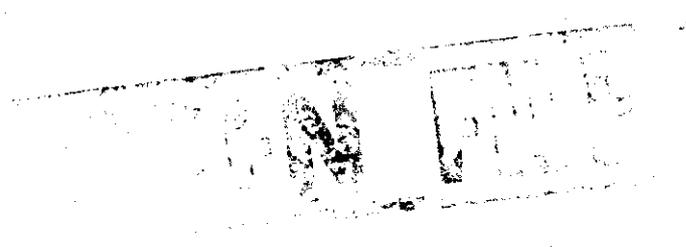


EL 43/70 ARTHUR RIVER

METALLURGICAL EVALUATION  
STUDIES.



86-2593



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1/Report 1001

WADI

KHD HUMBOLDT WEDAG AG

Cologne, July 25, 1985

IH-YM2 Wi/He -  
phone extension 658

KOVS ro

### Report

on

process engineering tests  
carried out with magnesite  
for Conzinc Riotinto Australia Ltd. (CRA),  
Melbourne/Australia

P.-No. 9-2121-5-0089

A.-No. 9-8125-9-5011

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P. DIR.	10 SEP 1986			FILE
	DEPT. OF MINES			
REF. No.				

#### 1. Summary

Following a very heedful reduction of the raw magnesite to a fineness of 100 % less than 0.12 mm, a magnesite concentrate of a MgO-content of 96 - 97 % and a SiO<sub>2</sub>-content of approx. 0.5 % (related to burnt magnesite) was produced by way of two-stage flotation at a concentrate recovery of more than 63.5 % .

**OPEN FILE**

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2. Material to be tested

On March 15, 1985 the research- and development center of KHD Humboldt Wedag AG received a magnesite sample of 300 kg from Messrs. Conzinc Riotinto Australia Ltd., Melbourne 3000, Australia.

The consignment included lump rock samples of a max. grain size of 400 mm.

3. Test objective

*Heck*

The test objective was to produce a magnesite concentrate of the following contents:

- MgO-content approx. 97 %
- SiO<sub>2</sub>-content less than 1 %
- Fe<sub>2</sub>O<sub>3</sub>-content less than 1 %.

All values are related to burnt magnesite. The ratio CaO - SiO<sub>2</sub> content was to be > 2.

The values below were reached by the customer during preliminary tests:

- MgO-content 97 %
- SiO<sub>2</sub>-content 0.5%
- CaO-content 1.4%
- Fe<sub>2</sub>O<sub>3</sub>-content 0.85 %

According to information by the customer, the MgO-recovery equalled 61 %.



#### 4. Test procedure and -results

After completion of a particle size analysis the overall sample was subjected to a reduction to a fineness of 100 % less than 31.5 mm. Subsequently, representative samples were extracted for the different tests.

##### 4.1 Raw material testing

##### 4.1.1 Chemical analysis

The wet-chemical analysis of a representative sample of the delivered magnesite yielded the following constituents:

MgO-content	43.81	%
SiO <sub>2</sub> -content	5.60	%
CaO-content	1.14	%
Fe <sub>2</sub> O <sub>3</sub> -content	0.51	%
Al <sub>2</sub> O <sub>3</sub> -content	0.05	%
loss on ignition	48.54	%

The following semi-quantitative analysis was made by means of X-ray emission analyzing:

element or oxide	contents*	
	portions % by weight (fraction)	
Na <sub>2</sub> O	not evidenced	
MgO	70	- 90
Al <sub>2</sub> O <sub>3</sub>	0.03	- 0.1
SiO <sub>2</sub>	3	- 7
P <sub>2</sub> O <sub>5</sub>	not evidenced	
SO <sub>3</sub>	0.03	- 0.07

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element or oxide	contents* portions % by weight (fraction)
Cl	traces
K <sub>2</sub> O	0.01 - 0.03
CaO	2 - 5
TiO <sub>2</sub>	0.005 - 0.02
Cr	0.01 - 0.03
Mn	0.05 - 0.2
Fe	0.8 - 1.5
Cu	0.05 - 0.2
Sr	traces
Ba	0.005 - 0.02
Zn	traces

\*contents related to burnt magnesite

#### 4.1.2 Moisture

By drying in a drying oven at  $106^{\circ}\text{C} \pm 2^{\circ}\text{C}$ , the moisture of the sample was determined at less than 0.1 %.

#### 4.1.3 Bulk density

The bulk density of a representative sample reduced by 100 % to a size less than 5.6 mm, equalled  $1.85 \text{ t/m}^3$ .



#### 4.1.4 Grain size distribution

The total delivered sample was subjected to dry sieving with three mesh widths and the coarse pieces were measured. The following grain size distribution resulted:

beyond	125	mm	72	%
	125 - 63	mm	23.5	%
	63 - 31.5	mm	3.2	%
less than	31.5	mm	1.3	%

The largest pieces had the following dimensions:  
400 x 200 x 110 mm, 350 x 300 x 290 mm and  
350 x 330 x 160 mm.

#### 4.1.5 Mineralogic testing

##### 4.1.5.1 X-ray powder diffraction method

The X-ray powder diffraction analysis of a representative sample of the raw material yielded the following minerals constituents:

1. magnesite                      main portion
2. dolomite                      secondary component
3. quartz                        low content
4. talcum                        very low content



#### 4.1.5.2 Microscopic investigation of thin- and polished sections of the raw material

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The following minerals of the stated fraction ranges were ascertained with the aid of microscopic investigations of thin- and polished sections:

mineral	fraction range	
	total mm	main portion mm
magnesite	approx. 0.005 - approx. 5	0.1 - 0.6
dolomite	0.01 - 0.65	> 0.05
quartz	0.005 - 0.5	< 0.2
goethite	0.01 - 0.3	> 0.1
talcum	0.05	finely grained
calcite	0.02 - 0.25	
mica	approx. 0.005 - 0.25	

The delivered raw material is a magnesite, being partly finely- and partly coarsely crystalline (enclosure 1), the main impurities of which are dolomite (enclosure 2) and quartz (enclosure 3). The dolomite occurs partly as veins (enclosure 4) and partly as fine (enclosure 5) and coarse inclusions in the magnesite structure. On the one hand it can be observed along the grain boundaries of the magnesite crystallites and on the other hand as inclusions in the crystallites. The actual dolomite for the predominant portion contains fine magnesite inclusions of a size from 0.005 mm to 0.1 mm.

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DEPOSIT

The quartz is present as binder between the magnesite crystallites (enclosure 6), but also as coarse inclusion in the magnesite (enclosure 7). It is partly idiomorphous and frequently includes - as infiltrated - fine and superfine inclusions of magnesite of a fraction range from 0.001 mm to 0.05 mm. To a minor degree, magnesite and quartz form an intimately intergrown, granular structure (enclosure 8), the maximum grain size of both minerals equalling 0.13 mm. This suggests two generations of mineralization, which likewise explains the idiomorphous formations of quartz and magnesite.

Moreover, quartz occurs as inclusions in the dolomite. Intergrowth, i.e. magnesite existing as binder between the particles in coarse quartz lots (enclosure 9), is observed to a minor degree only.

Goethite as pseudomorphosis of pyrite, is intergrown with magnesite and/or quartz. Talcum, for the major portion, occurs at the grain boundaries of the magnesite crystallites and as inclusions in the magnesite, although rarely only.

Calcite is present in the magnesite as inclusions and is frequently associated with dolomite. Also the coarser calcite inclusions mostly contain fine inclusions of magnesite (enclosure 12) (up to 0.030 mm, max.).

Mica could be observed exclusively as fine inclusions in the quartz.

The microscopic investigations suggest that grinding of 100 % less than approx. 0.12 mm would be suitable for processing the delivered raw magnesite. Due to the partly superfine intergrowth between quartz and magnesite and the fact that dolomite is the main gangue, it has to be presumed that a high magnesite recovery at a high MgO-concentration will hardly be realizable.

Idiomorphous  
- ic  
- Automorphous

An igneous rock mineral completely bounded by its characteristic crystal faces.

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#### 4.1.6 Specific gravity distribution of grain fractions

A representative sample of the raw material reduced to a fineness of 100 % less than 5.6 mm was subjected to wet classification at 0.5 mm. The wet residues retained were admitted to a tank filled with distilled water and transferred to a 0.1 mm sieve after 1 hour. Following a dripping-off period of 15 minutes, the material was immersed into an organic liquid of a tested specific gravity of 2.46 g/cm<sup>3</sup>, split into floats and sinks. The sinks were separated by sink-float tests directly afterwards at the next higher specific gravity. The specific gravity distribution of grain fractions obtained with chemical analyses of the specific gravity fractions can be taken from enclosure 13, showing that lowering of the SiO<sub>2</sub>-content is not possible for the grain size distribution selected by spec. gravity sizing.

#### 4.2 Flotation

The mineralogic test carried out with the raw magnesite as well as flotation tests revealed that comminution of 100 % less than approx. 0.125 mm is required for processing the magnesite.

##### 4.2.1 Grinding

Applied was a laboratory rod mill of a volumetric capacity of 5 litres. Eight rods made of V2A-steel of a diameter of 20 mm served as grinding media. The solids/water mass ratio equalled 1 : 1.

...



One kilogram, each, of the raw ore crushed by 100 % to a size less than 2 mm, was subjected to dry sieving at 0.12 mm and the residues retained on the sieve were ground for five minutes. Subsequently, the material ground was sieved wet at 0.12 mm, the residues retained were ground for five minutes. Following this, they were again subjected to wet classification and the remaining coarse fraction was again ground for three minutes. The grain size distribution of the total quantity of material ground is shown in the RRSB-grading graph in enclosure 14.

#### 4.2.2 Flotation tests

The flotation tests were carried out in a 3 l laboratory flotation cell, type WEDAG.

The solids content equalled 330 g/l, the tap water used had a hardness degree of 10° German hardness and the temperature of the pulp was 15°C.

SiO<sub>2</sub>-flotation as well as MgO-flotation were carried out fractionally, i.e. several products were separated by sink-float tests during each stage of flotation.

The advantage of this mode of flotation is that it enables a better evaluation of the different products and adding up of the different MgO-concentrates, depending on the SiO<sub>2</sub>- and CaO-content.

##### 4.2.2.1 Reagents

The following reagents were applied for flotation of the SiO<sub>2</sub>-impurities:

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EKOFAC T DD 95      200 g/t of ore      as well as  
RESANOL 450      120-150 g/t of ore      as  
collecting reagent/effervescing reagent  
combination.

The conditioning time for EKOFAC T DD 95 equals  
1 - 2 minutes and for RESANOL 450 approx. 5  
minutes.

Prior to the subsequent MgO-flotation, 200 g/ton of  
EKOFAC T DD 95 <sup>R</sup> and 400 - 500 g/ton of soda water-  
glass were added for deadening of calcite, dolomite  
and quartz.

Following a conditioning period of approx. 1 minute  
for these two reagents, the magnesite was separated  
in a sink- and float process with RESONAL A <sup>R</sup> (as  
10 % emulsion).

RESONAL A is a collecting-, effervescing reagent com-  
bination, specially developed for flotation of mag-  
nesite, which recovers magnesite highly selectively.

Since this reagent is emulsified very rapidly in the  
flotation pulp, special conditioning periods are not  
required.

MgO-product 1 and 2 = 300 g/ton of RESONAL A <sup>R</sup>  
MgO-product 3            = 200 g/ton of RESONAL A <sup>R</sup>

and, if required, for MgO-product 4 100 g/ton of  
RESONAL A <sup>R</sup>.



#### 4.2.2.2 Flotation period

As regards flotation of  $\text{SiO}_2$ , flotation periods between 8 and 10 minutes are required.

MgO-flotation requires approx. 5 minutes.

Including the reacting periods for  $\text{SiO}_2$ -flotation reagents and a sheer flotation period of approx. 8 minutes, 15 - 16 minutes shall be planned for the total silicic acid flotation. 1?

Including the reacting period required for the reagents for MgO-flotation and a flotation time of 5 minutes, a total of 7 minutes is necessary for MgO-flotation.

#### 4.2.2.3 Results

Apart from a number of flotation tests, which were evaluated only for the mass distributions and the  $\text{SiO}_2$ -contents, also the contents of MgO, CaO,  $\text{Fe}_2\text{O}_3$  as well as the losses on ignition of the different products were determined during tests 6139 and 6141.

The results are included in the enclosures, related on the one hand to non-ignited magnesite and on the other hand to burnt magnesite. They show that - at a recovery of 63 - 65 % - a concentrate was produced, being characterized as follows:

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test		6139	6141
concentrate recovery	%	63.83	65.30
contents (non-ignited)			
MgO	%	46.74	46.58
SiO <sub>2</sub>	%	0.27	0.23
CaO	%	0.59	0.62
Fe <sub>2</sub> O <sub>3</sub>	%	0.46	0.47
contents (ignited)			
MgO	%	96.65	95.76
SiO <sub>2</sub>	%	0.56	0.47
CaO	%	1.22	1.27
Fe <sub>2</sub> O <sub>3</sub>	%	0.96	0.97
		99.39	98.47

The MgO-recovery in the concentrate during the tests approx. amounted to 70 % (68.42 % non-ignited during test 6139, 71.30 % related to burnt magnesite). However, this value cannot unrestrictedly serve as a basis for characterizing the success of classifying, since magnesium oxide is not only included in valuable mineral magnesite, but also in the tailings dolomite.

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4.3 Sedimentation

4.3.1 SiO<sub>2</sub>-product

After a sedimentation period of 15 minutes, thickening of 400 g/l (575 g/l) in the feed to only 500 g/l (600 g/l) could be achieved without addition of flocculants during the sedimentation tests with the froth product from SiO<sub>2</sub>-flotation at a slightly turbid excess.

The sedimentation behaviour substantially improved only after addition of 15 g/m<sup>3</sup> of flocculant Praestol 2900/75 (enclosure 19, refer).

At an initial concentration of 400 g of solids in 1 l pulp, a clear water phase of 184 mm was obtained after 15 minutes. After this sedimentation period, the thickening degree equalled 878 g/l.

4.3.2 MgO-concentrate

No auxiliary sedimentation agents are required for thickening the magnesite concentrate, i.e. the froth from MgO-flotation. At an initial concentration of 530 g/l and 740 g/l, respectively, a solids content in the sedimented material of 1100 g/l and 1060 g/l, resp., were reached after a sedimentation period of 15 minutes (see enclosure 20).

At the low specific gravity of the feed pulp, a clear water phase of 180 mm was formed, of which 10 - 20 mm existed as froth, after the period mentioned above.

During all sedimentation tests carried out with the magnesite concentrate, a stable froth layer of a thickness of 10 - 50 mm, in exceptional cases up to 100 mm, was formed at the upper part of the clear water phase.

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#### 4.3.3 Tailings

As regards the residues from MgO-flotation, a small addition of auxiliary sedimentation agents is required, since no phase separation could be determined for the sedimentation tests in the vertical cylinder without addition of flocculants. After addition of 2.5 g/m<sup>3</sup> of Praestol 2900/74, a slightly turbid water phase of 327 mm (see enclosure 21) was formed within five minutes. At a solids content of the feed of 72.5 g/l, the final thickening degree equalled approx. 1100 g/l. A higher addition of flocculants did not improve the results.

#### 4.4 Filtering tests

The magnesite concentrate from the flotation tests was examined for its filtering capacity with the aid of a vertical suction filter. The filtering surface of this suction filter (0.01 m<sup>2</sup>) was covered with tissue M/PP 2425. Pulp of a solids content of 550 g/l and 1400 g/l, respectively, served as feed material. The results can be taken from the table included in enclosure 22. At the low specific gravity of the feed pulp, a residual moisture of 7.3 % was reached at a theoretic throughput of 730 kg/(hm<sup>2</sup>). With the thickened slime (1400 g/l), the calculated feed rate could be raised to 2  $\sqrt{}$ (hm<sup>2</sup>) at a residual moisture equalling 10 %.

The tests were carried out by us to the best of our knowledge and ability. A liability, in particular for the process engineering results of machines, plant sections or plants delivered by us can be undertaken by us only, if this has been agreed upon in writing.

KHD Humboldt Wedag AG

*[Handwritten signature]*  
 i.V. Dr. Kellerwessel i.V. Dr. Imhof  
Encl.

