
Water g	200	
Time min	5	
Speed rpm	60HZ	
Lime g		
End pH	pH	
End p80	um	



PRODUCT FLOATED
T28 Cyc Underflow

NOTES
500gm Feed

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	700	W/h	kWh/t

	pH	1.0 CuSO4	0.5 PAX	10.0 H2SO4	100.0 SSF	1.0 SPA7080	0.5 MIBC		Cond Time	Air L/min	Float Time	Cum Float Time	Wet Wt g	Con % Solids
Conditioning	4.5	51												
Conditioning S Ro C1	4.5		25				40			7-13	4.0	4.0	200	17
Conditioning S Ro C2	4.5		10							7-13	7.0	11.0	250	7
HIC Conditioning	4.0			40	202				5					
Condition	5.5				202				1					
Condition SSF						303			3					
Condition SPA	4.4					303	80		3	5-9	4.5	4.5	200	8
Sn Ro Con1						303			3	5-7	3.5	8.0	200	25
Condition	4.7					303			3	5-7	3.5	11.5	200	29
Sn Ro Con2						303			3	5-7	4.0	15.5	200	22
Condition	4.8					202			3	5-7	4.0	19.5	200	12
Sn Ro Con3						202			3	5-7	4.0	23.5	200	7
Condition	4.9					202			3	5-7	4.0	23.5	200	7
Sn Ro Con4						202			3	5-7	4.0	23.5	200	7
Condition	5.1					202			3	5-7	4.0	23.5	200	7
Sn Ro Con5						202			3	5-7	4.0	23.5	200	7
Condition	5.3					202			3	5-7	4.0	23.5	200	7
Sn Ro Con6						202			3	5-7	4.0	23.5	200	7
Condition	5.3					202			3	5-7	4.0	23.5	200	7
REAGENT TOTALS (g/h)		51	35	40	404	1618	240							

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	Mn %	DIST %
T31 S RoC1	33.6	6.8	0.61	4.4	30.5	11.0	1.26	52.7	22.5	58.3	22.1	3.5	0.22	3.4
S RoC2	18.6	3.8	1.00	4.0	24.6	4.9	0.35	8.1	7.73	11.1	32.5	2.8	0.39	3.3
SnRoC1	16.8	3.4	7.18	25.9	23.1	4.2	0.15	3.1	2.16	2.8	28.8	2.3	0.44	3.4
SnRoC2	50.6	10.2	2.69	29.3	28.1	15.3	0.09	5.7	1.12	4.4	25.8	6.1	0.73	17.0
SnRoC3	57.1	11.5	1.08	13.3	25.6	16.3	0.09	6.4	0.67	3.0	31.4	8.3	0.92	24.2
SnRoC4	43.4	8.8	0.66	6.2	20.4	9.5	0.06	3.2	0.70	2.3	41.3	8.3	0.79	15.8
SnRoC5	24.5	5.0	0.51	2.7	16.5	4.3	0.06	1.8	0.65	1.2	49.1	5.6	0.57	6.4
SnRoC6	14.3	2.9	0.36	1.1	13.5	2.1	0.07	1.2	0.52	0.6	43.4	2.9	0.41	2.7
Sn Ro T	235.6	47.6	0.26	13.2	12.9	32.5	0.06	17.6	0.90	16.4	55.0	60.3	0.22	23.8
CALC	494.5	100.0	0.94	100.0	18.8	100.0	0.16	100.0	2.62	100.0	43.5	100.0	0.44	100.0
ASSAY HEAD			0.93		18.7		0.16		2.45		44.1			0.56

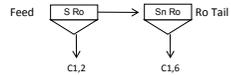
CUM PRODUCTS	CUM WT	WT %	Sn %	CUM %	Fe %	CUM %	As %	CUM %	S %	CUM %	SiO2 %	CUM %	Mn %	CUM %
T31 S RoC1	33.6	6.8	0.61	4.4	30.5	11.0	1.26	52.7	22.5	58.3	22.1	3.5	0.22	3.4
S RoC2	52.2	10.6	0.75	8.4	28.4	15.9	0.94	60.9	17.2	69.4	25.8	6.3	0.28	6.7
SnRoC1	16.8	3.4	7.18	25.9	23.1	4.2	0.15	3.1	2.16	2.8	28.8	2.3	0.44	3.4
SnRoC2	67.4	13.6	3.81	55.2	26.9	19.4	0.10	8.8	1.38	7.2	26.5	8.3	0.66	20.4
SnRoC3	124.5	25.2	2.56	68.5	26.7	35.7	0.10	15.2	1.05	10.1	28.8	16.7	0.78	44.5
SnRoC4	167.9	34.0	2.07	74.6	25.1	45.2	0.09	18.5	0.96	12.5	32.0	25.0	0.78	60.3
SnRoC5	192.4	38.9	1.87	77.3	24.0	49.6	0.08	20.3	0.92	13.7	34.2	30.6	0.75	66.7
SnRoC6	206.7	41.8	1.76	78.4	23.3	51.6	0.08	21.5	0.89	14.3	34.8	33.5	0.73	69.4

PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %	C %	DIST %	C organic %	DIST %	C inorganic %	DIST %
T31 S RoC1	33.6	6.8	0.46	3.3	2.33	4.5	4.26	3.7	2.09	5.7	0.43	19.7	1.66	5.0
S RoC2	18.6	3.8	0.74	2.9	2.89	3.1	6.63	3.2	3.04	4.6	0.37	9.4	0.37	0.6
SnRoC1	16.8	3.4	0.84	3.0	2.27	2.2	5.19	2.3	3.44	4.7	0.19	4.4	3.25	4.9
SnRoC2	50.6	10.2	0.72	7.8	2.41	6.9	3.91	5.1	5.36	22.1	0.09	6.2	5.27	24.1
SnRoC3	57.1	11.5	0.68	8.3	2.92	9.5	5.18	7.7	5.02	23.4	0.09	7.0	4.93	25.4
SnRoC4	43.4	8.8	0.78	7.2	3.18	7.8	6.86	7.7	3.55	12.6	0.09	5.3	3.46	13.6
SnRoC5	24.5	5.0	0.88	4.6	3.49	4.9	8.12	5.2	2.42	4.8	0.11	3.7	2.31	5.1
SnRoC6	14.3	2.9	0.92	2.8	3.40	2.8	7.86	2.9	1.96	2.3	0.12	2.3	1.83	2.4
Sn Ro T	235.6	47.6	1.19	60.0	4.36	58.4	10.2	62.3	1.03	19.8	0.13	41.9	0.89	18.9
CALC	494.5	100.0	0.95	100.0	3.56	100.0	7.80	100.0	2.48	100.0	0.15	100.0	2.24	100.0
ASSAY HEAD			0.98				7.87							

CUM PRODUCTS	CUM WT	WT %	CaO %	CUM %	MgO %	CUM %	Al2O3 %	CUM %	C %	CUM %	C organic %	CUM %	C inorganic %	CUM %
T31 S RoC1	33.6	6.8	0.46	3.3	2.33	4.5	4.26	3.7	2.09	5.7	0.43	19.7	1.66	5.0
S RoC2	52.2	10.6	0.56	6.2	2.53	7.5	5.10	6.9	2.43	10.3	0.41	29.2	1.20	5.7
SnRoC1	16.8	3.4	0.84	3.0	2.27	2.2	5.19	2.3	3.44	4.7	0.19	4.4	3.25	4.9
SnRoC2	67.4	13.6	0.75	10.8	2.38	9.1	4.23	7.4	4.88	26.8	0.11	10.6	4.77	29.0
SnRoC3	124.5	25.2	0.72	19.1	2.63	18.6	4.67	15.0	4.94	50.2	0.10	17.6	4.84	54.4
SnRoC4	167.9	34.0	0.73	26.4	2.77	26.4	5.23	22.8	4.58	62.8	0.10	23.0	4.48	68.0
SnRoC5	192.4	38.9	0.75	31.0	2.86	31.3	5.60	27.9	4.31	67.6	0.10	26.6	4.21	73.1
SnRoC6	206.7	41.8	0.76	33.8	2.90	34.1	5.76	30.8	4.15	69.9	0.10	29.0	4.04	75.4

PROJECT	T0879
TEST NO	133
DATE	280814
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC(2)	
Media type		
Solids kg	500	
Water g	200	
Time min	5	
Speed rpm	60HZ	
Lime g		
End pH	pH	
End p80	um	



PRODUCT FLOATED
T27 Cyc Underflow

NOTES
500gm Feed

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	700	W/h	
		kWh/t	

	pH	1.0 PAX	0.5 H2SO4	10.0 SSF	100.0 SPA7080	1.0 MIBC		Cond Time	Air L/min	Float Time	Cum Float Time	Wet Wt g	Con % Solids
Conditioning	4.8	51											
Conditioning S Ro C1	4.9		25			40			7-12	3.0	3.0	200	18
Conditioning S Ro C2			10						11-12	2.0	5.0	100	10
HIC Conditioning	4.0			20	203			5					
Condition	5.5				203			1					
Condition SSF						305		3		5-8	4.0	4.0	200
Condition SPA	4.8					305	80	3					8
Sn Ro Con1						305	40	3		5-7	3.5	7.5	200
Condition	5.1					305	20	3		5-7	3.0	10.5	200
Sn Ro Con2						305	20	3		5-7	3.5	14.0	200
Condition	5.4					203	20	3		5-7	4.0	18.0	200
Sn Ro Con3						203	20	3		5-7	3.5	21.5	200
Condition	5.5					203	20	3		5-7	4.0	200	3
Sn Ro Con4						203	20	3		5-7	4.0	200	3
Condition	5.7					203	20	3		5-7	4.0	200	3
Sn Ro Con5						203	20	3		5-7	4.0	200	3
Condition	5.8					203	20	3		5-7	4.0	200	3
Sn Ro Con6						203	20	3		5-7	4.0	200	3
Condition	5.8					203	20	3		5-7	4.0	200	3
REAGENT TOTALS (g/h)		51	36	20	406	1624	241						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T32 S RoC1	35.8	7.3	0.87	5.9	31.9	12.5	1.21	59.5	21.3	59.6	20.5	3.3	0.26	4.1
S RoC2	10.0	2.0	1.59	3.0	26.8	2.9	0.30	4.1	5.57	4.4	29.6	1.3	0.48	2.1
SnRoC1	15.9	3.2	6.02	18.2	21.4	3.7	0.08	1.7	1.26	1.6	35.0	2.5	0.60	4.2
SnRoC2	60.1	12.2	2.84	32.4	27.1	17.8	0.06	5.0	0.60	2.8	27.7	7.5	0.88	23.5
SnRoC3	48.5	9.8	1.19	10.9	24.3	12.9	0.05	3.3	0.49	1.9	35.5	7.8	0.92	19.8
SnRoC4	31.4	6.4	0.87	5.2	19.5	6.7	0.05	2.2	0.49	1.2	43.9	6.2	0.75	10.5
SnRoC5	15.4	3.1	0.82	2.4	17.6	3.0	0.07	1.5	0.61	0.7	46.8	3.3	0.62	4.2
SnRoC6	6.7	1.4	0.90	1.1	17.7	1.3	0.06	0.6	0.53	0.3	45.9	1.4	0.58	1.7
Sn Ro T	268.7	54.6	0.41	20.9	13.4	39.2	0.06	22.1	1.31	27.5	54.9	66.7	0.25	29.8
CALC	492.5	100.0	1.07	100.0	18.6	100.0	0.15	100.0	2.60	100.0	44.9	100.0	0.46	100.0
ASSAY HEAD			1.09		19.2		0.14		2.02		47.1		0.61	

CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T32 S RoC1	35.8	7.3	0.87	5.9	31.9	12.5	1.21	59.5	21.3	59.6	20.5	3.3	0.26	4.1
S RoC2	45.8	9.3	1.03	8.9	30.8	15.4	1.01	63.6	17.9	64.0	22.5	4.7	0.31	6.3
SnRoC1	15.9	3.2	6.02	18.2	21.4	3.7	0.08	1.7	1.26	1.6	35.0	2.5	0.60	4.2
SnRoC2	76.0	15.4	3.51	50.5	25.9	21.5	0.06	6.7	0.74	4.4	29.2	10.0	0.82	27.7
SnRoC3	124.5	25.3	2.60	61.5	25.3	34.4	0.06	10.0	0.64	6.2	31.7	17.8	0.86	47.5
SnRoC4	155.9	31.7	2.25	66.6	24.1	41.1	0.06	12.2	0.61	7.5	34.1	24.0	0.84	58.0
SnRoC5	171.3	34.8	2.13	69.0	23.5	44.1	0.06	13.7	0.61	8.2	35.3	27.3	0.82	62.2
SnRoC6	178.0	36.1	2.08	70.2	23.3	45.4	0.06	14.2	0.61	8.5	35.7	28.7	0.81	63.9

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	C %	DIST	C organic %	DIST	C inorganic %	DIST
T32 S RoC1	35.8	7.3	0.51	3.9	2.12	4.5	3.51	3.4	2.39	7.0	0.34	16.7	2.05	6.6
S RoC2	10.0	2.0	0.85	1.8	2.79	1.7	5.71	1.6	3.66	3.0	0.30	4.1	0.30	0.3
SnRoC1	15.9	3.2	0.70	2.4	2.17	2.1	4.71	2.0	3.94	5.1	0.14	3.0	3.80	5.4
SnRoC2	60.1	12.2	0.68	8.8	2.44	8.8	3.86	6.3	5.49	26.9	0.07	5.8	5.42	29.1
SnRoC3	48.5	9.8	0.71	7.4	2.76	8.0	5.09	6.7	4.59	18.2	0.10	6.6	4.50	19.5
SnRoC4	31.4	6.4	0.87	5.9	2.97	5.6	6.46	5.5	3.41	8.7	0.11	4.7	3.31	9.3
SnRoC5	15.4	3.1	1.05	3.5	3.35	3.1	7.34	3.1	2.69	3.4	0.12	2.5	2.57	3.5
SnRoC6	6.7	1.4	1.52	2.2	4.04	1.6	8.94	1.6	2.43	1.3	0.14	1.3	2.29	1.4
Sn Ro T	268.7	54.6	1.11	64.1	4.03	64.7	9.52	69.7	1.20	26.3	0.15	55.2	1.04	25.0
CALC	492.5	100.0	0.94	100.0	3.40	100.0	7.45	100.0	2.49	100.0	0.15	100.0	2.27	100.0
ASSAY HEAD			1.02		3.69		7.96							

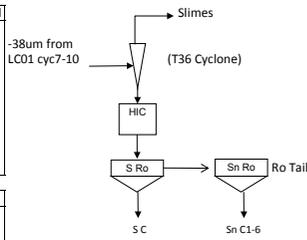
CUM PRODUCTS	CUM WT	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	C %	CUM	C organic %	CUM	C inorganic %	CUM
T32 S RoC1	35.8	7.3	0.51	3.9	2.12	4.5	3.51	3.4	2.39	7.0	0.34	16.7	2.05	6.6
S RoC2	45.8	9.3	0.58	5.8	2.27	6.2	3.99	5.0	2.67	10.0	0.33	20.8	1.67	6.8
SnRoC1	15.9	3.2	0.70	2.4	2.17	2.1	4.71	2.0	3.94	5.1	0.14	3.0	3.80	5.4
SnRoC2	76.0	15.4	0.68	11.2	2.38	10.8	4.04	8.4	5.17	32.1	0.08	8.8	5.08	34.5
SnRoC3	124.5	25.3	0.69	18.6	2.53	18.8	4.45	15.1	4.94	50.2	0.09	15.5	4.85	54.0
SnRoC4	155.9	31.7	0.73	24.5	2.62	24.4	4.85	20.6	4.63	59.0	0.09	20.2	4.54	63.3
SnRoC5	171.3	34.8	0.76	27.9	2.68	27.5	5.08	23.7	4.46	62.4	0.10	22.7	4.37	66.8
SnRoC6	178.0	36.1	0.79	30.1	2.74	29.1	5.22	25.3	4.38	63.7	0.10	24.0	4.29	68.2



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T38
DATE	120914
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Solids kg	1000	
Water g	1500	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80 um		



PRODUCT FLOATED
T37 Cyc Underflow

NOTES
1000gm Feed SSF hot water solution SPA hot water solution

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 SPA7080 g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Floater Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (25HZ)	3.5	496							5					
HIC Cond (60HZ)				297					5					
Fresh Water Wash														
Conditioning	5.5		25											
S Ro C	5.6					29			3-13		18.0	18.0	1530	16
Condition SSF	4.9			446					3					
Condition SPA					496				3					
Sn Ro Con1	4.8									3-9	5.0	5.0	210	19
Sn Ro Con2	5.1					5			8-14	5.0	10.0	210	16	
Sn Ro Con3	5.2				496				8-14	5.0	15.0	205	14	
Condition	4.6													
Sn Ro Con4	4.6					5			3-8	5.0	20.0	210	20	
Sn Ro Con5	4.8					5			5-9	5.0	25.0	215	21	
Sn Ro Con6	4.9								8-11	5.0	30.0	220	20	
REAGENT TOTALS (g/t)		496	25	744	992	44								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T38 S RoC	248.7	24.7	0.49	20.7	24.9	29.8	0.53	69.3	11.1	84.1	30.7	19.8	0.29	19.0
SnRoC1	40.2	4.0	2.30	15.7	29.0	5.6	0.15	3.2	3.33	4.1	22.5	2.3	0.51	5.4
SnRoC2	34.4	3.4	2.60	15.2	28.8	4.8	0.13	2.4	2.85	3.0	22.4	2.0	0.52	4.7
SnRoC3	29.4	2.9	2.23	11.1	27.2	3.9	0.11	1.7	2.09	1.9	24.9	1.9	0.50	3.9
SnRoC4	42.0	4.2	1.17	8.3	27.3	5.5	0.12	2.7	1.52	2.0	25.6	2.8	0.56	6.2
SnRoC5	44.2	4.4	1.20	9.0	27.5	5.9	0.10	2.3	0.81	1.1	26.8	3.1	0.61	7.1
SnRoC6	44.7	4.4	0.99	7.5	27.4	5.9	0.08	1.9	0.76	1.0	26.4	3.1	0.67	7.9
Sn Ro T	524.9	52.0	0.14	12.5	15.3	38.7	0.06	16.6	0.18	2.9	47.8	65.0	0.33	45.7
CALC	1008.5	100.0	0.58	100.0	20.6	100.0	0.19	100.0	3.24	100.0	38.2	100.0	0.38	100.0
ASSAY HEAD														

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe CUM	CUM	As CUM	CUM	S CUM	CUM	SiO2 CUM	CUM	Mn CUM	CUM
T38 S RoC	248.7	24.7	0.49	20.7	24.9	29.8	0.53	69.3	11.1	84.1	30.7	19.8	0.29	19.0
SnRoC1	40.2	4.0	2.30	15.7	29.0	5.6	0.15	3.2	3.33	4.1	22.5	2.3	0.51	5.4
SnRoC2	74.6	7.4	2.44	30.9	28.9	10.4	0.14	5.5	3.11	7.1	22.5	4.3	0.51	10.1
SnRoC3	104.0	10.3	2.38	42.0	28.4	14.2	0.13	7.2	2.82	9.0	23.1	6.2	0.51	14.0
SnRoC4	146.0	14.5	2.03	50.3	28.1	19.8	0.13	9.9	2.45	10.9	23.9	9.0	0.52	20.2
SnRoC5	190.2	18.9	1.84	59.3	28.0	25.6	0.12	12.2	2.07	12.0	24.5	12.1	0.54	27.3
SnRoC6	234.9	23.3	1.68	66.8	27.9	31.5	0.11	14.1	1.82	13.1	24.9	15.2	0.57	35.2

PRODUCTS	WT g	WT %	CaO	DIST	MgO	DIST	Al2O3	DIST
T38 S RoC	248.7	24.7	0.61	17.9	3.52	21.3	8.92	21.3
SnRoC1	40.2	4.0	0.37	1.8	2.89	2.8	6.31	2.4
SnRoC2	34.4	3.4	0.40	1.6	2.86	2.4	6.13	2.0
SnRoC3	29.4	2.9	0.45	1.6	2.94	2.1	6.64	1.9
SnRoC4	42.0	4.2	0.54	2.7	3.37	3.4	7.72	3.1
SnRoC5	44.2	4.4	0.63	3.3	3.49	3.7	7.64	3.2
SnRoC6	44.7	4.4	0.67	3.5	3.45	3.7	7.13	3.1
Sn Ro T	524.9	52.0	1.09	67.6	4.74	60.5	12.5	63.0
CALC	1008.5	100.0	0.84	100.0	4.08	100.0	10.3	100.0
ASSAY HEAD								

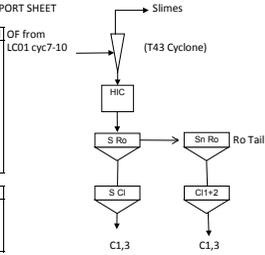
CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO	CUM	Al2O3	CUM
T38 S RoC	248.7	24.7	0.61	17.9	3.52	21.3	8.92	21.3
SnRoC1	40.2	4.0	0.37	1.8	2.89	2.8	6.31	2.4
SnRoC2	74.6	7.4	0.38	3.4	2.88	5.2	6.23	4.5
SnRoC3	104.0	10.3	0.40	4.9	2.89	7.3	6.34	6.3
SnRoC4	146.0	14.5	0.44	7.6	3.03	10.8	6.74	9.4
SnRoC5	190.2	18.9	0.49	10.9	3.14	14.5	6.95	12.7
SnRoC6	234.9	23.3	0.52	14.5	3.20	18.3	6.98	15.7



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	144
DATE	25/09/14
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media kg		
Media g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Line g		
End pH		
p80 μm		
kwh/t		



PRODUCT FLOATED
T43 Cyc Underflow

NOTES
Hic Slurry Density 50%

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	0.8	W/h	
	850	KWh/t	

	pH	10.0 H2SO4 g/t	0.5 SiPX g/t	1.0 SSF g/t	1.0 SPA7080 g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	3.5	1091		182					5					
Water Change														
Conditioning			45											
S Ro C	5.8					36				6-11	15.0	15.0	820	
Condition										4-5	1.5	16.5	80	29
S C1 C1	6.2	36												
Condition										5-9	2.0	18.5	100	11
S C1 C2	5.0									5-13	4.0	22.5	200	3
S C1 C3	5.0													
Condition SPA	4.5	455			546				3					
Sn Ro C1	4.2	182									5.0	5.0	200	
Condition					546	36				3-10	8.0	10.0	200	
Sn Ro C2	4.2													
Condition									3					
Sn C1 Con	4.2	36				9				0-5	5.0	18.0	250	
Sn C2 C1	3.2	36				9				0-3	3.0	21.0	20	33
Sn C2 C2										3-5	3.0	24.0	30	31
Sn C2 C3										3-5	5.0	29.0	100	23
REAGENT TOTALS (g/t)		2164	45	182	1091	90								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T44 S C1 C1	22.8	4.1	0.18	1.0	38.9	7.8	2.49	54.6	37.2	51.3	6.56	0.7	0.07	0.5
C2	11.1	2.0	0.35	1.0	33.8	3.3	0.97	10.3	23.4	15.7	17.3	0.9	0.19	0.7
C3	6.6	1.2	0.57	1.0	28.4	1.6	0.48	3.0	14.4	5.7	26.0	0.8	0.32	0.7
S C1 Tail	39.7	7.2	0.74	7.5	22.3	7.8	0.16	6.1	4.07	9.8	35.1	6.6	0.50	6.5
Sn C2 C1	6.6	1.2	3.36	5.7	36.2	2.1	0.12	0.8	2.50	1.0	8.79	0.3	1.00	2.2
C2	9.2	1.7	3.40	8.0	36.4	2.9	0.11	1.0	2.56	1.4	8.36	0.4	1.03	3.1
C3	22.5	4.1	3.05	17.5	36.9	7.3	0.08	1.7	1.22	1.7	8.42	0.9	1.15	8.5
Sn C2 Tail	24.6	4.5	2.07	13.0	32.1	6.9	0.09	2.1	1.67	2.5	17.1	2.0	1.19	9.6
Sn C1 Tail	28.7	5.2	1.56	11.4	28.5	7.2	0.08	2.2	1.21	2.1	22.7	3.1	1.10	10.3
Ro Tail	378.0	68.8	0.35	33.8	16.0	53.0	0.05	18.2	0.39	8.9	47.1	84.4	0.47	58.0
CALC	549.8	100.0	0.71	100.0	20.7	100.0	0.19	100.0	3.01	100.0	38.4	100.0	0.56	100.0
ASSAY HEAD			0.74		20.9		0.21		2.92		38.6		0.57	

CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T44 S C1 C1	22.8	4.1	0.18	1.0	38.9	7.8	2.49	54.6	37.2	51.3	6.56	0.7	0.07	0.5
C2	33.9	6.2	0.24	2.0	37.2	11.1	1.99	64.9	32.7	66.9	10.1	1.6	0.11	1.2
C3	40.5	7.4	0.29	3.0	35.8	12.7	1.75	67.9	29.7	72.7	12.7	2.4	0.14	1.9
S C1 Tail	80.2	14.6	0.51	10.5	29.1	20.5	0.96	74.0	17.0	82.4	23.8	9.0	0.32	8.4
Sn C2 C1	6.6	1.2	3.36	5.7	36.2	2.1	0.12	0.8	2.50	1.0	8.79	0.3	1.00	2.2
C2	15.8	2.9	3.38	13.7	36.3	5.0	0.11	1.7	2.53	2.4	8.54	0.6	1.02	5.3
C3	38.3	7.0	3.19	31.2	36.7	12.3	0.09	3.5	1.76	4.1	8.47	1.5	1.10	13.7
Sn C2 Tail	62.9	11.4	2.75	44.2	34.9	19.3	0.09	5.6	1.73	6.6	11.8	3.5	1.13	23.3
Sn C1 Tail	91.6	16.7	2.38	55.7	32.9	26.5	0.09	7.8	1.56	8.7	15.2	6.6	1.12	33.6

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST
T44 S C1 C1	22.8	4.1	0.15	0.6	1.10	1.2	1.20	0.6
C2	11.1	2.0	0.35	0.7	2.23	1.2	3.23	0.8
C3	6.6	1.2	0.51	0.6	3.14	1.0	5.56	0.8
S C1 Tail	39.7	7.2	0.76	5.4	3.66	6.8	8.82	7.4
Sn C2 C1	6.6	1.2	0.32	0.4	2.51	0.8	2.54	0.4
C2	9.2	1.7	0.32	0.5	2.45	1.1	2.30	0.4
C3	22.5	4.1	0.37	1.5	2.59	2.7	2.01	1.0
Sn C2 Tail	24.6	4.5	0.52	2.3	3.01	3.5	4.11	2.1
Sn C1 Tail	28.7	5.2	0.76	3.9	3.27	4.4	5.72	3.5
Ro Tail	378.0	68.8	1.23	84.0	4.39	77.5	10.4	83.1
CALC	549.8	100.0	1.01	100.0	3.89	100.0	8.60	100.0
ASSAY HEAD			1.05		3.91		8.60	

CUM PRODUCTS	CUM WT	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM
T44 S C1 C1	22.8	4.1	0.15	0.6	1.10	1.2	1.20	0.6
C2	33.9	6.2	0.22	1.3	1.47	2.3	1.86	1.3
C3	40.5	7.4	0.26	1.9	1.74	3.3	2.47	2.1
S C1 Tail	80.2	14.6	0.51	7.4	2.69	10.1	5.61	9.5
Sn C2 C1	6.6	1.2	0.32	0.4	2.51	0.8	2.54	0.4
C2	15.8	2.9	0.32	0.9	2.48	1.8	2.40	0.8
C3	38.3	7.0	0.35	2.4	2.54	4.5	2.17	1.8
Sn C2 Tail	62.9	11.4	0.42	4.7	2.73	8.0	2.93	3.9
Sn C1 Tail	91.6	16.7	0.52	8.7	2.90	12.4	3.80	7.4

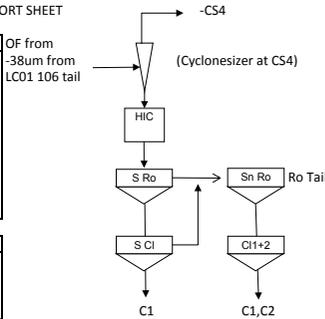


BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T45
DATE	011014
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Line g		
End pH		
End p80		

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
	0.8	W/h	
Speed	850	kWh/t	



PRODUCT FLOATED
-38 from LC01 -106 tail
Deslimed at CS4

NOTES
Hic Slurry Density 50%

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 SPA7080 g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	3.5	398		199					5					
Water Change			50						3	6-11	7.0	7.0	300	
Conditioning S Ro C	5.8					39				2-9	5.0	12.0	163	20
Condition S Cl1 C1	6.9					20			3					
Condition SPA	6.1			100					3		10.0	10.0	275	
Sn Ro C1					597	20			3					
Condition Sn Ro C2	6.8				597					5-11	10.0	20.0	330	
Condition Sn Ro C3	5.0	80			299	20			3					
Condition Sn Cl1 C1	6.0									7-8	5.0	25.0	170	
Sn Cl1 C1	6.4									0.5-11	12.0	37.0	415	
Sn Cl2 C1	6.5					10				0.5-1	1.0	38.0	20	55
SnCl2 C2	6.5									0.5-1	1.0	39.0	30	50
REAGENT TOTALS (g/t)		478	50	299	1494	108								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T45 S Cl1 C1	31.9	6.4	0.22	1.9	38.6	10.9	1.38	59.9	32.9	81.6	9.82	1.6	0.14	1.1
Sn Cl2 C1	10.9	2.2	3.63	10.6	37.7	3.6	0.08	1.2	0.86	0.7	6.13	0.4	1.46	3.9
C2	15.0	3.0	4.20	16.9	37.2	4.9	0.07	1.4	0.92	1.1	5.96	0.5	1.40	5.1
Sn Cl2 Tail	168.8	33.6	1.31	59.5	35.2	52.5	0.06	13.8	0.79	10.4	11.9	10.5	1.62	67.1
Sn Cl1 Tail	90.7	18.1	0.29	7.1	15.0	12.0	0.07	8.6	0.66	4.7	51.9	24.7	0.76	16.9
Ro Tail	184.8	36.8	0.08	4.0	9.87	16.1	0.06	15.1	0.11	1.6	64.2	62.3	0.13	5.9
CALC	502.1	100.0	0.74	100.0	22.6	100.0	0.15	100.0	2.56	100.0	37.9	100.0	0.81	100.0
ASSAY HEAD			0.75		22.1		0.14		2.57		37.0		0.79	

