

(b) Results

Test Product	Weight %	Assay % Sn	Distribution % Sn
Sulphide Cl Conc	9.008	0.35	11.23
+38 μm Superpanner Tin Conc	0.212	41.2	31.09
+38 μm Superpanner Tin Tail	0.802	6.30	18.00
(+38 μm Tin Ro Conc 1 to 10)	(1.014)	(13.6)	(49.09)
-38 +36.1 μm (C1) Tin Ro Conc	0.104	37.7	14.01
+26.8 μm (C2) Tin Ro Conc	0.103	12.0	4.41
+18.8 μm (C3) Tin Ro Conc	0.340	4.32	5.21
+12.4 μm (C4) Tin Ro Conc	1.086	1.03	3.98
+9.6 μm (C5) Tin Ro Conc	1.026	0.44	1.61
-9.6 μm (-C5) Tin Ro Conc	6.686	0.21	5.00
(-38 μm Tin Ro Conc 1 to 10)	(9.345)	(1.03)	(34.22)
(Tin Ro Conc 1 to 10)	(10.359)	(2.26)	(83.31)
Tin Ro Tail	80.633	0.019	5.46
Calc Head	100.00	0.28	100.00
Assay Head		0.29	

(c) Comments

- (i) Sulphide flotation cleaning did not improve rejection of cassiterite and consequently tin losses in sulphide concentrate product.
- (ii) For a grind size of 100% -150 μm , tin recovery in tin rougher concentrate appeared satisfactory with 50 min. of flotation time (10 stages) and 2.6 kg/t of collector PTAA (as compared to 30 min. and 1.6 kg/t of a finer grind 100% -75 μm in Test PC2/F8).
- (iii) A tin product of 13.6% Sn and containing 58.9% of the tin recovered in the tin rougher concentrate was obtained in the +38 μm fraction. A superpanner concentrate of 41.2% Sn at 63.3% recovery within the size fraction was produced.
- (iv) On the other hand, a tin product of 1.03% Sn containing 41.1% of the tin recovered in the tin rougher concentrate was obtained in the -38 μm fraction. A cyclosizing cone 1 product of 37.7% Sn at 40.9% recovery within the cyclosize fractions was produced and the result revealed that the tin enrichment took place in the coarsest fractions just below 38 μm .