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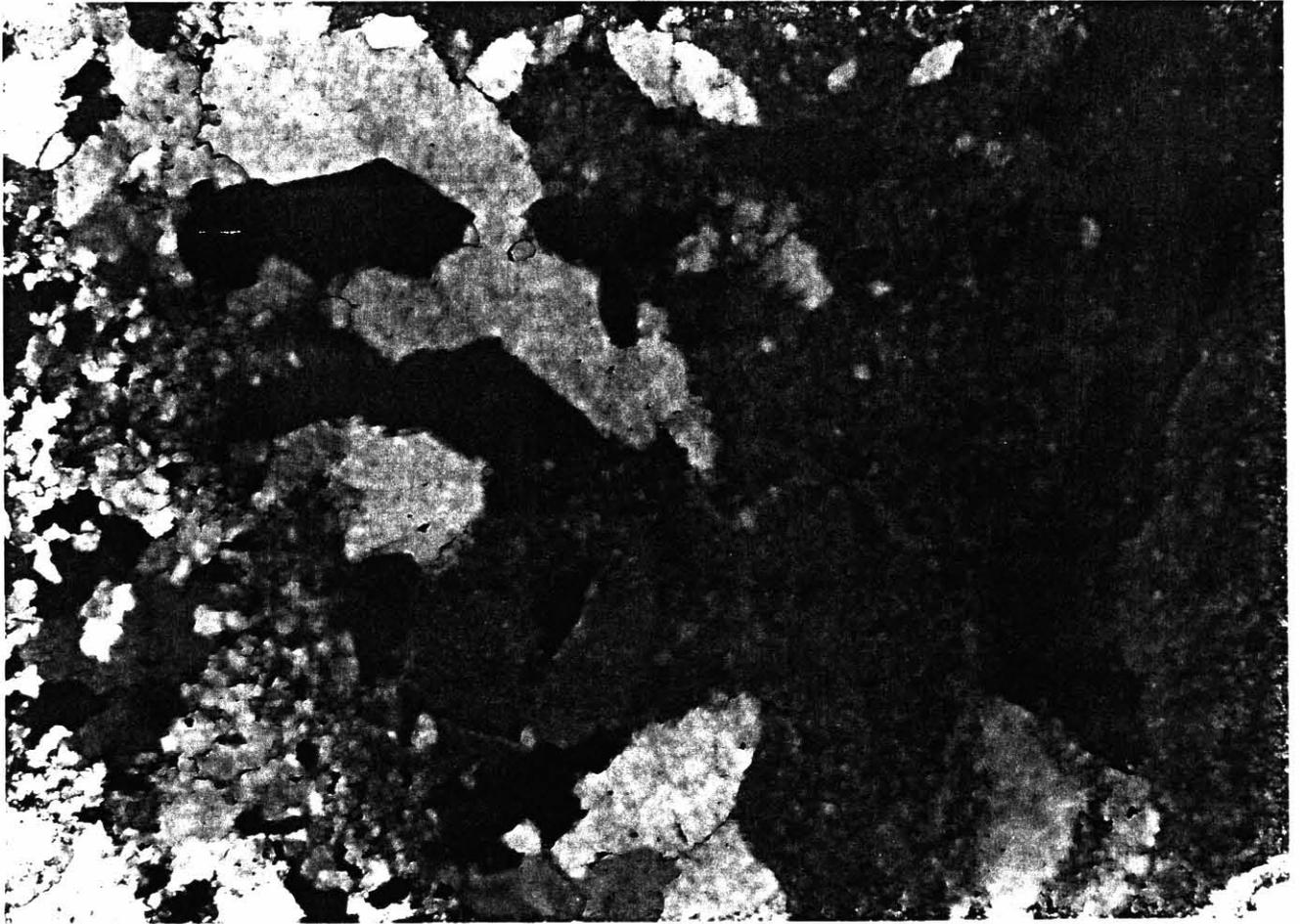


**KHD HUMBOLDT WEDAG AG**

Enclosure

- 1            Microphotograph no. 1
- 2            "                    "        2
- 3            "                    "        3
- 4            "                    "        4
- 5            "                    "        5
- 6            "                    "        6
- 7            "                    "        7
- 8            "                    "        8
- 9            "                    "        9
- 10           "                    "       10
- 11           "                    "       11
- 12           "                    "       12
- 13           Sink-Float-Analysis
- 14           Grading graph - feed -
- 15           Balanceflotation test 6139
- 16           "                    "       "        (dead burned basis)
- 17           "                    "       6141
- 18           "                    "       "        (dead burned basis)
- 19           Settling curve SiO<sub>2</sub>-product
- 20           "                    "       MgO-concentrate
- 21           "                    "       tailings
- 22           List of filtration tests MgO-concentrate

Enclosure 1



Microphotograph no. 1

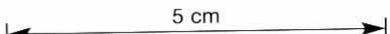
thin

 200  $\mu$ m  
section, N+

magnification - microscope 67 x )  
 enlargement - photograph 1.6x ) 107 x

Sample: Magnesite from Messrs. C.R.A., Australia

Magnesite (coloured), partly coarse-, partly fine-crystalline  
 exist next to each other. The fine-crystalline magnesite  
 (right-hand side of microphotograph) includes minute  
 quartz veins (light grey, dark grey to black).

 5 cm

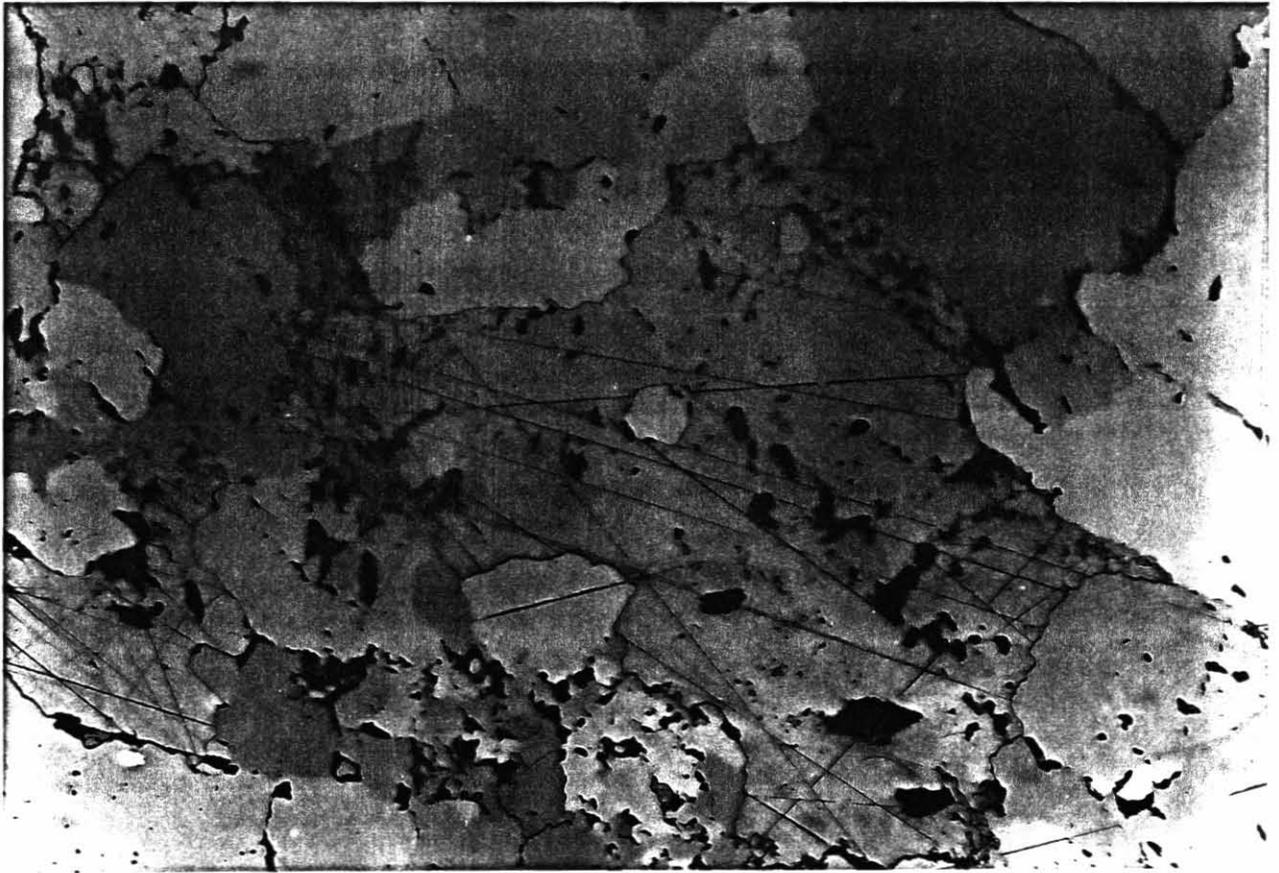
016

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John Dunbar

Enclosure 2



Microphotograph no. 2

polished section, etched with  
Al(NO<sub>3</sub>)<sub>3</sub>

magnification - microscope 100 x )  
enlargement - photograph 1.6 x ) 160 x

Sample: Magnesite from Messrs. C.R.A., Australia

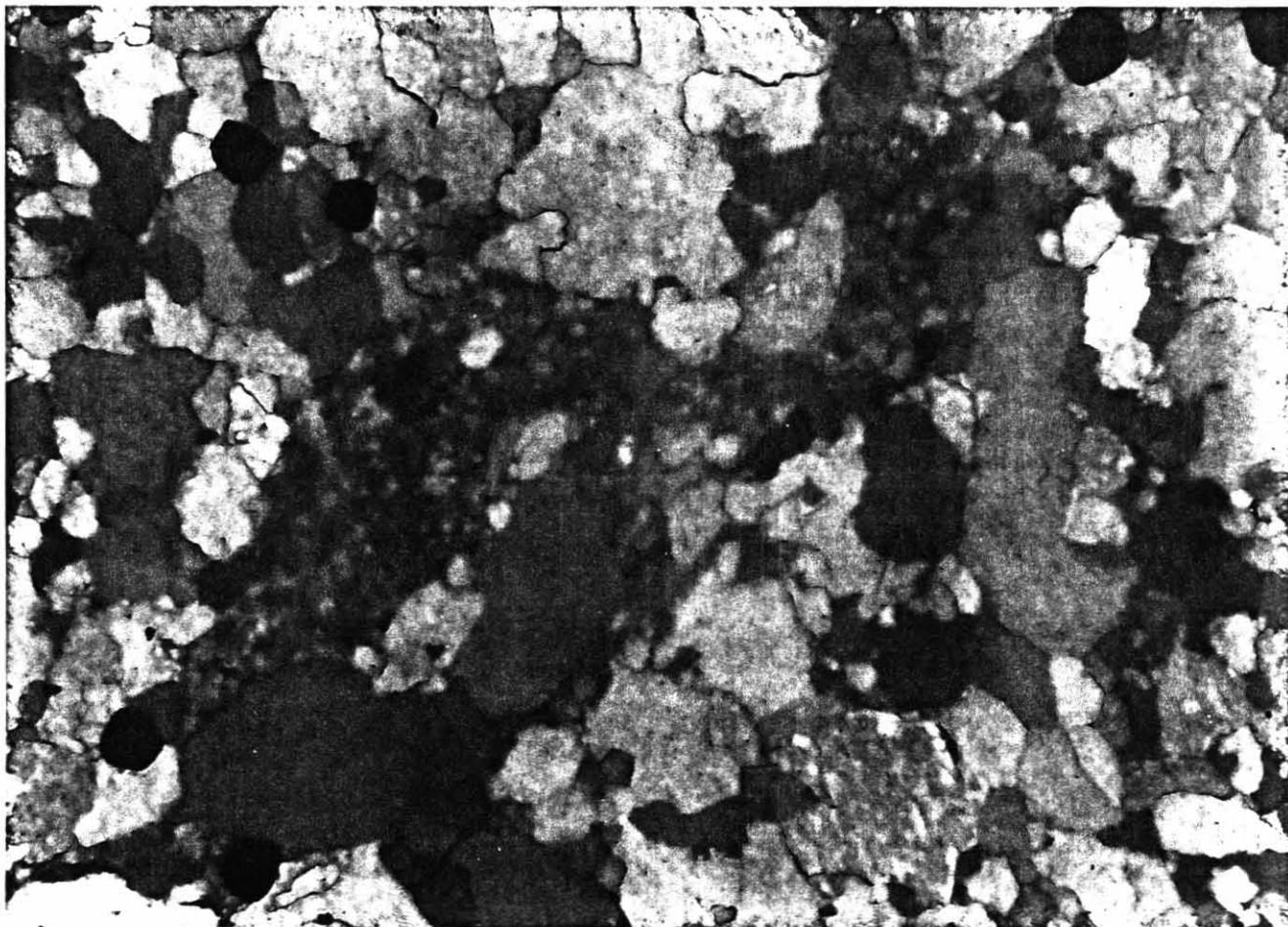
Coarser inclusions of dolomite (grey, etched; grinding scratches visible) in magnesite (grey, smooth).

The dolomite shows fine inclusions of magnesite.

Pores and cavities are black.

5 cm

## Enclosure 3



Microphotograph no. 3 thin section, N+  
 magnification - microscope 67 x )  
 enlargement - photograph 1.6x ) 107 x

Sample: Magnesite from Messrs. C.R.A., Australia

Outline microphotograph, magnesite structure (coloured, coarser crystalline) with inclusions of quartz (blue, red purple, yellow-brown) and goethite (black).

5 cm

018

Enclosure 4



Microphotograph no. 4

————— 0,1 mm  
 polished section, etched  
 with  $\text{Al}(\text{NO}_3)_3$

magnification - microscope 100 x ) 160 x  
 enlargement - photograph 1.6 x

Sample: Magnesite from Messrs. C.R.A., Australia

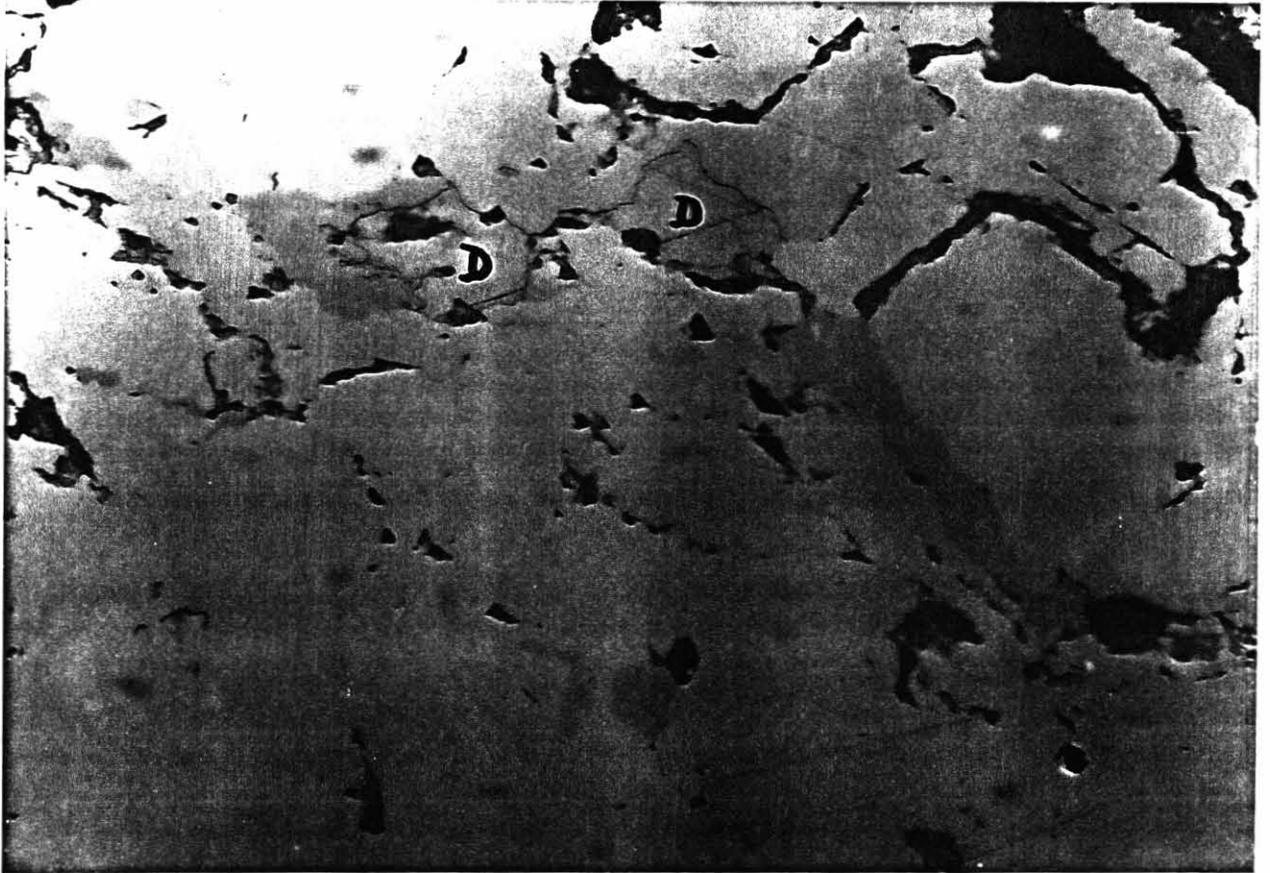
Dolomite vein (dark grey, etched; grinding scratches visible)  
 with coarser inclusions of magnesite (medium grey, smooth).

Pores and cavities are black.