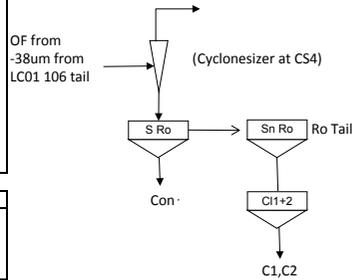
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T45 S Cl1 C1	31.9	6.4	0.22	1.9	38.6	10.9	1.38	59.9	32.9	81.6	9.82	1.6	0.14	1.1
Sn Cl2 C1	10.9	2.2	3.63	10.6	37.7	3.6	0.08	1.2	0.86	0.7	6.13	0.4	1.46	3.9
C2	25.9	5.2	3.96	27.6	37.4	8.6	0.07	2.6	0.89	1.8	6.03	0.8	1.43	9.1
Sn Cl2 Tail	194.7	38.8	1.66	87.1	35.5	61.0	0.06	16.4	0.80	12.2	11.1	11.4	1.59	76.1
Sn Cl1 Tail	285.4	56.8	1.23	94.1	29.0	73.0	0.06	25.0	0.76	16.8	24.1	36.1	1.33	93.0

PRODUCTS	WT g	WT %	CaO	DIST	MgO	DIST	Al2O3	DIST
T45 S Cl1 C1	31.9	6.4	0.27	1.5	1.04	2.0	1.96	1.8
Sn Cl2 C1	10.9	2.2	0.79	1.5	2.68	1.7	2.82	0.9
C2	15.0	3.0	0.78	2.0	2.55	2.3	2.71	1.2
Sn Cl2 Tail	168.8	33.6	0.87	25.5	3.04	30.3	3.76	18.6
Sn Cl1 Tail	90.7	18.1	1.65	25.9	3.09	16.5	7.72	20.5
Ro Tail	184.8	36.8	1.36	43.6	4.34	47.3	10.5	56.9
CALC	502.1	100.0	1.15	100.0	3.38	100.0	6.79	100.0
ASSAY HEAD			1.12		3.30		6.68	

CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO	CUM	Al2O3	CUM
T45 S Cl1 C1	31.9	6.4	0.27	1.5	1.04	2.0	1.96	1.8
Sn Cl2 C1	10.9	2.2	0.79	1.5	2.68	1.7	2.82	0.9
C2	25.9	5.2	0.78	3.5	2.60	4.0	2.76	2.1
Sn Cl2 Tail	194.7	38.8	0.86	29.0	2.98	34.2	3.63	20.7
Sn Cl1 Tail	285.4	56.8	1.11	54.9	3.02	50.8	4.93	41.2

PROJECT	T0879
TEST NO	T46
DATE	011014
TECHNICIAN	MW

Milling		Primary	Regrind
Mill type	HIC		
Media type	kg		
Solids	g	500	
Water	g	400	
Time	min	5.0	
Speed	rpm	60HZ	
Lime	g		
End pH	pH		
End p80	µm		



PRODUCT FLOATED	
-38 from LC01 -106 tail	
Deslimed at CS4	

NOTES	

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	0.8	W/h	
	850	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 SPA7080 g/t	0.5 MIBC g/t			Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
Conditioning S Ro C	6.5		50						3	6-11	7.0	7.0	300	12
Condition S Ro C1	4.4			199	298				3		10.0	10.0	345	
Condition S Ro C2	6.1				298				3	7-12	10.0	20.0	310	
Condition S Ro C3	6.4				199	20			3		5.0	25.0	150	
Sn Cl1 C1	6.1									1-11	12.0	37.0	395	
Sn Cl2 C1	6.3					10				0.5-1	1.0	38.0	20	52
SnCl2 C2	6.3									0.5-1	1.0	39.0	30	50
REAGENT TOTALS (g/t)			50	199	796	69								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	Mn %	DIST
T46 S Ro Con	34.7	6.9	0.61	5.6	34.1	10.4	1.27	59.0	27.5	73.5	11.6	2.1	0.31	2.6
Sn Cl2 C1	10.4	2.1	4.30	11.9	39.6	3.6	0.07	1.0	0.92	0.7	3.47	0.2	1.49	3.8
C2	14.9	3.0	4.83	19.2	40.1	5.3	0.09	1.8	0.88	1.0	3.19	0.3	1.47	5.4
Sn Cl2 Tail	135.8	27.0	1.36	49.2	38.1	45.5	0.07	12.7	1.08	11.3	8.42	6.1	1.62	53.9
Sn Cl1 Tail	64.4	12.8	0.41	7.0	23.1	13.1	0.07	6.0	1.55	7.7	35.0	12.0	1.31	20.7
Ro Tail	242.6	48.2	0.11	7.1	10.4	22.2	0.06	19.5	0.31	5.8	61.4	79.3	0.23	13.7
CALC	502.8	100.0	0.75	100.0	22.6	100.0	0.15	100.0	2.58	100.0	37.3	100.0	0.81	100.0
ASSAY HEAD			0.75		22.1		0.14		2.57		37.0		0.79	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	Mn %	CUM
T46 S Ro Con	34.7	6.9	0.61	5.6	34.1	10.4	1.27	59.0	27.5	73.5	11.6	2.1	0.31	2.6
Sn Cl2 C1	10.4	2.1	4.30	11.9	39.6	3.6	0.07	1.0	0.92	0.7	3.47	0.2	1.49	3.8
C2	25.3	5.0	4.61	31.1	39.9	8.9	0.08	2.8	0.90	1.7	3.31	0.4	1.48	9.2
Sn Cl2 Tail	161.1	32.0	1.87	80.2	38.4	54.3	0.07	15.5	1.05	13.0	7.62	6.5	1.60	63.0
Sn Cl1 Tail	225.5	44.8	1.45	87.3	34.0	67.4	0.07	21.5	1.19	20.7	15.4	18.5	1.52	83.7

PRODUCTS	WT g	WT %	CaO	DIST	MgO	DIST	Al2O3	DIST
T46 S Ro Con	34.7	6.9	2.56	15.8	1.74	3.6	2.64	2.7
Sn Cl2 C1	10.4	2.1	0.33	0.6	2.41	1.5	1.36	0.4
C2	14.9	3.0	0.30	0.8	2.39	2.1	1.21	0.5
Sn Cl2 Tail	135.8	27.0	0.51	12.3	2.88	23.2	2.56	10.3
Sn Cl1 Tail	64.4	12.8	1.09	12.5	3.24	12.4	6.55	12.5
Ro Tail	242.6	48.2	1.35	58.1	3.98	57.3	10.3	73.6
CALC	502.8	100.0	1.12	100.0	3.35	100.0	6.72	100.0
ASSAY HEAD			1.12		3.30		6.68	

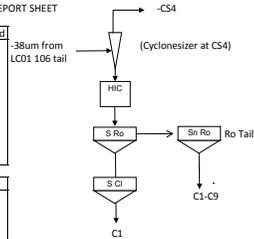
CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO	CUM	Al2O3	CUM
T46 S Ro Con	34.7	6.9	2.56	15.8	1.74	3.6	2.64	2.7
Sn Cl2 C1	10.4	2.1	0.33	0.6	2.41	1.5	1.36	0.4
C2	25.3	5.0	0.31	1.4	2.40	3.6	1.27	1.0
Sn Cl2 Tail	161.1	32.0	0.48	13.7	2.80	26.8	2.36	11.2
Sn Cl1 Tail	225.5	44.8	0.65	26.1	2.93	39.2	3.55	23.7



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	148
DATE	131014
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End pH0		



PRODUCT FLOATED	
-38 from LCO1 Cyc1-10-106 Tail	
Non Mags Deslimed at C54	

NOTES	
From T47 LIMS test	

Float Cell	Volume	Regrind Power
Rougher C1	2.5	Start
	1.5	Finish
Speed	850	W/h

	pH	10.0 H2SO4	0.5 SIPX	1.0 SSF	1.0 Na2SO3	1.0 SPA7080	0.495 MIBC	Cond	Air	Fleat	Cum	Wet	Con %
			g/t	g/t	g/t	g/t	g/t	Time	U/min	Time	Fleat	Wt	Solids
								min		min	Time	g	
HIC Cond (60HZ)	2.5	584		195				5					
Water Change													
Conditioning S Ro C	5.6		49				58	3	7-9	5.0	5.0	300	
Condition S C1 C1	6.6						19		3-7	3.5	8.5	120	24
Condition Condition	4.0	39		195	292			3					
Condition Sn Ro C1						292		3		3.0	3.0	125	22
Sn Ro C2	4.8								7-8	3.0	6.0	130	22
Sn Ro C3	4.9						19		6-7	3.0	9.0	135	19
Condition Sn Ro C4	5.5					292		3	6-8	3.0	12.0	150	34
Sn Ro C5	5.5						19		7-8	3.0	15.0	150	30
Sn Ro C6	5.8								7-9	3.0	18.0	130	24
Condition Sn Ro C7	6.2					292		3	7-9	3.0	21.0	115	15
Sn Ro C8	6.2						19		7-8	3.0	24.0	125	8
Sn Ro C9	6.2								7-9	3.0	27.0	110	6
REAGENT TOTALS (g/t)		623	49	389	292	876	135						

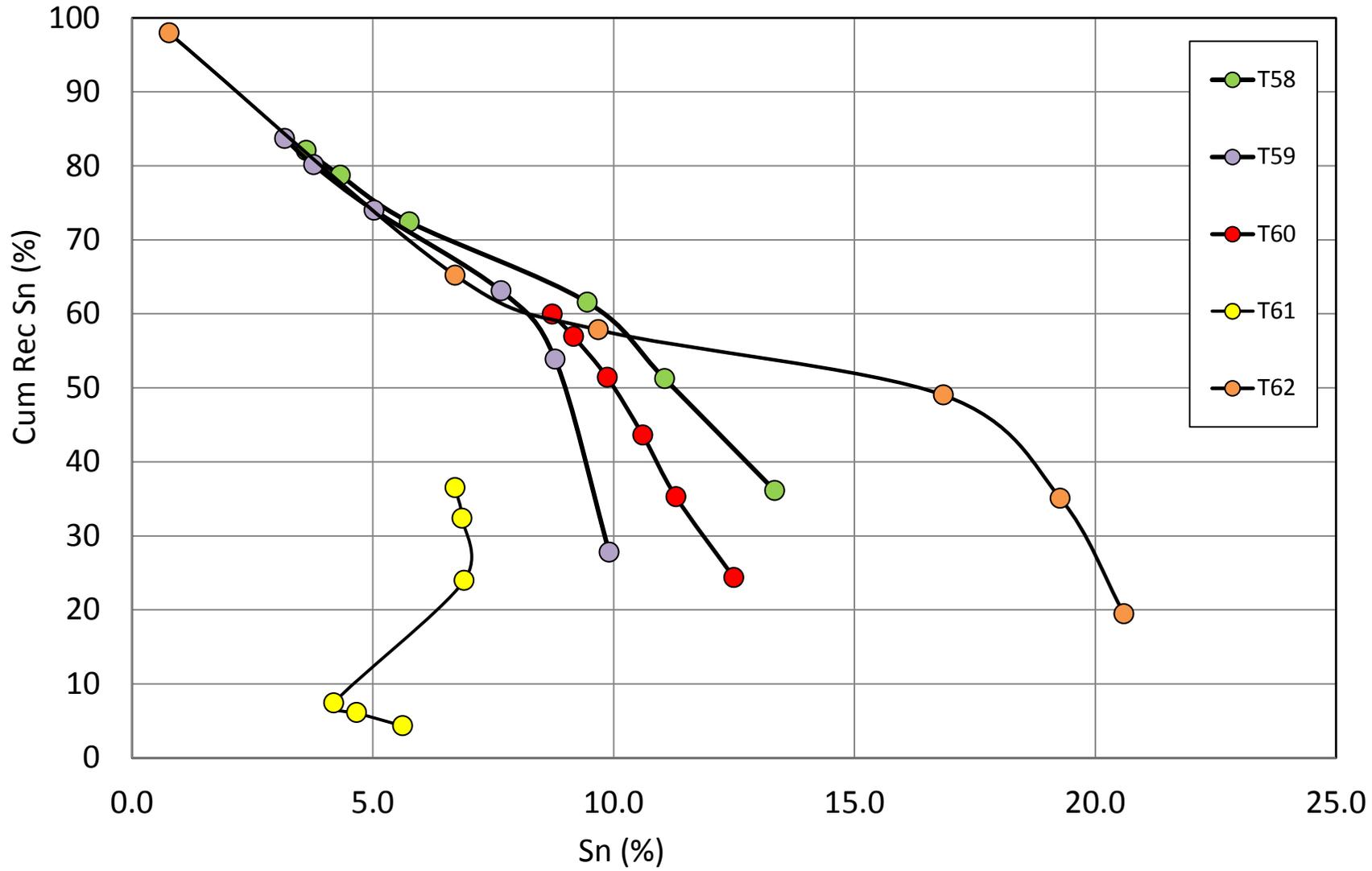
PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T48 S C1 C1	28.8	5.6	0.19	1.4	38.1	10.2	1.61	61.2	35.5	86.8	9.03	1.3	0.11	0.7
S C1 Tail	7.9	1.5	0.61	1.2	26.7	2.0	0.22	2.3	6.96	4.7	28.7	1.1	0.53	1.0
Sn Ro C1	27.8	5.4	7.29	50.5	33.1	8.5	0.05	1.8	0.43	1.0	5.73	0.8	1.62	10.5
C2	28.6	5.6	2.38	17.0	36.5	9.7	0.05	1.9	0.38	0.9	6.58	0.9	1.73	11.5
C3	25.6	5.0	1.29	8.2	36.4	8.6	0.05	1.7	0.41	0.9	8.41	1.1	1.59	9.5
C4	50.5	9.8	0.55	6.9	36.1	16.9	0.06	4.0	0.22	0.9	9.42	2.4	1.91	22.4
C5	44.7	8.7	0.42	4.7	30.2	12.5	0.06	3.5	0.38	1.4	17.1	3.8	1.75	18.2
C6	30.6	6.0	0.37	2.8	23.4	6.6	0.06	2.4	0.31	0.8	29.4	4.5	1.43	10.2
C7	17.7	3.4	0.28	1.2	20.3	3.3	0.06	1.4	0.24	0.4	32.2	2.8	1.54	6.3
C8	9.6	1.9	0.35	0.8	16.5	1.5	0.05	0.6	0.25	0.2	42.4	2.0	0.94	2.1
C9	7.0	1.4	0.31	0.5	14.5	0.9	0.05	0.5	0.28	0.2	48.0	1.7	0.71	1.2
Ro Tail	234.8	45.7	0.08	4.7	8.82	19.2	0.06	18.6	0.09	1.8	66.0	77.5	0.12	6.5
CALC	513.6	100.0	0.78	100.0	21.0	100.0	0.15	100.0	2.29	100.0	38.9	100.0	0.84	100.0
ASSAY HEAD			0.78		20.8		0.14		2.40		38.4		0.83	

CUM PRODUCTS	CUM WT	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T48 S C1 C1	28.8	5.6	0.19	1.36	38.1	10.2	1.61	61.2	35.5	86.8	9.03	1.30	0.11	0.74
S C1 Tail	36.7	7.1	0.28	2.6	35.6	12.1	1.31	63.5	29.4	91.5	13.3	2.4	0.20	1.7
Sn Ro C1	72.9	5.4	7.29	50.5	33.1	8.5	0.05	4.1	0.43	1.0	5.73	0.8	1.62	10.5
C2	56.4	11.0	4.80	67.5	34.8	18.2	0.05	6.0	0.40	1.9	6.16	1.7	1.68	22.0
C3	82.0	16.0	3.70	75.7	35.3	26.9	0.05	7.7	0.41	2.8	6.86	2.8	1.65	31.4
C4	132.5	25.8	2.50	82.6	35.6	43.8	0.05	11.7	0.34	3.8	7.84	5.2	1.75	53.8
C5	177.2	34.5	1.98	87.3	34.2	56.3	0.06	15.3	0.35	5.2	10.2	9.0	1.75	72.0
C6	207.8	40.5	1.74	90.1	32.7	62.9	0.06	17.7	0.34	6.0	13.0	13.5	1.70	82.2
C7	225.5	43.9	1.63	91.4	31.7	66.3	0.06	19.1	0.33	6.4	14.5	16.4	1.69	88.5
C8	235.1	45.8	1.57	92.2	31.1	67.7	0.06	19.7	0.33	6.6	15.7	18.4	1.66	90.6
C9	242.1	47.1	1.54	92.8	30.6	68.7	0.06	20.2	0.33	6.7	16.6	20.1	1.63	91.7

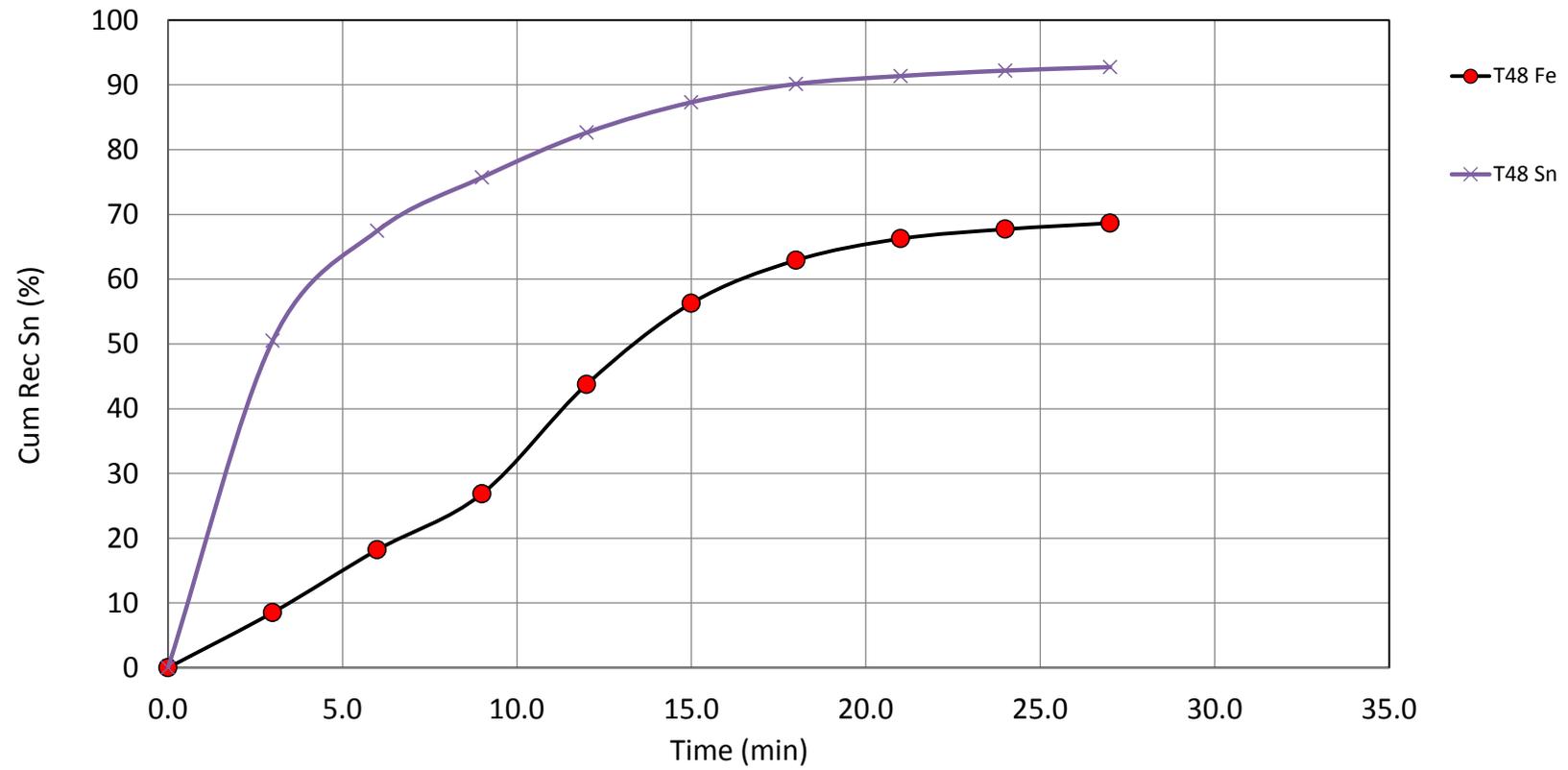
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST
T48 S C1 C1	28.8	5.6	0.24	1.2	1.13	1.9	1.76	1.7
S C1 Tail	7.9	1.5	0.87	1.2	2.96	1.4	5.23	1.4
Sn Ro C1	27.8	5.4	1.17	5.6	2.60	4.2	1.94	1.8
C2	28.6	5.6	0.82	4.0	2.90	4.8	2.23	2.1
C3	25.6	5.0	0.68	3.0	2.99	4.5	2.84	2.4
C4	28.6	9.8	0.82	7.1	2.90	8.5	2.23	3.7
C5	25.6	8.7	0.68	5.2	2.99	4.5	2.84	2.4
C6	25.6	6.0	0.68	3.6	2.99	4.5	2.84	2.4
C7	25.6	3.4	0.68	2.1	2.99	4.5	2.84	2.4
C8	25.6	1.9	0.68	1.1	2.99	4.5	2.84	2.4
C9	7.0	1.4	1.65	2.0	3.55	1.4	9.91	2.3
Ro Tail	234.8	45.7	1.59	64.0	4.04	55.3	9.69	75.1
CALC	491.5	100.0	1.14	100.0	3.34	100.0	5.90	100.0
ASSAY HEAD			1.22		3.44		6.86	

CUM PRODUCTS	CUM WT	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM
T48 S C1 C1	28.8	5.6	0.24	1.2	1.13	1.9	1.76	1.7
S C1 Tail	36.7	7.1	0.38	2.4	1.52	3.3	2.51	3.0
Sn Ro C1	72.9	5.4	1.17	5.6	2.60	4.2	1.94	1.8
C2	56.4	11.0	0.99	9.6	2.75	9.1	2.09	3.9
C3	82.0	16.0	0.89	12.6	2.83	13.5	2.32	6.3
C4	132.5	25.8	0.87	19.7	2.85	22.1	2.29	10.0
C5	177.2	34.5	0.82	24.9	2.89	26.5	2.43	12.4
C6	207.8	40.5	0.80	28.5	2.90	31.0	2.49	14.8
C7	225.5	43.9	0.79	30.5	2.91	35.5	2.52	17.2
C8	235.1	45.8	0.79	31.6	2.91	39.9	2.53	19.6
C9	242.1	47.1	0.81	33.6	2.93	41.4	2.74	21.9