————— 5 cm —————

019

Enclosure 5



Microphotograph no. 5

0,1 mm  
 polished section, etched  
 with  $\text{Al}(\text{NO}_3)_3$

magnification - microscope 200 x ) 320 x  
 enlargement - photograph 1.6 x )

Sample: magnesite from Messrs. C.R.A., Australia

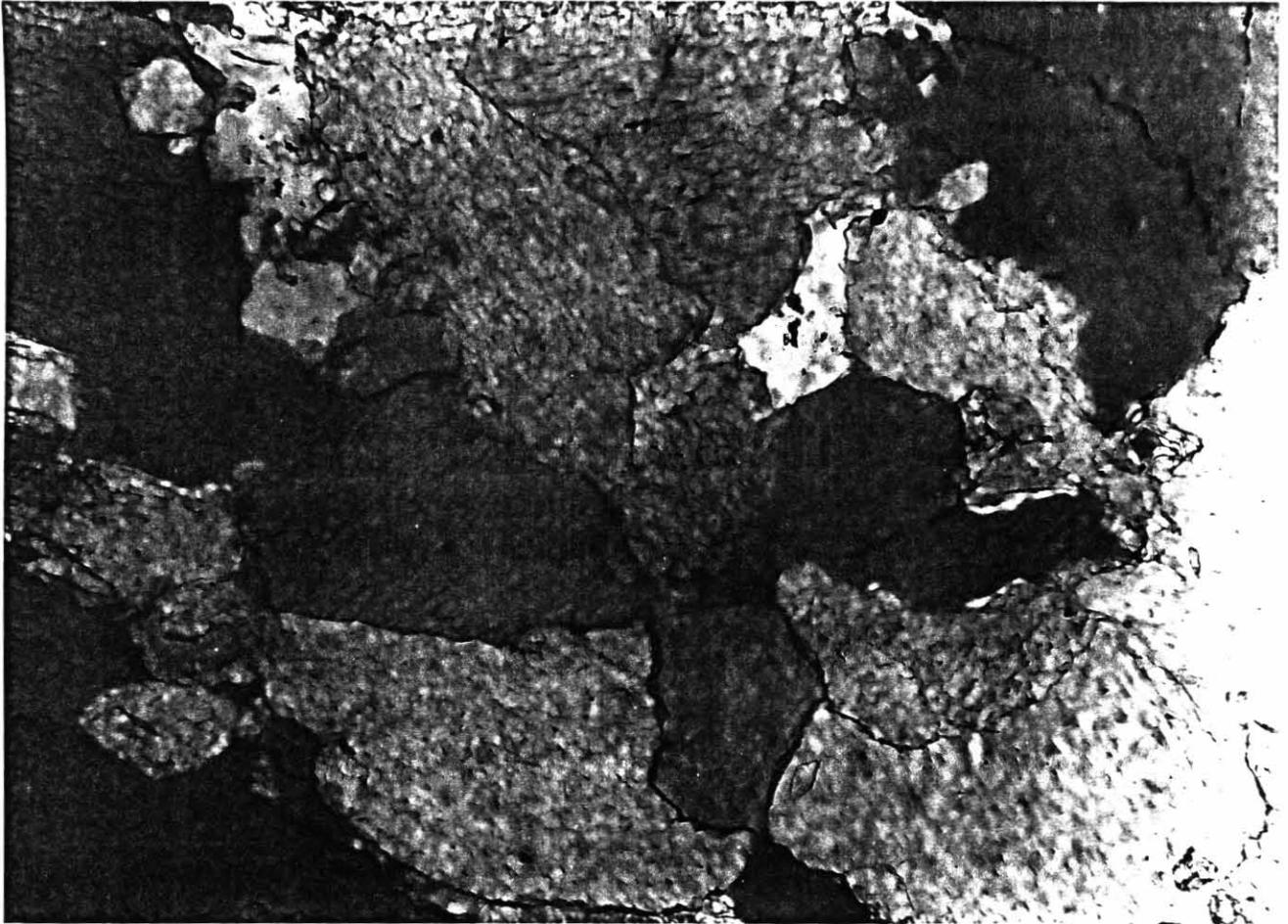
Fine inclusions of dolomite (grey, D) in magnesite (grey, smooth).

Pores and cavities are black.

5 cm

020

Enclosure 6



Microphotograph no. 6

thin

0,1 mm  
section, N+

magnification - microscope 160 x )  
 enlargement - photograph 1.6 x ) 256 x

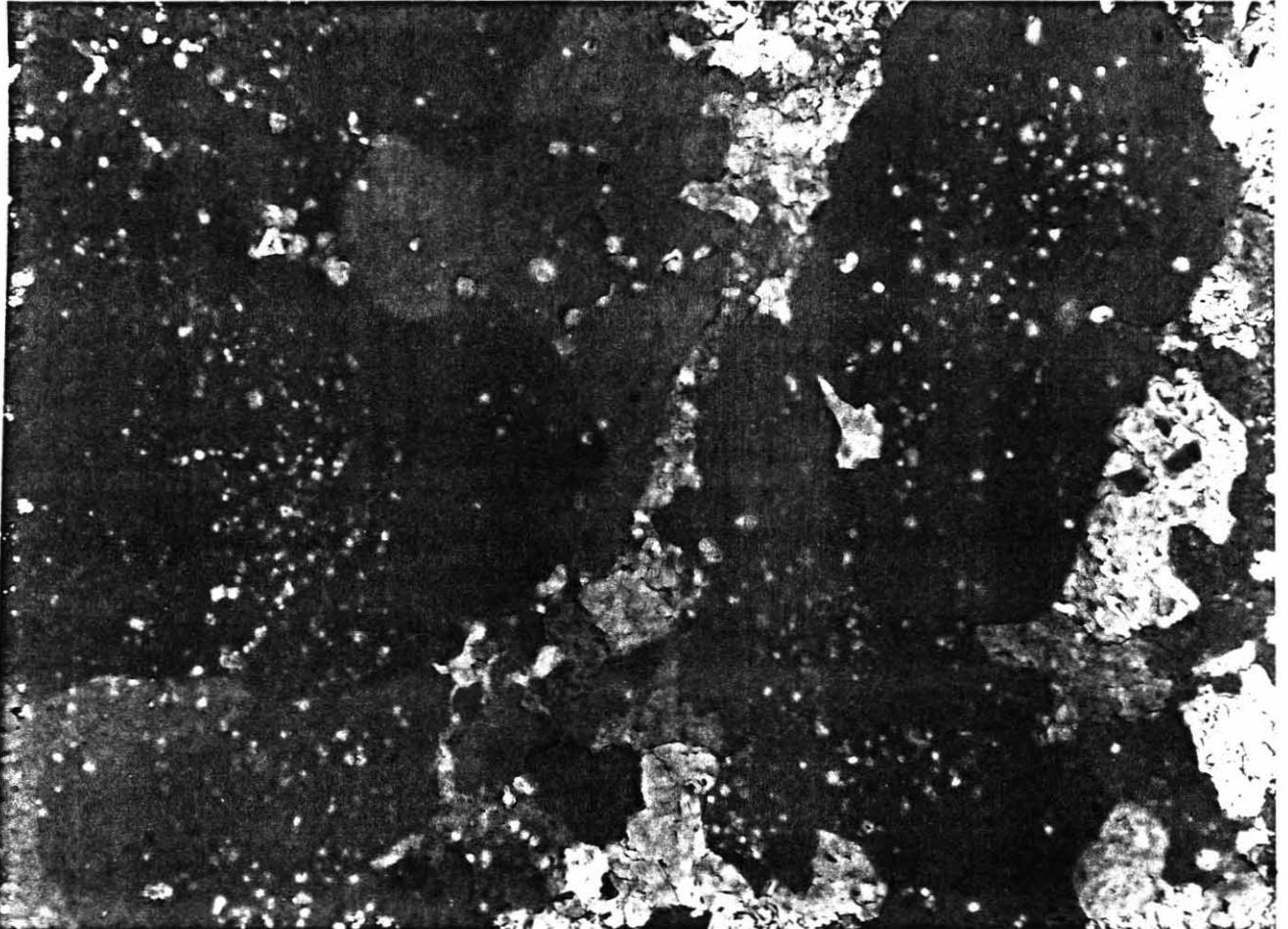
Sample: magnesite from Messrs. C.R.A., Australia

Quartz (blue, light blue, yellow, red purple) partly displaying minute inclusions of magnesite (yellow to yellowish-green) as binder between the various magnesite crystallites (blue-purple, grey-green and grey-pink).

5 cm

021

Enclosure 7



Microphotograph no. 7

————— 0,1mm  
 thin section,  
 N +

Magnification - microscope 160 x )  
 enlargement - photograph 1.6 x ) 256 x

Sample: magnesite from Messrs. C.R.A., Australia

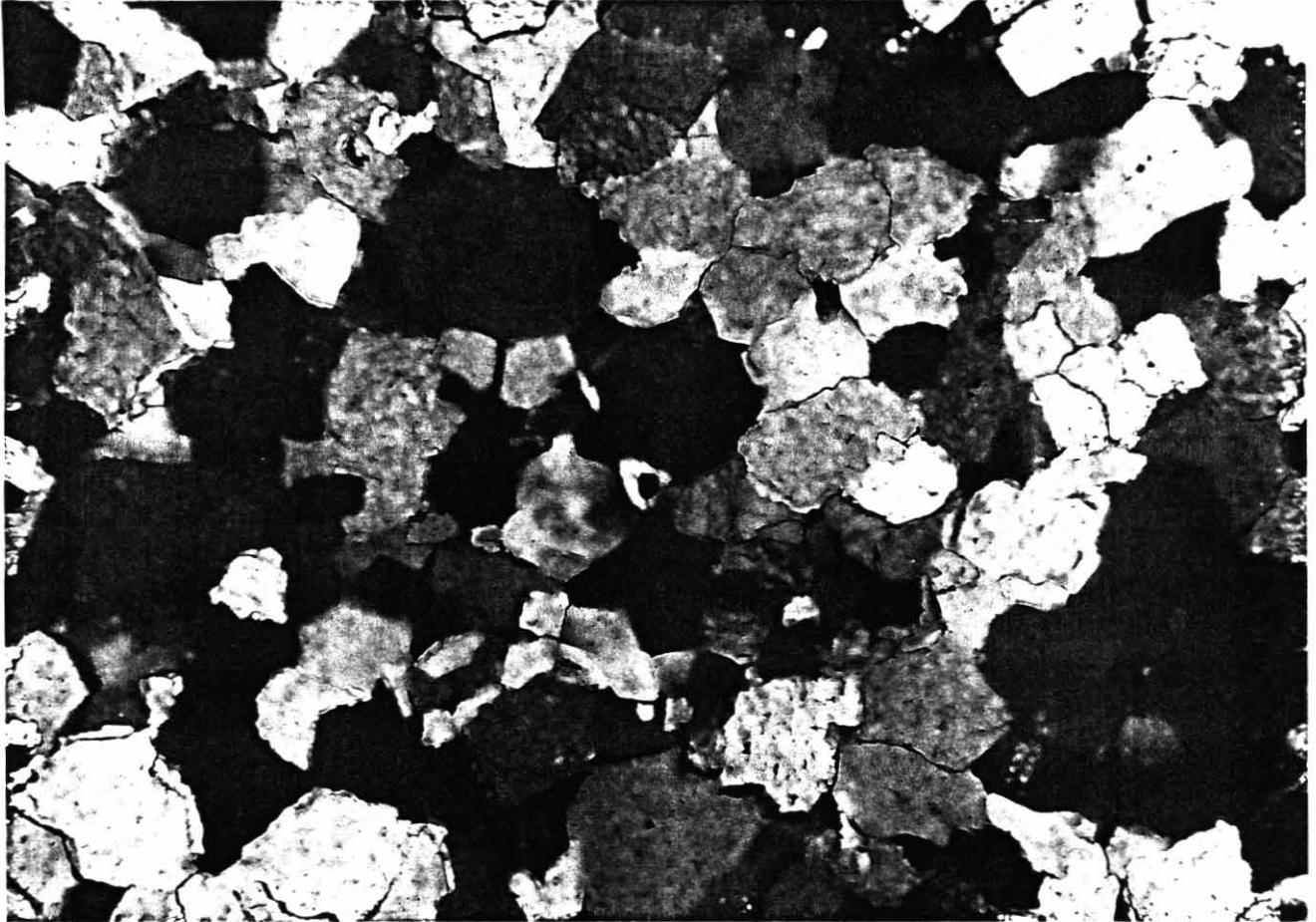
Quartz (orange-red, blue, red-purple, blue-purple),  
 partly idiomorphic texture with fine and superfine  
 inclusions of magnesite.

————— 5 cm —————

022

988024

Enclosure 8



0,1 mm  
thin section, N+

Microphotograph no. 8

magnification - microscope 160 x )  
enlargement - photograph 1.6 x ) 256 x

Sample: magnesite from Messrs. C.R.A., Australia

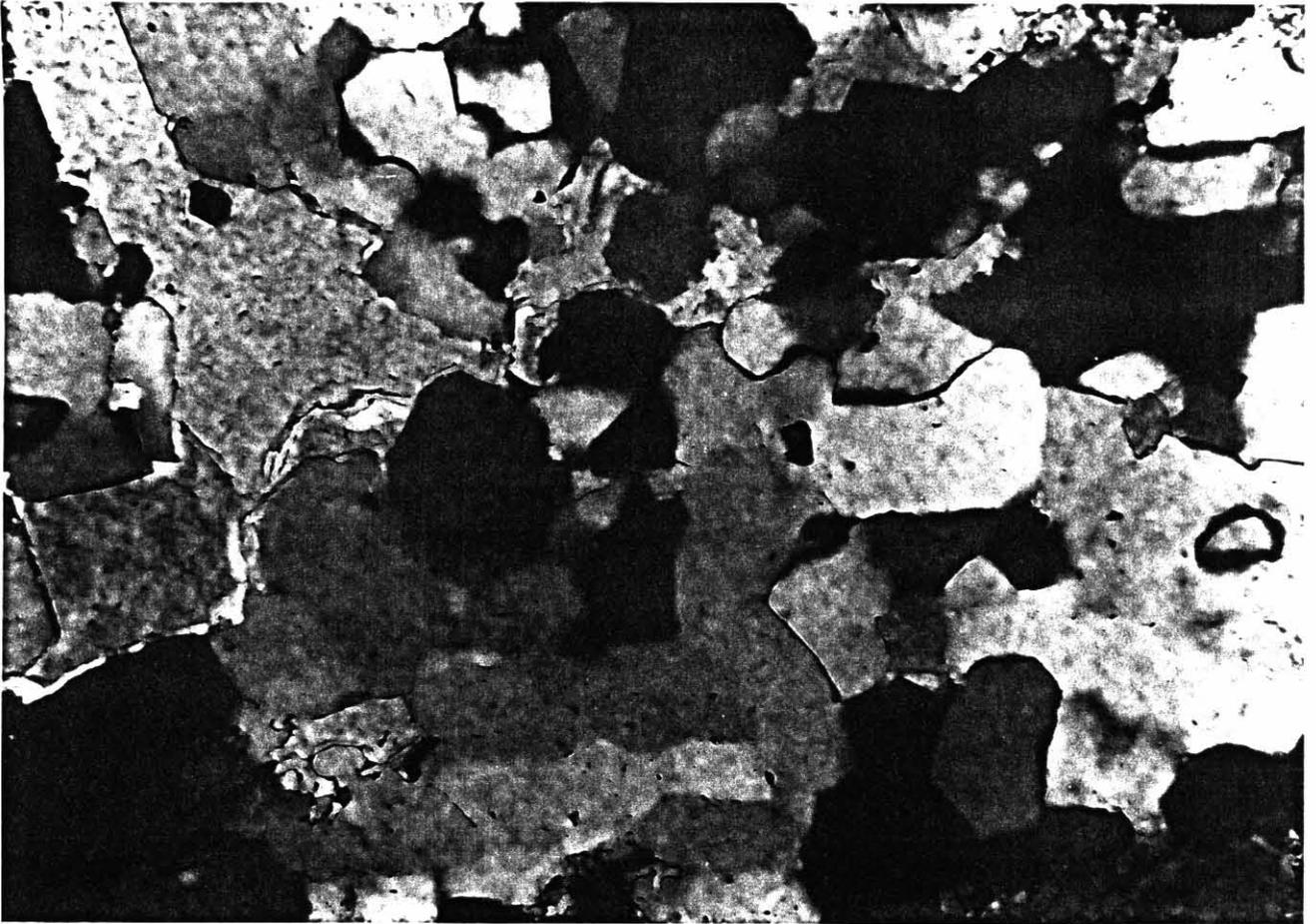
Intimate intergrowth between magnesite (coloured) and quartz (blue grey to black). The grainy structure of this batch is clearly displayed.

5 cm

023

988025

Enclosure 9



0,1mm

Microphotograph no. 9

thin

section, N+

Magnification - microscope 160 x )  
enlargement - photograph 1.6 x ) 256 x

Sample: magnesite from Messrs. C.R.A., Australia

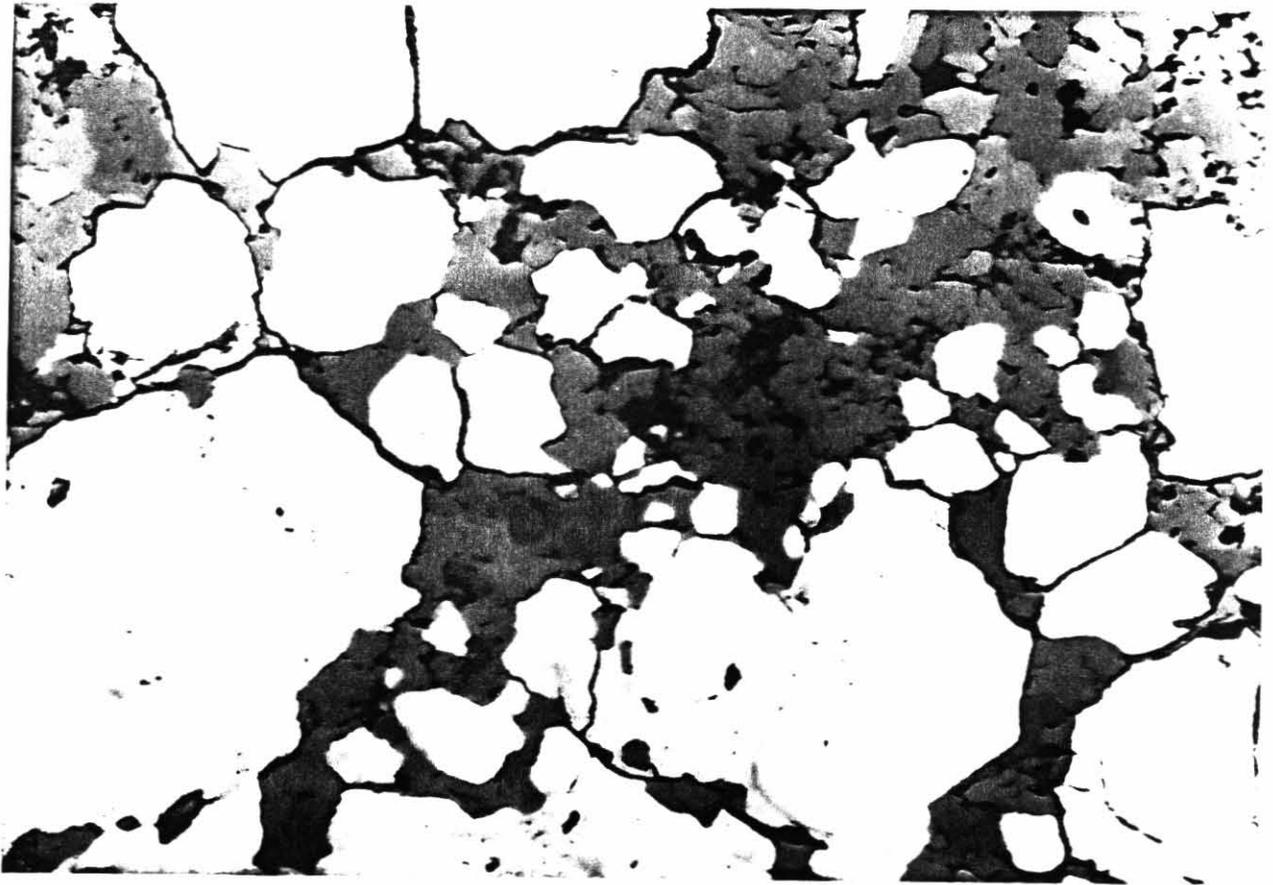
Magnesite (coloured) occurs as binder in quartz (light to dark grey and black). The sample displays occasional fine inclusions of quartz (black).

5 cm

024

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Enclosure 10



Microphotograph no. 10

0.1 mm  
polished section, etched  
with  $\text{Al}(\text{NO}_3)_3$

Magnification - microscope 100 x )  
enlargement - photograph 1.6 x ) 160 x

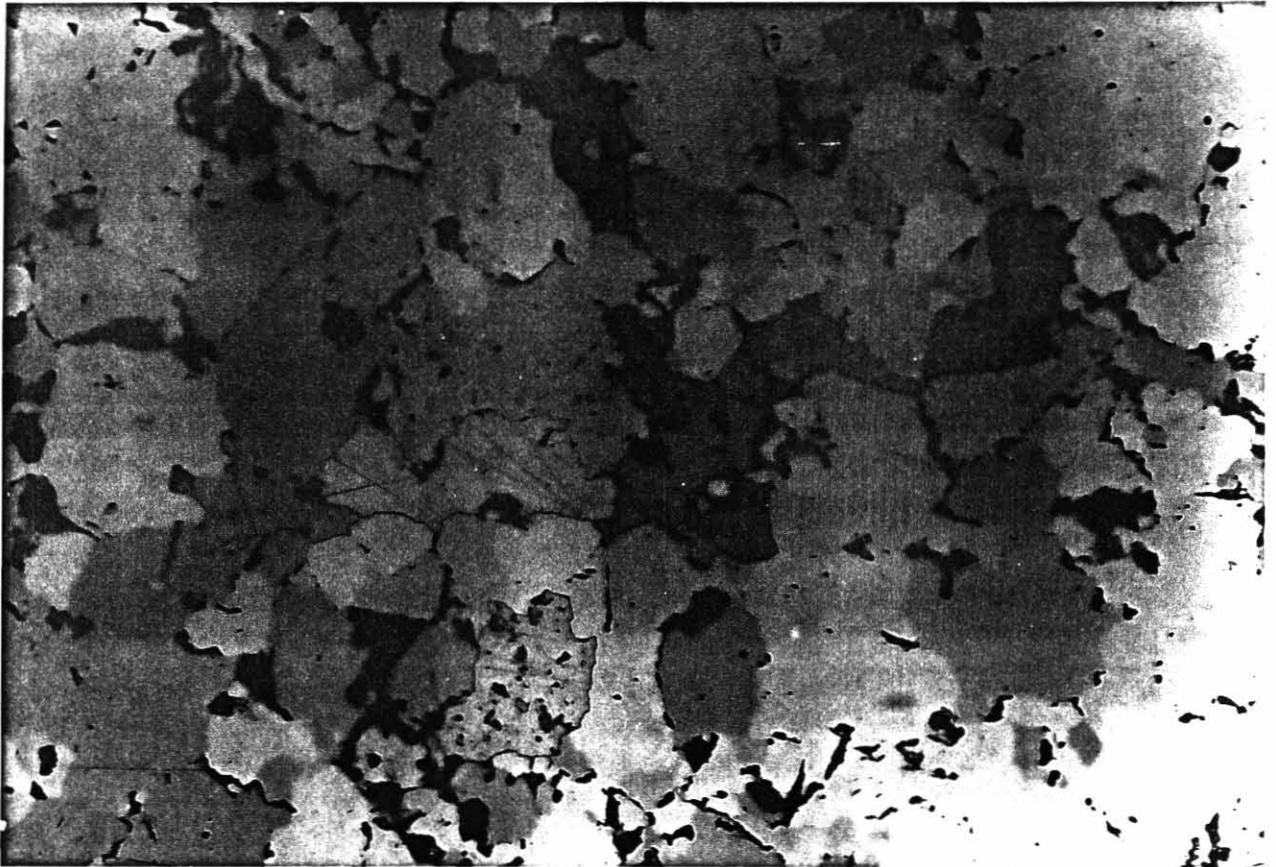
Sample: Magnesite from Messrs. C.R.A., Australia

Clusters of goethite (light grey) in magnesite (grey).

Pores and cavities are black.

5 cm

## Enclosure 11



————— 0,1 mm

Microphotograph no. 11

polished section, etched  
with  $\text{Al}(\text{NO}_3)_3$

Magnification - microscope 100 x )  
enlargement - photograph 1.6 x ) 160 x

Sample: magnesite from Messrs. C.R.A., Australia

Dolomite (grey, etched, displaying grinding scratches)  
and calcite (dark grey, etched, rough) occurring as  
fine inclusions in magnesite (light- to medium grey,  
smooth).

Pores and cavities are black.

————— 5 cm —————



Microphotograph no. 12

————— 0,1 mm  
polished section, etched  
with  $\text{Al}(\text{NO}_3)_3$

Magnification - microscope 100 x )  
enlargement - photograph 1.6 x ) 160 x

Sample: magnesite from Messrs. C.R.A., Australia

Fairly coarse calcite (dark grey, rough) occurring in addition to dolomite (grey, showing grinding scratches) as inclusion in the magnesite (light to medium grey, smooth). The calcite contains minute magnesite inclusions.

Pores and cavities are black.

————— 5 cm —————

027

SINK - FLOAT - ANALYSIS

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enclosure: 13  
 date: 06.05.1985  
 A.-Nr.: 9-8125-9-5011

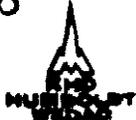
client: CRA Ltd. / Australia  
 material: Magnesite  
 grain size: 5.6 - 0.5 mm

density Kg/L	weight %	recovery add.%	I	MgO				I	CaO				I	SiO2				I
				grade %	recovery %	content add.%	content %		grade %	recovery %	content add.%	content %		grade %	recovery %	content add.%	content %	
-2.46	13.34	13.34	I	43.32	13.16	13.16	5.7789	I	1.15	15.06	15.06	.15341	I	6.87	15.70	15.70	.916458	I
2.46-2.54	2.88	16.22	I	43.18	2.83	16.00	1.2436	I	1.07	3.03	18.09	.030816	I	7.70	3.80	19.50	.22176	I
2.54-2.63	2.29	18.51	I	42.91	2.24	18.24	.9826	I	1.17	2.63	20.72	.026793	I	8.11	3.18	22.68	.185719	I
2.63-2.73	6.46	24.97	I	42.02	6.18	24.42	2.7145	I	1.30	8.25	28.97	.08398	I	9.77	10.81	33.49	.631142	I
2.73-2.77	10.43	35.40	I	42.88	10.19	34.61	4.4724	I	1.46	14.95	43.92	.152278	I	8.11	14.49	47.98	.845873	I
2.77-2.83	23.50	58.90	I	43.69	23.39	58.00	10.2672	I	.93	21.46	65.38	.21855	I	5.95	23.95	71.94	1.39825	I
2.83-2.88	5.67	64.57	I	44.69	5.77	63.77	2.5339	I	.79	4.40	69.78	.044793	I	4.57	4.44	76.38	.259119	I
+2.88	13.69	78.26	I	45.80	14.28	78.05	6.2700	I	.39	5.24	75.02	.053391	I	3.07	7.20	83.58	.420283	I
- 0.5 mm	21.74	100.00	I	44.31	21.95	100.00	9.6330	I	1.17	24.98	100.00	.254358	I	4.41	16.42	100.00	.958734	I
Summe:	100.00	---	I	43.81	100.00	---	43.8961	I	1.14	100.00	---	1.01837	I	5.60	100.00	---	5.83734	I

+  
0.5  
mm

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028



Körnungsnetz / Grading graph  
Diagramme granulométrique

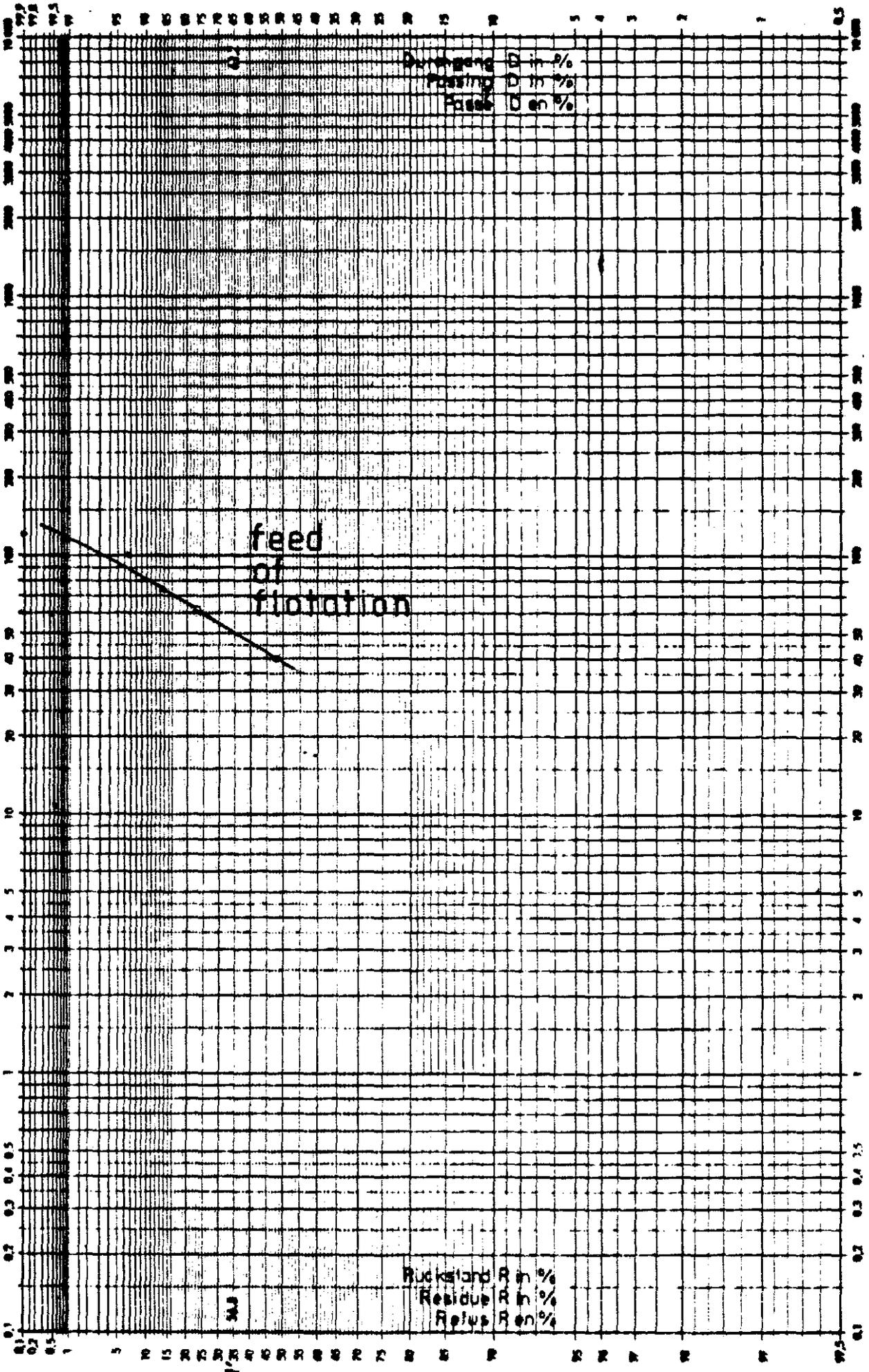
Enclosure: 14  
Datum: 25.7.85  
Date: 25.7.85

Machine: Rad mill  
Appareil: Rad mill

Firma: CRA  
Customer: CRA  
Client: CRA

Stoff: Magnesite  
Material: Magnesite  
Produit: Magnesite

Korngröße d in µm (mm) / Grain size d in µm (mm) / Dimension des grains d en µm (mm)



Übergang D in %  
Passing D in %  
Fasse D en %

Rückstand R in %  
Residue R in %  
Retus R en %

feed  
of  
flotation

BALANCE

Test 6139

029

enclosure : 15  
 date: 25.05.1985  
 A. - Nr.: 9-8125-9-5011

client: CRA Ltd. / Australia  
 material: magnesite discharge of the rod mill  
 84 % - 0.075 mm, 52 % - 0.040 mm  
 procedure: flotation test 6139  
 Humboldt Wedag 3 l - flotation cell

product	weight recovery I				MgO				CaO				SiO2						
	%	add.%	I	I	grade	recovery	content	I	grade	recovery	content	I	grade	recovery	content	I			
SiO2-product 1	7.95	7.95	I	I	28.69	5.23	5.23	2.2809	I	.61	4.35	4.35	.0485	I	38.70	53.23	53.23	3.0767	I
SiO2-product 2	17.13	25.08	I	I	39.71	15.60	20.83	6.8023	I	.71	10.91	15.26	.1216	I	14.43	42.76	95.99	2.4719	I
MgO-product 1	9.19	34.27	I	I	46.25	9.75	30.58	4.2504	I	.74	6.10	21.36	.0680	I	1.06	1.69	97.68	.0974	I
MgO-product 2	49.64	83.91	I	I	47.00	53.50	84.08	23.3308	I	.39	17.37	38.73	.1936	I	.13	1.12	98.79	.0645	I
MgO-product 3	10.73	94.64	I	I	45.10	11.10	95.18	4.8392	I	2.31	22.23	60.96	.2479	I	.22	.41	99.20	.0236	I
tailings	5.36	100.00	I	I	39.21	4.82	100.00	2.1017	I	8.12	39.04	100.00	.4352	I	.86	.80	100.00	.0461	I
feed	100.00	---	I	I	43.81	100.00	---	43.6052	I	1.14	100.00	---	1.1148	I	5.60	100.00	---	5.7802	I

product	weight recovery I				MgO				CaO				SiO2						
	%	add.%	I	I	grade	recovery	content	I	grade	recovery	content	I	grade	recovery	content	I			
SiO2 - product	25.08	25.08	I	I	36.22	20.83	20.83	9.0840	I	.68	15.30	15.30	.1705	I	22.12	96.00	96.00	5.5477	I
MgO-concentrate	63.83	88.91	I	I	46.74	68.42	89.25	29.8341	I	.59	33.78	49.07	.3766	I	.27	2.98	98.98	.1723	I
tailings	11.09	100.00	I	I	42.25	10.75	100.00	4.6855	I	5.12	50.93	100.00	.5678	I	.53	1.02	100.00	.0588	I
feed	100.00	---	I	I	43.81	100.00	---	43.6036	I	1.14	100.00	---	1.1149	I	5.60	100.00	---	5.7788	I

Assays

	SiO <sub>2</sub> reject (25.6% of feed)	MgO Product (64.6% of feed)	Tail (9.8% of feed)	← Assays - both tests
MgO	36.2 / 36.8	46.74 / 46.58	42.25 / 41.68	
CaO	0.68 / 0.66	0.59 / 0.62	5.12 / 5.47	
SiO <sub>2</sub>	22.1 / 21.15	0.27 / 0.23	0.53 / 0.45	
Fe <sub>2</sub> O <sub>3</sub>	na	0.46 / 0.47	na	

030

BALANCE

enclosure : 16  
 date: 25.05.1985  
 A. - Nr.: 9-8125-9-5011

client: CRA Ltd. / Australia  
 material: magnesite discharge of the rod mill  
 84 % - 0.075 mm, 52 % - 0.040 mm  
 procedure: flotation test 6139  
 Humboldt Wedag 31 - flotation cell

dead burned basis

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %
SiO2-product 1	7.95	7.95	I	41.27	3.79	3.79	3.2810	.88	3.20	3.20	.0700	55.67	47.56	47.56	4.4258
SiO2-product 2	17.13	25.08	I	70.82	14.02	17.81	12.1315	1.27	9.96	13.17	.2176	25.74	47.39	94.95	4.4093
MgO-product 1	9.19	34.27	I	94.33	10.02	27.83	8.6689	1.51	6.36	19.52	.1388	2.16	2.13	97.08	.1985
MgO-product 2	49.64	83.91	I	97.53	55.95	83.79	48.4139	.81	18.42	37.94	.4021	.27	1.44	98.52	.1340
MgO-product 3	10.73	94.64	I	92.21	11.44	95.22	9.8941	4.72	23.20	61.14	.5065	.45	.52	99.04	.0483
tailings	5.36	100.00	I	77.13	4.78	100.00	4.1342	15.83	38.86	100.00	.8485	1.66	.96	100.00	.0890
feed	100.00	---	I	85.13	100.00	---	86.5236	2.22	100.00	---	2.1833	10.88	100.00	---	9.3048

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %
SiO2 - product	25.08	25.08	I	61.45	17.81	17.81	15.4117	1.15	13.19	13.19	.2884	35.23	94.93	94.93	8.8357
MgO-concentrate	63.83	88.91	I	96.65	71.30	89.12	61.6917	1.22	35.62	48.81	.7787	.56	3.84	98.77	.3574
tailings	11.09	100.00	I	84.92	10.88	100.00	9.4176	10.09	51.19	100.00	1.1190	1.03	1.23	100.00	.1142
feed	100.00	---	I	85.13	100.00	---	86.5210	2.22	100.00	---	2.1861	10.88	100.00	---	9.3074