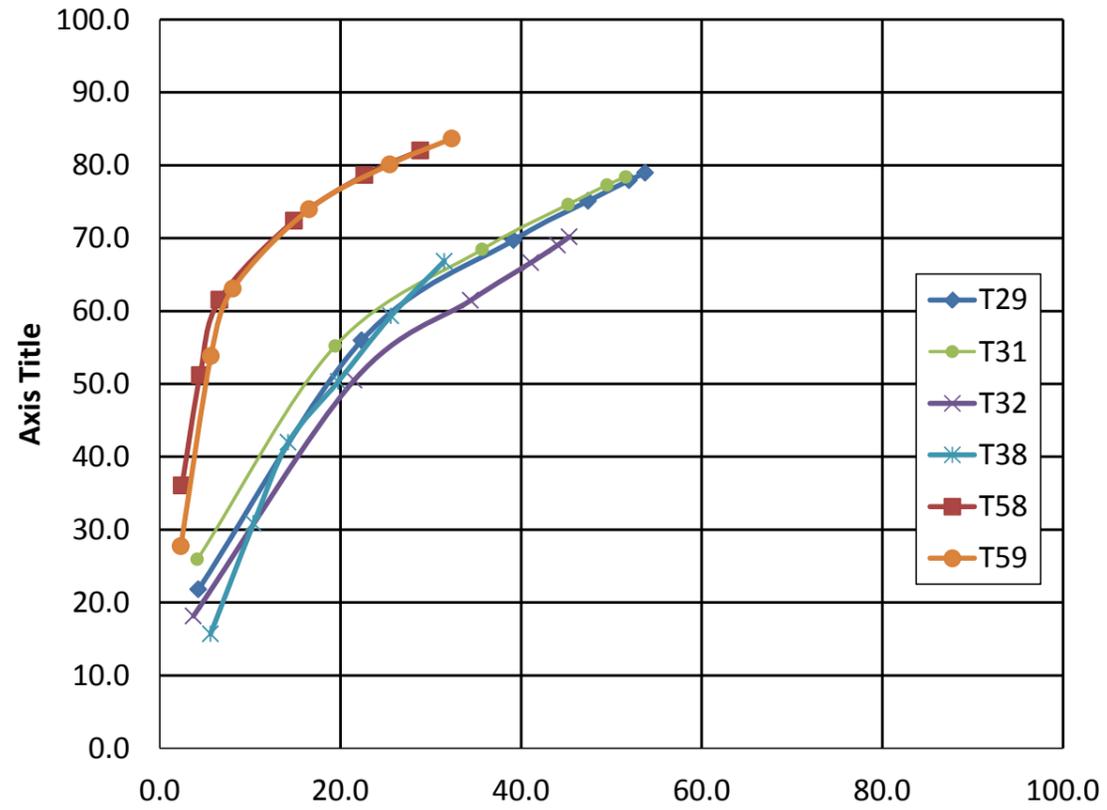
Rougher Sn Grade vs Recovery



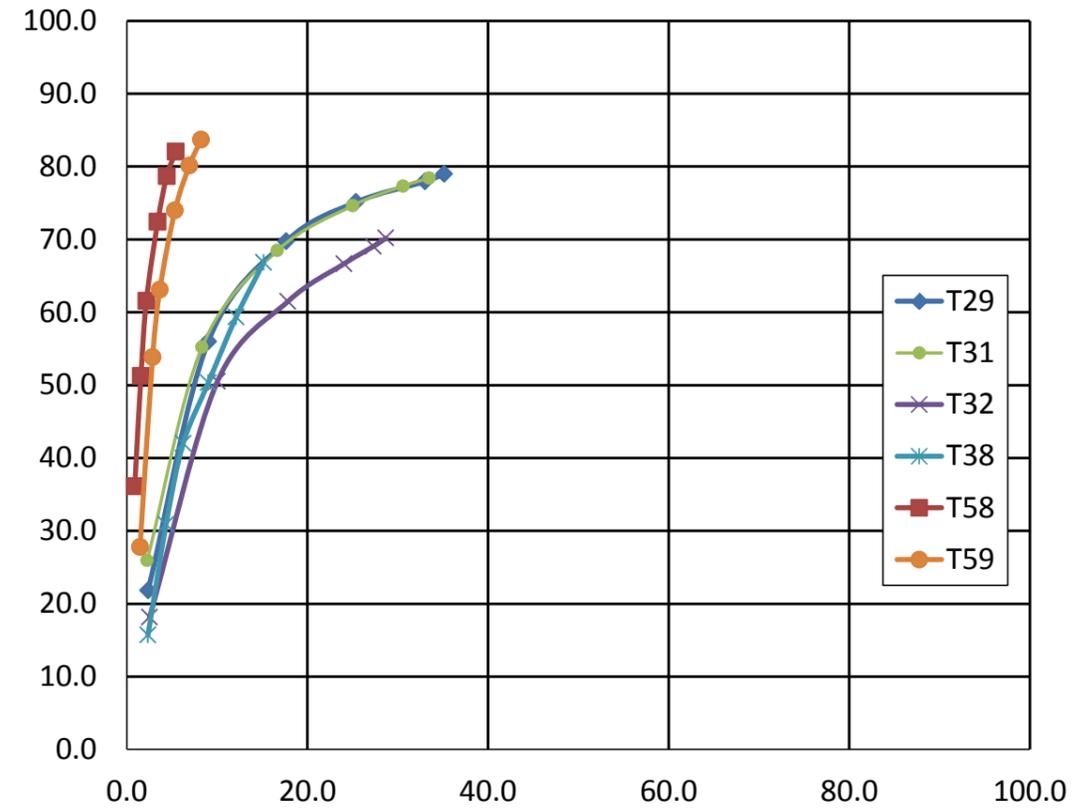
Rougher Sn Recovery vs Time



Roughing Fe vs Sn Rec



Roughing SiO2 vs Sn Rec

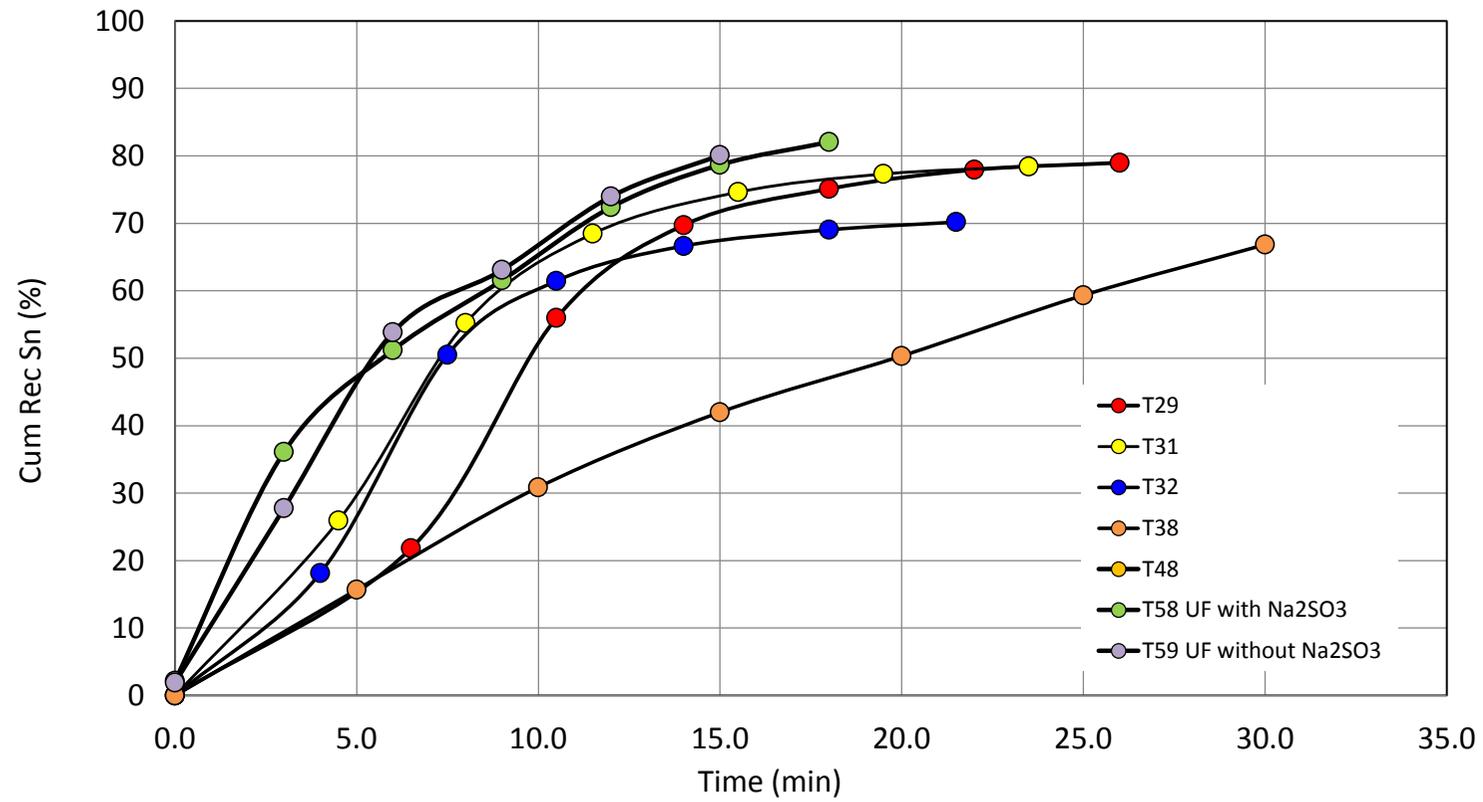


Make larger deslime cut

Use copper sulphate
Use Pax in sulphide float

Use low spa doses
Use low frother dose in roughing

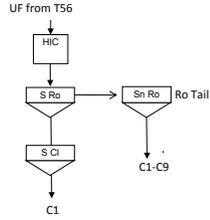
Rougher Sn Recovery vs Time



PROJECT	T0879
TEST NO	T58
DATE	0
TECHNICIAN	SL

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End p80		

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	



PRODUCT FLOATED	
UF from T56	

NOTES	
UF from T56	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	401		200				5					
Water Change			50					3	7-9	6.0	6.0	175	
Conditioning S Ro C	5.7						60						
Condition S C1 C1	6.6								1-3	5.5	11.5	90	32
Condition Condition	4.0	180		200				3					
Condition Sn Ro C1	3.9				301	301		3		3.0	3.0	125	9
Condition Sn Ro C2	4.2							3		3.0	6.0	130	6
Condition Sn Ro C3	4.5								7-8	3.0	9.0	135	6
Condition Sn Ro C4	4.6					100		3		3.0	12.0	150	16
Condition Sn Ro C5	4.6						20		9-11	3.0	15.0	150	15
Condition Sn Ro C6	4.7						20		9-11	3.0	18.0	130	14
Condition Sn Ro C6	4.8						20		9-11	3.0	18.0	130	14
REAGENT TOTALS (g/t)		581	50	401	301	401	99						

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	MnO %	DIST %
T58 S C1 C1	29.0	5.8	0.14	1.0	42.4	11.1	1.30	49.9	24.5	72.3	6.43	1.0	0.08	0.6
S C1 Tail	8.1	1.6	0.56	1.1	33.6	2.5	1.12	12.0	14.0	11.5	19.9	0.8	0.39	0.8
Sn Ro C1	10.8	2.2	13.4	36.1	25.1	2.5	0.12	1.7	1.45	1.6	15.6	0.9	0.68	1.9
C2	7.7	1.5	7.85	15.1	28.7	2.0	0.10	1.0	1.16	0.9	17.0	0.7	0.77	1.6
C3	7.5	1.5	5.50	10.3	31.9	2.2	0.08	0.8	0.79	0.6	15.4	0.6	0.86	1.7
C4	24.2	4.9	1.79	10.8	37.7	8.3	0.06	1.9	0.58	1.4	9.97	1.3	1.31	8.3
C5	22.4	4.5	1.12	6.3	38.6	7.8	0.06	1.8	0.46	1.0	8.56	1.0	1.46	8.6
C6	18.0	3.6	0.75	3.4	38.0	6.2	0.06	1.4	0.42	0.8	10.6	1.0	1.55	7.3
Ro Tail	371.1	74.4	0.17	15.8	17.2	57.6	0.06	29.5	0.26	9.8	47.9	92.8	0.71	69.2
CALC	498.8	100.0	0.80	100.0	22.2	100.0	0.15	100.0	1.97	100.0	38.4	100.0	0.76	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

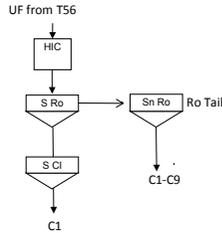
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM %	Fe %	CUM %	As %	CUM %	S %	CUM %	SiO2 %	CUM %	MnO %	CUM %
T58 S C1 C1	29.0	5.8	0.14	1.02	42.4	11.1	1.30	49.9	24.5	72.3	6.43	0.97	0.08	0.61
S C1 Tail	37.1	7.4	0.23	2.2	40.5	13.6	1.26	61.9	22.2	83.8	9.37	1.8	0.15	1.4
Sn Ro C1	10.8	2.2	13.4	36.1	25.1	2.5	0.12	13.7	1.45	1.6	15.6	0.9	0.68	1.9
C2	18.5	3.7	11.1	51.2	26.6	4.4	0.11	14.7	1.33	2.5	16.2	1.6	0.72	3.5
C3	26.0	5.2	9.46	61.6	28.1	6.6	0.10	15.5	1.17	3.1	15.9	2.2	0.76	5.2
C4	50.2	10.1	5.76	72.4	32.7	14.9	0.08	17.5	0.89	4.5	13.1	3.4	1.02	13.5
C5	72.6	14.6	4.43	78.7	34.5	22.7	0.08	19.2	0.76	5.6	11.7	4.4	1.16	22.1
C6	90.6	18.2	3.62	82.1	35.2	28.9	0.07	20.7	0.69	6.4	11.5	5.4	1.24	29.4

PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %
T58 S C1 C1	29.0	5.8	0.20	1.0	0.70	1.2	1.37	1.1
S C1 Tail	8.1	1.6	0.58	0.8	2.35	1.1	4.41	1.0
Sn Ro C1	10.8	2.2	1.55	2.9	2.10	1.3	4.24	1.3
C2	7.7	1.5	1.23	1.6	2.42	1.1	4.42	1.0
C3	7.5	1.5	0.98	1.3	2.48	1.1	4.00	0.8
C4	7.7	4.9	1.23	5.1	2.42	3.5	4.42	3.0
C5	7.5	4.5	0.98	3.8	2.48	3.3	4.00	2.5
C6	7.5	3.6	0.98	3.0	2.48	2.6	4.00	2.0
Ro Tail	371.1	74.4	1.27	80.6	3.85	84.7	8.31	87.2
CALC	456.9	100.0	1.17	100.0	3.38	100.0	7.09	100.0
ASSAY HEAD			1.12		3.38		6.89	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM %	MgO %	CUM %	Al2O3 %	CUM %
T58 S C1 C1	29.0	5.8	0.20	1.0	0.70	1.2	1.37	1.1
S C1 Tail	37.1	7.4	0.28	1.8	1.06	2.3	2.03	2.1
Sn Ro C1	10.8	2.2	1.55	2.9	2.10	1.3	4.24	1.3
C2	18.5	3.7	1.42	4.5	2.23	2.4	4.31	2.3
C3	26.0	5.2	1.29	5.7	2.30	3.6	4.22	3.1
C4	50.2	10.1	1.26	10.8	2.36	7.0	4.32	6.1
C5	72.6	14.6	1.17	14.6	2.40	10.3	4.22	8.7
C6	90.6	18.2	1.14	17.6	2.41	13.0	4.18	10.7

PROJECT	T0879
TEST NO	T59
DATE	0
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T56

NOTES
UF from T56

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 SPA7080 g/t	0.495 MIBC g/t			Cond Time min	Air L/min	Floater Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	440		200					5					
Water Change			50					3						
Conditioning S Ro C	6.0			200		79			7-9	5.0	5.0		175	
Condition Condition	4.0	200						3						
Condition Condition	3.8				300			3						
Condition Condition	4.0							3						
Sn Ro C1	4.3					20			7-8	3.0	3.0		125	9
Sn Ro C2	4.5								6-7	3.0	9.0		130	10
Sn Ro C3					100			3					135	6
Condition Sn Ro C4	4.7					20			6-8	3.0	12.0		150	17
Sn Ro C5	4.8								7-8	3.0	15.0		150	17
Sn Ro C6	4.8								7-9	3.0	18.0		130	16
REAGENT TOTALS (g/t)		639	50	400	400	119								

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T59 S Ro C	34.8	7.0	0.22	1.9	39.9	12.5	1.34	59.8	33.9	83.8	8.98	1.6	0.14	1.3
Sn Ro C1	11.2	2.2	9.91	27.8	23.0	2.3	0.15	2.2	1.78	1.4	25.0	1.5	0.52	1.5
C2	13.3	2.7	7.84	26.1	27.7	3.3	0.12	2.0	1.10	1.0	20.1	1.4	0.62	2.1
C3	8.4	1.7	4.40	9.2	32.3	2.4	0.11	1.2	0.89	0.5	18.3	0.8	0.74	1.6
C4	25.9	5.2	1.68	10.9	36.1	8.4	0.07	2.3	0.57	1.0	12.4	1.7	1.21	8.1
C5	26.1	5.2	0.94	6.1	37.9	8.9	0.08	2.7	0.36	0.7	11.8	1.6	1.44	9.7
C6	20.6	4.1	0.69	3.6	37.0	6.9	0.08	2.1	0.50	0.7	11.9	1.3	1.52	8.1
Ro Tail	360.2	72.0	0.16	14.4	17.0	55.1	0.06	27.7	0.42	10.7	48.0	90.2	0.73	67.7
CALC	500.5	100.0	0.80	100.0	22.1	100.0	0.16	100.0	2.81	100.0	38.3	100.0	0.78	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T59 S Ro C	34.8	7.0	0.22	1.92	39.9	12.5	1.34	59.8	33.9	83.8	8.98	1.63	0.14	1.25
Sn Ro C1	11.2	2.2	9.91	27.8	23.0	2.3	0.15	2.2	1.78	1.4	25.0	1.5	0.52	1.5
C2	24.5	4.9	8.79	53.8	25.6	5.7	0.13	4.2	1.41	2.5	22.3	2.9	0.57	3.6
C3	32.9	6.6	7.67	63.1	27.3	8.1	0.13	5.4	1.28	3.0	21.3	3.7	0.62	5.2
C4	58.8	11.7	5.03	74.0	31.2	16.5	0.10	7.7	0.97	4.0	17.4	5.3	0.88	13.3
C5	84.9	17.0	3.77	80.1	33.2	25.5	0.10	10.4	0.78	4.7	15.7	6.9	1.05	23.0
C6	105.5	21.1	3.17	83.7	34.0	32.4	0.09	12.5	0.73	5.4	14.9	8.2	1.14	31.0

PRODUCTS	WT g	WT %	CaO	DIST	MgO	DIST	Al2O3	DIST
T59 S Ro C	34.8	7.0	0.30	1.8	0.99	2.1	1.97	1.9
Sn Ro C1	11.2	2.2	1.49	2.9	2.20	1.5	5.67	1.8
C2	13.3	2.7	1.28	2.9	2.18	1.7	4.79	1.8
C3	8.4	1.7	0.94	1.4	2.48	1.2	4.76	1.1
C4	13.3	5.2	1.28	5.7	2.18	3.4	4.79	3.5
C5	8.4	5.2	0.94	4.2	2.48	3.9	4.76	3.5
C6	8.4	4.1	0.94	3.3	2.48	3.0	4.76	2.7
Ro Tail	360.2	72.0	1.25	77.7	3.87	83.2	8.30	83.7
CALC	458.0	100.0	1.16	100.0	3.35	100.0	7.14	100.0
ASSAY HEAD			1.12		3.38		6.89	

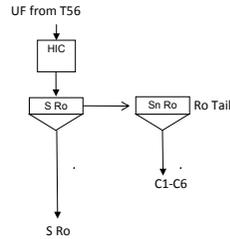
CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO	CUM	Al2O3	CUM
T59 S Ro C	34.8	7.0	0.30	1.8	0.99	2.1	1.97	1.9
Sn Ro C1	11.2	2.2	1.49	2.9	2.20	1.5	5.67	1.8
C2	24.5	4.9	1.38	5.8	2.19	3.2	5.19	3.6
C3	32.9	6.6	1.26	7.2	2.26	4.4	5.08	4.7
C4	58.8	11.7	1.27	12.9	2.23	7.8	4.95	8.2
C5	84.9	17.0	1.17	17.1	2.30	11.7	4.89	11.6
C6	105.5	21.1	1.12	20.5	2.34	14.7	4.87	14.4



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T60
DATE	02/12/14
TECHNICIAN	MW

Milling		Primary	Regrind
Mill type	HIC		
Media type			
Media kg			
Solids g	500		
Water g	400		
Time min	5.0		
Speed rpm	60HZ		
Lime g			
End pH			
End p80			



PRODUCT FLOATED	
UF from T56	

NOTES	
UF from T56	

Float Cell		Volume	Regrind Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	399		200				5					
Water Change Conditioning S Ro C	5.2		50					3	7-9	6.0	6.0	175	
Condition Condition	5.0	100		200				3					
Condition	4.0				299			3					
Condition	4.2					299		3					
Sn Ro C1	4.4								7-8	3.0	3.0	125	6
Sn Ro C2	4.4								6-7	3.0	6.0	130	4
Sn Ro C3	4.5								9-11	3.0	9.0	135	3
Sn Ro C4	4.5					20			9-11	3.0	12.0	150	3
Sn Ro C5	4.5								9-11	3.0	15.0	150	3
Sn Ro C6	4.6					20			9-11	3.0	18.0	130	2
REAGENT TOTALS (g/t)		499	50	399	299	299	99						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T60 S Ro C	34.5	6.9	0.24	2.1	38.1	12.0	1.02	41.5	32.6	82.3	10.4	1.9	0.16	1.4
Sn Ro C1	7.9	1.6	12.5	24.3	23.4	1.7	0.25	2.3	1.94	1.1	16.5	0.7	0.55	1.1
C2	4.7	0.9	9.30	10.9	24.5	1.1	0.22	1.2	1.72	0.6	19.4	0.5	0.54	0.7
C3	4.0	0.8	8.43	8.4	25.5	0.9	0.21	1.0	1.39	0.4	19.5	0.4	0.54	0.6
C4	4.4	0.9	7.11	7.8	26.4	1.1	0.19	1.0	1.16	0.4	20.6	0.5	0.57	0.7
C5	4.0	0.8	5.52	5.5	26.5	1.0	0.17	0.8	0.88	0.3	22.8	0.5	0.62	0.7
C6	2.7	0.5	4.59	3.0	27.1	0.7	0.16	0.5	1.07	0.2	23.2	0.3	0.62	0.4
Ro Tail	438.7	87.6	0.35	38.0	20.4	81.6	0.10	51.7	0.46	14.8	41.4	95.3	0.82	94.4
CALC	500.9	100.0	0.81	100.0	21.9	100.0	0.17	100.0	2.73	100.0	38.1	100.0	0.76	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T60 S Ro C	34.5	6.9	0.24	2.05	38.1	12.0	1.02	41.5	32.6	82.3	10.4	1.87	0.16	1.45
Sn Ro C1	7.9	1.6	12.5	24.3	23.4	1.7	0.25	2.3	1.94	1.1	16.5	0.7	0.55	1.1
C2	12.6	2.5	11.3	35.2	23.8	2.7	0.24	3.5	1.86	1.7	17.6	1.2	0.55	1.8
C3	16.6	3.3	10.6	43.6	24.2	3.7	0.23	4.5	1.74	2.1	18.0	1.6	0.54	2.4
C4	21.0	4.2	9.87	51.4	24.7	4.7	0.22	5.5	1.62	2.5	18.6	2.0	0.55	3.0
C5	25.1	5.0	9.17	56.9	25.0	5.7	0.21	6.3	1.50	2.8	19.3	2.5	0.56	3.7
C6	27.7	5.5	8.73	59.9	25.2	6.4	0.21	6.8	1.46	3.0	19.6	2.9	0.57	4.1

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST
T60 S Ro C	34.5	6.9	0.31	1.9	1.19	2.4	2.25	2.2
Sn Ro C1	7.9	1.6	2.75	3.9	2.21	1.0	5.10	1.2
C2	4.7	0.9	1.88	1.6	2.50	0.7	5.69	0.8
C3	4.0	0.8	1.41	1.0	2.56	0.6	5.62	0.6
C4	4.7	0.9	1.88	1.5	2.50	0.6	5.69	0.7
C5	4.0	0.8	1.41	1.0	2.56	0.6	5.62	0.6
C6	4.0	0.5	1.41	0.7	2.56	0.4	5.62	0.4
Ro Tail	438.7	87.6	1.11	88.3	3.69	93.7	7.42	93.4
CALC	502.5	100.0	1.10	100.0	3.45	100.0	6.96	100.0
ASSAY HEAD			1.12		3.38		6.89	

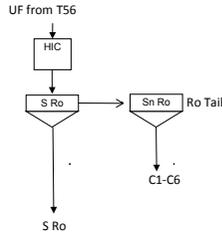
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM
T60 S Ro C	34.5	6.9	0.31	1.9	1.19	2.4	2.25	2.2
Sn Ro C1	7.9	1.6	2.75	3.9	2.21	1.0	5.10	1.2
C2	12.6	2.5	2.42	5.5	2.32	1.7	5.32	1.9
C3	16.6	3.3	2.18	6.6	2.38	2.3	5.39	2.6
C4	21.0	4.2	2.12	8.1	2.40	2.9	5.46	3.3
C5	25.1	5.0	2.00	9.1	2.43	3.5	5.48	3.9
C6	27.7	5.5	1.95	9.8	2.44	3.9	5.50	4.4



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T61
DATE	01/12/14
TECHNICIAN	SL

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T56

NOTES
UF from T56 12 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	298		199				5					
Water Change								3					
Conditioning S Ro C	3.7		50				59		7-9	6.0	6.0	175	
Condition	3.8			199				3					
Condition	3.4				298			3					
Condition	3.3					298		3					
Sn Ro C1	3.5								8-10	3.0	3.0	125	2
Sn Ro C2	3.5								6-7	3.0	6.0	130	2
Sn Ro C3	3.6					99		3		3.0	9.0	135	1
Condition	3.4						20		9-11	3.0	12.0	150	5
Sn Ro C4	3.5						20		9-11	3.0	15.0	150	3
Sn Ro C5	3.6						20		9-11	3.0	18.0	130	2
Sn Ro C6													
REAGENT TOTALS (g/t)		298	50	398	298	398	98						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T61 S Ro Conc	36.2	7.2	0.25	2.3	38.0	12.4	1.07	44.2	30.5	84.8	10.5	1.9	0.16	1.5
Sn Ro C1	3.1	0.6	5.62	4.3	25.1	0.7	0.30	1.0	2.75	0.6	20.7	0.3	0.86	0.7
C2	2.2	0.4	3.32	1.8	21.3	0.4	0.24	0.6	2.38	0.4	31.0	0.3	0.59	0.3
C3	1.8	0.4	2.81	1.3	21.1	0.3	0.21	0.4	1.41	0.2	32.8	0.3	0.59	0.3
C4	6.8	1.4	9.68	16.6	23.7	1.5	0.17	1.3	1.20	0.6	16.9	0.6	0.78	1.4
C5	5.0	1.0	6.75	8.4	24.8	1.1	0.17	1.0	1.13	0.4	21.0	0.5	0.79	1.0
C6	2.9	0.6	5.75	4.1	23.5	0.6	0.18	0.6	1.16	0.3	25.0	0.4	0.67	0.5
Ro Tail	444.7	88.5	0.55	61.3	20.7	83.0	0.10	50.8	0.37	12.6	41.8	95.6	0.82	94.3
CALC	502.6	100.00	0.79	100.0	22.1	100.0	0.17	100.0	2.59	100.0	38.7	100.0	0.77	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

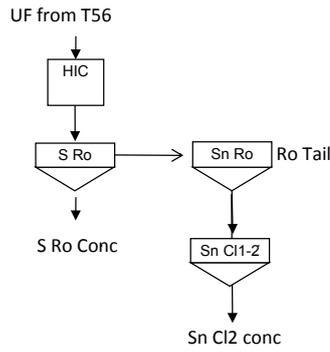
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T61 S Ro Conc	36.2	7.2	0.25	2.27	38.0	12.4	1.07	44.2	30.5	84.8	10.5	1.95	0.16	1.50
Sn Ro C1	3.1	0.6	5.62	4.3	25.1	0.7	0.30	1.0	2.75	0.6	20.7	0.3	0.86	0.7
C2	5.2	1.0	4.67	6.1	23.5	1.1	0.28	1.6	2.60	1.0	25.0	0.7	0.75	1.0
C3	7.0	1.4	4.19	7.4	22.9	1.5	0.26	2.1	2.29	1.2	27.0	1.0	0.71	1.3
C4	13.9	2.8	6.90	23.9	23.3	2.9	0.21	3.4	1.75	1.9	22.0	1.6	0.74	2.7
C5	18.8	3.7	6.86	32.4	23.7	4.0	0.20	4.4	1.59	2.3	21.7	2.1	0.76	3.7
C6	21.7	4.3	6.71	36.5	23.7	4.6	0.20	5.0	1.53	2.6	22.2	2.5	0.74	4.2

PRODUCTS	WT g	WT %	CaO	DIST	MgO %	DIST	Al2O3	DIST
T61 S Ro Conc	36.2	7.2	0.33	2.2	1.34	2.8	2.35	2.4
Sn Ro C1	3.1	0.6	1.75	1.0	3.10	0.5	6.77	0.6
C2	2.2	0.4	1.75	0.7	3.51	0.4	8.54	0.5
C3	1.8	0.4	1.70	0.6	3.66	0.4	8.75	0.4
C4	2.2	1.4	1.75	2.2	3.51	1.4	8.54	1.7
C5	1.8	1.0	1.70	1.5	3.66	1.0	8.75	1.2
C6	1.8	0.6	1.70	0.9	3.66	0.6	8.75	0.7
Ro Tail	444.7	88.5	1.13	91.0	3.66	92.9	7.34	92.4
CALC	493.7	100.00	1.10	100.0	3.49	100.0	7.03	100.0
ASSAY HEAD			1.12		3.38		6.89	

CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO %	CUM	Al2O3	CUM
T61 S Ro Conc	36.2	7.2	0.33	2.2	1.34	2.8	2.35	2.4
Sn Ro C1	3.1	0.6	1.75	1.0	3.10	0.5	6.77	0.6
C2	5.2	1.0	1.75	1.7	3.27	1.0	7.50	1.1
C3	7.0	1.4	1.74	2.2	3.37	1.4	7.82	1.6
C4	13.9	2.8	1.74	4.4	3.44	2.7	8.18	3.2
C5	18.8	3.7	1.73	5.9	3.50	3.8	8.33	4.4
C6	21.7	4.3	1.73	6.8	3.52	4.4	8.38	5.2

PROJECT	T0879
TEST NO	T62
DATE	02/12/14
TECHNICIAN	MW

Milling		Primary	Regrind
Mill type		HIC	
Media type			
Media kg			
Solids g		500	
Water g		400	
Time min		5.0	
Speed rpm		60HZ	
Lime g			
End pH			
End p80			



PRODUCT FLOATED
UF from T56

NOTES
UF from T56

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
		W/h	
Speed	850	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	400		200					5					
Water Change									3					
Conditioning S Ro C	5.2		50				59			7-9	6.0	6.0	175	
Condition	4.0	180		200					3					
Condition	3.9				300				3					
Condition	4.1					300			3		9.0	9.0	380	
Sn Ro C1						100								
Condition Sn Ro C2	4.3						20			7-8	3.0	12.0	120	
Sn Cl1 Conc	4.6									3-9	9.5	21.5	250	
Sn Cl2 C1	5.5									1-4	2.0	14.0	20	17
Sn Cl2 C2	5.5									4-8	2.5		30	11
Sn Cl2 C3	5.5									5-7	5.0		60	7
REAGENT TOTALS (g/t)		580	50	400	300	400	79							

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T62 S Ro C	33.3	6.7	0.23	2.1	39.0	11.9	1.13	48.5	31.6	81.0	9.69	1.7	0.15	1.3
Sn Cl2 C1	3.5	0.7	20.6	19.4	25.4	0.8	0.14	0.6	0.71	0.2	6.48	0.1	0.37	0.3
Sn Cl2 C2	3.2	0.6	17.9	15.6	25.4	0.8	0.16	0.7	1.40	0.3	7.90	0.1	0.38	0.3
Sn Cl2 C3	4.0	0.8	12.8	13.9	30.8	1.1	0.15	0.8	1.25	0.4	8.90	0.2	0.43	0.5
Sn Cl2 Tail	11.3	2.3	2.88	8.8	34.3	3.5	0.14	2.0	1.12	1.0	15.2	0.9	0.80	2.4
Sn Cl1 Tail	13.8	2.8	1.97	7.4	30.6	3.9	0.16	2.8	1.04	1.1	19.8	1.4	1.13	4.1
Ro Tail	431.3	86.2	0.28	32.7	19.8	78.0	0.08	44.5	0.48	15.9	42.3	95.5	0.80	91.1
CALC	500.4	100.0	0.74	100.0	21.8	100.0	0.15	100.0	2.59	100.0	38.2	100.0	0.76	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

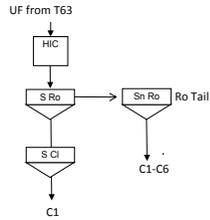
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T62 S Ro C	33.3	6.7	0.23	2.08	39.0	11.9	1.13	48.5	31.6	81.0	9.69	1.69	0.15	1.32
Sn Cl2 C1	3.5	0.7	20.6	19.4	25.4	0.8	0.14	0.6	0.71	0.2	6.48	0.1	0.37	0.3
Sn Cl2 C2	6.7	1.3	19.3	35.1	25.4	1.6	0.15	1.3	1.04	0.5	7.16	0.3	0.37	0.7
Sn Cl2 C3	10.7	2.1	16.8	49.0	27.4	2.7	0.15	2.1	1.12	0.9	7.81	0.4	0.40	1.1
Sn Cl2 Tail	22.0	4.4	9.68	57.8	31.0	6.2	0.14	4.1	1.12	1.9	11.6	1.3	0.60	3.5
Sn Cl1 Tail	35.8	7.2	6.71	65.2	30.8	10.1	0.15	7.0	1.09	3.0	14.7	2.8	0.81	7.6
Ro Tail	467.1	93.3	0.77	97.9	20.6	88.1	0.09	51.5	0.53	19.0	40.2	98.3	0.80	98.7

PRODUCTS	WT g	WT %	CaO	DIST	MgO	DIST	Al2O3	DIST
T62 S Ro C	33.3	6.7	0.30	1.2	1.09	4.3	2.09	4.7
Sn Cl2 C1	3.5	0.7	2.85	1.2	1.40	0.6	2.30	0.5
Sn Cl2 C2	3.2	0.6	2.17	0.8	1.54	0.6	2.71	0.6
Sn Cl2 C3	4.0	0.8	1.80	0.8	1.76	0.8	3.02	0.8
Sn Cl2 Tail	3.2	2.3	2.17	2.9	1.54	2.0	2.71	2.1
Sn Cl1 Tail	4.0	2.8	1.80	2.9	1.76	2.8	3.02	2.8
Ro Tail	4.0	86.2	1.80	90.3	1.76	88.9	3.02	88.4
CALC	55.30	100.0	1.72	100.0	1.71	100.0	2.94	100.0
ASSAY HEAD			1.12		3.38		6.89	