D. Burned Basis

MgO  
 CaO  
 SiO2  
 Fe2O3

SiO2 Reject      2c  
 61.45 / 64.86      39  
 1.15 / 1.15      1.15  
 35.23 / 31.95      573  
 na      1.87

MgO Product      2c  
 96.65 / 95.76      97.0  
 1.22 / 1.27      1.44  
 0.56 / 0.47      20.5  
 0.96 / 0.97      0.85

Tail      2c  
 84.92 / 83.10      90.0  
 10.09 / 10.81      4.3  
 1.03 / 0.88      20.5  
 na      1.69

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131

BALANCE

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enclosure : 17  
 date: 25.05.1985  
 A. - Nr.: 9-8125-9-5011

client: CRA Ltd. / Australia  
 material: magnesite discharge of the rod mill  
           84 % - 0.075 mm, 52 % - 0.040 mm  
 procedure: flotation test 6141  
           Humboldt Wedag 3 1 - flotation cell

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %
SiO2-product 1	8.32	8.32	I	25.80	4.92	4.92	2.1466	.55	4.40	4.40	.0458	45.06	65.25	65.25	3.7490
SiO2-product 2	11.51	19.83	I	39.51	10.43	15.35	4.5476	.72	7.97	12.37	.0829	14.82	29.69	94.95	1.7058
MgO-product 1	9.45	29.28	I	46.17	10.01	25.36	4.3631	.71	6.45	18.82	.0671	1.59	2.62	97.56	.1503
MgO-product 2	59.30	88.58	I	46.71	63.53	88.89	27.6990	.50	28.51	47.33	.2965	.16	1.65	99.21	.0949
MgO-product 3	6.78	95.36	I	44.47	6.92	95.81	3.0151	2.90	18.90	66.23	.1966	.25	.30	99.51	.0170
tailings	4.64	100.00	I	39.41	4.19	100.00	1.8286	7.57	33.77	100.00	.3512	.61	.49	100.00	.0283
feed	100.00	---	I	43.81	100.00	---	43.5999	1.14	100.00	---	1.0401	5.60	100.00	---	5.7452

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %	grade %	recovery %	add.%	content %
SiO2 - product	26.28	26.28	I	36.80	22.18	22.18	9.6710	.66	16.70	16.70	.1734	21.15	96.73	96.73	5.5582
MgO-concentrate	65.30	91.58	I	46.58	69.77	91.95	30.4167	.62	38.97	55.67	.4049	.23	2.61	99.34	.1502
tailings	8.42	100.00	I	41.68	8.05	100.00	3.5095	5.47	44.33	100.00	.4606	.45	.66	100.00	.0379
feed	100.00	---	I	43.81	100.00	---	43.5972	1.14	100.00	---	1.0389	5.60	100.00	---	5.7463

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BALANCE

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enclosure : 18  
 date: 25.05.1985  
 A. - Nr.: 9-8125-9-5011

client: CRA Ltd. / Australia  
 material: magnesite discharge of the rod mill  
           84 % - 0.075 mm, 52 % - 0.040 mm  
 procedure: flotation test 6141  
           Humboldt Wedag 3 l - flotation cell

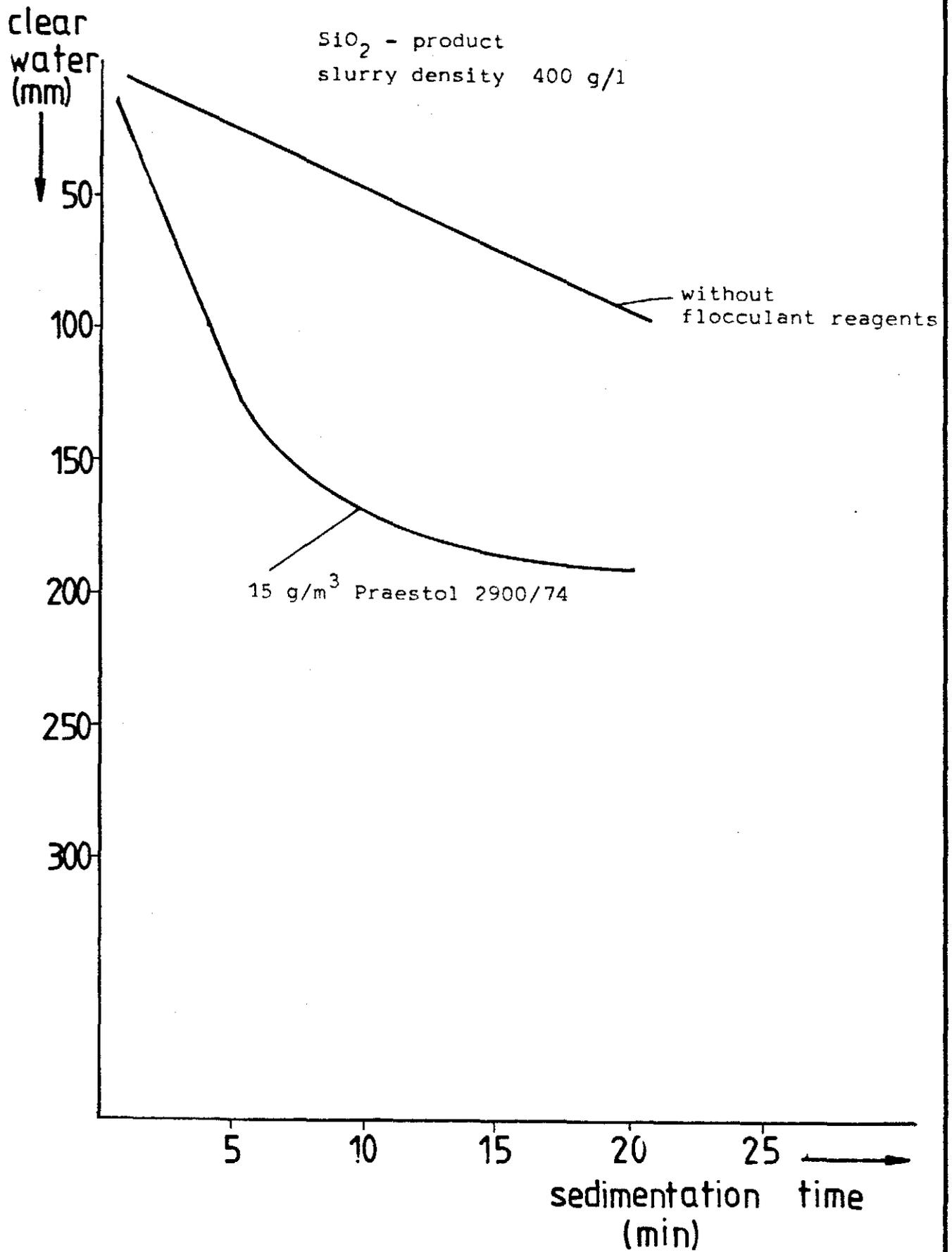
dead burned basis

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade	recovery	add.%	content	grade	recovery	add.%	content	grade	recovery	add.%	content
SiO2-product 1	8.32	8.32	I	35.51	3.41	3.41	2.9544	.76	3.09	3.09	.0632	62.02	58.79	58.79	5.1601
SiO2-product 2	11.51	19.83	I	70.15	9.33	12.74	8.0743	1.28	7.21	10.30	.1473	26.31	34.50	93.29	3.0283
MgO-product 1	9.45	29.28	I	93.29	10.18	22.92	8.8159	1.43	6.61	16.92	.1351	3.21	3.46	96.75	.3033
MgO-product 2	59.30	88.58	I	96.15	65.86	88.78	57.0170	1.03	29.89	46.80	.6108	.33	2.23	98.98	.1957
MgO-product 3	6.78	95.36	I	90.46	7.08	95.87	6.1332	5.90	19.57	66.38	.4000	.51	.39	99.37	.0346
tailings	4.64	100.00	I	77.11	4.13	100.00	3.5779	14.81	33.62	100.00	.6872	1.19	.63	100.00	.0552
feed	100.00	---	I	85.13	100.00	---	86.5726	2.22	100.00	---	2.0437	10.88	100.00	---	8.7772

product	weight recovery			MgO				CaO				SiO2			
	%	add.%	I	grade	recovery	add.%	content	grade	recovery	add.%	content	grade	recovery	add.%	content
SiO2 - product	26.28	26.28	I	64.86	19.69	19.69	17.0452	1.15	14.80	14.80	.3022	31.95	95.66	95.66	8.3965
MgO-concentrate	65.30	91.58	I	95.76	72.23	91.92	62.5313	1.27	40.62	55.42	.8293	.47	3.50	99.16	.3069
tailings	8.42	100.00	I	83.10	8.08	100.00	6.9970	10.81	44.58	100.00	.9102	.88	.84	100.00	.0741
feed	100.00	---	I	85.13	100.00	---	86.5735	2.22	100.00	---	2.0417	10.88	100.00	---	8.7775

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034



**KHD HUMBOLDT WEDAG AG**

D. Dir.	A.O.	C.G.	E.O.	REG. No.
	10 SEP 1986			
	DEPT. OF MINES			
REF. No.				

988036

# Forschungs- und Versuchsanstalt

## Bericht über

REPORT

on

process-engineering tests  
carried out with magnesite  
for Conzinc Riotinto Australia Ltd. (CRA),  
Melbourne/Australia

P.-No. 9-2121-5-6089

A.-No. 9-8125-9-5011



KHD HUMBOLDT WEDAG AG

Köln-Porz, August 06, 1985

IH-YM 2 Wi/He - phone  
ext. 658

KOVs ro

Supplement to

R E P O R T

on

process-engineering tests  
carried out with magnesite  
for Conzinc Riotinto Australia Ltd. (CRA),  
Melbourne/Australia

P.-No. 9-2121-5-6089

A.-No. 9-8125-9-5011

### 1. Summary

The tests carried out for producing a larger quantity of magnesite concentrate have shown that the particle size distribution of the flotation feed is of considerable importance. Regarding the MgO-recovery, the results achieved by the laboratory flotation tests, during which the size of the samples was reduced by means of rod grinding, could not be achieved with the ground product of the ball mill. This is probably attributable to the higher fines portion in the product discharged from the ball mill as against the product discharged from the rod mill.

During a multiple-batch test, a magnesite product of an MgO-content of approx. 97 % and an SiO<sub>2</sub>-content of 0.58 % (related to burnt magnesite) was produced by way of three-stage flotation at a concentrate recovery of 57.6 %.



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## 2. Size reduction

### 2.1 Preliminary size reduction

For production of the required quantity of concentrate and implementation of the multiple-batch test, approx. 150 kg of raw magnesite were crushed to a fineness of 100 % less than 5.6 mm by way of a jaw crusher with intermediately arranged sieve. The product had the following particle size distribution:

product jaw crusher / feed - ball mill

grain size mm		portions in % by weight	cumulative portions in % by weight
	+ 4	21.3	21.3
4	- 2.8	21.9	43.2
2.8	- 2	12.4	55.6
2	- 1	15.8	71.4
1	- 0.5	8.4	79.8
0.5	- 0.315	3.0	82.8
0.315	- 0.18	2.8	85.6
0.18	- 0.125	1.7	87.3
	- 0.125	12.7	100.0

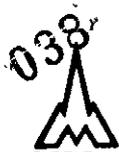
### 2.2 Grinding

A discontinuously operating ball mill of 600 mm diameter with obliquely arranged grinding vessel with a contents of 50 l was applied for fine grinding.

The grinding vessel made of wear-resistant cast steel is arranged as rotation ellipsoid at an inclination of  $30^\circ$ . The operating speed equals  $n = 50 \text{ min}^{-1}$ . The drive has a capacity of 1.1 kW. The ball charge was selected as follows:

ball diameter	mm	mass	kg
	40		40
	30		36
	25		13
	± 20		11

During all grinding tests the solids/water-mass ratio equalled 1 and the feed quantity / batch approx. amounted to 20 kg of magnesite. Grinding was done batchwise in closed-circuit operation - mill - sieve - mill. After each grinding operation the total ground material was subjected to wet classification by means of a vibratory screen (make Sweco), which was covered by a 0.142 mm-screen deck. The residues retained, mixed with raw magnesite (together approx. 20 kg) served as feed material for next batch grinding. A circulating load of approx. 30 % resulted for each batch at a grinding period of 10 minutes. The particle size distribution of the combined ground product after six batches including chemical analyses of the fractions can be taken from enclosure 1. During a second closed-circuit grinding the grinding period was shortened to 6 minutes/batch, which resulted in an increase of the circulating load to more than 100 %.

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However, the sizing characteristic obtained essentially corresponds to that for the first grinding operation.

In case of the two grinding operations carried out in the ball mill, the particle size distribution of the feed material for the laboratory flotation tests could not be exactly reached. Rod grinding combined with intermediate sieving in the laboratory mill was more heedful (see enclosure 2), i.e. it produced less quantities of superfine material.

### 3. Flotation

The results of the laboratory flotation tests could be applied to the tests for production of the concentrate quantity only to a limited degree. On the one hand the quantity of reagents had to be adjusted due to the higher hardness of the water (approx. 15° German hardness instead of 10° German hardness). Proportioning of the calcite- and dolomite depressing agent EKOFACD DD 95 had to be reduced considerably and addition of the magnesite collector RESANOL A had to be increased, at least during the tests without medium-size material.

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On the other hand, the flotation periods and the mode of operation had to be modified due to the varying mode of grinding (grinding in a ball mill instead of grinding in a rod mill). On the whole,  $\text{SiO}_2$ -flotation of the product discharged from the ball mill was less selective than that of the product discharged from the rod mill, which probably is attributable to the higher fines portion of less than approx. 0.01 mm in the ground product. The  $\text{SiO}_2$ -froth always contained a not insignificant portion of magnesite. Since the required purity in the  $\text{MgO}$ -concentrate for this material in a two-stage flotation process without secondary cleaning can be achieved only if the quartz during  $\text{SiO}_2$ -flotation is recovered at approx. 95 % in the froth product, a higher loss of magnesite will occur in this processing stage at lower selectivity.

For partly making good for this loss of recovery, it was required to accept a lower  $\text{SiO}_2$ -recovery during  $\text{SiO}_2$ -flotation and to subject the froth of magnesite flotation to secondary cleaning (see enclosure 3).

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### 3.1 Multiple-batch test

A multiple-batch test was carried out after a series of preliminary tests for matching the proportioning rate of reagents to the changed conditions. To that end, a Humboldt-cell of a capacity of 18 l with double wobble agitator was applied. 6 kg of ground raw magnesite of a fineness of 86 % less than 0.090 mm were fed per batch.

The reagents below were applied for SiO<sub>2</sub>-flotation:

EKOFACT DD 95	75 g/t of ore
RESANOL 450	150 g/t of ore in three batches (80 g/t at the beginning, 2 x 35 g/t during flotation)

The conditioning period for EKOFACT DD 95 equalled two minutes and five minutes for RESANOL 450 (1st addition). The overall duration of flotation equalled 8 - 10 minutes.

Prior to subsequent MgO-flotation, soda waterglass at a proportioning rate of 400 g/t of ore was admitted for deadening the quartz. The collecting-/effervescing reagent combination RESANOL A was admitted after a conditioning period of approx. 1 minute. MgO-flotation was started after a short period of conditioning. RESANOL A was added twice.

During the preliminary tests carried out with the water of greater hardness and during the first runs of the multiple-batch test, the required proportioning rate for RESANOL A amounted to 800 - 1000 g/t of ore.

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As from batch 10 of the multiple-batch test up to the end of flotation, the consumption could be reduced to 500 g/t of ore due to recycling of the medium-size.

Compared to the laboratory tests, addition of EKOFAC DD 95 had to be strongly reduced, since the magnesite recovery was substantially lowered upon higher proportioning rates.

Contrary to the laboratory tests, provision was made for a secondary cleaning stage for flotation of magnesite. The magnesite froth was collected, mixed with soda waterglass (300 g/t of raw ore, resp. approx. 450 g/t of magnesite froth) and subjected to secondary flotation after a short conditioning period. The cleaned froth was the final magnesite concentrate and the residues retained in the cell (approx. 10 % by weight related to raw ore and 15 - 20 % by weight related to the magnesite concentrate, respectively) were added to the next batch after completion of  $\text{SiO}_2$ -flotation (see en-closure 3).

The products obtained from flotation of the last batch were dried, weighed and chemical analyses were made. The product distribution is listed on next page.

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Product	% by weight	loss on ignition %	MgO-content %	SiO <sub>2</sub> -content %	CaO-content %	Fe <sub>2</sub> O <sub>3</sub> -content %
SiO <sub>2</sub> -product	<u>32.04</u>	<u>42.00</u>	<u>39.00</u>	<u>16.41</u>	<u>0.86</u>	<u>0.72</u>
MgO-concentrate	57.64	51.41	47.17	0.28	0.3	0.51
tailings	<u>10.32</u>	<u>48.12</u>	<u>40.52</u>	<u>3.71</u>	<u>10.31</u>	<u>1.38</u>
feed (calc.100 (found)		- 48.54	43.87 43.81	5.80 5.60	1.00 1.14	0.67 0.51
medium-size (circulating load)	10.60	50.64	45.36	0.93	1.83	0.82
sum	110.60					

By variation of the admitting rate of depressing agent, the ratio of the CaO/SiO<sub>2</sub>-contents can probably be raised to more than 2.

9



### 3.2 Secondary cleaning of the SiO<sub>2</sub>-product

An SiO<sub>2</sub>-product of one cycle of the multiple-batch test was subjected to secondary cleaning. After a flotation period of 3 minutes for the froth product without addition of reagents, RESANOL 450 (60 g/t) was added and SiO<sub>2</sub>-flotation was discontinued after additional 3 minutes. Following this, attempts were made to win a froth product of low SiO<sub>2</sub>-content by means of soda waterglass as depressing reagent and RESANOL A as collecting/effervescing reagent. The product distribution shown below reveals that this objective could not be reached.

Product	% by weight	SiO <sub>2</sub> -content %
froth 1	45	25.7
froth 2	46)	2.3)
	55	7.75
residues	9)	35.6)
SiO <sub>2</sub> -product	100	15.8

### 3.3 Production of concentrate

A total of 57 kg of final concentrate was produced from the magnesite products of the multiple-batch test as well as from the previous tests carried out with the 18 l-Humboldt-flotation cell. The chemical composition of this concentrate calculated on the basis of the analyses for the different products is as follows:

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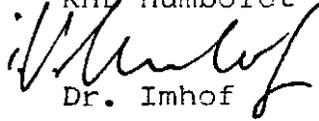
**KHD HUMBOLDT WEDAG AG**

10

	non-ignited	ignited
MgO-content (%):	46.91	96.54
CaO-content (%):	0.40	0.81
SiO <sub>2</sub> -content(%):	0.27	0.55
Fe <sub>2</sub> O <sub>3</sub> -content (%):	0.5	1.03

The tests were carried out by us to the best of our knowledge and ability. A liability, in particular for the process engineering results of machines, plant sections or plants delivered by us, can be undertaken by us only if this has been agreed upon in writing.

KHD Humboldt Wedag AG

  
Dr. Imhof  
Dr. Bleckmann

045

BALANCE

enclosure : 1  
 date: 25.05.1985  
 A. - Nr.: 9-8125-9-5011

client: CRA Ltd. / Australia  
 material: magnesit discharge of the ball mill  
           1st grinding  
 procedure: Grain size distribution with  
           chemical analysis

grain size mm	weight			I	MgO				I	CaO				I	SiO2				I
	%	add.%	recovery		grade	recovery	add.%	content		grade	recovery	add.%	content		grade	recovery	add.%	content	
+	.090	23.13	23.13	I	42.68	22.59	22.59	9.8719	I	1.33	28.25	28.25	.3076	I	8.03	35.04	35.04	1.8573	I
.090 -	.063	13.43	36.56	I	43.02	13.22	35.81	5.7776	I	1.15	14.18	42.44	.1544	I	6.20	15.71	50.75	.8327	I
.063 -	.040	12.21	48.77	I	43.59	12.18	47.99	5.3223	I	1.05	11.77	54.21	.1282	I	5.49	12.65	63.39	.6703	I
.040 -	.032	6.28	55.05	I	44.57	6.40	54.39	2.7990	I	1.08	6.23	60.44	.0678	I	4.46	5.28	68.68	.2801	I
.032 -	.020	14.59	69.64	I	43.77	14.61	69.01	6.3860	I	1.10	14.74	75.18	.1605	I	4.97	13.68	82.36	.7251	I
.020 -	.000	30.36	100.00	I	44.61	30.99	100.00	13.5436	I	.89	24.82	100.00	.2702	I	3.08	17.64	100.00	.9351	I
feed:	100.00	---	---	I	43.81	100.00	---	43.7004	I	1.14	100.00	---	1.0888	I	5.60	100.00	---	5.3006	I

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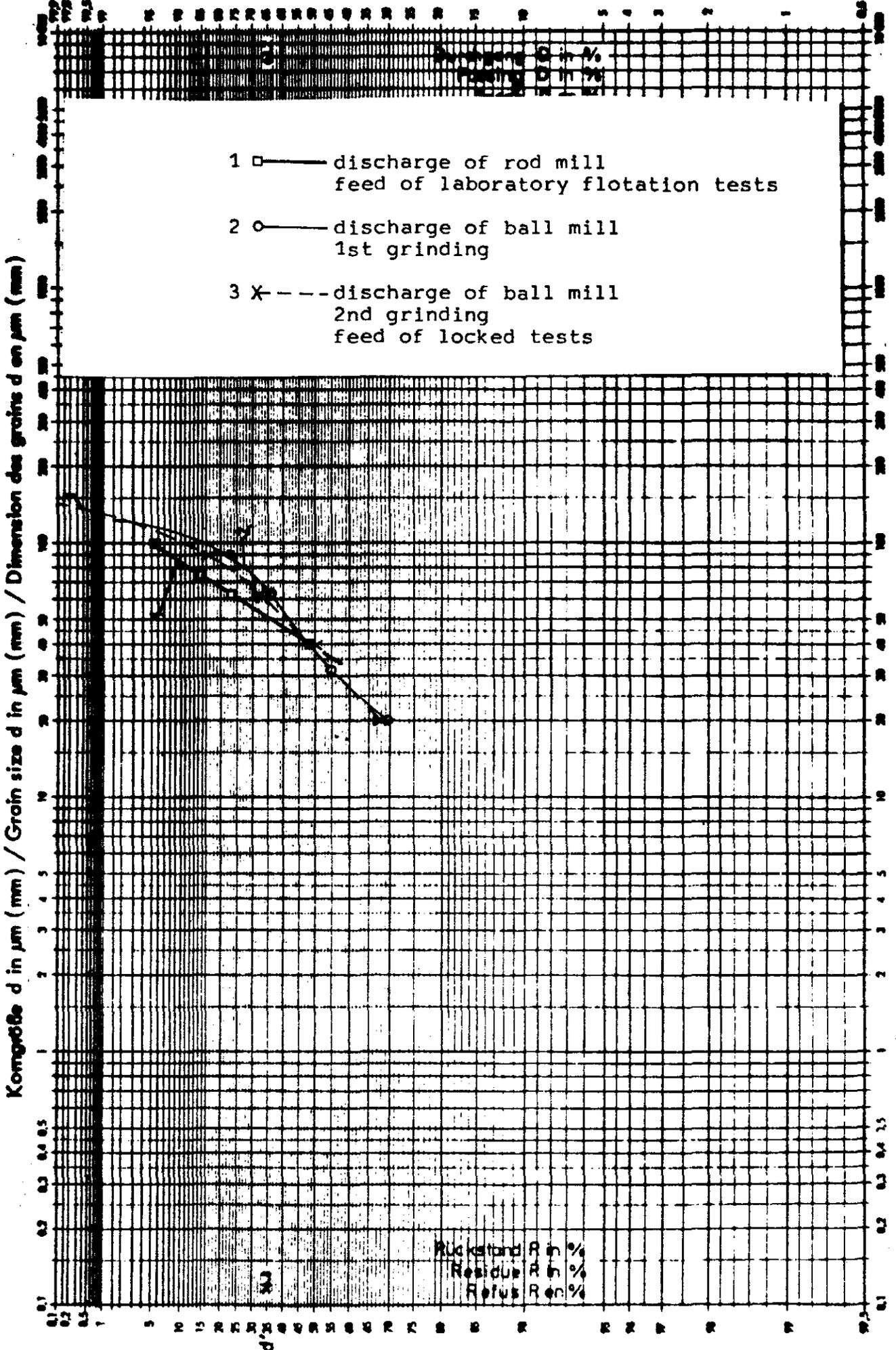
# Körnnetz / Grading graph Diagramme granulométrique

enclosure: 2  
Datum: 15.07.85  
Date: 15.07.85

Machines: ROD MILL  
Machines: BALL MILL  
Appareil:

Firma: CRA Australia  
Customer: CRA Australia  
Client:

Stoff: MAGNESITE  
Material: MAGNESITE  
Produit:

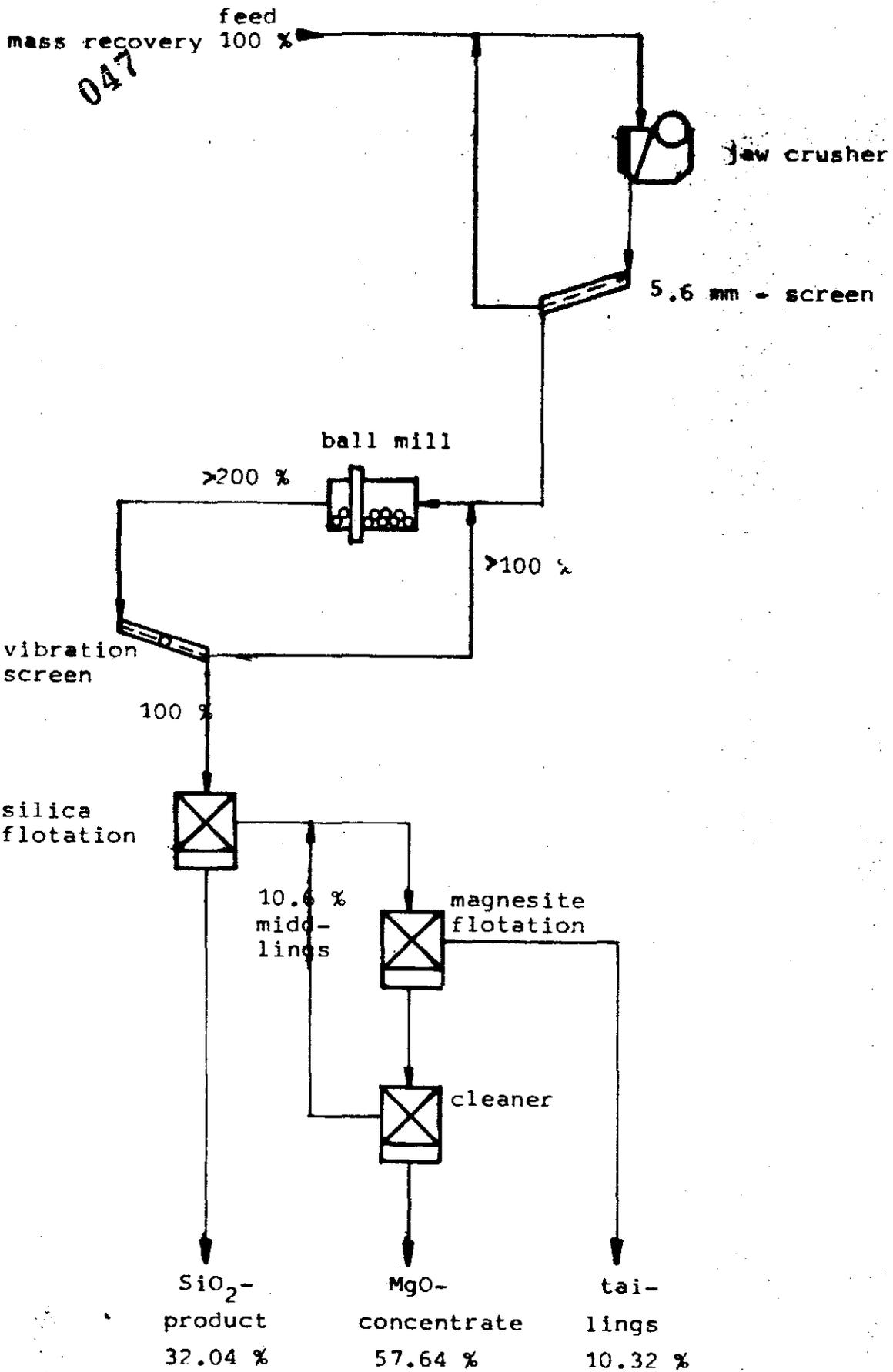




MAGNESITE  
Flow - sheet locked test

enclosure 3

22.7.85





**KHD HUMBOLDT WEDAG AG**

## **Forschungs- und Versuchsanstalt**

### **Bericht über**

process-engineering tests carried  
out with magnesite  
for Conzinc Rio Tinto Australia Ltd. (CRA),  
Melbourne/Australia  
P.-No. 9-2121-5-0089  
A.-No. 9-8125-9-5011



2nd supplement to

## Report

on

process-engineering tests carried out  
with magnesite  
for Conzinc Riotinto Australia Ltd. (CRA),  
Melbourne/Australia  
P.-No. 9-2121-5-0089  
A.-No. 9-8125-9-5011

### Microprobe and scanning electron microscopy (SEM) investigation

Microprobe and SEM investigation of a raw magnesite sample was carried out to look in a more detailed way at the texture of the minerals which were identified by means of optical microscopy. (Compare with Report dated July 25, 1985, chapter 4.15 Mineralogie testing).

For that examination the sample has been used the microphotographs no. 3 and no. 7 (thin sections) of which have been shown in the Report dated July 25, 1985.

...

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This report describes implementation as well as the results of investigation and tests carried out in our test centres and laboratories. We hold the copyright of this report and pertinent illustrations and other representations, if any; duplicates of the report etc. or its transfer to or making it available or disclosing the contents, also in an abridged form, to third parties, is not permitted. Moreover, without our previous express approval, the report etc. must not be used for a different purpose than entrusted with the party receiving. - All rights with regard to granting of a patent, design registration or other protective rights, are reserved. -

**KHD Humboldt Wedag AG**

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Blatt 2 zum Brief vom August, 23, 1985

an Conzinc Riotinto Australia Ltd. (CRA)



**KHD HUMBOLDT WEDAG AG**

In general the SEM investigation can confirm the paragenesis which has been found by optical microscopy. Furthermore, a sulfide mineral, pyrite, was found as idiomorphic grains at the rims of magnesite and as inclusions in magnesite, dolomite and quartz. But most of the pyrite is changed into goethite. This corresponds to the observation, that there are alteration products of quartz, magnesite and goethite as a result of weathering process.

Fig. 1 a shows an aggregate of secondary quartz which is xenomorphic surrounded by well defined grains of magnesite.

The secondary quartz itself has inclusions of magnesite which are probably remains of a solution process.

The magnesite in solution may have precipitated as small veins and then this type of magnesite is a cementate between the different grains.

X-ray element distributions (fig.: 1b-d) of the area, which is to be seen in fig. 1 a were made to give an improved representation of quartz and magnesite.

The C-Ka distribution (fig.: 1d) shows enrichments of carbon in the cracks and between the grain boundaries resulting from preparation of the samples.

Table 1 gives some typical analyses of the carbonates magnesite, dolomite and calcite which were carried out by careful electron microprobe analysis using the energy dispersive system.

The tests were carried out by us to the best of our knowledge and ability. A liability, in particular for the process engineering results of machines, plant sections or plants delivered by us, can be undertaken by us only if this has been agreed upon in writing.

KHD Humboldt Wedag AG

- Dr. Kellerwessel - - Dr. Bleckmann -

Enclosures

-FIG. 1a-

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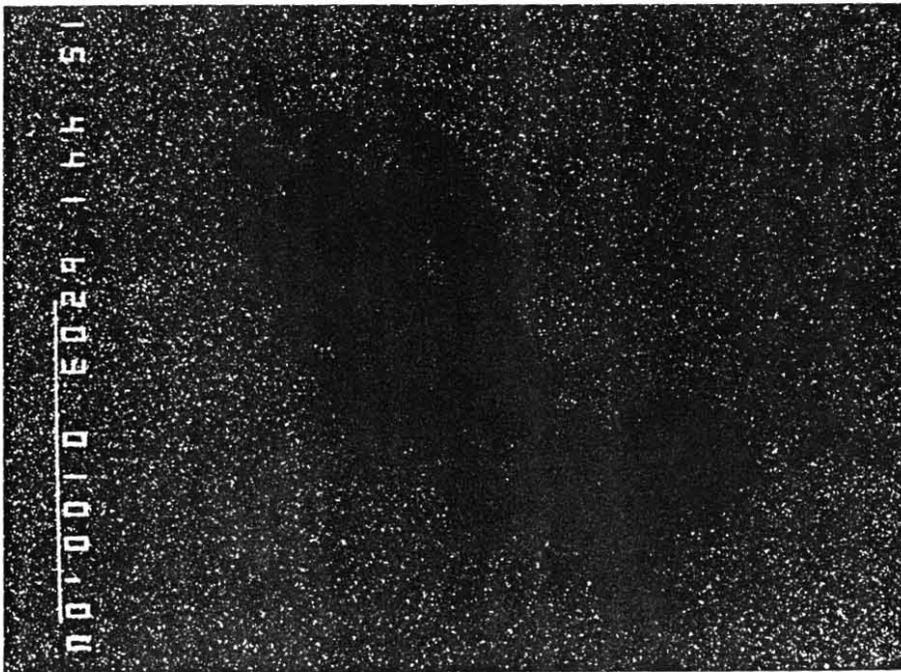


COMPO IMAGE

100 μm

XENOMORPHIC QUARTZ (CENTER) SURROUNDED BY MAGNESITE (GREY)

-FIG. 1b-



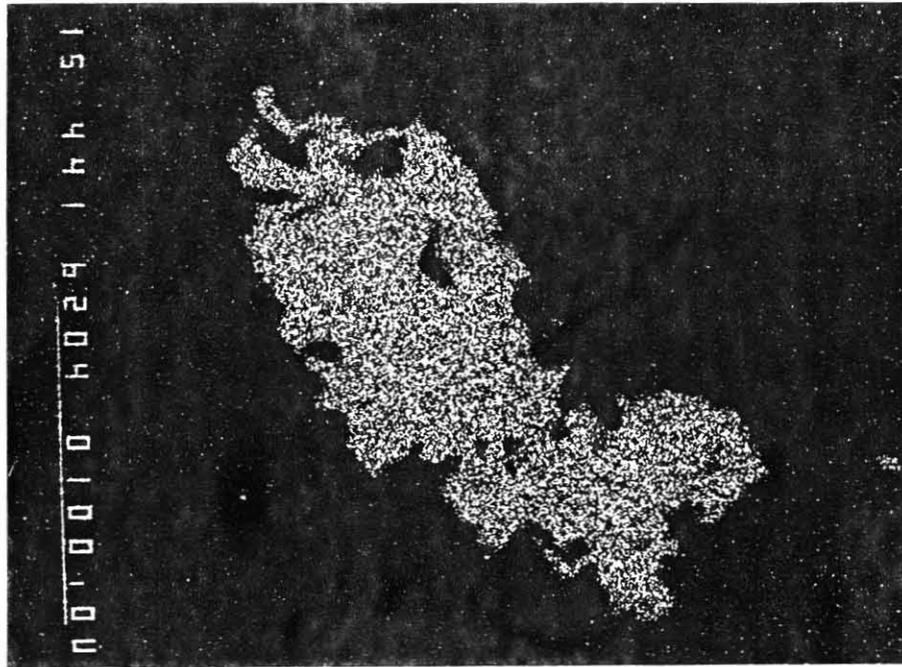
100 μm

Mg K<sub>α</sub>-DISTRIBUTION OF AREA GIVEN IN FIG. 1a

5 cm

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-FIG. 1c-





SETTLING CURVE

MgO - concentrate

enclosure  
20

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053

clear  
water  
(mm)