CUM PRODUCTS	CUM Wt	WT %	CaO	CUM	MgO	CUM	Al2O3	CUM
T62 S Ro C	33.3	6.7	0.30	1.2	1.09	4.3	2.09	4.7
Sn Cl2 C1	3.5	0.7	2.85	1.2	1.40	0.6	2.30	0.5
Sn Cl2 C2	6.7	1.3	2.52	2.0	1.47	1.2	2.50	1.1
Sn Cl2 C3	10.7	2.1	2.25	2.8	1.58	2.0	2.69	2.0
Sn Cl2 Tail	22.0	4.4	2.21	5.7	1.56	4.0	2.70	4.0
Sn Cl1 Tail	35.8	7.2	2.05	8.6	1.64	6.9	2.82	6.9
Ro Tail	467.1	93.3	1.82	98.8	1.75	95.7	3.00	95.3

PROJECT	T0879
TEST NO	T64
DATE	04/12/14
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T63

NOTES
UF from T63 Cut at 6 micron

Float Cell	Volume	Regrind Power
Rougher	2.5	Start
		Finish
Speed	850	W/h
		kWh/t

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	397		199				5					
Water Change			50					3	7-9	7.5	7.5	300	
S Ro C	5.1						59		6-9	3.0	10.5	120	25
Condition S C1 C1	6.3			199			10						
Condition	5.2	179			298			3		3.0	3.0	125	6
Condition	4.2					298		3		3.0	6.0	130	5
Sn Ro C1	4.4							3		3.0	9.0	135	5
Sn Ro C2	4.5								9-10	3.0	12.0	150	8
Sn Ro C3	4.6								10-12	3.0	15.0	150	7
Condition	4.7					99		3	9-12	3.0	18.0	130	6
Sn Ro C4	4.8						20		9-11	3.0			
Sn Ro C5	4.8								9-11	3.0			
Sn Ro C6	4.8												
REAGENT TOTALS (g/t)		576	50	397	298	397	88						

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	MnO %	DIST %
T64 S C1 C1	29.9	5.9	0.13	1.1	40.5	11.4	1.45	57.4	36.5	80.5	6.90	1.1	0.08	0.7
S C1 Tail	11.1	2.2	0.52	1.7	27.1	2.8	0.54	7.9	8.62	7.1	28.9	1.6	0.43	1.4
Sn Ro C1	6.9	1.4	8.80	17.4	22.6	1.5	0.15	1.4	2.77	1.4	24.5	0.9	0.47	1.0
C2	6.3	1.3	7.66	13.9	23.0	1.4	0.12	1.0	2.07	1.0	26.2	0.8	0.50	0.9
C3	6.2	1.2	6.11	10.9	23.0	1.3	0.11	0.9	1.82	0.8	27.2	0.9	0.50	0.9
C4	11.3	2.2	4.50	14.6	28.4	3.0	0.11	1.6	1.03	0.9	24.0	1.4	0.61	2.1
C5	10.3	2.0	2.96	8.7	28.7	2.8	0.10	1.4	1.08	0.8	23.0	1.2	0.63	1.9
C6	7.5	1.5	2.05	4.4	29.7	2.1	0.10	1.0	0.96	0.5	23.7	0.9	0.70	1.6
Ro Tail	414.1	82.2	0.23	27.4	19.0	73.8	0.05	27.4	0.23	7.0	43.2	91.3	0.72	89.4
CALC	503.5	100.0	0.69	100.0	21.1	100.0	0.15	100.0	2.69	100.0	38.9	100.0	0.66	100.0
ASSAY HEAD			0.76		21.5		0.17		2.55		39.3		0.68	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM DIST %	Fe %	CUM DIST %	As %	CUM DIST %	S %	CUM DIST %	SiO2 %	CUM DIST %	MnO %	CUM DIST %
T64 S C1 C1	29.9	5.9	0.13	1.12	40.5	11.4	1.45	57.4	36.5	80.5	6.90	1.05	0.08	0.72
S C1 Tail	41.0	8.1	0.24	2.8	36.9	14.2	1.20	65.3	29.0	87.6	12.9	2.7	0.17	2.1
Sn Ro C1	6.9	1.4	8.80	17.4	22.6	1.5	0.15	9.3	2.77	1.4	24.5	0.9	0.47	1.0
C2	13.2	2.6	8.26	31.3	22.8	2.8	0.14	10.3	2.44	2.4	25.3	1.7	0.48	1.9
C3	19.4	3.9	7.57	42.2	22.9	4.2	0.13	11.2	2.24	3.2	25.9	2.6	0.49	2.8
C4	30.7	6.1	6.44	56.7	24.9	7.2	0.12	12.8	1.79	4.1	25.2	3.9	0.53	4.9
C5	40.9	8.1	5.57	65.5	25.8	9.9	0.12	14.2	1.62	4.9	24.7	5.1	0.56	6.8
C6	48.4	9.6	5.02	69.9	26.4	12.0	0.11	15.2	1.51	5.4	24.5	6.1	0.58	8.4

PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %
T64 S C1 C1	29.9	5.9	0.18	1.0	0.81	1.3	1.42	1.1
S C1 Tail	11.1	2.2	0.97	2.1	3.32	2.0	6.79	1.9
Sn Ro C1	6.9	1.4	0.59	0.8	2.75	1.0	6.86	1.2
C2	6.3	1.3	0.70	0.9	2.81	1.0	6.89	1.1
C3	6.2	1.2	0.73	0.9	2.97	1.0	6.97	1.1
C4	6.3	2.2	0.70	1.5	2.81	1.7	6.89	2.0
C5	6.2	2.0	0.73	1.5	2.97	1.7	6.97	1.8
C6	6.2	1.5	0.73	1.1	2.97	1.2	6.97	1.3
Ro Tail	414.1	82.2	1.12	90.3	3.92	89.0	8.30	88.4
CALC	493.2	100.0	1.02	100.0	3.62	100.0	7.73	100.0
ASSAY HEAD			1.05		3.68		7.68	

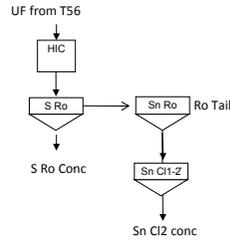
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM DIST %	MgO %	CUM DIST %	Al2O3 %	CUM DIST %
T64 S C1 C1	29.9	5.9	0.18	1.0	0.81	1.3	1.42	1.1
S C1 Tail	41.0	8.1	0.39	3.1	1.49	3.3	2.87	3.0
Sn Ro C1	6.9	1.4	0.59	0.8	2.75	1.0	6.86	1.2
C2	13.2	2.6	0.64	1.6	2.78	2.0	6.87	2.3
C3	19.4	3.9	0.67	2.5	2.84	3.0	6.91	3.4
C4	30.7	6.1	0.68	4.1	2.83	4.8	6.90	5.4
C5	40.9	8.1	0.69	5.5	2.86	6.4	6.92	7.3
C6	48.4	9.6	0.70	6.6	2.88	7.6	6.93	8.6



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T65
DATE	05/12/14
TECHNICIAN	MW

Milling		Primary	Regrind
Mill type	HIC		
Media type			
Media kg			
Solids g	500		
Water g	400		
Time min	5.0		
Speed rpm	60HZ		
Lime g			
End pH			
End p80			



PRODUCT FLOATED	
UF from T56	

NOTES	
UF from T56 12 micron	

Float Cell	Volume	Regrind Power
Rougher	2.5	Start
C1	1.5	Finish
	0.8	W/h
Speed	850	kWh/t

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	199		199					5					
Water Change Conditioning			50						3	7-9	6.0	6.0	175	
S Ro C	5.0						59							
Condition	4.0	100		199					3					
Condition	3.9				299				3					
Condition	4.1					299			3		9.0	9.0	390	
Sn Ro C1						100								
Condition							20		3	7-8	9.5	18.5	430	
Sn Ro C2	4.3									3-11	9.0	27.5	350	
Sn Cl1 Conc	4.8									1-4	2.0	20.5	20	16
Sn Cl2 C1	5.5									4-8	2.5	30	8	8
Sn Cl2 C2	5.5									5-7	5.0	60	5	5
Sn Cl2 C3	5.5													
REAGENT TOTALS (g/t)		299	50	398	299	398	79							

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T65 S Ro C	34.3	6.8	0.24	2.1	38.7	11.9	0.97	44.3	30.9	78.8	10.3	1.8	0.16	1.4
Sn Cl2 C1	3.1	0.6	19.8	15.6	25.4	0.7	0.19	0.8	1.00	0.2	6.84	0.1	0.48	0.4
Sn Cl2 C2	2.5	0.5	16.9	10.6	24.4	0.5	0.20	0.7	1.74	0.3	8.29	0.1	0.44	0.3
Sn Cl2 C3	3.2	0.6	15.0	12.1	26.7	0.8	0.22	0.9	1.58	0.4	9.36	0.2	0.49	0.4
Sn Cl2 Tail	10.5	2.1	4.97	13.3	31.9	3.0	0.22	3.1	1.61	1.3	13.0	0.7	0.89	2.5
Sn Cl1 Tail	21.2	4.2	2.34	12.6	29.2	5.6	0.17	4.8	1.16	1.8	21.3	2.4	1.10	6.1
Ro Tail	427.4	85.1	0.31	33.6	20.2	77.5	0.08	45.5	0.54	17.2	42.1	94.7	0.79	88.9
CALC	502.2	100.0	0.78	100.0	22.2	100.0	0.15	100.0	2.68	100.0	37.8	100.0	0.76	100.0
ASSAY HEAD			0.78		22.1		0.16		2.43		37.9		0.77	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T65 S Ro C	34.3	6.8	0.24	2.09	38.7	11.9	0.97	44.3	30.9	78.8	10.3	1.85	0.16	1.44
Sn Cl2 C1	3.1	0.6	19.8	15.6	25.4	0.7	0.19	0.8	1.00	0.2	6.84	0.1	0.48	0.4
Sn Cl2 C2	5.6	1.1	18.5	26.3	25.0	1.3	0.19	1.4	1.33	0.6	7.48	0.2	0.46	0.7
Sn Cl2 C3	8.8	1.8	17.2	38.4	25.6	2.0	0.20	2.4	1.42	0.9	8.16	0.4	0.47	1.1
Sn Cl2 Tail	19.3	3.8	10.5	51.7	29.0	5.0	0.21	5.5	1.52	2.2	10.8	1.1	0.70	3.6
Sn Cl1 Tail	40.5	8.1	6.25	64.3	29.1	10.6	0.19	10.2	1.33	4.0	16.3	3.5	0.91	9.7
Ro Tail	467.9	93.2	0.82	97.9	21.0	88.1	0.09	55.7	0.61	21.2	39.9	98.2	0.80	98.6

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST
T65 S Ro C	34.3	6.8	0.29	0.9	1.17	4.4	2.29	4.9
Sn Cl2 C1	3.1	0.6	3.34	1.0	1.56	0.5	2.51	0.5
Sn Cl2 C2	2.5	0.5	2.52	0.6	1.65	0.5	2.97	0.5
Sn Cl2 C3	3.2	0.6	2.21	0.7	1.85	0.7	3.29	0.7
Sn Cl2 Tail	2.5	2.1	2.52	2.5	1.65	1.9	2.97	1.9
Sn Cl1 Tail	3.2	4.2	2.21	4.5	1.85	4.3	3.29	4.3
Ro Tail	3.2	85.1	2.21	89.8	1.85	87.6	3.29	87.3
CALC	51.95	100.0	2.09	100.0	1.80	100.0	3.21	100.0
ASSAY HEAD			1.12		3.38		6.89	

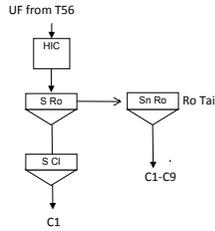
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM
T65 S Ro C	34.3	6.8	0.29	0.9	1.17	4.4	2.29	4.9
Sn Cl2 C1	3.1	0.6	3.34	1.0	1.56	0.5	2.51	0.5
Sn Cl2 C2	5.6	1.1	2.98	1.6	1.60	1.0	2.71	0.9
Sn Cl2 C3	8.8	1.8	2.70	2.3	1.69	1.6	2.92	1.6
Sn Cl2 Tail	19.3	3.8	2.60	4.8	1.67	3.6	2.95	3.5
Sn Cl1 Tail	40.5	8.1	2.40	9.2	1.76	7.9	3.13	7.9
Ro Tail	467.9	93.2	2.23	99.1	1.84	95.6	3.28	95.1



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T67
DATE	15/12/14
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T63

NOTES
UF from T63 Cut at 6 micron

Float Cell	Volume	Regrind Power
Rougher	2.5	Start
Cl1	1.5	Finish
Speed	0.8	W/h
	750	kWh/t

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MiBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	499		200				5					
Water Change													
Conditioning S Ro C	5.3		50				59	3	7-9	7.5	7.5	300	
Condition S Cl1 C1	6.3						10		6-9	3.0	10.5	120	23
Condition	5.6	120		200				3					
Condition	4.2				300			3					
Condition	4.4					300		3		15.0	15.0	670	
Sn Ro C1							10						
Condition	4.5					100		3					
Sn Ro C2	4.7								10-12	15.0	30.0	730	
Condition													
Sn Cl1 C	5.1								9-12	3.0	33.0	330	
Sn Cl2 C1	5.7						20		9-11	3.0	36.0	20	8
Sn Cl2 C2									9-11	3.0	39.0	30	6
Sn Cl2 C3	5.7								9-11	3.0	42.0	65	3
REAGENT TOTALS (g/t)		619	50	399	300	399	99						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T67 S Cl1 C1	27.6	5.5	0.15	1.2	40.3	10.2	1.34	44.6	36.4	76.3	7.36	1.0	0.08	0.6
S Cl1 Tail	12.4	2.5	0.58	2.1	28.7	3.3	0.82	12.3	9.65	9.1	25.8	1.6	0.38	1.4
Sn Cl2 C1	1.5	0.3	21.7	9.4	18.5	0.3	0.29	0.5	1.89	0.2	11.0	0.1	0.28	0.1
C2	1.9	0.4	19.2	10.6	20.1	0.4	0.25	0.6	1.51	0.2	12.4	0.1	0.30	0.2
C3	2.1	0.4	14.5	8.9	22.1	0.4	0.24	0.6	2.49	0.4	15.3	0.2	0.33	0.2
Sn Cl2 Tail	8.8	1.8	3.63	9.2	25.5	2.1	0.21	2.2	2.37	1.6	26.7	1.2	0.49	1.3
Sn Cl1 Tail	41.3	8.2	2.06	24.6	23.6	8.9	0.20	10.0	1.34	4.2	32.4	6.6	0.66	7.9
Ro Tail	405.0	80.9	0.29	33.9	20.1	74.5	0.06	29.3	0.26	8.0	45.0	89.4	0.75	88.3
CALC	500.7	100.0	0.69	100.0	21.8	100.0	0.17	100.0	2.63	100.0	40.7	100.0	0.69	100.0
ASSAY HEAD			0.76		21.5		0.17		2.55		39.3		0.68	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T67 S Cl1 C1	27.6	5.5	0.15	1.20	40.3	10.2	1.34	44.6	36.4	76.3	7.36	1.00	0.08	0.64
S Cl1 Tail	40.0	8.0	0.28	3.3	36.7	13.4	1.18	56.8	28.1	85.4	13.1	2.6	0.17	2.0
Sn Cl2 C1	1.5	0.3	21.7	9.4	18.5	0.3	0.29	12.8	1.89	0.2	11.0	0.1	0.28	0.1
C2	3.4	0.7	20.3	20.0	19.4	0.6	0.27	13.4	1.68	0.4	11.8	0.2	0.29	0.3
C3	5.6	1.1	18.0	29.0	20.4	1.0	0.26	14.0	1.99	0.8	13.1	0.4	0.31	0.5
Sn Cl2 Tail	14.4	2.9	2.91	38.2	23.5	3.1	0.23	16.2	2.22	2.4	21.4	1.5	0.42	1.7
Sn Cl1 Tail	55.7	11.1	3.90	62.8	23.6	12.0	0.21	26.2	1.57	6.6	29.6	8.1	0.60	9.7

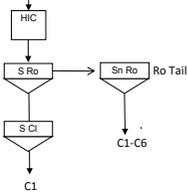
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T67 S Cl1 C1	27.6	5.5	0.19	2.9	1.11	3.2	1.55	2.1	0.79	1.5
S Cl1 Tail	12.4	2.5	0.64	4.3	3.15	4.1	5.94	3.6	2.44	2.1
Sn Cl2 C1	1.5	0.3	0.35	0.3	1.52	0.2	3.13	0.2	1.94	0.2
C2	1.9	0.4	0.35	0.4	1.68	0.3	3.53	0.3	2.13	0.3
C3	2.1	0.4	0.37	0.4	1.92	0.4	4.20	0.4	2.55	0.4
Sn Cl2 Tail	1.9	1.8	0.35	1.7	1.68	1.6	3.53	1.5	2.93	1.8
Sn Cl1 Tail	2.1	8.2	0.37	8.3	1.92	8.3	4.20	8.5	3.21	9.4
Ro Tail	2.1	80.9	0.37	81.7	1.92	81.8	4.20	83.3	2.93	84.2
CALC	51.76	100.0	0.37	100.0	1.90	100.0	4.08	100.0	2.82	100.0
ASSAY HEAD			1.05		3.68		7.68		2.79	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T67 S Cl1 C1	27.6	5.5	0.19	2.9	1.11	3.2	1.55	2.1	0.79	1.5
S Cl1 Tail	40.0	8.0	0.33	7.2	1.74	7.3	2.91	5.7	1.30	3.7
Sn Cl2 C1	1.5	0.3	0.35	0.3	1.52	0.2	3.13	0.2	1.94	0.2
C2	3.4	0.7	0.35	0.7	1.61	0.6	3.35	0.6	2.05	0.5
C3	5.6	1.1	0.36	1.1	1.73	1.0	3.68	1.0	2.24	0.9
Sn Cl2 Tail	14.4	2.9	0.35	2.8	1.70	2.6	3.59	2.5	2.66	2.7
Sn Cl1 Tail	55.7	11.1	0.37	11.1	1.86	10.9	4.04	11.0	3.07	12.1

PROJECT	T0879
TEST NO	168
DATE	13/01/15
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Line g		
End pH		
End p80		

Cyc 11-31 -40 Fine Tails O/F



PRODUCT FLOATED
Cyc 11-31 -40 Fine Tails O/F

NOTES
Cyc 11-31 -40 Fine Tails O/F

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	298		198				5					
Water Change			50					3	7-15	15.0	15.0	560	
Conditioning S Ro C	5.3						59						
Condition S C1 C1	5.8			198				3	6-9	3.0	18.0	120	21
Condition Condition	5.4	298			298			3		4.0	4.0	125	6
Sn Ro C1	4.2						9.8214	3		3.5	7.5	130	5
Sn Ro C2	4.4							3	9-10	3.0	10.5	135	5
Sn Ro C3	4.6								10-12	3.0	10.5	135	5
Condition	4.7				99			3					
Sn Ro C4	4.6								9-12	3.0	13.5	150	7
Sn Ro C5	4.8						20		9-11	3.0	16.5	150	6
Sn Ro C6	4.8								9-11	3.0	19.5	130	6
REAGENT TOTALS (g/t)		595	50	397	298	397	88						

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	MnO %	DIST %
T68 S C1 C1	24.9	4.9	0.14	1.2	38.2	9.2	1.52	42.1	36.2	65.5	7.43	1.0	0.05	0.6
S C1 Tail	21.7	4.3	0.43	3.3	23.9	5.0	0.38	9.2	7.53	11.9	32.6	3.7	0.27	2.8
Sn Ro C1	7.3	1.4	3.38	8.7	25.1	1.8	0.17	1.4	3.99	2.1	28.3	1.1	0.33	1.2
C2	6.9	1.4	2.79	6.8	24.0	1.6	0.15	1.2	2.70	1.4	30.8	1.1	0.34	1.1
C3	6.4	1.3	2.20	5.0	23.1	1.4	0.14	1.0	2.58	1.2	32.2	1.1	0.34	1.0
C4	9.9	2.0	2.65	9.3	25.8	2.5	0.15	1.7	1.85	1.3	29.6	1.5	0.39	1.9
C5	8.7	1.7	2.52	7.8	24.6	2.1	0.13	1.3	2.38	1.5	28.0	1.3	0.37	1.5
C6	7.7	1.5	2.08	5.7	23.8	1.8	0.13	1.1	1.99	1.1	30.5	1.2	0.37	1.4
Ro Tail	410.5	81.4	0.36	52.3	18.9	74.7	0.09	41.1	0.47	14.0	41.6	88.2	0.45	88.5
CALC	504.0	100.0	0.56	100.0	20.5	100.0	0.18	100.0	2.73	100.0	38.4	100.0	0.41	100.0
ASSAY HEAD			0.56		20.9		0.19		2.76		38.7		0.43	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM %	Fe %	CUM %	As %	CUM %	S %	CUM %	SiO2 %	CUM %	MnO %	CUM %
T68 S C1 C1	24.9	4.9	0.14	1.23	38.2	9.18	1.52	42.1	36.2	65.5	7.43	0.96	0.05	0.60
S C1 Tail	46.6	9.2	0.28	4.5	31.5	14.2	0.99	51.3	22.8	77.4	19.2	4.6	0.15	3.4
Sn Ro C1	7.3	1.4	3.38	8.7	25.1	1.8	0.17	10.6	3.99	2.1	28.3	1.1	0.33	1.2
C2	14.2	2.8	3.09	15.5	24.6	3.4	0.16	11.7	3.36	3.5	29.5	2.2	0.33	2.3
C3	20.6	4.1	2.82	20.5	24.1	4.8	0.15	12.7	3.12	4.7	30.3	3.2	0.34	3.3
C4	30.5	6.1	2.76	29.8	24.7	7.3	0.15	14.4	2.71	6.0	30.1	4.7	0.35	5.2
C5	39.2	7.8	2.71	37.5	24.6	9.3	0.15	15.6	2.63	7.5	29.6	6.0	0.36	6.7
C6	46.9	9.3	2.61	43.2	24.5	11.1	0.14	16.7	2.53	8.6	29.8	7.2	0.36	8.1

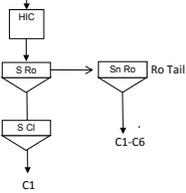
PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %
T68 S C1 C1	24.9	4.9	0.14	0.8	1.43	1.8	1.54	0.8
S C1 Tail	21.7	4.3	0.65	3.2	4.11	4.4	9.38	4.2
Sn Ro C1	7.3	1.4	0.47	0.8	3.34	1.2	8.59	1.3
C2	6.9	1.4	0.54	0.9	3.56	1.2	9.27	1.3
C3	6.4	1.3	0.58	0.8	3.73	1.2	9.75	1.3
C4	6.9	1.4	0.54	1.2	3.56	1.7	9.27	1.9
C5	6.4	1.3	0.58	1.2	3.73	1.6	9.75	1.8
C6	6.4	1.3	0.58	1.0	3.73	1.4	9.75	1.6
Ro Tail	410.5	81.4	0.96	90.1	4.24	85.5	10.1	85.9
CALC	497.4	100.0	0.87	100.0	4.04	100.0	9.58	100.0
ASSAY HEAD			0.89		4.00		9.49	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM %	MgO %	CUM %	Al2O3 %	CUM %
T68 S C1 C1	24.9	4.9	0.14	0.8	1.43	1.8	1.54	0.8
S C1 Tail	46.6	9.2	0.38	4.0	2.68	6.1	5.19	5.0
Sn Ro C1	7.3	1.4	0.47	0.8	3.34	1.2	8.59	1.3
C2	14.2	2.8	0.50	1.6	3.45	2.4	8.92	2.6
C3	20.6	4.1	0.53	2.5	3.53	3.6	9.18	3.9
C4	30.5	6.1	0.53	3.7	3.54	5.3	9.21	5.8
C5	39.2	7.8	0.54	4.9	3.58	6.9	9.33	7.6
C6	46.9	9.3	0.55	5.9	3.61	8.3	9.40	9.1

PROJECT	T0879
TEST NO	169
DATE	13/01/15
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End p80		

Cyc 11-31 -40 Fine Tails O/F +CS6



PRODUCT FLOATED
Cyc 11-31
-40 Fine Tails O/F +CS6

NOTES
LC01 Cyc 11- 31 Cyclone
40 Fine Tail Comb
from centrifuge
6 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	
		kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	783		196				5					
Water Change			49					3	7-9	8.5	8.5	440	
Conditioning S Ro C	5.0						58						
Condition S C1 C1	5.8						10		6-9	3.0	11.5	120	21
Condition Condition	5.2	176		196	294	294		3		3.0	3.0	125	7
Condition Sn Ro C1	4.4							3		3.0	6.0	130	7
Condition Sn Ro C2	4.5						10		9-10	3.0	9.0	135	6
Condition Sn Ro C3	4.6					98		3	10-12	3.0	12.0	150	8
Condition Sn Ro C4	5.0						19		9-12	3.0	15.0	150	7
Condition Sn Ro C5	4.6								9-11	3.0	18.0	130	6
Condition Sn Ro C6	4.7								9-11	3.0			
REAGENT TOTALS (g/t)		959	49	392	294	392	97						

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	MnO %	DIST %
T69 S C1 C1	24.8	4.9	0.13	1.1	39.6	9.4	1.61	45.3	36.6	67.5	6.83	0.9	0.05	0.6
S C1 Tail	19.2	3.8	0.43	2.9	25.3	4.6	0.42	9.1	7.56	10.8	30.3	2.9	0.27	2.4
Sn Ro C1	9.0	1.8	3.92	12.3	25.7	2.2	0.17	1.7	4.19	2.8	25.2	1.1	0.34	1.4
C2	8.6	1.7	3.55	10.6	24.4	2.0	0.15	1.5	3.16	2.0	27.7	1.2	0.35	1.4
C3	7.6	1.5	2.90	7.7	24.1	1.7	0.14	1.2	2.78	1.6	29.1	1.1	0.36	1.2
C4	11.8	2.3	2.54	10.4	25.2	2.8	0.08	1.1	2.16	1.9	24.0	1.4	0.38	2.0
C5	10.8	2.1	2.13	8.0	25.4	2.6	0.13	1.6	1.95	1.6	28.3	1.5	0.40	2.0
C6	8.2	1.6	1.96	5.6	25.9	2.0	0.13	1.2	1.39	0.8	28.9	1.2	0.42	1.6
Ro Tail	410.7	80.4	0.29	41.4	18.5	72.5	0.08	37.3	0.36	11.0	42.7	88.6	0.47	87.5
CALC	510.7	100.0	0.56	100.0	20.5	100.0	0.17	100.0	2.63	100.0	38.8	100.0	0.43	100.0
ASSAY HEAD			0.57		20.7		0.18		2.85		39.3		0.44	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM %	Fe %	CUM %	As %	CUM %	S %	CUM %	SiO2 %	CUM %	MnO %	CUM %
T69 S C1 C1	24.8	4.9	0.13	1.12	39.6	9.38	1.61	45.3	36.6	67.5	6.83	0.86	0.05	0.56
S C1 Tail	44.0	8.6	0.26	4.0	33.4	14.0	1.09	54.4	23.9	78.3	17.1	3.8	0.15	2.9
Sn Ro C1	9.0	1.8	3.92	12.3	25.7	2.2	0.17	10.9	4.19	2.8	25.2	1.1	0.34	1.4
C2	17.6	3.4	3.74	22.9	25.1	4.2	0.16	12.3	3.69	4.8	26.4	2.3	0.34	2.8
C3	25.2	4.9	3.49	30.6	24.8	6.0	0.15	13.6	3.41	6.4	27.2	3.5	0.35	4.0
C4	37.0	7.2	3.18	41.0	24.9	8.8	0.13	14.6	3.01	8.3	26.2	4.9	0.36	6.0
C5	47.8	9.4	2.95	49.0	25.0	11.4	0.13	16.2	2.77	9.9	26.7	6.4	0.37	8.0
C6	56.0	11.0	2.80	54.6	25.1	13.4	0.13	17.4	2.57	10.7	27.0	7.6	0.38	9.5

PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %
T69 S C1 C1	24.8	4.9	0.15	0.8	1.23	1.5	1.50	0.8
S C1 Tail	19.2	3.8	0.60	2.6	3.82	3.6	8.52	3.4
Sn Ro C1	9.0	1.8	0.44	0.9	3.09	1.4	7.38	1.4
C2	8.6	1.7	0.51	1.0	3.24	1.4	7.96	1.4
C3	7.6	1.5	0.54	0.9	3.39	1.3	8.32	1.3
C4	8.6	2.3	0.51	1.3	3.24	1.9	7.96	2.0
C5	7.6	2.1	0.54	1.3	3.39	1.8	8.32	1.9
C6	7.6	1.6	0.54	1.0	3.39	1.4	8.32	1.4
Ro Tail	410.7	80.4	0.99	90.2	4.21	85.7	10.0	86.3
CALC	503.7	100.0	0.88	100.0	3.95	100.0	9.32	100.0
ASSAY HEAD			0.91		4.02		9.32	