50

100

150

200

250

slurry density of feed 740 g/l

slurry density  
of feed 530 g/l

5

10

15

20

25

(min)

sedimentation time →



SETTLING CURVE  
tailings

enclosure  
21

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054

clear  
water  
(mm)



50

100

150

200

250

300

tailings  
slurry density of feed: 72.5 g/l  
floculant reagent: 2.5 g/m<sup>3</sup> Praestol  
2900/74

5

10

15

20

25

sedimentation time (mm)

List of filtration tests  
MgO-concentrate

-----

055

test no.	slurry density	suction time	drying time	height	filtration cake weight		moisture	calc. capacity (dry)
					wet	dry		
	g/l	sec	sec	mm	g	g	%	kg/(h · m <sup>2</sup> )
4	553	40	40	16	316	284	10,1	1022
5	553	40	80	20	328	304	7,3	730
6	553	40	60	20	320	294	8,1	852
11	1400	20	60	36	667	598	10,3	2153
12	1400	20	40	35	680	606	10,9	2909
13	1400	20	80	34,5	664	602	9,2	1746

Table 1:

mineral	MgO-grade %	SiO <sub>2</sub> -grade %	CaO-grade %	MnO-grade %	Fe <sub>2</sub> O <sub>3</sub> -grade %	sum %
magnesite	47,54	0,18	-	0,26	0,52	48,50
magnesite	45,94	0,20	-	0,30	1,95	48,39
dolomite	22,36	0,22	30,02	-	0,41	53,01
calcite	-	-	54,92	0,38	0,44	55,78

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058

T E S T R E P O R T

Refractory tests with magnesite  
flotation concentrate carried out

for

KHD HUMBOLDT WEDAG AG  
ABT. IH-MV1, BOCHUM/FRG

prepared by

REFRATORIES CONSULTING &  
ENGINEERING AG  
RADENTHEIN/AUSTRIA

Radenthein, 1986/02/25

VERSO2/Kn/Kü Nr. 056

059

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CONTENTS

- 1.0.0 Introduction
- 2.0.0 Scope of test program
- 3.0.0 General information
- 4.0.0 Course of test work
  - 4.1.0 Flotation concentrate characteristics
  - 4.2.0 Calcination tests
  - 4.3.0 Compacting tests
  - 4.4.0 Sintering tests
  - 4.5.0 Extension of test program
    - 4.5.1 Scope of additional tests work
    - 4.5.2 Conclusions from additional tests work

060

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SUMMARY

Raw magnesite, originating from a deposit in NW-Tasmania was beneficiated in KHD's test facilities to flotation concentrate with + 97 % MgO content. RCE was requested to carry out refractory tests in a 3-step program which was mutually agreed upon after detailed discussions between KHD and RCE. Tests covered under step 1 aimed to determine optimum conditions for producing maximum sinter densities and to produce sufficient MgO sinter from the remaining sample quantity for subsequent refractory tests of step 2.

The tests carried out according scope of tests defined under step 1 gave completely unsatisfactory results with sinter densities at 1850 °C of max. 2,69 g/cm<sup>3</sup>. The rate of calcination showed no influence on the final sinter density (BSD) and the compactibility of the caustic MgO produced at 800 °C (= highest reactivity), 850 °C, 900 °C and 950 °C was equally poor for all samples.

At this stage KHD agreed with RCE to extend the scope of sintering tests in order to cover the complete range of technological possibilities for achieving high sinter densities.

This included single step sintering of raw concentrate in original and finely ground modification up to 2-stage calcining/ sintering of original and finely ground MgO produced at an optimum temperature of 800 °C for calcination and 1850 °C for sintering. Fine grinding of caustic MgO increased the sinter density along with an increased fineness. The best sinter density of 3,15 g/cm<sup>3</sup> was achieved with a fineness of the caustic MgO of 98 % minus 32 micron, a figure which was still far away from the target of + 3,30 g/cm<sup>3</sup>.

MgO Periclase 3.67-3.90 sinter quality.  
MgCO<sub>3</sub> magnesite 3.0-3.12 " "

061

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A certain chance to improve the sinter density further exists in ultra-fine grinding of the caustic MgO and by increasing the sintering temperature. But from a technical and economical point of view it is hardly to imagine that an industrial scale operation will be feasible based on such a complex technology.

Considering above circumstances and facts and after consultations with the customer in Australia, KHD advised RCE to carry out no further tests and to prepare a formal test report.

Questions raised by CRA regarding the poor sintering properties of this sample in comparison with the samples from NW-Tasmania tested by RCE in 1974 have already been commented in a separate telex addressed to KHD on 1986/02/21.

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1.0.0<sup>062</sup> INTRODUCTION

Against official KHD-order no. 9-8125-9-5018-001/4029 dated 1985/10/02 RCE was requested to carry out laboratory scale refractory tests in a 3-step program:

- Refractory tests up to sinter product
- Refractory tests with pieces of bricks
- Basic information and plant data

For this purpose on 1985/09/25 RCE received a quantity of 56 kg magnesite flotation concentrate which was produced in KHD's test facilities.

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## 2.0.0 SCOPE OF TEST PROGRAM

### 2.1.0 REFRACTORY TESTS UP TO SINTER PRODUCT

- Calcination tests at 3 different temperatures
- Sintering tests and determination of sinter densities and best suited temperature
- Calcination of total concentrate sample at best suited temperature
- Sintering tests at different temperatures
- Determination of sinter density, water absorption, apparent porosity and primary crystal size
- Expertise and comparison of sinter with other marketable sinters of equivalent composition

### 2.2.0 REFRACTORY TESTS WITH PIECES PRODUCED FROM SINTER

- Pressing of sinter produced under item 2.1
- Determination of brick density, apparent porosity and other relevant parameters after firing
- Determination of refractoriness under load and temperature
- Expertise and comparison with well known products

### 2.3.0 INFORMATIONS AND PLANT DATA

Based on the results of testwork outlined under items 2.1 and 2.2 basic information and data will be given regarding operation costs of a production plant, process, parameters, retention time, costs for calcination, briquetting and sintering, etc.

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3.0.0 GENERAL INFORMATION

Already in 1974 RCE had carried out beneficiation and sintering tests with raw magnesite origination from NW-Tasmania (Lions River Deposit, Victory Deposit, Arthur River Main Outcrop). Based on these results it was obvious that a single step burning process, even after fine grinding of flotations concentrate to minus 40 micron, will not yield the required sinter density of plus 3,30 g/cm<sup>3</sup>. But this goal in 1974 was reached by applying a two step burning process including fine grinding of the pre-calcined material.

According to information received from KHD the test material obviously originated from the same area of magnesite mineralization in NW-Tasmania with basically similar mineralogical features.

For above reason, our general experience with similar types of magnesite and according to the latest trend in industrial scale sintering technology aiming at highest possible sinter densities, a single step sintering process was not envisaged to be feasible right from the beginning and the investigation programm was focused on a 2-step calcination/sintering process.

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#### 4.0.0 COURSE OF TEST WORK

#### 4.1.0 FLOTATION CONCENTRATE CHARACTERISTICS

The total quantity of flotation concentrate supplied by KHD was thoroughly mixed in order to assure an optimum homogeneity for the subsequent tests.

#### 4.1.1 CHEMICAL ANALYSIS

After homogenization the following chemical analysis of the flotation concentrate was determined by X-ray fluorescent analysis. According to general practice of our laboratories for reasons of accuracy MgO is calculated as difference to 100 %. All figures represent ignited conditions, therefore the value for "loss on ignition" (L.O.I.) is put into brackets.

SiO <sub>2</sub>	0,40 %
Fe <sub>2</sub> O <sub>3</sub>	0,95 %
Al <sub>2</sub> O <sub>3</sub>	0,05 %
Mn <sub>3</sub> O <sub>4</sub>	0,16 %
Cr <sub>2</sub> O <sub>3</sub>	0,01 %
CaO	1,12 %
MgO (Diff.)	97,31 %
L.O.I.	(51,45 %)
CaO/SiO <sub>2</sub> ratio	2,80

066

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4.1.2 GRAIN SIZE DISTRIBUTION

Determination of grain size, also in case of caustic calcined material, was carried out by use of a CILAS-Lasergranolumeter.

Grain size (micron)	Grain size distribution (Vol.-%)
192	-
128	5,6
96	10,7
64	36,2
48	49,7
32	70,8
24	81,2
16	7,9
12	91,8
8	94,0
6	95,6
4	96,7
3	97,4
2	97,7
1,5	98,3
1	98,5

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#### 4.2.0 CALCINATION TESTS

Calcining of flotation concentrate was carried out batch-wise in a laboratory muffle furnace with charges of 1 kilogram each. Retention time of the samples at specific calcining temperatures was 30 minutes. In order to cover the whole range of possibly applicable calcining temperatures for achieving of maximum sinter densities the tests were extended to 4 calcining temperatures instead of 3 originally planned, namely 800 °C, 850 °C, 900 °C and 950 °C. For each sample of caustic calcined MgO produced at above temperatures the "loss on ignition" (L.O.I.) was determined which is the usually applied figure for defining the rate of calcination.

In addition the specific surface in (m<sup>2</sup>/g) according to BET-method was determined which describes the reactivity of the caustic calcined MgO. A highly reactiv MgO, equivalent to a high specific surface is one parameter for achieving favourable compacting properties respectively good green densities of the briquetted caustic MgO which normally also influences the final sinter density in a positive way.

In addition the grain size distribution of the calcined samples was determined by CILAS-granolumeter. The results are enclosed under table 2-5.

The results from the calcining tests for test samples no. 1 - 4 are summarized under item 4.4.0 (sintering tests).

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4.3.0 COMPACTING TESTS

The caustic calcined MgO samples produced at 800 °C, 850 °C, 900 °C and 950 °C were compacted in cylindrical moulds by means of a piston press applying a standard pressure of 150 N/mm<sup>2</sup>. The size of the compacted MgO cylinders was 50 mm in diameter and 30 mm in height. Despite of the differing rate of calcination respectively reactivity the green density (RD) of the samples was unexpectedly low and more or less the same, ranging from 1,39 g/cm<sup>3</sup> to 1,45 g/cm<sup>3</sup>. Comparable MgO qualities show green densities in the range of 1,90 g/cm<sup>3</sup> to 2,20 g/cm<sup>3</sup>.

The test results for samples no 1 - 4 are summarized under item 4.4.0 (sintering tests).

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4.4.0 SINTERING TESTS

Sintering of the test samples was carried out in a high temperature chamber type laboratory kiln at different temperatures, namely 1750 °C and 1850 °C. Heating up requires approximately 8 hours and the sample is placed into the kiln at roughly 500 °C. Retention at a specified temperature is 4 hours. The sinter bulk specific density or BSD for samples no. 1 - 4 sintered, at 1750 °C, was practically the same and completely unsatisfactory. Even an increase of the sintering temperature to 1850 °C did not change the results apart from a negligible increase by 0,04 g/cm<sup>3</sup> to a maximum of 2,69 g/cm:

Sample no.	Calcined MgO			Raw density RD (g/cm <sup>3</sup> )	Sintered MgO BSD (g/cm <sup>3</sup> )	
	Calc. temp. (°C)	L.O.I. (%)	BET (m <sup>2</sup> /g)		1750 °C	1850 °C
1	800	0,34	39,344	1,45	2,65	2,69
2	850	0,14	17,445	1,39	2,63	2,69
3	900	0,08	11,848	1,43	2,56	2,62
4	950	0,06	4,656	1,41	2,65	2,69

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#### 4.5.0 EXTENSION OF TEST PROGRAM

The unexpected negative results of course did not allow to carry out the tests according to original schedule. In order to continue with refractory tests outlined under step 2 of the program a sinter density of 3,30 g/cm<sup>3</sup> was considered as a minimum.

At this stage KHD was informed about the negative results and RCE suggested to carry out additional tests which might lead to a satisfactory sinter density and should cover the complete range of possibilities from single step firing of raw flotation concentrate to 2-step firing including fine grinding of material. This proposal was accepted by KHD.

#### 4.5.1 SCOPE OF ADDITIONAL TEST WORK

For calcination of magnesite the optimum temperature of 800 °C, determined during initial test work, was maintained. Incidentally this is the same calcining temperature applied in RCE's 1974 tests with magnesite from NW-Tasmania.

##### Sample no. 5

Original flotation concentrate (grain size analysis table no. 1) as supplied by KHD was mixed with 20 % caustic MgO produced at a calcining temperature of 800 °C. After addition of 3 % Kieserite (MgSO<sub>4</sub>) solution with a concentration of 28 ° Bè the mixture was compacted to cylindrical shape sizing 50 mm in diameter and 30 mm in height. Pressure applied was 150 N/mm<sup>2</sup>. Green density (RD) of the compacted material was 2,15 g/cm<sup>3</sup>, sinter density after firing at 1850 °C 2,38 g/cm<sup>3</sup> only.

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This traditional technology in principle is identical with present large scale production in Radenthein (Radex) and many other major refractory producers operating on the basis of natural magnesite.

Sample no. 6

Original flotation concentrate was ground to 100 % minus 48 microns in a laboratory rod mill (grain size analysis table 6). After mixing with 20 % caustic MgO (calcining temperature 800 °C) and addition of 3 % Kieserite solution at 28 ° Be the sample was compacted as described above and sintered at 1850 °C. Compared with sample no. 5 fine grinding raised the sinter density from 2,38 g/cm<sup>3</sup> to 2,82 g/cm<sup>3</sup> only.

Sample no. 7

Caustic MgO produced at 800 °C calcination temperature was compacted without addition of any binder to standard size cylinders as above. No grinding of the concentrate or caustic calcined MgO took place (cross-check to sample no. 1). The green density of 1,39 g/cm<sup>3</sup> and sinter density of 2,67 g/cm<sup>3</sup> were practically identical with sample no. 1 proving that tests were carried out correctly.

Sample no. 8

Caustic MgO produced at 800 °C was ground to a fineness of 100 % minus 64 micron and subsequently compacted without addition of binder to standard size cylinders (grain size distribution table 7).

The green density could be raised to 1,60 g/cm<sup>3</sup> and the sinter density to 3,03 g/cm<sup>3</sup> which still was far below the target of + 3,30 g/cm<sup>3</sup>.

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072

Sample no. 9

Caustic MgO produced at 800 °C was ground to a fineness of 100 % minus 48 micron or approximately 98 % minus 32 micron (grain size distribution table 8). With above measures almost all natural magnesite types can be dead burned to satisfactory high sinter densities.

Unfortunately not so in this specific case. The green density remained at the same level as for sample no. 8. Though the sinter density increased further to 3,15 g/cm<sup>3</sup> this figure was still disappointingly low.

Diagram 1 illustrates and compares the grain size distribution characteristic of the various samples.

4.5.2 SUMMARY OF RESULTS FROM ADDITIONAL TESTS

Sample no.	Sample preparation	RD (g/cm <sup>3</sup> )	BSD at 1850 °C (g/cm <sup>3</sup> )
5	Orig.flot.conc. +20% caustic MgO +3% Kieserite solution	2,15	2,38
6	Ground flot.conc. +20% caustic MgO +3% MgSO <sub>4</sub>	2,15	2,82
7	Caustic MgO in original grain size, 800 °C	1,39	2,67
8	Caustic MgO (800 °C) ground to 100% -64 micron	1,60	3,03
9	Caustic MgO (800 °C) ground to 100% -48 micron	1,58	3,15

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4.5.2 CONCLUSIONS FROM ADDITIONAL TEST RESULTS

RCE informed KHD about the negative results and hinted out on the principal possibility and chance that a sufficient high sinter density might be achieved by super fine grinding of caustic MgO aimings at a maximum content of minus 10 micron particles in combination with an increase in sinter temperature to 1950 °C. Basing an industrial production on such a technology can hardly be justified commercialy with respect to investment and operating costs.

Under these circumstances RCE proposed to cancel further tests planned according original schedule. After consultation with the Australian customer KHD confirmed that RCE should terminate further tests. Further RCE was requested to air-freight the remaining sample of approx. 40 kg original KHD-concentrate and the small sinter samples from the various test to CRA Exploration Pty. Ltd/Australia which meanwhile has been effected.

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ENCLOSURES

Table 1: Grain size distribution  
Original flotation concentrate

Table 2: Grain size distribution  
caustic MgO, 800 °C

Table 3: Grain size distribution  
caustic MgO, 850 °C

Table 4: Grain size distribution  
caustic MgO, 900 °C

Table 5: Grain size distribution  
caustic MgO, 950 °C

Table 6: Grain size distribution  
Raw flotation concentrate  
ground to minus 48 micron

Table 7: Grain size distribution  
caustic MgO, 800 °C  
ground to 100 % minus  
48 micron

Table 8: Grain size distribution  
caustic MgO, 800 °C  
ground to 48 % minus  
32 micron

Diagram 1: Graphical comparison of  
grain size distribution of  
various samples

Diagram 2: Temperature profile of high  
temperature laboratory  
sintering tests

075

Körnungsanalyse Nr. 208Datum 1985 10 16

Flotationskonzentrat Tasmanien original			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	
	Fractions- %	ΣFrakt. - %		
•200				
128 - 200	5,6	5,6		
96 - 128	5,1	10,7		
64 - 96	25,5	36,2		
48 - 64	13,5	49,7		
32 - 48	21,1	70,8		
24 - 32	10,4	81,2		
16 - 24	6,7	87,9		
12 - 16	3,9	91,8		
8 - 12	2,2	94,0		
6 - 8	1,6	95,6		
4 - 6	1,1	96,7		
3 - 4	0,7	97,4		
2 - 3	0,3	97,7		
15 - 2	0,6	98,3		
1 - 15	0,2	98,5		
-1	1,5	100,0		

GRANULOMETRE 715 E256	
95-10-16	
FR. 7055. RM. KONZENTRAT	
:	
1	898,5 %
1,5	898,3 %
2	897,7 %
3	897,4 %
4	896,7 %
6	895,6 %
8	894,8 %
12	891,8 %
16	887,9 %
24	881,2 %
32	878,8 %
48	849,7 %
64	836,2 %
96	818,7 %
128	805,6 %
192	800,8 %
59% - PUNKT = 847,8	
VOLUMENVERTEILUNG	

## 076 Körnungsanalyse Nr. 218

Datum 1985 11 15

Flotationskonzentrat Tasmanien Kauster 800°C			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E266 95-11-15 FR-7055-800.C-1 P
	Fraktions- %	ΣFrakt. - %		
+200				
128 - 200				
96 - 128	2,7	2,7		1 898,4 % 1,5 898,1 % 2 897,5 % 3 896,8 % 4 895,8 % 6 894,2 % 8 892,8 % 12 889,5 % 16 884,8 % 24 873,6 % 32 868,4 % 48 853,4 % 64 821,1 % 96 802,7 % 128 800,0 % 192 800,0 %
64 - 96	18,4	21,1		
48 - 64	12,3	33,4		
32 - 48	22,0	60,4		
24 - 32	13,2	73,6		
16 - 24	10,4	84,0		
12 - 16	4,5	88,5		
8 - 12	3,5	92,0		
6 - 8	2,2	94,2		50% - PUNKT = 839,2
4 - 6	1,6	95,8		VOLUMENVERTEILUNG
3 - 4	1,0	96,8		
2 - 3	0,7	97,5		
15 - 2	0,6	98,1		
1 - 15	0,3	98,4		
-1	1,6	100,0		

077

Körnungsanalyse Nr. 220Datum 1985 11 15

Flotationskonzentrat Tasmanien Kauster 850°C			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E266 95-11-15 FA-7055-850.C-1 R
	Fraktions- %	ΣFrakt. - %		
+200				
128 - 200				
96 - 128	3,0	3,0		1 098,4 % 1,5 098,2 % 2 097,8 % 3 097,2 % 4 096,3 % 6 094,5 % 8 092,4 % 12 089,1 % 16 084,0 % 24 073,5 % 32 059,8 % 48 032,9 % 64 019,9 % 96 003,0 % 128 000,0 % 192 000,0 %
64 - 96	16,9	19,9		
48 - 64	13,0	32,9		
32 - 48	26,9	59,8		
24 - 32	13,7	73,5		
16 - 24	10,5	84,0		
12 - 16	5,1	89,1		
8 - 12	3,3	92,4		
6 - 8	2,1	94,5		50% - PUNKT = 037,9
4 - 6	1,8	96,3		VOLUMENVERTEILUNG
3 - 4	0,9	97,2		
2 - 3	0,6	97,8		
15 - 2	0,4	98,2		
1 - 15	0,2	98,4		
-1	1,6	100,0		

078

Table 4

988080

Körnungsanalyse Nr. 222Datum 1985 11 15

Flotationskonzentrat Tasmanien Kauster 900 °C			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E256 95-11-15 FA-7055-900.C-1 R
	Fraktions- %	ΣFrakt. - %		
>200				
128 - 200				
96 - 128	2,1	2,1		1 898,5 % 1,5 898,3 % 2 898,0 % 3 897,6 % 4 896,7 % 6 895,8 % 8 893,8 % 12 889,4 % 16 884,4 % 24 873,2 % 32 859,5 % 48 831,8 % 64 819,6 % 96 802,1 % 128 800,0 % 192 800,0 %
64 - 96	17,5	19,6		
48 - 64	12,2	31,8		
32 - 48	27,7	59,5		
24 - 32	13,7	73,2		
16 - 24	11,2	84,4		
12 - 16	5,0	89,4		
8 - 12	3,6	93,0		
6 - 8	2,0	95,0		50% - PUNKT = 837,5
4 - 6	1,7	96,7		VOLUMENVERTEILUNG
3 - 4	0,9	97,6		
2 - 3	0,4	98,0		
15 - 2	0,3	98,3		
1 - 15	0,2	98,5		
-1	1,5	100,0		

079

# Körnungsanalyse Nr. 224

Datum 1985 11 15

Flotationskonzentrat Tasmanien Kauster 950°C			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E255 95-11-15 FA-7055-950.C-1 R
	Fraktions- %	ΣFrakt. - %		
>200				
128 - 200				
96 - 128	2,6	2,6		1 898,7 % 1,5 898,6 % 2 898,5 % 3 898,2 % 4 897,4 % 6 895,9 % 8 894,1 % 12 890,5 % 16 885,3 % 24 873,9 % 32 860,2 % 48 833,1 % 64 820,8 % 96 802,6 % 128 800,0 % 192 800,0 %
64 - 96	18,2	20,8		
48 - 64	12,3	33,1		
32 - 48	27,1	60,2		
24 - 32	13,7	73,9		
16 - 24	11,4	85,3		
12 - 16	5,2	90,5		
8 - 12	3,6	94,1		
6 - 8	1,8	95,9		59% - PUNKT = 939,1
4 - 6	1,5	97,4		VOLUMENVERTEILUNG
3 - 4	0,8	98,2		
2 - 3	0,3	98,5		
15 - 2	0,1	98,6		
1 - 15	0,1	98,7		
-1	1,3	100,0		

080  
 Körnungsanalyse Nr. 226
Datum 1985.11.26

Flotationskonzentrat Tasmanien gemahlen <48µm			Cilas Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E255 FR-7055 Konz. 20h. 0,5 kg 1 Std. gem. Siabmühle
	Fraktions- %	ΣFrakt. - %		
>200				
128 - 200				
96 - 128				
64 - 96	-	-		
48 - 64	0,1	0,1		
32 - 48	8,3	8,4		
24 - 32	9,5	17,9		
16 - 24	17,3	35,2		
12 - 16	10,0	45,2		
8 - 12	10,3	55,5		
6 - 8	6,9	62,4		
4 - 6	7,9	70,3		
3 - 4	5,1	75,4		
2 - 3	6,6	82,0		
15 - 2	6,4	88,4		
1 - 15	2,8	91,2		
-1	8,8	100,0		

1	891,2 %
1,5	888,4 %
2	882,0 %
3	875,4 %
4	870,3 %
6	862,4 %
8	855,5 %
12	845,2 %
16	835,2 %
24	817,9 %
32	808,4 %
48	800,1 %
64	800,1 %
96	800,0 %
128	800,0 %
192	800,0 %

50% - PUNKT = 810,2

VOLUMENVERTEILUNG

Körnungsanalyse Nr. 227Datum 1985 11 26

Flotationskonzentrat Tasmanien  Kauster 800°C gemahlen < 48µm			Cilas  Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E266 95-11-26 FR-7055-30MI.-800.C ?
	Fraktions- %	ΣFrakt. - %		
+200				
128 - 200				
96 - 128				
64 - 96				
48 - 64	0,6	0,6		
32 - 48	6,6	7,2		
24 - 32	7,7	14,9		
16 - 24	16,5	31,4		
12 - 16	11,7	43,1		
8 - 12	14,0	57,1		
6 - 8	8,7	65,8		
4 - 6	8,3	74,1		
3 - 4	4,3	78,4		
2 - 3	5,6	84,0		
15 - 2	6,4	90,4		
1 - 15	2,6	93,0		
-1	7,0	100,0		

1	893,8 %
1,5	898,4 %
2	884,8 %
3	878,4 %
4	874,1 %
6	865,8 %
8	857,1 %
12	843,1 %
16	831,4 %
24	814,9 %
32	807,2 %
48	800,6 %
64	800,6 %
96	800,8 %
128	800,8 %
192	800,8 %

50% - PUNKT = 810,8

VOLUMENVERTEILUNG

082

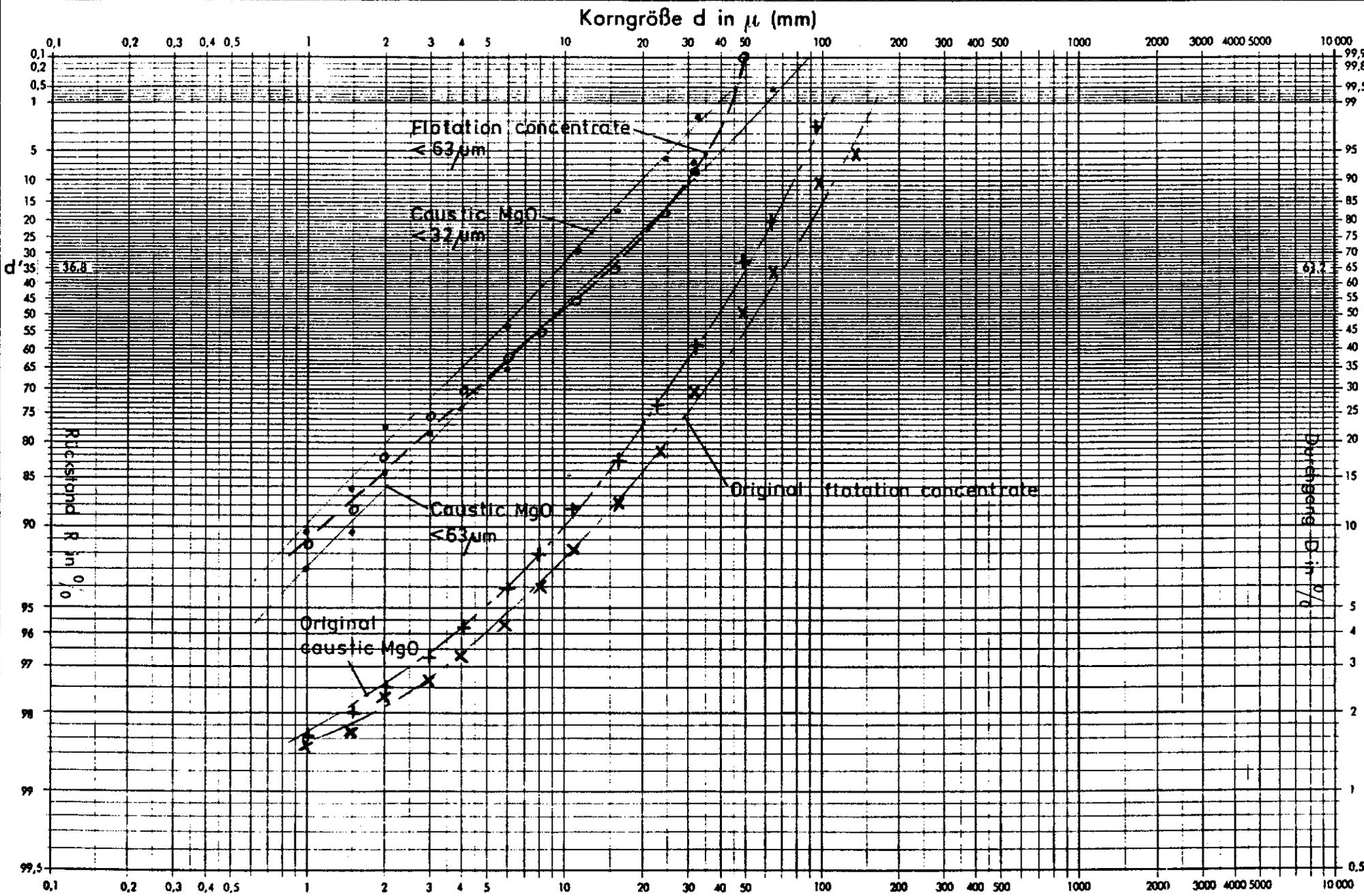
Körnungsanalyse Nr. 228Datum 1985 11 26

Flotationskonzentrat Tasmanien  Kauster 800°C gemahlen < 32µm			Cilas  Lasergranulometer	
Kornfraktion (µm)	Siebrückstand		Bemerkung	GRANULOMETRE 715 E266 95-11-26 FA-7055-800.C-1STD.GEM. R
	Fraktions- %	ΣFrakt. - %		
+200				
128 - 200				
96 - 128				
64 - 96				
48 - 64				
32 - 48	1,8	1,8		1 898,5 %
24 - 32	4,5	6,3		1,5 896,8 %
16 - 24	11,7	18,0		2 877,3 %
12 - 16	11,7	29,7		3 869,6 %
8 - 12	13,8	43,5		4 863,7 %
6 - 8	10,3	53,8		6 853,8 %
4 - 6	9,9	63,7		8 843,5 %
3 - 4	5,9	69,6		12 829,7 %
2 - 3	7,7	77,3		16 818,8 %
15 - 2	9,5	86,8		24 806,3 %
1 - 15	3,7	90,5		32 801,8 %
-1	9,5	100,0		48 800,0 %
				64 800,0 %
				96 800,0 %
				128 800,0 %
				192 800,0 %

50% - PUNKT = 896,7

VOLUMENVERTEILUNG

083



Stoff: Flot. conc.  
Maschine: Tasmania  
Cilas: Lasergr

Körnungsnetz

Nr. ....  
Datum: 85-11-26  
985085

Temperature profile of high temperature laboratory kiln  
for sintering of magnesite

084

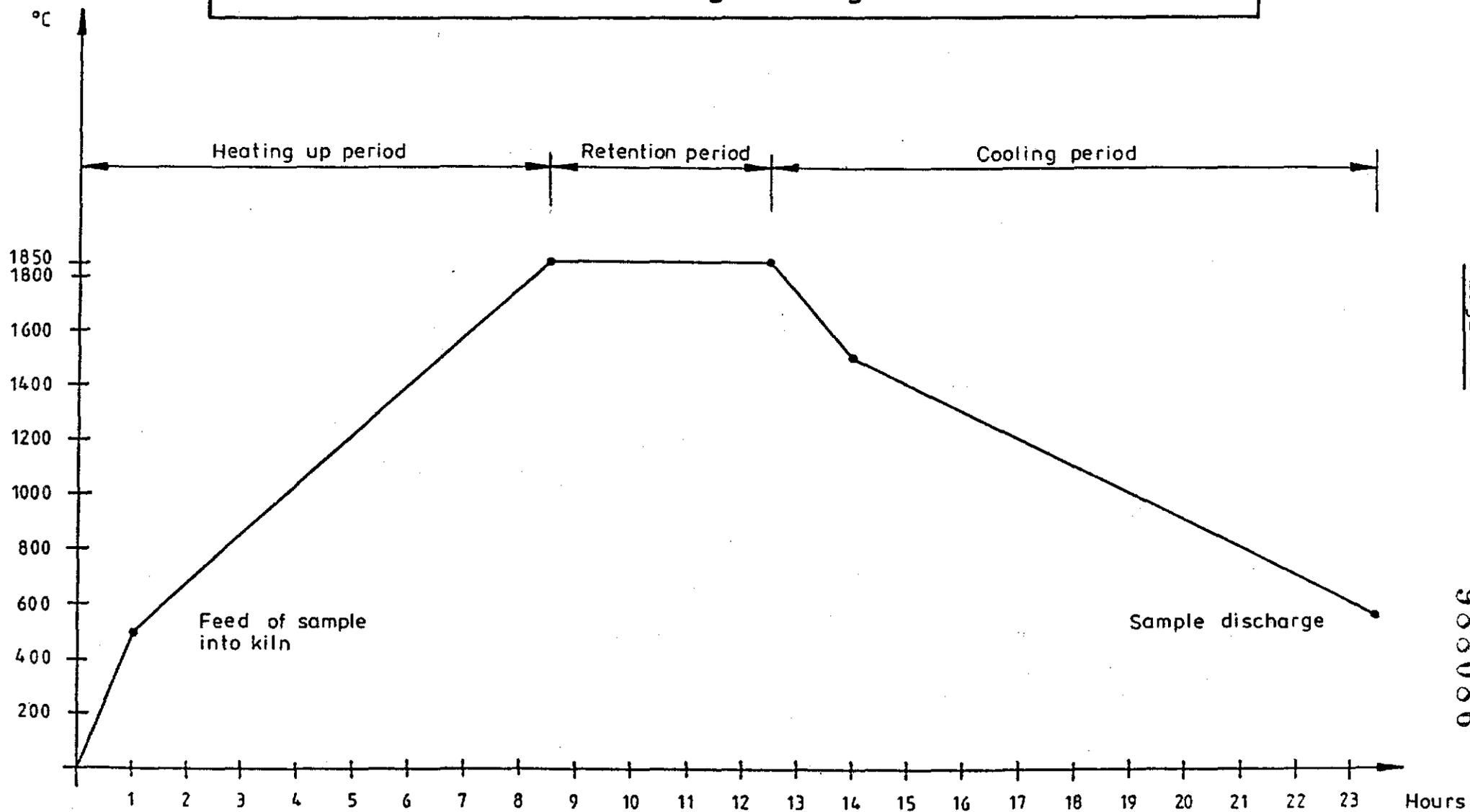


Diagram 2

988086