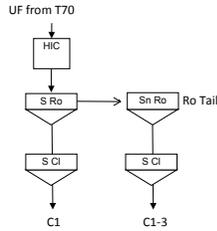
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM %	MgO %	CUM %	Al2O3 %	CUM %
T69 S C1 C1	24.8	4.9	0.15	0.8	1.23	1.5	1.50	0.8
S C1 Tail	44.0	8.6	0.35	3.4	2.36	5.1	4.56	4.2
Sn Ro C1	9.0	1.8	0.44	0.9	3.09	1.4	7.38	1.4
C2	17.6	3.4	0.47	1.9	3.16	2.8	7.66	2.8
C3	25.2	4.9	0.49	2.8	3.23	4.0	7.86	4.2
C4	37.0	7.2	0.50	4.1	3.23	5.9	7.89	6.1
C5	47.8	9.4	0.51	5.4	3.27	7.7	7.99	8.0
C6	56.0	11.0	0.51	6.4	3.29	9.1	8.04	9.5



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	171
DATE	230115
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED	
UF from T70	

NOTES	
LC01 Cyc 11- 31 Cyclone	
-40 Fine Tail Comb	
UF from T70	
6 micron	

Float Cell	Volume	Regrind Power
Rougher	2.5	Start
Cl1	1.5	Finish
Speed	0.8	W/h
	750	kWh/t

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MiBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	592		197				5					
Water Change													
Conditioning S Ro C	5.4		49				59	3	7-9	7.5	7.5	300	
Condition S Cl C1	6.4						10		3-7	3.0	10.5	120	23
Condition	5.6	197		197				3					
Condition	4.2				296			3					
Condition	4.4					296		3		15.0	15.0	670	
Sn Ro C1	4.8					99	20						
Condition Sn Ro C2	4.9							3	10-12	15.0	30.0	730	
Condition Sn Cl C	5.0								9-12	6.0	36.0	330	
Sn Cl2 C1	5.6								0.5-1	1.0	37.0	20	6
Sn Cl2 C2									1-2	1.5	38.5	30	6
Sn Cl2 C3	5.7								2-5	3.0	41.5	60	4
REAGENT TOTALS (g/t)		789	49	395	296	395	88						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T71 S Cl1 C1	27.2	5.4	0.15	1.3	40.8	10.3	1.48	47.6	37.3	72.0	6.92	5.2	0.06	0.7
S Cl1 Tail	12.6	2.5	0.46	1.9	27.7	3.2	0.61	9.1	11.8	10.6	27.0	9.5	0.26	1.4
Sn Cl2 C1	1.2	0.2	20.8	8.1	20.0	0.2	0.14	0.2	2.50	0.2	11.8	0.4	0.22	0.1
C2	1.9	0.4	17.9	10.7	21.8	0.4	0.12	0.3	2.51	0.3	12.6	0.7	0.24	0.2
C3	2.5	0.5	13.4	10.8	24.0	0.6	0.14	0.4	3.11	0.6	14.9	1.0	0.26	0.3
Sn Cl2 Tail	9.8	1.9	4.11	12.9	26.5	2.4	0.15	1.7	2.45	1.7	26.1	7.1	0.32	1.3
Sn Cl1 Tail	45.5	9.0	1.22	17.8	22.1	9.3	0.13	7.0	1.85	6.0	35.0	44.4	0.37	7.1
Ro Tail	406.0	80.1	0.28	36.5	19.5	73.5	0.07	33.6	0.30	8.6	2.80	31.7	0.52	88.9
CALC	506.7	100.0	0.62	100.0	21.2	100.0	0.17	100.0	2.78	100.0	7.08	100.0	0.47	100.0
ASSAY HEAD			0.64		21.2		0.18		2.86		39.0		0.47	

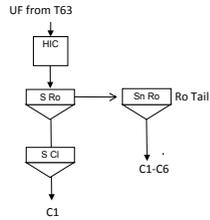
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T71 S Cl1 C1	27.2	5.4	0.15	1.31	40.8	10.3	1.48	47.6	37.3	72.0	6.92	5.24	0.06	0.69
S Cl1 Tail	39.8	7.9	0.25	3.2	36.7	13.5	1.20	56.7	29.2	82.6	13.3	14.7	0.12	2.1
Sn Cl2 C1	1.2	0.2	20.8	8.1	20.0	0.2	0.14	0.2	2.50	0.2	11.8	0.4	0.22	0.1
C2	3.1	0.6	19.0	18.8	21.1	0.6	0.13	0.6	2.51	0.5	12.3	1.1	0.23	0.3
C3	5.6	1.1	16.5	29.7	22.4	1.2	0.13	10.0	2.78	1.1	13.4	2.1	0.24	0.6
Sn Cl2 Tail	15.4	3.0	8.62	42.6	25.0	3.6	0.14	11.7	2.57	2.8	21.5	9.2	0.29	1.9
Sn Cl1 Tail	60.9	12.0	3.09	60.4	22.8	12.9	0.13	18.7	2.03	8.8	31.6	53.6	0.35	9.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T71 S Cl1 C1	27.2	5.4	0.17	2.8	1.13	3.2	1.44	2.0	0.61	1.3
S Cl1 Tail	12.6	2.5	0.58	4.4	3.31	4.4	6.97	4.6	2.02	1.9
Sn Cl2 C1	1.2	0.2	0.33	0.2	1.64	0.2	3.14	0.2	2.08	0.2
C2	1.9	0.4	0.32	0.4	1.73	0.3	3.38	0.3	2.24	0.3
C3	2.5	0.5	0.33	0.5	1.89	0.5	3.85	0.5	2.63	0.5
Sn Cl2 Tail	9.8	1.9	0.32	1.9	1.73	1.8	3.38	1.7	2.71	2.0
Sn Cl1 Tail	45.5	9.0	0.33	9.1	1.89	9.0	3.85	9.1	2.57	8.9
Ro Tail	2.5	80.1	0.33	80.8	1.89	80.5	3.85	81.5	2.73	84.8
CALC	52.32	100.0	0.33	100.0	1.88	100.0	3.79	100.0	2.58	100.0
ASSAY HEAD			0.95		3.86		8.42		2.50	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T71 S Cl1 C1	27.2	5.4	0.17	2.8	1.13	3.2	1.44	2.0	0.61	1.3
S Cl1 Tail	39.8	7.9	0.30	7.2	1.82	7.6	3.19	6.6	1.06	3.2
Sn Cl2 C1	1.2	0.2	0.33	0.2	1.64	0.2	3.14	0.2	2.08	0.2
C2	3.1	0.6	0.32	0.6	1.69	0.5	3.29	0.5	2.18	0.5
C3	5.6	1.1	0.33	1.1	1.78	1.0	3.54	1.0	2.38	1.0
Sn Cl2 Tail	15.4	3.0	0.32	3.0	1.75	2.8	3.44	2.8	2.59	3.1
Sn Cl1 Tail	60.9	12.0	0.33	12.0	1.85	11.9	3.75	11.9	2.58	12.0

PROJECT	T0879
TEST NO	T72
DATE	280115
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T70

NOTES
LC01 Cyc 11- 31 Cyclone
40 Fine Tail Comb
UF from T70
6 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
S C11	1.5	Finish	
Speed	850	W/h	kWh/t

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	3.1	394		197				5					
Water Change			49					3	7-9	7.5	7.5	300	
Conditioning S Ro C	5.6						59		6-9	3.0	10.5	120	22
Condition S C11 C1	6.7			197			10						
Condition	5.9	177			296			3		3.0	3.0	125	6
Condition	4.7					296		3		3.0	6.0	130	5
Condition	4.9							3		3.0	9.0	135	8
Sn Ro C1	5.1								9-10	3.0	12.0	150	6
Sn Ro C2	5.2								10-12	3.0	15.0	150	5
Sn Ro C3	5.1					99		3	9-12	3.0	18.0	130	9
Condition	5.2						20		9-11	3.0			
Sn Ro C4	5.2								9-11	3.0			
Sn Ro C5	5.2								9-11	3.0			
Sn Ro C6	5.2												
REAGENT TOTALS (g/t)		572	49	394	296	394	88						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T72 S C11 C1	26.6	5.2	0.17	1.3	41.2	10.2	1.54	49.4	36.8	74.5	7.14	0.9	0.08	0.7
S C11 Tail	6.8	1.3	0.46	0.9	27.6	1.8	0.71	5.8	12.2	6.3	27.6	0.9	0.34	0.7
Sn Ro C1	6.9	1.4	5.82	12.0	22.4	1.4	0.22	1.8	3.85	2.0	30.7	1.1	0.40	0.9
C2	6.2	1.2	5.10	9.4	21.8	1.3	0.16	1.2	2.57	1.2	31.8	1.0	0.43	0.9
C3	10.2	2.0	3.87	11.8	21.9	2.1	0.15	1.8	2.33	1.8	32.8	1.7	0.44	1.4
C4	9.3	1.8	4.64	12.9	24.0	2.1	0.14	1.6	1.31	0.9	28.9	1.3	0.48	1.4
C5	7.8	1.5	2.91	6.8	23.4	1.7	0.11	1.0	1.51	0.9	31.3	1.2	0.50	1.3
C6	11.9	2.3	2.35	8.3	24.3	2.7	0.12	1.7	1.53	1.4	31.4	1.9	0.51	1.9
Ro Tail	421.7	83.1	0.29	36.5	19.5	76.7	0.07	35.6	0.34	10.9	43.0	90.0	0.67	90.8
CALC	507.4	100.0	0.66	100.0	21.1	100.0	0.16	100.0	2.59	100.0	39.7	100.0	0.61	100.0
ASSAY HEAD			0.64		21.2		0.18		2.86		39.0		0.47	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T72 S C11 C1	26.6	5.2	0.17	1.35	41.2	10.2	1.54	49.4	36.8	74.5	7.14	0.94	0.08	0.68
S C11 Tail	33.4	6.6	0.23	2.3	38.4	12.0	1.37	55.2	31.8	80.8	11.3	1.9	0.13	1.4
Sn Ro C1	6.9	1.4	5.82	12.0	22.4	1.4	0.22	7.7	3.85	2.0	30.7	1.1	0.40	0.9
C2	13.1	2.6	5.48	21.4	22.1	2.7	0.19	8.8	3.24	3.2	31.2	2.0	0.41	1.7
C3	23.3	4.6	4.77	33.2	22.0	4.8	0.17	10.7	2.84	5.0	31.9	3.7	0.43	3.2
C4	32.6	6.4	4.74	46.1	22.6	6.9	0.16	12.3	2.41	6.0	31.1	5.0	0.44	4.6
C5	40.4	8.0	4.38	52.9	22.7	8.6	0.15	13.3	2.23	6.9	31.1	6.2	0.45	5.9
C6	52.3	10.3	3.92	61.2	23.1	11.3	0.15	15.0	2.07	8.3	31.2	8.1	0.47	7.8

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST
T72 S C11 C1	26.6	5.2	0.17	0.9	1.14	1.6	1.43	0.9
S C11 Tail	6.8	1.3	0.62	0.9	3.23	1.1	6.97	1.1
Sn Ro C1	6.9	1.4	0.71	1.0	3.26	1.2	7.29	1.2
C2	6.2	1.2	0.65	0.8	3.32	1.1	7.75	1.1
C3	10.2	2.0	0.61	1.3	3.36	1.8	8.14	2.0
C4	6.2	1.8	0.65	1.2	3.32	1.6	7.75	1.7
C5	10.2	1.5	0.61	1.0	3.36	1.4	8.14	1.5
C6	10.2	2.3	0.61	1.5	3.36	2.1	8.14	2.3
Ro Tail	421.7	83.1	1.07	91.5	4.04	88.3	8.90	88.3
CALC	505.0	100.0	0.97	100.0	3.80	100.0	8.38	100.0
ASSAY HEAD			0.95		3.86		8.42	

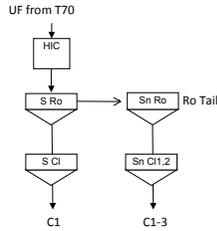
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM
T72 S C11 C1	26.6	5.2	0.17	0.9	1.14	1.6	1.43	0.9
S C11 Tail	33.4	6.6	0.26	1.8	1.57	2.7	2.56	2.0
Sn Ro C1	6.9	1.4	0.71	1.0	3.26	1.2	7.29	1.2
C2	13.1	2.6	0.68	1.8	3.29	2.2	7.51	2.3
C3	23.3	4.6	0.65	3.1	3.32	4.0	7.78	4.3
C4	32.6	6.4	0.65	4.3	3.32	5.6	7.77	6.0
C5	40.4	8.0	0.64	5.3	3.33	7.0	7.85	7.5
C6	52.3	10.3	0.64	6.7	3.33	9.0	7.91	9.7



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	173
DATE	050215
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T70

NOTES
LC01 Cyc 11- 31 Cyclone
-40 Fine Tail Comb
from centrifuge
6 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
Cl1	1.5	Finish	
Speed	0.8	W/h	
	750	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MiBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	4.8	391		196				5					
Water Change													
Conditioning S Ro C	5.4		49				58	3	6-9	4.5	4.5	300	
Condition S Cl C1	6.4						10		3-7	3.0	7.5	120	22
Condition	5.6	196		196				3					
Condition	4.3				293			3					
Condition	4.6					293		3		15.0	15.0	670	
Sn Ro C1							19						
Condition	4.8					98		3					
Sn Ro C2	5.1								5-12	15.0	30.0	730	
Condition	5.2									6.0	36.0	330	
Sn Cl1 C	5.6								2-12	1.0	37.0	20	12
Sn Cl2 C1									0.5-1	1.5	38.5	30	10
Sn Cl2 C2									1-2	3.0	41.5	60	5
Sn Cl2 C3	5.7								2-5	3.0			
REAGENT TOTALS (g/t)		587	49	391	293	391	87						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T73 S Cl1 C1	26.5	5.2	0.13	1.1	40.8	10.0	1.46	36.3	37.2	69.6	6.57	0.9	0.06	0.7
S Cl1 Tail	12.5	2.4	0.47	1.9	28.5	3.3	0.74	8.7	13.5	11.9	25.6	1.6	0.27	1.4
Sn Cl2 C1	2.3	0.5	15.9	11.6	24.1	0.5	0.05	0.1	1.94	0.3	13.6	0.2	0.29	0.3
C2	3.0	0.6	12.9	12.2	24.8	0.7	0.18	0.5	1.80	0.4	15.6	0.2	0.31	0.4
C3	3.3	0.6	8.86	9.1	25.9	0.8	0.06	0.2	2.36	0.5	19.7	0.3	0.33	0.4
Sn Cl2 Tail	14.2	2.8	3.33	15.0	26.1	3.4	0.20	2.7	2.07	2.1	28.7	2.1	0.36	2.1
Sn Cl1 Tail	54.0	10.6	1.27	21.7	21.9	11.0	0.21	10.6	1.66	6.3	35.9	9.9	0.40	8.9
Ro Tail	395.6	77.4	0.22	27.5	19.2	70.3	0.11	40.9	0.32	8.9	42.1	84.8	0.53	85.9
CALC	511.4	100.0	0.62	100.0	21.1	100.0	0.21	100.0	2.77	100.0	38.4	100.0	0.48	100.0
ASSAY HEAD			0.62		20.8		0.14		2.58		37.5		0.62	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T73 S Cl1 C1	26.5	5.2	0.13	1.09	40.8	10.0	1.46	36.3	37.2	69.6	6.57	0.89	0.06	0.65
S Cl1 Tail	39.0	7.6	0.24	2.9	36.9	13.3	1.23	45.0	29.6	81.4	12.7	2.5	0.13	2.0
Sn Cl2 C1	2.3	0.5	15.9	11.6	24.1	0.5	0.05	0.1	1.94	0.3	13.6	0.2	0.29	0.3
C2	5.3	1.0	14.2	23.8	24.5	1.2	0.12	9.3	1.86	0.7	14.7	0.4	0.30	0.7
C3	8.6	1.7	12.2	32.9	25.0	2.0	0.10	9.5	2.05	1.2	16.6	0.7	0.31	1.1
Sn Cl2 Tail	22.8	4.4	6.65	47.8	25.7	5.4	0.16	12.2	2.06	3.3	24.1	2.8	0.34	3.2
Sn Cl1 Tail	76.8	15.0	2.86	69.5	23.0	16.4	0.20	22.8	1.78	9.6	32.4	12.7	0.38	12.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T73 S Cl1 C1	26.5	5.2	0.16	2.6	0.85	2.3	1.12	1.5	0.66	1.3
S Cl1 Tail	12.5	2.4	0.53	4.1	2.99	3.8	6.35	3.9	1.89	1.8
Sn Cl2 C1	2.3	0.5	0.30	0.4	1.68	0.4	3.04	0.3	3.26	0.6
C2	3.0	0.6	0.30	0.6	1.70	0.5	3.40	0.5	3.37	0.8
C3	3.3	0.6	0.32	0.6	1.96	0.6	4.09	0.7	3.39	0.8
Sn Cl2 Tail	3.0	2.8	0.30	2.6	1.70	2.5	3.40	2.4	3.04	3.3
Sn Cl1 Tail	3.3	10.6	0.32	10.7	1.96	10.8	4.09	10.9	2.68	11.1
Ro Tail	3.3	77.4	0.32	78.3	1.96	79.1	4.09	79.8	2.63	80.2
CALC	57.04	100.0	0.32	100.0	1.92	100.0	3.96	100.0	2.54	100.0
ASSAY HEAD			0.96		3.61		8.24		2.58	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T73 S Cl1 C1	26.5	5.2	0.16	2.6	0.85	2.3	1.12	1.5	0.66	1.3
S Cl1 Tail	39.0	7.6	0.28	6.7	1.54	6.1	2.80	5.4	1.05	3.2
Sn Cl2 C1	2.3	0.5	0.30	0.4	1.68	0.4	3.04	0.3	3.26	0.6
C2	5.3	1.0	0.30	1.0	1.69	0.9	3.24	0.8	3.32	1.4
C3	8.6	1.7	0.31	1.6	1.79	1.6	3.57	1.5	3.35	2.2
Sn Cl2 Tail	22.8	4.4	0.30	4.3	1.74	4.0	3.46	3.9	3.16	5.5
Sn Cl1 Tail	76.8	15.0	0.31	15.0	1.89	14.8	3.90	14.8	2.82	16.7

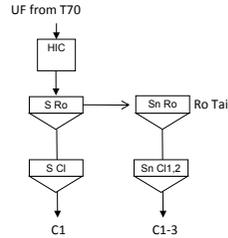


BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T74
DATE	110215
TECHNICIAN	MW

Milling		Primary	Regrind
Mill type	HIC		
Media type			
Media kg			
Solids g	500		
Water g	400		
Time min	5.0		
Speed rpm	60HZ		
Lime g			
End pH			
End p80			

kwh/t		Regrind Power
Float Cell	Volume	Start
Rougher C1	2.5	Finish
Speed	750	W/h
		kWh/t



PRODUCT FLOATED	
UF from T70	

NOTES	
LC01 Cyc 11- 31 Cyclone	
40 Fine Tail Comb	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	596		199				5					
Water Change			50					3	6-9	4.5	4.5	300	
Conditioning S Ro C	5.3						59						
Condition	5.4	199		199				3					
Condition	4.2				298			3					
Condition	4.4					298		3					
Sn Ro C1	4.8					99	20	3		9.0	9.0	390	
Condition	4.9								5-12	9.0	18.0	430	
Sn Ro C2	4.9												
Condition	5.1								2-12	7.5	25.5	420	
Sn Cl1 C	5.7								0.5-1	1.0	26.5	30	4
Sn Cl2 C1	5.9								1-4	2.5	29.0	60	2
Sn Cl2 C2									4-5	3.5	32.5	60	2
Sn Cl2 C3													
REAGENT TOTALS (g/t)		794	50	397	298	397	79						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T74 S Ro C1	36.8	7.3	0.22	2.8	38.0	12.9	1.10	60.9	20.1	74.6	13.7	2.5	0.12	1.9
Sn Cl2 C1	1.1	0.2	22.8	8.5	18.7	0.2	0.14	0.2	3.49	0.4	12.5	0.1	0.20	0.1
C2	1.2	0.2	18.1	7.1	21.1	0.2	0.17	0.3	4.29	0.5	14.0	0.1	0.22	0.1
C3	1.1	0.2	10.8	3.9	23.9	0.2	0.21	0.3	5.47	0.6	18.4	0.1	0.24	0.1
Sn Cl2 Tail	6.5	1.3	4.14	9.2	24.8	1.5	0.17	1.7	3.37	2.2	27.1	0.9	0.28	0.8
Sn Cl1 Tail	23.4	4.6	1.20	9.6	21.8	4.7	0.11	3.9	1.98	4.7	36.4	4.3	0.35	3.5
Ro Tail	433.7	86.1	0.40	59.0	20.1	80.3	0.05	32.7	0.39	17.1	42.5	92.1	0.51	93.6
CALC	503.7	100.0	0.58	100.0	21.6	100.0	0.13	100.0	1.97	100.0	39.7	100.0	0.47	100.0
ASSAY HEAD			0.62		20.8		0.14		2.58		37.5		0.62	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T74 S Ro C1	36.8	7.3	0.22	2.76	38.0	12.9	1.10	60.9	20.1	74.6	13.7	2.52	0.12	1.87
Sn Cl2 C1	1.1	0.2	22.8	8.5	18.7	0.2	0.14	0.2	3.49	0.4	12.5	0.1	0.20	0.1
C2	2.3	0.4	20.4	15.6	19.9	0.4	0.16	0.5	3.90	0.9	13.2	0.1	0.21	0.2
C3	3.3	0.7	17.3	19.5	21.2	0.6	0.17	0.9	4.40	1.5	14.9	0.2	0.22	0.3
Sn Cl2 Tail	9.8	1.9	8.58	28.6	23.6	2.1	0.17	2.5	3.72	3.7	23.0	1.1	0.26	1.1
Sn Cl1 Tail	33.2	6.6	3.38	38.2	22.3	6.8	0.13	6.4	2.49	8.4	32.4	5.4	0.32	4.5

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	norganic %	DIST
T74 S Ro C1	36.8	7.3	0.28	5.8	1.66	5.6	3.23	5.2	1.01	2.9
Sn Cl2 C1	1.1	0.2	0.29	0.2	1.70	0.2	3.13	0.1	1.86	0.2
C2	1.2	0.2	0.30	0.2	1.76	0.2	3.58	0.2	2.09	0.2
C3	1.1	0.2	0.36	0.2	2.23	0.2	4.66	0.2	2.30	0.2
Sn Cl2 Tail	1.2	1.3	0.30	1.1	1.76	1.0	3.58	1.0	2.31	1.2
Sn Cl1 Tail	1.1	4.6	0.36	4.7	2.23	4.8	4.66	4.8	2.27	4.1
Ro Tail	1.1	86.1	0.36	87.8	2.23	88.1	4.66	88.5	2.71	91.3
CALC	43.39	100.0	0.35	100.0	2.18	100.0	4.54	100.0	2.56	100.0
ASSAY HEAD			0.96		3.61		8.24		2.58	

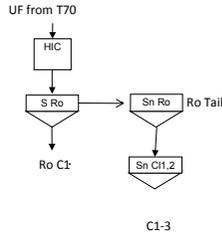
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	norganic %	CUM
T74 S Ro C1	36.8	7.3	0.28	5.8	1.66	5.6	3.23	5.2	1.01	2.9
Sn Cl2 C1	1.1	0.2	0.29	0.2	1.70	0.2	3.13	0.1	1.86	0.2
C2	2.3	0.4	0.30	0.4	1.73	0.4	3.36	0.3	1.98	0.3
C3	3.3	0.7	0.32	0.6	1.89	0.6	3.78	0.5	2.08	0.5
Sn Cl2 Tail	9.8	1.9	0.31	1.7	1.80	1.6	3.65	1.6	2.23	1.7
Sn Cl1 Tail	33.2	6.6	0.34	6.4	2.10	6.4	4.36	6.3	2.26	5.8



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T75
DATE	110215
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T70

NOTES
LC01 Cyc 11- 31 Cyclone
40 Fine Tail Comb

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	0.8	W/h	
	750	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t		Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	595		198					5					
Water Change									3					
Conditioning			50							6-9	4.5	4.5	300	
S Ro C	5.3						59							
Condition	5.6	198		198					3					
Condition	4.3				298				3					
Condition	4.7					298			3					
Sn Ro C1	4.8						20				9.0	9.0	390	
Condition	4.9								3					
Sn Ro C2	4.9									5-12	9.0	18.0	430	
HIC Cond (60HZ)	3.3			99					5					
Condition	4.6								3					
Condition	4.6					99			3					
Sn C1 C	4.6									2-12	7.5	25.5	420	
Sn C1 C1	5.2									0.5-1	1.0	26.5	30	6
Sn C1 C2										1-4	2.5	29.0	60	5
Sn C1 C3	5.3									4-5	3.5	32.5	60	3
REAGENT TOTALS (g/t)		794	50	496	397	496	79							

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T75 S Ro C1	36.8	7.3	0.22	2.8	38.0	13.2	1.10	61.3	20.1	70.6	13.7	2.6	0.12	1.9
Sn C1 C1	1.7	0.3	18.4	10.8	22.5	0.4	0.16	0.4	3.40	0.6	11.9	0.1	0.24	0.2
C2	3.2	0.6	12.6	13.9	25.2	0.8	0.12	0.6	4.00	1.2	14.6	0.2	0.26	0.4
C3	1.7	0.3	7.70	4.3	27.2	0.4	0.17	0.4	3.93	0.6	18.4	0.2	0.29	0.2
Sn C1 C2 Tail	7.1	1.4	2.35	5.7	25.2	1.7	0.16	1.7	3.77	2.6	26.8	1.0	0.32	1.0
Sn C1 Tail	19.3	3.8	0.50	3.3	19.7	3.6	0.09	2.6	1.56	2.9	40.7	4.0	0.34	2.8
Ro Tail	434.1	86.1	0.40	59.2	19.5	79.9	0.05	32.9	0.52	21.5	41.5	91.9	0.50	93.5
CALC	503.9	100.0	0.58	100.0	21.0	100.0	0.13	100.0	2.08	100.0	38.9	100.0	0.46	100.0
ASSAY HEAD			0.62		20.8		0.14		2.58		37.5		0.62	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T75 S Ro C1	36.8	7.3	0.22	2.76	38.0	13.2	1.10	61.3	20.1	70.6	13.7	2.57	0.12	1.90
Sn C1 C1	1.7	0.3	18.4	10.8	22.5	0.4	0.16	0.4	3.40	0.6	11.9	0.1	0.24	0.2
C2	5.0	1.0	14.6	24.7	24.3	1.1	0.13	1.0	3.79	1.8	13.7	0.3	0.25	0.5
C3	6.6	1.3	12.9	29.0	25.0	1.6	0.14	1.4	3.83	2.4	14.8	0.5	0.26	0.7
Sn C1 C2 Tail	13.7	2.7	7.42	34.7	25.1	3.3	0.15	3.2	3.80	5.0	21.0	1.5	0.29	1.7
Sn C1 Tail	33.0	6.6	3.38	38.0	21.9	6.8	0.12	5.8	2.49	7.8	32.5	5.5	0.32	4.6

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T75 S Ro C1	36.8	7.3	0.28	6.3	1.66	5.9	3.23	5.0	0.94	2.7
Sn C1 C1	1.7	0.3	0.26	0.3	1.58	0.3	3.32	0.2	2.31	0.3
C2	3.2	0.6	0.28	0.6	1.78	0.6	3.94	0.5	2.62	0.7
C3	1.7	0.3	0.33	0.3	2.09	0.3	4.91	0.3	2.83	0.4
Sn C1 C2 Tail	3.2	1.4	0.28	1.2	1.78	1.2	3.94	1.2	2.74	1.5
Sn C1 Tail	1.7	3.8	0.33	3.9	2.09	3.9	4.91	3.9	1.91	2.9
Ro Tail	1.7	86.1	0.33	87.4	2.09	87.8	4.91	88.8	2.73	91.6
CALC	49.96	100.0	0.33	100.0	2.05	100.0	4.76	100.0	2.57	100.0
ASSAY HEAD			0.96		3.61		8.24		2.58	

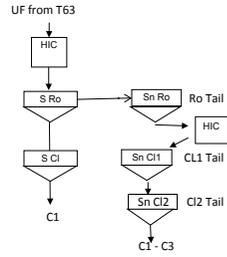
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T75 S Ro C1	36.8	7.3	0.28	6.3	1.66	5.9	3.23	5.0	0.94	2.7
Sn C1 C1	1.7	0.3	0.26	0.3	1.58	0.3	3.32	0.2	2.31	0.3
C2	5.0	1.0	0.27	0.8	1.71	0.8	3.72	0.8	2.51	1.0
C3	6.6	1.3	0.29	1.2	1.81	1.2	4.02	1.1	2.59	1.3
Sn C1 C2 Tail	13.7	2.7	0.28	2.4	1.79	2.4	3.98	2.3	2.67	2.8
Sn C1 Tail	33.0	6.6	0.31	6.3	1.97	6.3	4.52	6.2	2.23	5.7



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T76
DATE	190215
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80		



PRODUCT FLOATED
UF from T70

NOTES
UF from T70 6 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	0.8	W/h	
	750	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	1203		200				5					
Water Change			50										
Conditioning S Ro C	5.2						60	3	7-9	7.5	7.5	300	
Condition S Cl1 C1	6.4						10		3-7	3.0	10.5	120	20
Condition Condition	5.3	241		200				3					
Condition Condition	4.2				301			3					
Condition Condition	4.4					301		3					
Sn Ro C1	4.6						20	3		9.0	9.0	405	
Condition	4.8					100		3					
Sn Ro C2	4.8			100			20	3	9-13	17.0	26.0	950	
HIC Condition					100			5					
Condition						100		3					
Sn Cl1 C	5.0						20	3	5-12	7.0	33.0	420	
Sn Cl2 C1	5.2								0.5-1	1.5	34.5	30	11
Sn Cl2 C2	5.4								2-5	2.5	37.0	60	10
Sn Cl2 C3	5.4								5-7	3.5	40.5	100	5
REAGENT TOTALS (g/t)		1443	50	501	401	601	129						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T76 S Cl1 C1	23.9	4.8	0.13	0.9	37.7	8.6	1.17	42.1	37.8	67.9	6.75	0.8	0.07	0.5
S Cl1 Tail	12.4	2.5	0.42	1.6	33.4	4.0	1.05	19.6	16.2	15.1	21.3	1.4	0.29	1.1
Sn Cl2 C1	3.4	0.7	16.2	16.7	23.2	0.8	0.12	0.6	2.13	0.5	14.2	0.2	0.30	0.3
C2	6.1	1.2	12.5	23.0	25.0	1.5	0.12	1.1	2.07	1.0	16.0	0.5	0.33	0.6
C3	5.0	1.0	7.67	11.7	27.6	1.3	0.12	0.9	2.32	0.9	18.6	0.5	0.39	0.6
Sn Cl2 Tail	11.3	2.3	3.21	11.0	28.5	3.1	0.12	2.0	1.85	1.6	24.7	1.4	0.50	1.8
Sn Cl1 Tail	28.3	5.7	0.50	4.3	20.4	5.5	0.07	3.0	1.07	2.3	38.9	5.6	0.56	5.0
Ro Tail	408.4	81.9	0.25	30.8	19.3	75.2	0.05	30.7	0.35	10.7	42.8	89.5	0.70	90.0
CALC	498.9	100.00	0.66	100.0	20.9	100.0	0.13	100.0	2.67	100.0	39.1	100.0	0.64	100.0
ASSAY HEAD			0.76		21.5		0.17		2.55		39.3		0.68	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T76 S Cl1 C1	23.9	4.8	0.13	0.94	37.7	8.62	1.17	42.1	37.8	67.9	6.75	0.83	0.07	0.53
S Cl1 Tail	36.3	7.3	0.23	2.5	36.2	12.6	1.13	61.6	30.4	83.0	11.7	2.2	0.15	1.7
Sn Cl2 C1	3.4	0.7	16.2	16.7	23.2	0.8	0.12	20.2	2.13	0.5	14.2	0.2	0.30	0.3
C2	9.6	1.9	13.8	39.8	24.4	2.2	0.12	21.3	2.09	1.5	15.4	0.8	0.32	1.0
C3	14.6	2.9	11.7	51.4	25.5	3.6	0.12	22.2	2.17	2.4	16.5	1.2	0.34	1.6
Sn Cl2 Tail	25.9	5.2	7.98	62.4	26.8	6.6	0.12	24.3	2.03	4.0	20.1	2.7	0.41	3.4
Sn Cl1 Tail	54.2	10.9	4.07	66.7	23.5	12.2	0.09	27.2	1.53	6.2	29.9	8.3	0.49	8.3

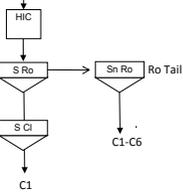
PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T76 S Cl1 C1	23.9	4.8	0.14	1.9	0.85	2.0	1.40	1.4	0.68	1.2
S Cl1 Tail	12.4	2.5	0.46	3.3	2.50	3.0	4.85	2.6	1.94	1.8
Sn Cl2 C1	3.4	0.7	0.29	0.6	1.67	0.6	3.91	0.6	2.00	0.5
C2	6.1	1.2	0.32	1.1	1.80	1.1	4.14	1.1	2.36	1.1
C3	5.0	1.0	0.36	1.0	2.15	1.0	4.83	1.1	2.81	1.0
Sn Cl2 Tail	6.1	2.3	0.32	2.1	1.80	2.0	4.14	2.0	2.95	2.4
Sn Cl1 Tail	5.0	5.7	0.36	5.8	2.15	5.9	4.83	5.9	2.59	5.4
Ro Tail	5.0	81.9	0.36	84.2	2.15	84.6	4.83	85.3	2.90	86.7
CALC	67.07	100.00	0.35	100.0	2.08	100.0	4.64	100.0	2.74	100.0
ASSAY HEAD			1.05		3.68		7.68		2.79	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T76 S Cl1 C1	23.9	4.8	0.14	1.9	0.85	2.0	1.40	1.4	0.68	1.2
S Cl1 Tail	36.3	7.3	0.25	5.2	1.41	4.9	2.58	4.0	1.11	2.9
Sn Cl2 C1	3.4	0.7	0.29	0.6	1.67	0.6	3.91	0.6	2.00	0.5
C2	9.6	1.9	0.31	1.7	1.75	1.6	4.06	1.7	2.23	1.6
C3	14.6	2.9	0.33	2.7	1.89	2.7	4.32	2.7	2.43	2.6
Sn Cl2 Tail	25.9	5.2	0.32	4.8	1.85	4.6	4.24	4.7	2.66	5.0
Sn Cl1 Tail	54.2	10.9	0.34	10.6	2.01	10.5	4.55	10.7	2.62	10.4

PROJECT	T0879
TEST NO	T78
DATE	24/02/15
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg	500	
Solids g	400	
Water g	5.0	
Time min	60HZ	
Speed rpm		
Lime g		
End pH		
End p80		

Cyc 11-31 -40 Fine Tails O/F +CS6



PRODUCT FLOATED
Cyc 11-31 -40 Fine Tails O/F +CS6

NOTES
LC01 Cyc 11- 31 Cyclone 40 Fine Tail Comb from centrifuge 6 micron Test routine per T69 EDTA Leach residue (T77)

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
		Finish	
Speed	850	W/h	

	pH	10.0 H2SO4 g/t	0.5 SF g/t	1.0 SIPX g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.6	1251		208				5					
Water Change			52					3	7-9	8.5	8.5	440	
Conditioning S Ro C	4.9						62		6-9	3.0	11.5	120	14
Condition S Cl1 C1	5.9			208			10						
Condition	5.1	208			313	313		3		3.0	3.0	125	3
Condition	4.2							3		3.0	6.0	130	2
Sn Ro C1	4.4							3		3.0	9.0	135	3
Sn Ro C2	4.5						10		9-10	3.0	12.0	150	2
Sn Ro C3	4.6								10-12	3.0	15.0	150	3
Condition						104		3		3.0	18.0	130	2
Sn Ro C4	5.0						21		9-12	3.0			
Sn Ro C5	4.6								9-11	3.0			
Sn Ro C6	4.7								9-11	3.0			
REAGENT TOTALS (g/t)		1459	52	417	313	417	103						

PRODUCTS	WT g	WT %	Sn %	DIST %	Fe %	DIST %	As %	DIST %	S %	DIST %	SiO2 %	DIST %	MnO %	DIST %
T78 S Cl1 C1	17.3	3.6	0.16	0.9	38.9	6.7	0.66	19.2	37.6	53.0	8.94	0.8	0.10	0.6
S Cl1 Tail	16.9	3.5	0.40	2.3	27.7	4.7	0.33	9.4	13.8	18.9	26.8	2.4	0.34	2.1
Sn Ro C1	3.4	0.7	0.61	0.7	22.2	0.8	0.24	1.4	5.16	1.4	35.0	0.6	0.42	0.5
C2	2.7	0.6	0.57	0.5	21.9	0.6	0.21	1.0	4.05	0.9	35.7	0.5	0.41	0.4
C3	3.5	0.7	0.55	0.7	21.8	0.8	0.20	1.2	2.87	0.8	37.8	0.7	0.44	0.6
C4	3.7	0.8	1.11	1.4	21.0	0.8	0.20	1.2	2.47	0.7	35.9	0.7	0.43	0.6
C5	4.3	0.9	0.92	1.3	21.0	0.9	0.19	1.4	1.71	0.6	37.9	0.9	0.46	0.7
C6	3.1	0.6	0.80	0.8	20.4	0.6	0.18	0.9	1.93	0.5	37.7	0.6	0.43	0.5
Ro Tail	424.8	88.6	0.63	91.3	19.8	84.1	0.09	64.3	0.67	23.2	41.0	92.7	0.62	94.1
CALC	479.7	100.0	0.61	100.0	20.8	100.0	0.12	100.0	2.56	100.0	39.2	100.0	0.58	100.0
ASSAY HEAD			0.57		20.7		0.18		2.85		39.3		0.44	

CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM %	Fe %	CUM %	As %	CUM %	S %	CUM %	SiO2 %	CUM %	MnO %	CUM %
T78 S Cl1 C1	17.3	3.6	0.16	0.94	38.9	6.75	0.66	19.2	37.6	53.0	8.94	0.82	0.10	0.62
S Cl1 Tail	34.2	7.1	0.28	3.2	33.4	11.4	0.50	28.6	25.8	71.9	17.8	3.2	0.22	2.7
Sn Ro C1	3.4	0.7	0.61	0.7	22.2	0.8	0.24	10.8	5.16	1.4	35.0	0.6	0.42	0.5
C2	6.1	1.3	0.59	1.2	22.1	1.3	0.23	11.7	4.67	2.3	35.3	1.1	0.42	0.9
C3	9.6	2.0	0.58	1.9	22.0	2.1	0.22	12.9	4.01	3.1	36.2	1.9	0.42	1.5
C4	13.3	2.8	0.73	3.3	21.7	2.9	0.21	14.1	3.58	3.9	36.1	2.6	0.43	2.0
C5	17.6	3.7	0.77	4.6	21.5	3.8	0.21	15.5	3.13	4.5	36.6	3.4	0.43	2.7
C6	20.7	4.3	0.78	5.5	21.4	4.4	0.20	16.4	2.95	5.0	36.7	4.0	0.43	3.2

PRODUCTS	WT g	WT %	CaO %	DIST %	MgO %	DIST %	Al2O3 %	DIST %
T78 S Cl1 C1	17.3	3.6	0.17	0.7	1.26	1.2	1.82	0.8
S Cl1 Tail	16.9	3.5	0.53	2.0	3.13	3.0	6.97	2.9
Sn Ro C1	3.4	0.7	0.63	0.5	4.29	0.8	9.23	0.8
C2	2.7	0.6	0.65	0.4	4.22	0.6	10.0	0.7
C3	3.5	0.7	0.72	0.6	4.29	0.8	10.3	0.9
C4	2.7	0.8	0.65	0.5	4.22	0.9	10.0	0.9
C5	3.5	0.9	0.72	0.7	4.29	1.0	10.3	1.1
C6	3.5	0.6	0.72	0.5	4.29	0.7	10.3	0.8
Ro Tail	424.8	88.6	0.98	94.1	3.81	90.8	8.58	91.1
CALC	478.3	100.0	0.92	100.0	3.71	100.0	8.34	100.0
ASSAY HEAD			0.91		4.02		9.32	

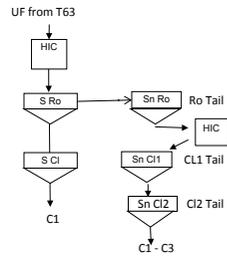
CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM %	MgO %	CUM %	Al2O3 %	CUM %
T78 S Cl1 C1	17.3	3.6	0.17	0.7	1.26	1.2	1.82	0.8
S Cl1 Tail	34.2	7.1	0.35	2.7	2.18	4.2	4.36	3.7
Sn Ro C1	3.4	0.7	0.63	0.5	4.29	0.8	9.23	0.8
C2	6.1	1.3	0.64	0.9	4.26	1.5	9.57	1.5
C3	9.6	2.0	0.67	1.5	4.27	2.3	9.84	2.4
C4	13.3	2.8	0.66	2.0	4.26	3.2	9.88	3.3
C5	17.6	3.7	0.68	2.7	4.26	4.2	9.98	4.4
C6	20.7	4.3	0.68	3.2	4.27	5.0	10.0	5.2



BURNIE LABORATORY: ROUGHER FLOTATION REPORT SHEET

PROJECT	T0879
TEST NO	T79
DATE	020315
TECHNICIAN	MW

Milling	Primary	Regrind
Mill type	HIC	
Media type		
Media kg		
Solids g	500	
Water g	400	
Time min	5.0	
Speed rpm	60HZ	
Lime g		
End pH		
End p80 μ m		



PRODUCT FLOATED
UF from T63

NOTES
UF from T63
Cut at 6 micron

Float Cell	Volume	Regrind	Power
Rougher	2.5	Start	
C1	1.5	Finish	
Speed	0.8	W/h	
	750	kWh/t	

	pH	10.0 H2SO4 g/t	0.5 SIPX g/t	1.0 SSF g/t	1.0 Na2SO3 g/t	1.0 SPA7080 g/t	0.495 MIBC g/t	Cond Time min	Air L/min	Float Time min	Cum Float Time	Wet Wt g	Con % Solids
HIC Cond (60HZ)	2.5	1010		202				5					
Water Change			50										
Conditioning													
S Ro C	5.3						60	3	7-9	7.5	7.5	350	
Condition													
S Cl1 C1	6.4						10		3-7	3.0	10.5	120	19
Condition	5.3	242		202				3					
Condition	4.2							3					
Condition	4.4				303	454		3					
Sn Ro C1	4.4					101	20	3		9.0	9.0	400	
Condition	4.6							3					
Sn Ro C2	4.6			101			20	3	9-13	17.0	26.0	400	
Condition					101	101		5					
Condition								3					
Sn Cl1 C	5.1						20	3	5-12	8.0	34.0	420	
Sn Cl2 C1	5.4							3	0.5-2	1.5	35.5	30	15
Sn Cl2 C2	5.5							3	2-5	2.5	38.0	60	10
Sn Cl2 C3	5.6							3	5-7	3.5	41.5	100	5
REAGENT TOTALS (g/t)		1252	50	505	404	656	130						

PRODUCTS	WT g	WT %	Sn %	DIST	Fe %	DIST	As %	DIST	S %	DIST	SiO2 %	DIST	MnO %	DIST
T76 S C1 C1	22.6	4.6	0.14	1.0	40.7	8.8	1.17	41.0	37.7	64.5	10.1	1.2	0.08	0.6
S C1 Tail	13.6	2.7	0.41	1.8	32.9	4.3	0.97	20.4	17.1	17.6	21.2	1.5	0.29	1.3
Sn Cl2 C1	4.4	0.9	14.7	20.4	25.2	1.1	0.10	0.7	1.81	0.6	13.5	0.3	0.36	0.5
C2	6.0	1.2	10.5	19.7	27.3	1.6	0.11	1.0	1.76	0.8	16.0	0.5	0.42	0.8
C3	5.2	1.1	6.62	10.9	30.3	1.5	0.14	1.1	2.01	0.8	27.3	0.7	0.51	0.8
Sn Cl2 Tail	10.9	2.2	2.80	9.6	31.6	3.3	0.11	1.9	1.64	1.4	22.5	1.3	0.62	2.2
Sn Cl1 Tail	26.4	5.3	0.70	5.8	22.7	5.7	0.06	2.5	1.21	2.4	36.8	5.0	0.68	5.7
Ro Tail	406.2	82.0	0.24	30.8	19.1	73.9	0.05	31.5	0.39	12.0	42.5	89.5	0.68	88.1
CALC	495.3	100.0	0.64	100.0	21.2	100.0	0.13	100.0	2.67	100.0	39.0	100.0	0.63	100.0
ASSAY HEAD			0.76		21.5		0.17		2.55		39.3		0.68	

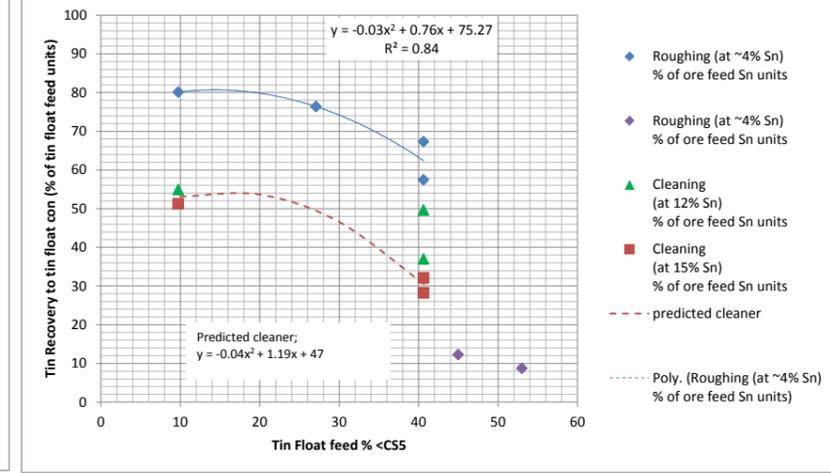
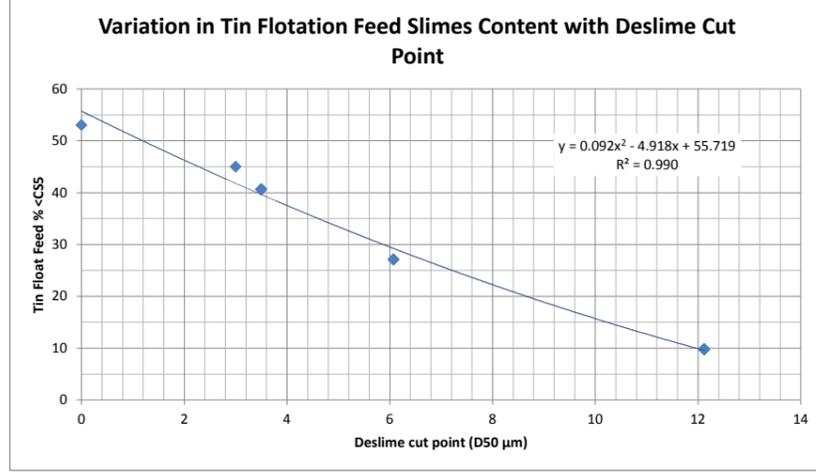
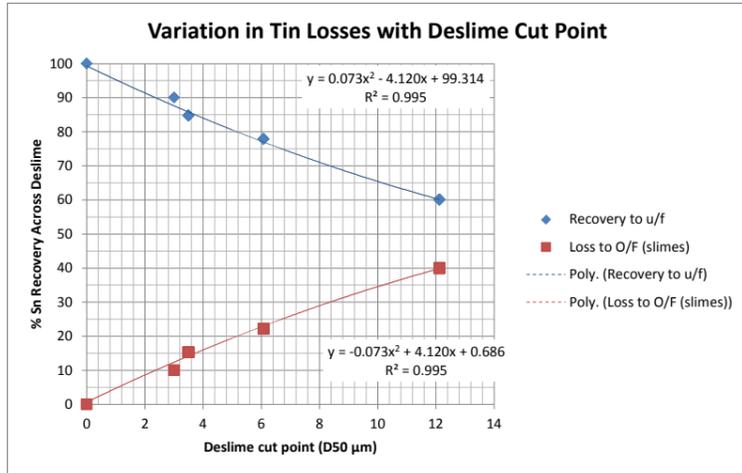
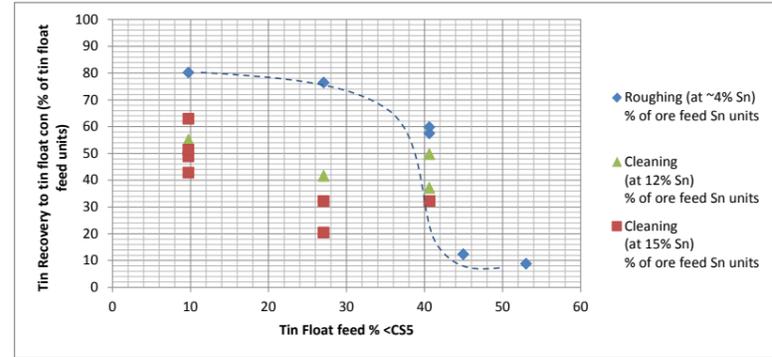
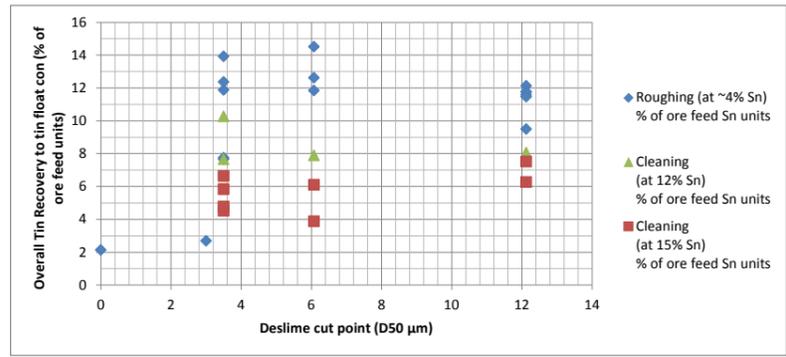
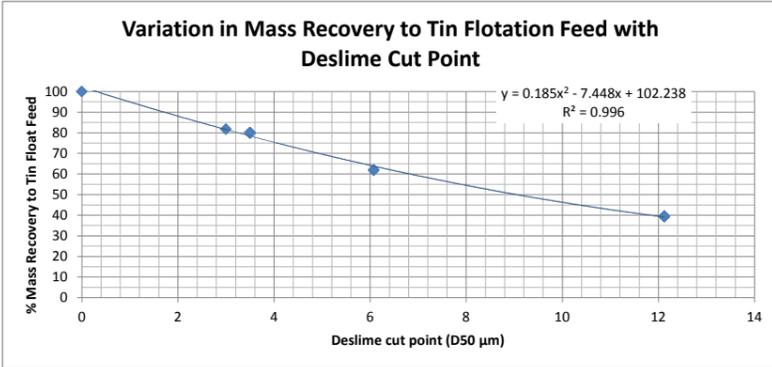
CUM PRODUCTS	CUM Wt	WT %	Sn %	CUM	Fe %	CUM	As %	CUM	S %	CUM	SiO2 %	CUM	MnO %	CUM
T76 S C1 C1	22.6	4.6	0.14	1.00	40.7	8.76	1.17	41.0	37.7	64.5	10.1	1.18	0.08	0.58
S C1 Tail	36.2	7.3	0.24	2.8	37.8	13.0	1.09	61.4	30.0	82.1	14.2	2.7	0.16	1.8
Sn Cl2 C1	4.4	0.9	14.7	20.4	25.2	1.1	0.10	21.1	1.81	0.6	13.5	0.3	0.36	0.5
C2	10.4	2.1	12.3	40.1	26.4	2.6	0.11	22.1	1.78	1.4	14.9	0.8	0.39	1.3
C3	15.6	3.1	10.4	51.0	27.7	4.1	0.12	23.3	1.86	2.2	19.1	1.5	0.43	2.2
Sn Cl2 Tail	26.5	5.3	7.25	60.6	29.3	7.4	0.11	25.1	1.77	3.5	20.5	2.8	0.51	4.3
Sn Cl1 Tail	52.9	10.7	3.98	66.5	26.0	13.1	0.09	27.6	1.49	6.0	28.6	7.8	0.59	10.0

PRODUCTS	WT g	WT %	CaO %	DIST	MgO %	DIST	Al2O3 %	DIST	horganic %	DIST
T76 S C1 C1	22.6	4.6	0.19	1.9	1.11	1.9	2.97	1.6	0.73	1.3
S C1 Tail	13.6	2.7	0.48	2.9	2.53	2.5	5.35	1.7	1.71	1.8
Sn Cl2 C1	4.4	0.9	0.31	0.6	1.69	0.5	3.49	0.4	2.50	0.9
C2	6.0	1.2	0.35	0.9	1.96	0.9	4.38	0.6	2.99	1.4
C3	5.2	1.1	0.48	1.1	2.86	1.1	9.17	1.1	3.42	1.4
Sn Cl2 Tail	6.0	2.2	0.35	1.7	1.96	1.6	4.38	1.1	3.54	3.0
Sn Cl1 Tail	5.2	5.3	0.48	5.6	2.86	5.6	9.17	5.7	3.01	6.2
Ro Tail	5.2	82.0	0.48	85.4	2.86	85.9	9.17	87.8	2.65	84.0
CALC	68.19	100.0	0.46	100.0	2.73	100.0	8.57	100.0	2.59	100.0
ASSAY HEAD			1.05		3.68		7.68		2.79	

CUM PRODUCTS	CUM Wt	WT %	CaO %	CUM	MgO %	CUM	Al2O3 %	CUM	horganic %	CUM
T76 S C1 C1	22.6	4.6	0.19	1.9	1.11	1.9	2.97	1.6	0.73	1.3
S C1 Tail	36.2	7.3	0.30	4.7	1.64	4.4	3.86	3.3	1.10	3.1
Sn Cl2 C1	4.4	0.9	0.31	0.6	1.69	0.5	3.49	0.4	2.50	0.9
C2	10.4	2.1	0.33	1.5	1.85	1.4	4.00	1.0	2.78	2.3
C3	15.6	3.1	0.38	2.6	2.18	2.5	5.73	2.1	3.00	3.6
Sn Cl2 Tail	26.5	5.3	0.37	4.3	2.09	4.1	5.17	3.2	3.22	6.7
Sn Cl1 Tail	52.9	10.7	0.42	9.8	2.48	9.7	7.17	8.9	3.11	12.9

Summary of Tin Flotation Tests T58 to T79

Date of deslime test	Date of float test	Time elapsed (days) from deslime to float test	Time elapsed (days) from 'comparable test'	Tin Flotation Test No.	Feed material			Deslime mass recovery to u/f % wt	Sulfide scav.				Tin float					Tin Flotation Response				Deslime Performance		Overall Tin department to Deslime feed % of ore feed Sn units	Overall Tin to Tin Float Feed % of ore feed Sn units	Overall Tin recovery to flotation con			Overall Tin loss to Slime Tails % of ore feed Sn units	Overall Tin loss to Tin Float Tails % of ore feed Sn units	Combine loss; slimes + TFT % of ore feed Sn units			
					Deslime cut point (D50) μm	Produced from test no.	% <CS5 (<8 μm)		H ₂ SO ₄ g/t	SSF g/t	Water change	SIPX g/t	H ₂ SO ₄ g/t	SSF g/t	Na ₂ SO ₃ g/t	SPA7080 g/t	MIBC g/t	Roughing		Cleaning		Tin recovery to U/F	Tin loss to O/F			Roughing (at ~4% Sn) % of ore feed Sn units	Cleaning (at 12% Sn) % of ore feed Sn units	Cleaning (at 15% Sn) % of ore feed Sn units						
																		Grade (% Sn)	Recovery	Grade (% Sn)	Cleaning recovery													
24/11/2014	24/11/2014	0	0	T58	12.1	UF from T56	9.7	39.3	401	200	yes	50	180	200	301	401	99	4.0	80.2			9.0	62.9	60.1	39.9	24.4	14.7	11.8			9.7			
24/11/2014	24/11/2014	0	0	T59	12.1	UF from T56	9.7	39.3	440	200	yes	50	200	200	0	400	119	4.0	79.0			9.0	48.9	60.1	39.9	24.4	14.7	11.6			9.7			
24/11/2014	02/12/14	8		T60	12.1	UF from T56	9.7	39.3	399	200	yes	50	100	200	299	299	99	4.0	82.7					60.1	39.9	24.4	14.7	12.1			9.7			
24/11/2014	01/12/14	7	1	T61	12.1	UF from T56	9.7	39.3	298	199	no	50	0	199	298	398	98	4.0	64.7					60.1	39.9	24.4	14.7	9.5			9.7			
24/11/2014	02/12/14	8		T62	12.1	UF from T56	9.7	39.3	400	200	yes	50	180	200	300	400	79	4.0	80.1	12.0	55.0	15.0	51.3	60.1	39.9	24.4	14.7	11.7	8.1	7.5	7.1	16.9		
24/11/2014	05/12/14	11	3	T65	12.1	UF from T56	9.7	39.3	199	199	yes	50	100	199	299	398	79	4.0	78.2			15.0	42.8	60.1	39.9	24.4	14.7	11.5			9.7	8.4	18.1	
3/12/2014	04/12/14	1		T64	6.1	UF from T63	27.1	61.8	397	199	yes	50	179	199	298	397	88	4.0	76.4					77.8	22.2	24.4	19.0	14.5			5.4			
3/12/2014	15/12/14	12	11	T67	6.1	UF from T63	27.1	61.8	499	200	yes	50	120	200	300	399	99	4.0	62.3			15.0	32.1	77.8	22.2	24.4	19.0	11.8			6.1	5.4	12.9	18.3
3/12/2014	2/03/2015	89		T79	6.1	UF from T63	27.1	61.8	1010	202	yes	50	242	303	404	656	130	4.0	66.4	12.0	41.6	14.7	20.4	77.8	22.2	24.4	19.0	12.6	7.9	3.9	5.4	15.1	20.5	
22/01/2015	23/01/2015	1		T71	4	UF from T70	40.6	79.9	592	197	yes	49	197	197	296	395	88	4.0	57.5	12.0	37.0	15.0	32.1	84.7	15.3	24.4	20.7	11.9			6.6	3.7	14.0	17.8
22/01/2015	28/01/2015	6	5	T72	4	UF from T70	40.6	79.9	394	197	yes	49	177	197	296	394	88	4.0	59.8					84.7	15.3	24.4	20.7	12.4			6.6	3.7		
22/01/2015	11/02/15	20	19	T74	4	UF from T70	40.6	79.9	596	199	yes	50	199	199	298	397	79	4.0	37.1			15.0	21.9	84.7	15.3	24.4	20.7	7.7			4.5	3.7	16.1	19.9
22/01/2015	11/02/15	20	19	T75	4	UF from T70	40.6	79.9	595	198	yes	50	198	298	397	496	79	4.0	37.5			15.0	23.1	84.7	15.3	24.4	20.7	7.8			4.8	3.7	15.9	19.6
22/01/2015	19/2/15	28	27	T76	4	UF from T70	40.6	79.9	1203	200	yes	50	241	301	401	601	129	4.0	67.3	12.0	49.7	15.0	28.2	84.7	15.3	24.4	20.7	13.9	10.3	5.8	3.7	14.8	18.6	
				T69	3	LC Cyc 11-31: - 40 Fine Tails + O/F, +CS6	45.0	81.7	783	196	yes	49	176	196	294	392	97	3.9	12.3					90	10.0	24.4	22.0	2.7				2.4		
13/01/2015	13/01/15	0		T68	0	LC Cyc 11-31: - 40 Fine Tails + O/F	53.0	100.0	298	198	yes	50	298	198	298	397	88	3.4	8.7					100	0.0	24.4	24.4	2.1				0.0		
13/01/2015	13/01/15	0	0																															





WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 12 – Final Tin Flotation Concentrate Analysis



McKnight
Mineralogy

ABN 65962932907

PO Box 451 Buninyong
VIC 3357

Ph 03 53279262
M 0407860394
s.mcknight@ballarat.edu.au
mineralogy@hotmail.com

QXRD Analysis of Scheelite Concentrate 932013 Supplied by ALS Metallurgy Burnie

Attn: Shengli Zhao
John Glen

S W McKnight
26/3/2015

Samples Supplied

Tin concentrates:

879829 CL2 CONC LOW GRADE COMP
879830 CL2 CONC MEDIUM GRADE COMP

887517 T43 S CLI CON

Results wt% (semiquantitative)

#879829 CL2 CONC LOW GRADE COMP

Phase	Weight%
Siderite	37.1
Cassiterite	13.1
Quartz	11.7
Rutile	11.5
Magnetite	7.5
Chlorite	4.6
Pyrite	3.9
Dravite/tourmaline	3.1
Anatase	2.8
Microcline	1.4
Diaspore?	1.4
Muscovite	1.2
Apatite	0.6
Calcite	0
Dolomite	0
Actinolite/tremolite	0

#879829 CL2 CONC LOW GRADE COMP

Element Distributions - approximate

		Cassiterite	Anatase	Rutile	Siderite	Quartz	Pyrite	Calcite 2	Apatite	Microcline	Muscovite	Magnetite	Actinolite	Dravite	Dolomite	Diaspore	Chlorite
Element	Totals	13.1	2.8	11.5	37.1	11.7	3.9	0	0.6	1.4	1.2	7.5	0	3.1	0	1.4	4.6
Sn	10.36	10.36															
O	38.42	2.79	1.13	4.59	15.38	6.22		0	0.24	0.67	0.57	2.08		1.62	0	0.74	2.39
Ti	8.56		1.69	6.87													
Fe	25.13				17.89		1.8					5.44					
C	3.85				3.85			0							0		
Si	7.4					5.46				0.44	0.25			0.55			0.7
S	2.07						2.07										
Ca	0.24							0	0.24						0		
P	0.11								0.11								
H	0.11								0		0.01			0.01		0.02	0.07
Cl	0.01								0.01								
F	0.02								0.02								
K	0.32									0.2	0.12						
Al	1.98									0.14	0.24			0.53		0.62	0.45
Na	0.08													0.08			
Mg	1.25													0.24	0		1.01
B	0.11													0.11			

#879830 CL2 CONC MEDIUM GRADE COMP

Phase	Weight%
Siderite	34.2
Cassiterite	18.9
Rutile	12
Quartz	10.2
Magnetite	9.1
Pyrite	2.9
Anatase	2.6
Apatite	2.4
Chlorite	2.1
Dravite/tourmaline	1.9
Diaspore?	1.6
Microcline	1.3
Muscovite	0.7
Calcite	0
Dolomite	0
Actinolite	0

#879830 CL2 CONC MEDIUM GRADE COMP

Element Distributions - approximate

		Cassiterite	Anatase	Rutile	Siderite	Quartz	Pyrite	Calcite	Apatite, Apatite,	Microcline	Muscovite	Magnetite	Actinolite	Dravite	Dolomite	Diaspore	Chlorite
Element	Totals	18.9	2.6	12	34.2	10.2	2.9	0	2.4	1.3	0.7	9.1	0	1.9	0	1.6	2.1
Sn	14.92	14.92															
O	36.82	4.02	1.04	4.82	14.17	5.46		0	0.91	0.6	0.36	2.52		1	0	0.84	1.08
Ti	8.77		1.55	7.21													
Fe	24.42				16.49		1.33					6.59					
C	3.55				3.55			0							0		
Si	6					4.79				0.4	0.16			0.34			0.31
S	1.53						1.53										
Ca	0.91							0	0.9						0		
P	0.43								0.43								
H	0.07								0		0			0.01		0.03	0.03
Cl	0.04								0.04								
F	0.07								0.07								
K	0.26									0.18	0.07						
Al	1.51									0.13	0.15			0.33		0.7	0.2
Na	0.05													0.05			
Mg	0.6													0.15	0		0.45
B	0.07													0.07			

#887517 T43 S CLI CON

Phase	Weight%
Talc (triclinic)	37
Pyrite	31.5
Antigorite	7.7
Pyrrhotite	3.8
Calcite	3.3
Albite	2.8
Quartz	2.7
Apatite	2.2
Siderite	2.1
Phlogophite -Fe	2.1
Actinolite	1.7
Cassiterite	1.1
Magnetite	0.9
Chlorite	0.7
Dravite	0.3
Dolomite	0.1
Diaspore	0

#887517 T43 S CLI CON

Element Distributions - approximate

		Albite	Cassiterite	Siderite	Quartz	Pyrite	Calcite	Apatite	Magnetite	Antigorite	Talc	Actinolite	Dravite	Dolomite	Diaspore	Chlorite	Pyrrhotite-4C 1	Phlogopit e, -Fe
Element	Totals	2.8	1.1	2.1	2.7	31.5	3.3	2.2	0.9	7.7	37	1.7	0.3	0.1	0	0.7	3.8	2.1
Na	0.27	0.25											0.01					0.01
Al	0.43	0.29											0.05		0	0.07		0.01
Si	13.69	0.91			1.25						10.97		0.05			0.11		0.4
O	26.78	1.39	0.23	0.89	1.42		1.56	0.83	0.24		18.75		0.16	0.03	0	0.37		0.91
Sn	0.85		0.85															
Fe	18.89			1.03		14.66			0.63								2.31	0.26
C	0.62			0.22			0.39							0.01				
S	18.35					16.83											1.51	
Ca	2.15						1.3	0.83						0.01				0.01
P	0.39							0.39										
H	0.22							0			0.2		0		0	0.01		0.01
Cl	0.04							0.04										
F	0.06							0.06										
Mg	7.65										7.12		0.02	0.01		0.16		0.33
B	0.01												0.01					
K	0.19																	0.19



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 13 – Concentrate Leach Results



BURNIE LABORATORY: BATCH ATMOSPHERIC LEACH RESULTS SHEET

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	100
Total Liquor Mass (gm)	114.9
Liquor SG (kg/L)	1.147

PROJECT	T0879
TEST NO	T52
DATE	181114
TECHNICIAN	BR

Start acid g/l	242
Start liq ml	100
start acid g	24
end acid g/l	34
end liq ml	87
end acid g	3
acid consumed g	21
acid consumption kg/t	420

LEACH CONDITIONS

Beaker Volume (ml)	200
Agitator (type)	mag
Agitator (rpm)	
N2 Sparge (lpm)	5
Start Temp (deg)	90
Leach Time (hrs)	4.0
Start Solids (gm)	50.6
Liquor Volume Used (l)	0.10

LEACH FEED SAMPLE DETAILS			
Non-Mags			
4hr Leach			
End liquor diluted by 50% with water due to precipitate			

MASS BALANCE

Beaker Mass (gm)	147.3
Ag (gm)	0
Start Solids (gm)	50.6
Start Liquor (gm)	112.6
Total Start Mass (gm)	310.5
Total End Mass (gm)	278.36
End Solids Mass (gm)	28.5
End Liquor SG (kg/L)	1.1805
Calc End Liquor (gm)	102.6
Calc End Liquor (L)	0.087
End Free Acid (g/L)	34.2
End Fe2+ (g/L)	46.3

Mins	Temp	Start pH	N2 Flow (lpm)
0	85	0.13	0
1	85	0.18	5
60	90	0.90	5
120	85	1.06	5
180	90	0.80	5
240	90	1.10	5

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(g/L)	Rec (%)	(g/L)	Rec (%)	(g/L)	Rec (%)	(g/L)	Rec (%)	(g/L)	Rec (%)	(g/L)	Rec (%)	(g/L)	Rec (%)
Start Liquor	0.1	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0
Final Liquor	0.1	0.008	0.0	107.60	80.5	0.02	4.4	5.36	89.1	0.62	18.9	7.36	86.4	4.66	51.4

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al		C inorg	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Start Solids	50.6	27.60		21.80		0.11		1.29		1.19		2.25		2.71			
Final Residue	28.5	46.90	100.0	7.94	19.5	0.14	95.6	0.20	10.9	0.81	81.1	0.35	13.6	1.34	48.6	0.86	11.5

Calc Feed	50.6	26.42		22.95		0.08		1.03		0.57		1.46		1.56			
Assay Feed		27.60		21.80		0.11		1.29		1.19		2.25		2.71		4.23	

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	100
Total Liquor Mass (gm)	114.9
Liquor SG (kg/L)	1.147

LEACH CONDITIONS

Beaker Volume (ml)	200
Agitator (type)	mag
Agitator (rpm)	
N2 Sparge (lpm)	5
Start Temp (deg)	90
Leach Time (hrs)	6.0
Start Solids (gm)	50.0
Liquor Volume Used (l)	0.10

MASS BALANCE

Beaker Mass (gm)	139.11
Agit (gm)	0
Start Solids (gm)	50
Start Liquor (gm)	111
Total Start Mass (gm)	300.11
Total End Mass (gm)	303.26
End Solids Mass (gm)	27.0
End Liquor SG (kg/L)	1.2684
Calc End Liquor (gm)	137.2
Calc End Liquor (L)	0.108
End Free Acid (g/L)	28.8
End Fe2+ (g/L)	70.3

PROJECT	T0879
TEST NO	T53
DATE	191114
TECHNICIAN	BR

LEACH FEED SAMPLE DETAILS
Non-Mags
6hr Leach

Start acid g/l	242
Start liq ml	100
start acid g	24
end acid g/l	29
end liq ml	108
end acid g	3
acid consumed g	21
acid consumption kg/t	422

Mins	Temp	Start pH	N2 Flow (lpm)
0	90	0.12	0
7	90	0.42	5
60	90	0.71	5
120	90	0.83	5
180	85	1.05	5
240	90	1.08	5
300	90	1.15	5
360	90	1.15	5

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al			
		(g/L)	Rec (%)														
Start Liquor	0.1	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0		
Final Liquor	0.1	0.006	0.0	83.00	83.2	0.01	3.6	4.00	92.0	0.54	24.1	5.23	87.7	3.13	49.3		

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al		C inorg	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Start Solids	50.0	27.60		21.80		0.11		1.29		1.19		2.25		2.71			
Final Residue	27.0	50.30	100.0	6.71	16.8	0.15	96.4	0.14	8.0	0.68	75.9	0.29	12.3	1.29	50.7	0.62	7.9

Calc Feed	50.0	27.11		21.57		0.08		0.94		0.48		1.29		1.37			
Assay Feed		27.60		21.80		0.11		1.29		1.19		2.25		2.71		4.23	

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	1000
Total Liquor Mass (gm)	1148.6
Liquor SG (kg/L)	1.147

PROJECT	T0879
TEST NO	T54
DATE	191114
TECHNICIAN	BR

Start acid g/l	242
start acid g	23.7
end acid g	1.5
acid consumed g	22.2
acid consumption kg/t	443

LEACH CONDITIONS

Beaker Volume (ml)	200
Agitator (type)	mag
Agitator (rpm)	
N2 Sparge (lpm)	5
Start Temp (deg)	90
Leach Time (hrs)	6.0
Start Solids (gm)	50.0
Liquor Volume Used (l)	0.10

LEACH FEED SAMPLE DETAILS			
Non-Mags			
8hr Leach			

MASS BALANCE

Beaker Mass (gm)	139.82
Agi (gm)	0
Start Solids (gm)	50
Start Liquor (gm)	112.2
Total Start Mass (gm)	302.02
Total End Mass (gm)	299.87
End Solids Mass (gm)	27.7
End Liquor SG (kg/L)	1.2685
Calc End Liquor (gm)	132.4
Calc End Liquor (L)	0.104
End Free Acid (g/L)	14.5
End Fe2+ (g/L)	71.1

Mins	Temp	Start pH	N2 Flow (lpm)
0	90	0.10	0
7	90	0.35	5
60	90	0.76	5
120	90	0.89	5
180	85	1.11	5
240	95	0.82	5
300	90	1.22	5
360	90	1.15	5
420	85	1.23	5
480	90	1.25	5

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al			
		(g/L)	Rec (%)														
Start Liquor	0.1	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0		
Final Liquor	0.1	0.007	0.0	86.40	81.6	0.01	4.0	4.15	90.7	0.55	24.6	5.20	84.9	3.19	47.8		

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al		CO3	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Start Solids	50.0	27.60		21.80		0.11		1.29		1.19		2.25		2.71			
Final Residue	27.7	47.70	100.0	7.34	18.4	0.13	96.0	0.16	9.3	0.63	75.4	0.35	15.1	1.31	52.2	2.90	7.6

Calc Feed	50.0	26.40		22.10		0.07		0.95		0.46		1.28		1.39			
Assay Feed		27.60		21.80		0.11		1.29		1.19		2.25		2.71		21.15	



BURNIE LABORATORY: BATCH ATMOSPHERIC LEACH RESULTS SHEET

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	800
Total Liquor Mass (gm)	888.0
Liquor SG (kg/L)	1.1118

PROJECT	T0879
TEST NO	T66
DATE	081214
TECHNICIAN	MW

Start acid g/l	242
Start liq ml	799
start acid g	193
end acid g/l	30
end liq ml	830
end acid g	25
acid consumed g	168
acid consumption kg/t	560

LEACH CONDITIONS

Beaker Volume (ml)	2000
Agitator (type)	RT
Agitator (rpm)	250
N2 Blanket (lpm)	1
Start Temp (deg)	90
Leach Time (hrs)	8.0
Start Solids (gm)	300.0
Liquor Volume Used (l)	0.800

LEACH FEED SAMPLE DETAILS
T57 Float Ro Tail

MASS BALANCE

Beaker Mass (gm)	861.2
Agg (gm)	235.3
Start Solids (gm)	300
Start Liquor (gm)	888
Total Start Mass (gm)	2284.5
Total End Mass (gm)	2291.2
End Solids Mass (gm)	153.4
End Liquor SG (kg/L)	1.2553
Calc End Liquor (gm)	1041.3
Calc End Liquor (L)	30.400
End Free Acid (g/L)	30.4
End Fe2+ (g/L)	63.9

Hrs	Temp	Start pH	N2 Flow (lpm)
0	90	-0.9	1
1	90	0.36	1
2	90	0.59	1
3	90	0.71	1
4	90	0.74	1
5	90	0.77	1
6	90	0.77	1
7	90	0.77	1
8	90	0.77	1

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(g/L)	Rec (%)												
Start Liquor	0.8	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0
Final Liquor	0.8	0.008	0.0	74.30	91.3	0.01	4.0	3.91	95.1	0.72	35.8	4.95	82.7	2.77	35.0

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Start Solids	300.0	28.80		21.00		0.10		1.10		1.20		2.60		2.70	
Final Residue	153.4	55.25	100.0	3.82	8.7	0.13	96.0	0.11	4.9	0.70	64.2	0.56	17.3	2.79	65.0

Calc Feed	300.0	28.25		22.50		0.07		1.14		0.56		1.66		2.19	
Assay Feed		28.80		21.00		0.10		1.10		1.20		2.60		2.70	



BURNIE LABORATORY: BATCH ATMOSPHERIC LEACH RESULTS SHEET

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	100
Total Liquor Mass (gm)	104.8
H2SO4 g/L	100.0
Start Free Acid g/L	98.0
Liquor SG (kg/L)	1.058

PROJECT	T0879
TEST NO	T80
DATE	180315
TECHNICIAN	MW/DG

start acid	g	9.7
end acid	g	6.8
acid consumption	g	2.9
acid consumption	kg/t	480

LEACH CONDITIONS

Beaker Volume (ml)	150
Agitator (type)	mag
Start Temp (deg)	90
Leach Time (hrs)	8.0
Start Solids (gm)	6.0086
Liquor Volume Used (l)	0.100

LEACH FEED SAMPLE DETAILS

Float Products
Cl2 Conc Medium Grade
N2 Blanket at Start

MASS BALANCE

Beaker Mass (gm)	46.6
Mag stirrer (gm)	3.48
Start Solids (gm)	6.0086
Start Liquor (gm)	104.8
Total Start Mass (gm)	160.89
Total End Mass (gm)	160.33
End Solids Mass (gm)	2.8384
End Liquor SG (kg/L)	1.0865
Calc End Liquor (gm)	107.4
Calc End Liquor (L)	0.099
End Free Acid (g/L)	69.0

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al			
		(g/L)	Rec (%)														
Start Liquor	0.100	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0		
Final Liquor	0.099	0.015	0.2	14.50	92.5	0.01	28.4	0.19	95.7	0.37	94.8	0.58	80.4	0.52	29.6		

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al		C inorg	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Final Residue	2.8384	28.10	100.0	4.12	7.5	0.05	71.6	0.03	4.3	0.07	5.2	0.49	19.6	4.29	70.4		

Calc Feed	6.0086	13.27		25.80		0.03		0.33		0.64		1.18		2.88			
-----------	--------	-------	--	-------	--	------	--	------	--	------	--	------	--	------	--	--	--



BURNIE LABORATORY: BATCH ATMOSPHERIC LEACH RESULTS SHEET

LIQUOR MAKE UP

LEACH TYPE	Acid
Liquor Volume (ml)	100
Total Liquor Mass (gm)	105.1
H2SO4 g/L	100.0
Start Free Acid g/L	98.0
Liquor SG (kg/L)	1.058

PROJECT	T0879
TEST NO	T81
DATE	180315
TECHNICIAN	MW/DG

start acid	g	9.7
end acid	g	6.6
acid consumption	g	3.2
acid consumption	kg/t	528

LEACH CONDITIONS

Beaker Volume (ml)	150
Agitator (type)	mag
Start Temp (deg)	90
Leach Time (hrs)	8.0
Start Solids (gm)	6.0069
Liquor Volume Used (l)	0.100

LEACH FEED SAMPLE DETAILS	
Float Products	
Cl2 Conc Low Grade	
N2 Blanket at Start	

MASS BALANCE

Beaker Mass (gm)	48.08
Mag stirrer (gm)	3.44
Start Solids (gm)	6.0086
Start Liquor (gm)	105.1
Total Start Mass (gm)	162.63
Total End Mass (gm)	165.08
End Solids Mass (gm)	2.5996
End Liquor SG (kg/L)	1.0801
Calc End Liquor (gm)	111.0
Calc End Liquor (L)	0.103
End Free Acid (g/L)	63.9

RESULTS

Stream	Vol (L)	Sn		Fe		As		Mn		Ca		Mg		Al			
		(g/L)	Rec (%)														
Start Liquor	0.100	0.0	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0	0.00	0.0		
Final Liquor	0.103	0.009	0.2	15.45	93.4	0.06	81.9	0.20	98.7	0.15	88.3	0.62	81.2	0.58	30.2		

Stream	Mass (gm)	Sn		Fe		As		Mn		Ca		Mg		Al		C inorg	
		(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)	(%)	Rec (%)
Final Residue	2.5996	20.70	100.0	4.30	6.6	0.05	18.1	0.01	1.3	0.08	11.7	0.57	18.8	5.26	69.8		

Calc Feed	6.0086	8.96		28.28		0.12		0.34		0.30		1.31		3.26			
-----------	--------	------	--	-------	--	------	--	------	--	------	--	------	--	------	--	--	--



WorleyParsons

resources & energy

EcoNomics™

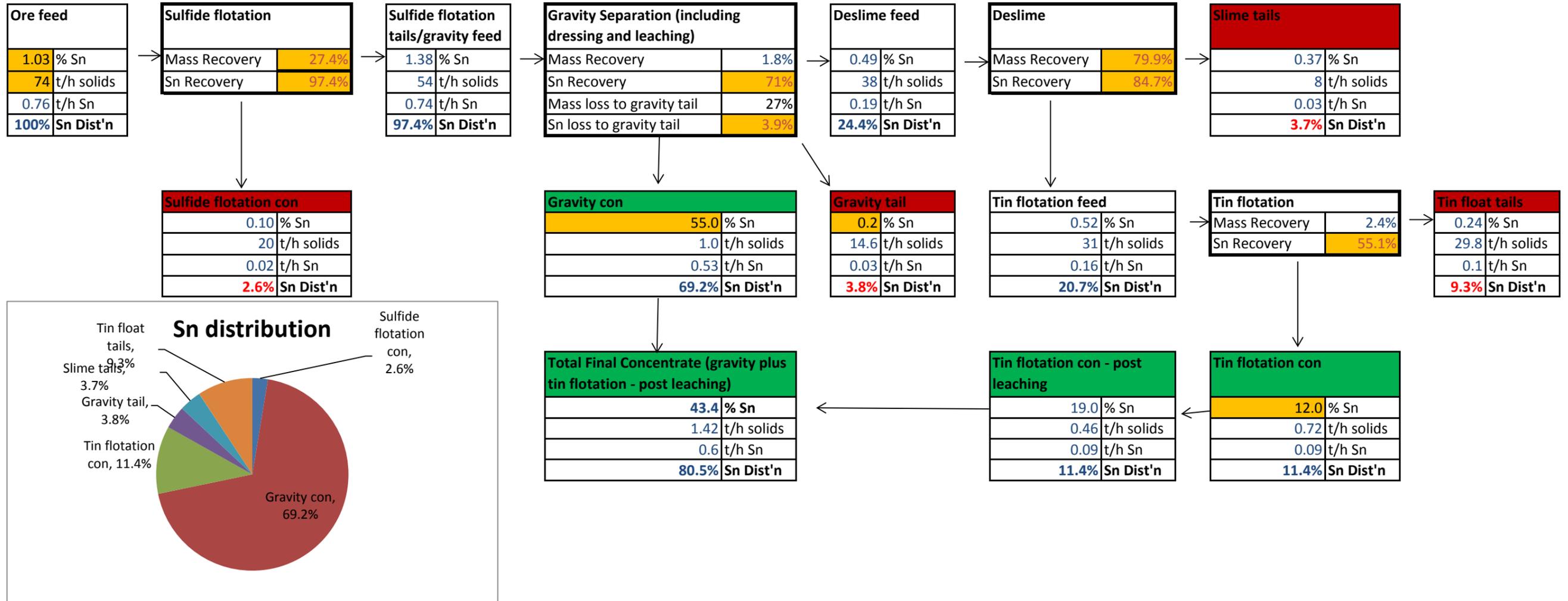
STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

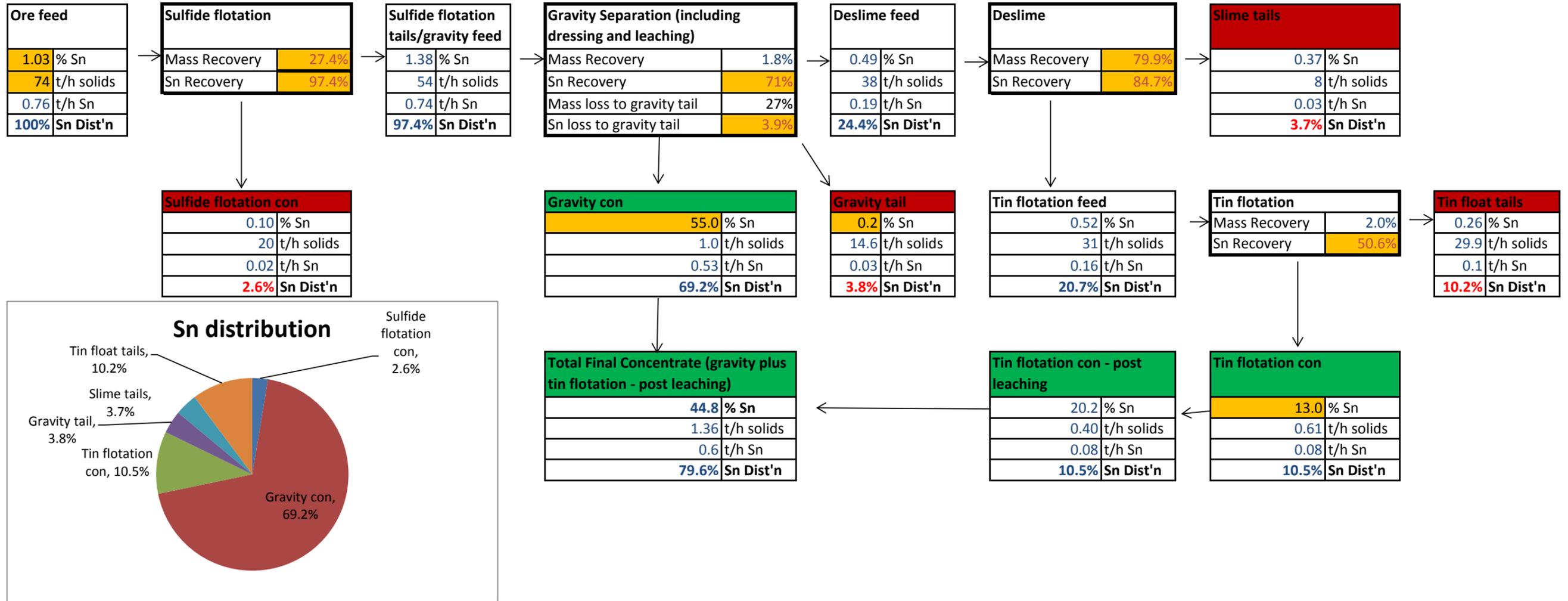
SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 14 – Overall Tin Balances

Demonstrated; 4 micron deslime (deslime test T70, tin float test T76) 12% Sn float con



Demonstrated; 4 micron deslime (deslime test T70, tin float test T76) 13% Sn float con



Demonstrated; 4 micron deslime (deslime test T70, tin float test T76) 14% Sn float con

Ore feed	
1.03	% Sn
74	t/h solids
0.76	t/h Sn
100%	Sn Dist'n

Sulfide flotation	
Mass Recovery	27.4%
Sn Recovery	97.4%

Sulfide flotation tails/gravity feed	
1.38	% Sn
54	t/h solids
0.74	t/h Sn
97.4%	Sn Dist'n

Gravity Separation (including dressing and leaching)	
Mass Recovery	1.8%
Sn Recovery	71%
Mass loss to gravity tail	27%
Sn loss to gravity tail	3.9%

Deslime feed	
0.49	% Sn
38	t/h solids
0.19	t/h Sn
24.4%	Sn Dist'n

Deslime	
Mass Recovery	79.9%
Sn Recovery	84.7%

Slime tails	
0.37	% Sn
8	t/h solids
0.03	t/h Sn
3.7%	Sn Dist'n

Sulfide flotation con	
0.10	% Sn
20	t/h solids
0.02	t/h Sn
2.6%	Sn Dist'n

Gravity con	
55.0	% Sn
1.0	t/h solids
0.53	t/h Sn
69.2%	Sn Dist'n

Gravity tail	
0.2	% Sn
14.6	t/h solids
0.03	t/h Sn
3.8%	Sn Dist'n

Tin flotation feed	
0.52	% Sn
31	t/h solids
0.16	t/h Sn
20.7%	Sn Dist'n

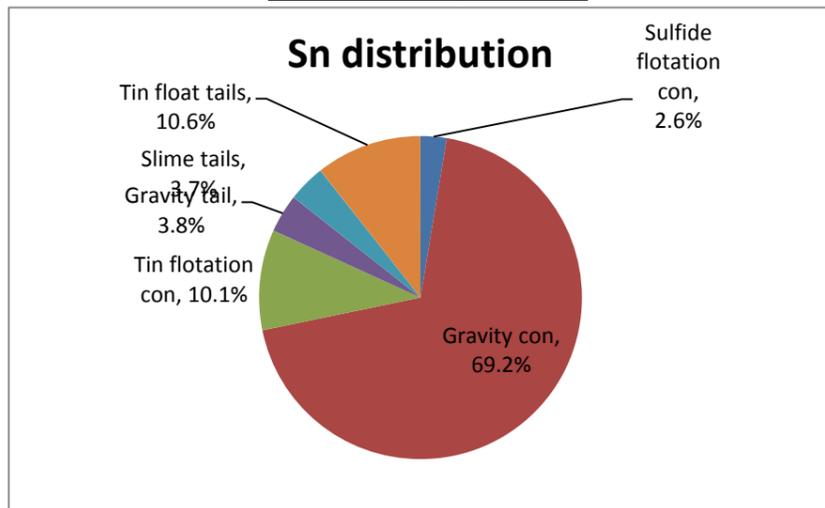
Tin flotation	
Mass Recovery	1.8%
Sn Recovery	48.6%

Tin float tails	
0.27	% Sn
30.0	t/h solids
0.1	t/h Sn
10.6%	Sn Dist'n

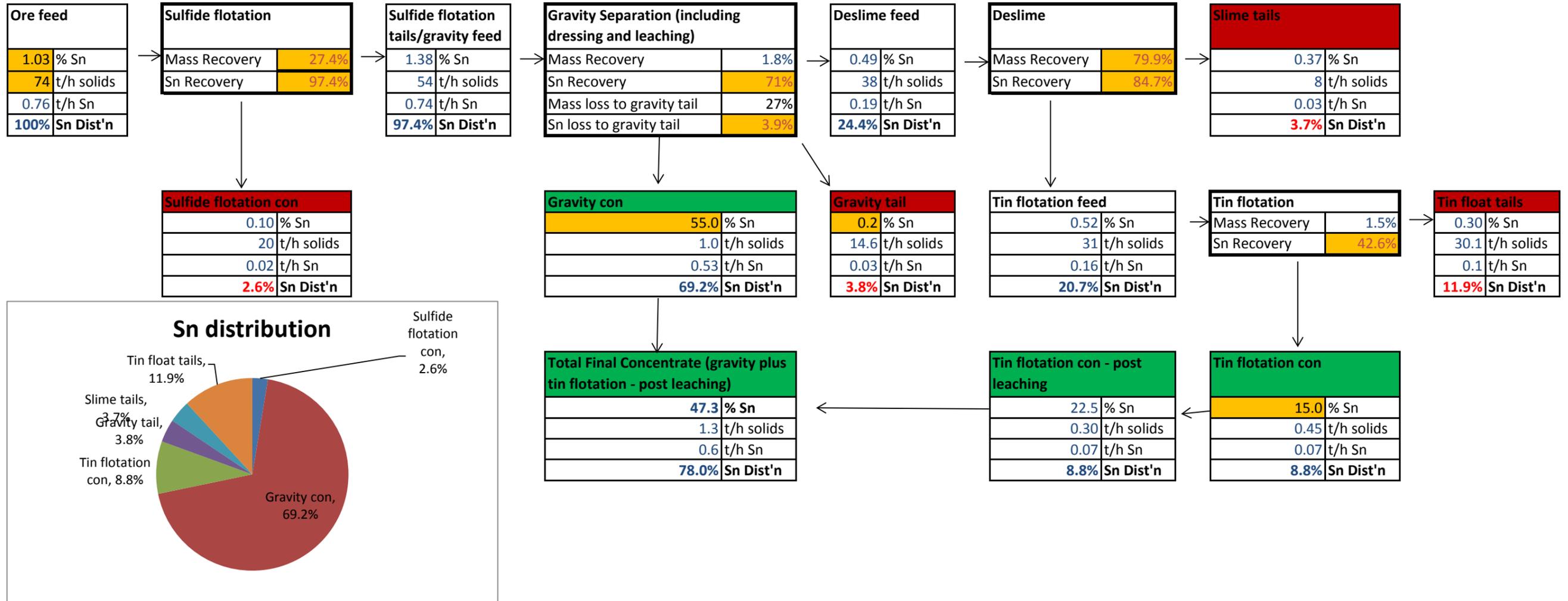
Total Final Concentrate (gravity plus tin flotation - post leaching)	
45.8	% Sn
1.32	t/h solids
0.6	t/h Sn
79.2%	Sn Dist'n

Tin flotation con - post leaching	
21.3	% Sn
0.36	t/h solids
0.08	t/h Sn
10.1%	Sn Dist'n

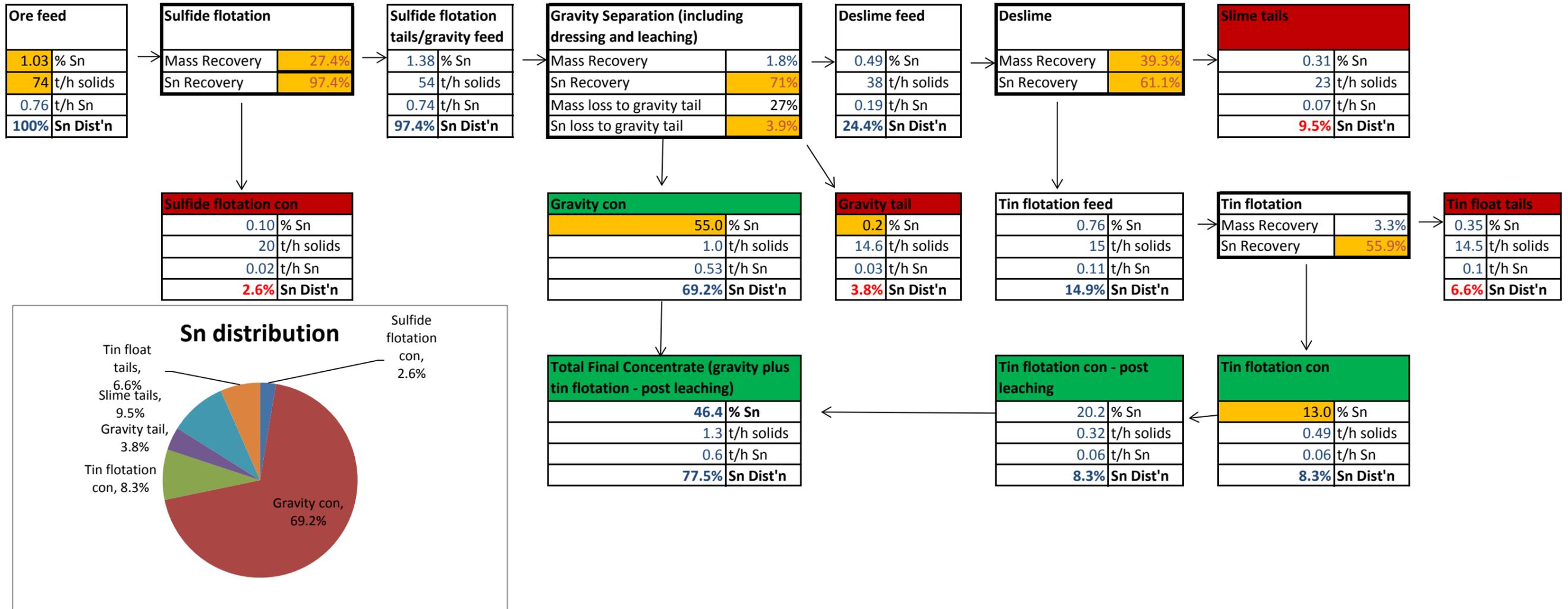
Tin flotation con	
14.0	% Sn
0.55	t/h solids
0.08	t/h Sn
10.1%	Sn Dist'n



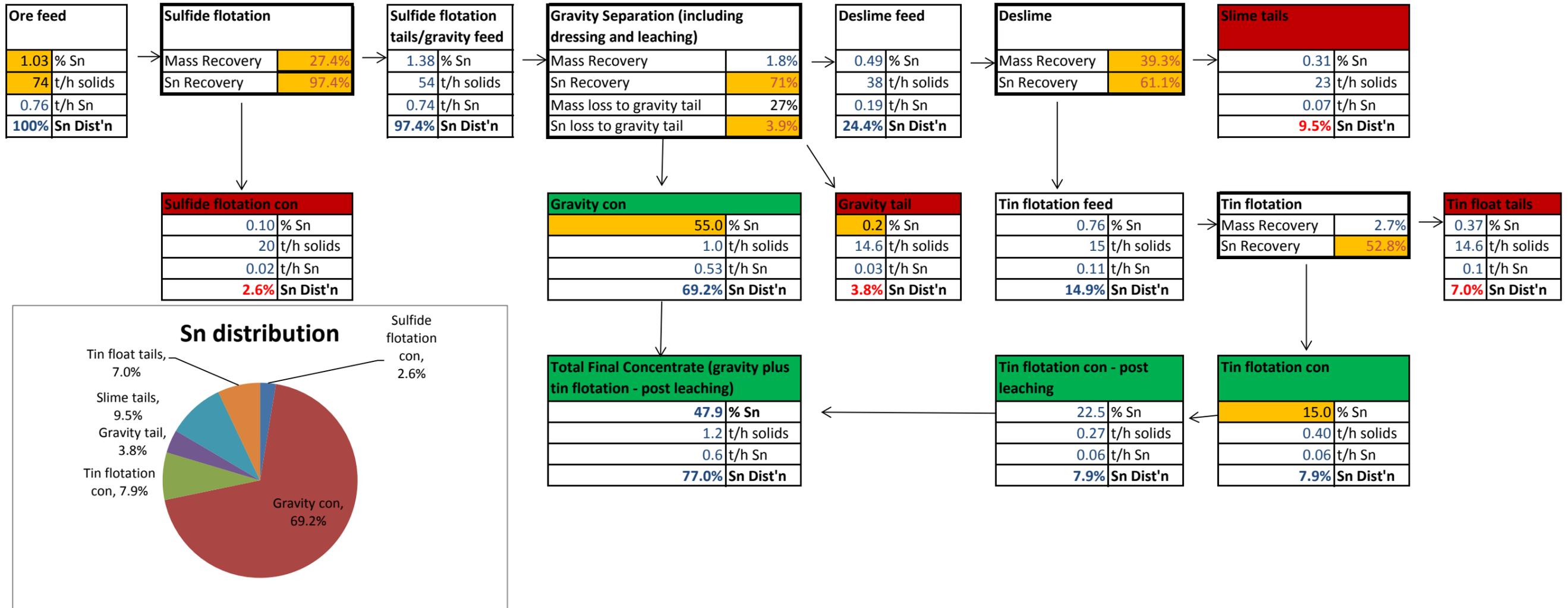
Demonstrated; 4 micron deslime (deslime test T70, tin float test T76) 15% Sn float con



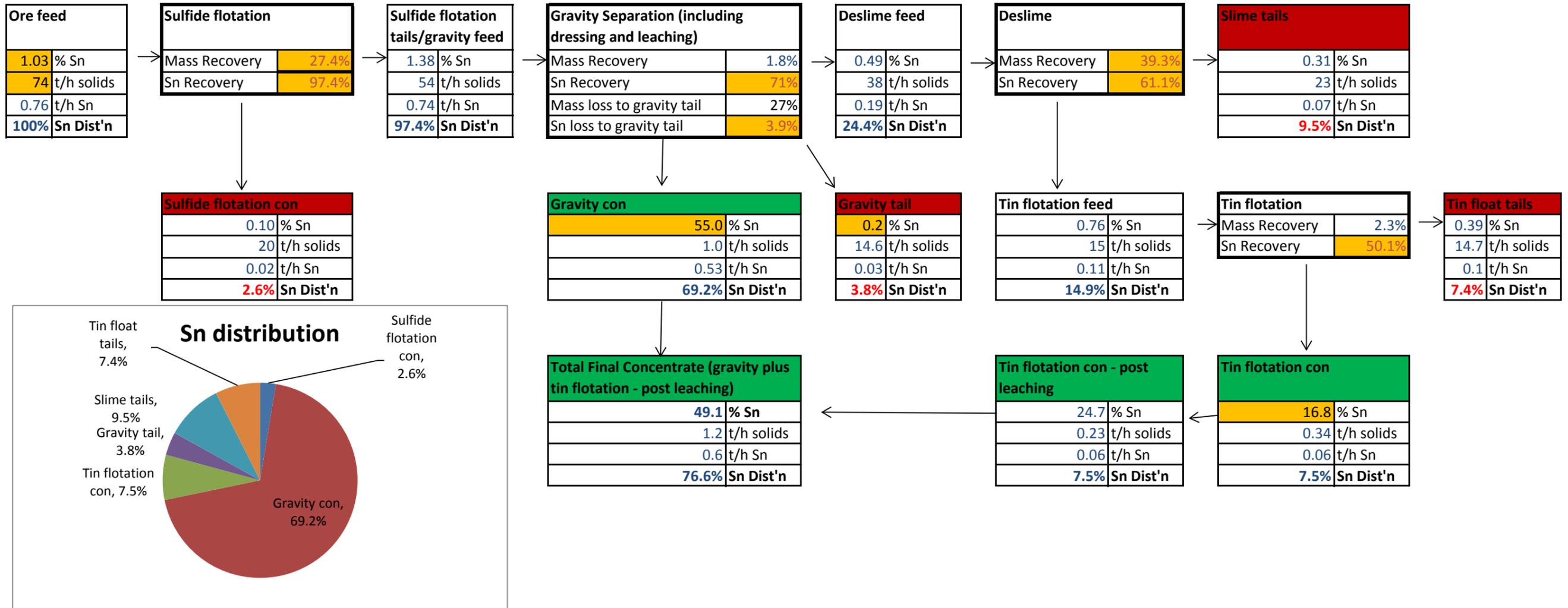
Demonstrated; 12 micron deslime (deslime test T56, tin float test T62)



Demonstrated; 12 micron deslime (deslime test T56, tin float test T62)



Demonstrated; 12 micron deslime (deslime test T56, tin float test T62)





WorleyParsons

resources & energy

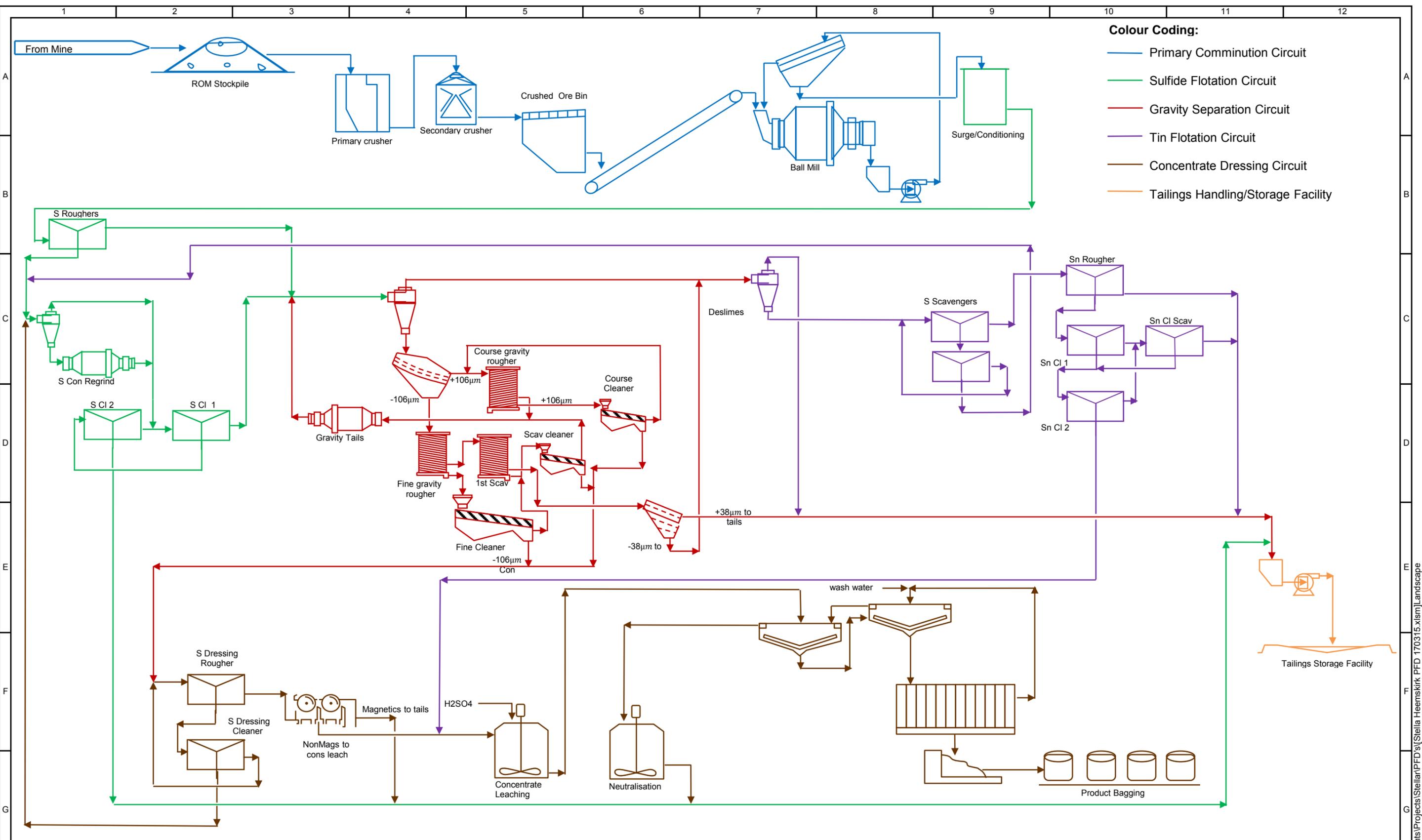
EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 15 – Proposed Process Flowsheet



	DRAWN: J. Resta DATE: 11/3/2015						 resources & energy		Heemskirk Tin Project Process Flowsheet																																						
	CHECKED: DATE:										SCALE		DRAWING NUMBER																																		
	ENGINEER: DATE:										REV		B																																		
	PROC ENG: DATE:																																														
DRAWING No.		TITLE		No.	DATE	DRAWN	CHECKED	APPROVED	DESCRIPTION	ENG	CLIENT																																				
					11-03-15	J. Resta			Heemskirk Tin Process Flowsheet																																						
					29-09-14	L.Bartsch																																									
<table border="1"> <thead> <tr> <th colspan="12">REVISIONS</th> </tr> <tr> <th>No.</th> <th>DATE</th> <th>DRAWN</th> <th>CHECKED</th> <th>APPROVED</th> <th>DESCRIPTION</th> <th>ENG</th> <th>CLIENT</th> <th>PROC ENG</th> <th>DATE</th> <th>SCALE</th> <th>DRAWING NUMBER</th> </tr> </thead> <tbody> <tr> <td> </td> </tr> </tbody> </table>												REVISIONS												No.	DATE	DRAWN	CHECKED	APPROVED	DESCRIPTION	ENG	CLIENT	PROC ENG	DATE	SCALE	DRAWING NUMBER												
REVISIONS																																															
No.	DATE	DRAWN	CHECKED	APPROVED	DESCRIPTION	ENG	CLIENT	PROC ENG	DATE	SCALE	DRAWING NUMBER																																				



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 16 – Testwork Scope of Work



WorleyParsons

resources & energy

Minerals & Metals

Level 12, 333 Collins Street

Melbourne VIC 3000

Australia

Telephone: +61 3 8676 3500

Facsimile: +61 3 8676 3505

www.worleyparsons.com

ABN 61 001 279 812

4 April 2014

Ref:

File:

John Glen, ALS Ammtec Burnie
39 River Road
Wivenhoe
Tasmania 7320

John

HEEMSKIRK TIN PROJECT – FURTHER FLOWSHEET DEVELOPMENT TESTWORK

WorleyParsons is currently assisting Stellar Resources with the ongoing development of the Heemskirk Tin project with a view to progressing this towards a Bankable Feasibility Study.

Significant additional flowsheet development and optimisation testwork is required, particularly with respect to tin flotation. The majority of this work is best undertaken for a single large composite “typical” of the major ore types. This will allow more robust testing to be undertaken (particularly in tin flotation).

Key aims of this work are;

- Achieve improved overall performance with respect to tin recovery to saleable concentrate grades
- Better define the optimum flowsheet, process design criteria and expected performance
- Demonstrate achievable overall tin recovery to saleable concentrate grades

Later work will focus on ore variability testing, and other work necessary to support the BFS.

We invite you to submit a proposal for the testwork detailed below. All purchase orders for the program will be raised by Stellar Resources.

1. GENERAL

1.1 Reporting

Progressive report of the results of the testwork program will be essential to timely completion of the study.

- All testwork results are to be reported, in spreadsheet format, on a progressive basis as results become available. These are to be reported to both WorleyParsons and Stellar Resources.
- A final data report will be required on completion of all testwork.



2. TESTWORK

Suggested nominal targets for various circuits are below;

- Sulfide flotation tails S grade: ~3-4%
- Sulfide flotation concentrate S grade: ~42% (~80% sulfide mineral)
- Gravity concentrate Sn grade: ~50% Sn post sulfide dressing, post leaching. Target grade should be reviewed based on outcomes of leach and NSR assessments.
- Tin flotation feed S grade: <~1.0-0.5%
- Tin flotation concentrate Sn grade: ~15% or better
- Final tin concentrate (post sulfide dressing, post leaching):
 - Sn grade ~45-50%, pending further analysis
 - S grade - around 2-3% S, preferably <0.5%

These will be reviewed as further work (both testwork and other assessments such as NSR and concentrate leach modelling) progress.

Whole of ore treatment will be considered as the base case for the majority of the flowsheet development work outlined in this program. HMS sinks + fines product is to be tested under the "optimised" downstream flowsheet/conditions developed for the whole of ore.

2.1 Samples

Severn bulk composite:

A "Severn bulk composite" sample is to be produced from ½ core from holes ZS-109, ZS-111, ZS-111W, ZS-112a, ZS-112b, ZS-112c, ZS-112d, ZS-112W, ZS-115, ZS-120, ZS-123 currently in storage. Refer "Met Intercepts (JR040314).xlsx" for details.

This will be used for the majority of the flowsheet development/optimisation work.

Variability composites:

¼ core from holes ZS-109, ZS-111, ZS-111W, ZS-112a, ZS-112b, ZS-112c, ZS-112d, ZS-112W, ZS-115, ZS-120, ZS-123 is currently in storage on site. This will be held in reserve to produce variability composites for testing of the "optimised" flowsheet.

2.1.1 Sample Characterisation

Characterisation work will be completed on the following samples;

- 'Severn bulk composite'
- Other variability composites (as applicable)

Characterisation work will consist of the following;

- Head assay
- Size by size assay
- Optical mineralogy – Fully and Sn scan
- QXRD



- Multi-element ICP scan
- SG determination
- Heavy liquid testing

2.2 Comminution

Bond rod mill and ball mill work indices should be determined for the following samples;

- 'Severn bulk composite'
- Other variability composites (as applicable)

2.3 Heavy Media Separation

Whole of ore treatment will be considered as the base case for the majority of the flowsheet development work outlined in this program.

- Heavy media testing (via DRS pilot rig) is to be completed on the "Severn bulk composite" to access achievable performance, and provide comparison with heavy liquid testing.
- Sufficient sinks + fines product should be produced from the "Severn bulk composite" to allow testing of the "optimised" downstream flowsheet.

2.3.1 Heavy liquid testing on previous composites

Heavy liquid testing should be completed on the following samples (if suitable rejects are available) to allow comparison with previous heavy media results;

- T0819 floats comp 4
- T0819 floats+sinks+fines
- T0714 comp 2 and 3

2.4 Sulfide Flotation

Sulfide flotation results utilising guar and adequate regrind to date are quite good.

Further work;

- Optimisation of both primary and regrind size/energy input over the ranges of;
 - Primary grind ~250 – 100 µm
 - Regrind ~75 – 30 µm
- Rougher rate tests to better quantify residence time requirements
- Lock cycle testing of 'optimised' sulfide flotation conditions
- Generation of sulfide flotation tailings under 'optimum' conditions for downstream testwork
 - Sulfide flotation work to produce sulfide flotation tailings for downstream work should ensure tailings at an appropriate S grade are produced



2.5 Gravity Separation

Further work needs to be completed on sulfide flotation tailings which are at an appropriate target sulfur grade (~3-4% S) following optimisation of sulfide flotation.

This must be aimed at producing target final con grades (both Sn and S) taking into account impacts of sulfide dressing and concentrate leach, and should aim to produce a range of grade recovery points to allow more thorough assessment of optimum grade target.

Further work;

- Lock cycle testing at various (say 3) grade recovery points (suggest adjusting table angle to achieve this?)
- Production of de-slime/tin flotation feed material
- Sulfide dressing flotation
 - Further work is required to better quantify achievable performance in terms of S rejection and Sn losses, and design criteria (particularly rate)
 - Investigate where in the circuit sulfide dressing flotation is best carried out. There may be some benefits in placing this further upstream; say following gravity roughing, or alternatively scavenging following sulfide flotation.
- Application of UF Falcon on
 - Fine gravity tails
 - Tin float feed
- Destination of fine gravity tails – The most appropriate destination, to either final tails or tin flotation feed, needs to be assessed
 - Comparative tin flotation tests under 'optimised' conditions should be completed with fine gravity tails included and excluded from tin flotation feed
 - For the purposes of generating tin flotation feed material fine gravity tails should be included in tin flotation feed.

2.6 Deslime and Tin Flotation

Deslime and tin flotation tests should be completed at larger scale than in previous work, to provide more robust results and allow cleaning stages in particular to be completed at more realistic pulp densities.

Areas for further testwork:

- De-slime cut point optimisation
 - De-slime testwork should be completed utilising the cyclone test rig
 - Suggested cut points; D50 ~7, ~10 and ~15 μm
 - Suggest tin float conditions as per T0797 test 4-6
- Tin flotation feed pre-treatment
 - Via WHIMS (utilising SLon)
 - Via UF Falcon



- WHIMS + UF Falcon
 - Suggest tin float conditions as per T0797 test 4-6
- Sulfide scavenger flotation optimisation
- Optimisation of mass pull in roughing – roughing tests should target maximum selectivity against Fe and SiO₂.
- Reagents for further investigation;
 - Acid, SSF, SPA (refer T0797 test 4-6)
 - Dispersants
 - Huntsman Polymax T10 (PEO)
 - Huntsman Polymax T12 (PEO)
 - Others??
 - NaSH
 - Oxalic acid (refer T0630 test 51 and 52)
 - Sodium silicate (refer T0630 test 26)

Initial tests investigating the above should be completed as roughing tests to allow appropriate mass pulls (maximising selectivity) for subsequent cleaning tests to be determined.

Lock cycle testing should be completed once conditions have been further optimised.

Other areas for further investigation;

- Application of UF Falcon within the tin flotation circuit –
 - this may have benefits in reducing losses to slimes - slimes scavenging
 - tin float concentrate cleaning
- Application of Wet High Intensity Magnetic Separation for rejection of siderite in cleaning circuit

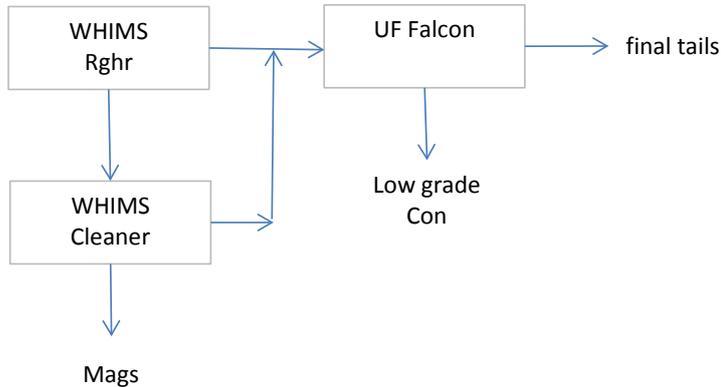
2.6.1 Cleaning of tin flotation concentrate by gravity means

Further upgrading of tin flotation concentrate by super panning showed considerable promise in T0630 test 28/29.

This should be investigated once tin flotation conditions have been further optimised, utilising either super panner or Mozley table.

2.7 WHIMS plus UF Falcon

Sighter WHIMS testwork has shown the potential to reject considerable siderite, and provide a moderate Sn upgrade into the non-mags product. In combination with UF Falcon (see below) with further optimisation they may be some potential to produce a low grade concentrate suitable for blended with the gravity concentrate as an alternative to tin flotation.



It is suggested a sighter test be completed to test this concept.

Suggested WHIMS conditions;

- Feed density; rghr ~25% solids, cleaner ~10% solids
- Field strength ~10,000 gauss

2.8 Concentrate Leaching

Concentrate leach tests are to be completed on selected samples; both gravity and tin flotation concentrates, and appropriate blends of these, generated from testwork.

Concentrate leach test conditions;

- Grind size; as is
- Mass solids; TBA
- Start Liquor volume ; TBA
- Start Liquor composition; 100 g/l H₂SO₄
- Acid addition; add concentrated acid to maintain pH 0.5 throughout tests
- Gas Sparging; none
- Temperature; 80°C
- Leach Time; 60, 120, 240, 360 minutes (majority of tests will be conducted for a single time of 4 hours only)

pH of tests should be monitored and maintained at 0.5 throughout, with all acid additions recorded.

2.8.1 Samples from previous testwork

The following samples generated from previous testwork are to be leached under the conditions above for a fixed time of 4 hours.

- T0797 test 4 flotation concentrates
- T0797 test 6 flotation concentrates
- T0819 test 13 flotation concentrates



- T0714 LC02 concentrates
- T0819 LC01 concentrate

2.9 Assays

2.9.1 Solids Analysis

- Feed solids and products produced from all tests should be analysed for; Sn, Fe, As, Mg, Ca, Mn, SiO₂, Al, S, CO₃ by XRF fusion/Leco
- All composite head samples should be analysed for; acid soluble Sn, SG, ICP multi-elemental scans
- Feed solids and products produced from all tests should be analysed for; QXRD, acid soluble Sn

2.9.2 Liquor analysis

- All liquor samples from concentrate leach tests should be analysed for; Fe(total), Mn, Mg, Al and Ca by AAS
- All leach liquor end samples should be analysed for; Sn, Fe²⁺, H₂SO₄ by titration in addition to the above

Please contact me if you have any questions on the proposed testwork.

Yours faithfully

J Resta

WorleyParsons



WorleyParsons

resources & energy

EcoNomics™

STELLAR RESOURCES LIMITED

HEEMSKIRK TIN PROJECT

SEVERN FURTHER FLOWSHEET DEVELOPMENT AND OPTIMISATION

Appendix 17 – ALS Metallurgy Report

(yet to be received at the time of writing)